

US 20040118131A1

(19) United States (12) Patent Application Publication (10) Pub. No.: US 2004/0118131 A1

Jun. 24, 2004 (43) **Pub. Date:**

Standafer

(54) SYSTEM AND METHOD FOR ENHANCING **COOLING OF A FEED PRODUCT DURING** PRODUCTION

(76) Inventor: Paul A. Standafer, Worthington, MN (US)

> Correspondence Address: S. Wade Johnson **DORSEY & WHITNEY LLP Suite 1500 50 South Sixth Street** Minneapolis, MN 55402-1498 (US)

- (21) Appl. No.: 10/328,720
- (22) Filed: Dec. 23, 2002

Publication Classification

- (51) Int. Cl.⁷ F25D 13/06; F25C 5/14

(57) ABSTRACT

A system for enhancing the cooling of a product stream, wherein the product stream is a livestock feed product, is disclosed. The system has a reduction station and a conveyor system with a conveyor belt routed through the reduction station. The conveyor belt is used to transport the product stream through the reduction station. The reduction station increases the surface area to volume ratio of the product stream.













FIG. 5a





SYSTEM AND METHOD FOR ENHANCING COOLING OF A FEED PRODUCT DURING PRODUCTION

FIELD OF THE INVENTION

[0001] The invention relates to a system and method for cooling a product stream during its production.

BACKGROUND OF THE INVENTION

[0002] Feed supplements have been used for many years as vehicles to provide energy, protein, minerals, vitamins and medicaments to animals, especially livestock. Molassesbased feed supplements have been an especially popular and effective form of livestock feed supplement. Since molasses is highly palatable to livestock, a molasses-based feed supplement must be consumption limiting to prevent livestock from over indulging in any one visit to the supplement.

[0003] One method of making a molasses-based feed supplement consumption limiting is to provide it to livestock in the form of a hard and durable low-moisture feed block. Low-moisture feed blocks are made by heating a fluid mixture of molasses and other nutrients until the mixture is fully dehydrated. The mixture is then poured into a form or tub and cooled.

[0004] While heating is necessary to fully dehydrate a molasses-based feed supplement to achieve a feed block that is hard and durable, heat causes thermal degradation of sugars such as those found in molasses. Heat also causes thermal degradation of the nutrients contained in the feed supplement, creating reaction products that are often indigestible to the animals eating the feed supplement. Thermal degradation is especially problematic for processors of molasses-based feed supplements because the molasses supplied to feed supplement processors often vary from supply to supply. As a result, it can be difficult to fine-tune the dehydration process so as to minimize thermal degradation.

[0005] The longer the feed supplement remains in a heated state, the greater the thermal degradation of the sugars and nutrients and the greater the creation of indigestible reaction products. Failure to adequately decrease the temperature of the feed supplement prior to placing the supplement in a form or barrel can cause the supplement to react and to increase its temperature on its own. This can result in complete degradation of the supplement. Complete degradation of the supplement is more likely to occur when the supplement is manufactured during high ambient temperature conditions. Thus, it is advantageous to rapidly reduce the temperature of the molasses-based feed supplement once the supplement has exited the dehydration process.

[0006] There is a need in the art for a system and method that rapidly reduces the temperature of a fully dehydrated molasses-based feed supplement once the supplement has exited the dehydration process.

BRIEF SUMMARY OF THE INVENTION

[0007] The invention, in one embodiment, is a system for enhancing the cooling of a product stream during production wherein the product stream is a livestock feed product. The system has a squeeze roller and a conveyor system with a conveying belt. The squeeze roller is located above the conveyor belt. A livestock feed product is routed between the conveyor belt and the squeeze roller thereby reducing the product in height and increasing the product in width. This is done to facilitate cooling of the product stream.

[0008] The invention, in another embodiment, is a system for increasing the surface area of a product stream wherein the product stream is an animal feed product to be cooled. The system has a reduction station and a conveyor system. The conveyor system has a conveyor belt routed through the reduction station. The conveyor belt is used to transport the product stream through the reduction station. The reduction station reduces the product stream in height and increases the product stream in width.

[0009] The invention, in yet another embodiment, is a method for increasing the surface area of a product stream wherein the product stream is an animal feed product to be cooled. The product stream is directed onto a conveyor belt and conveyed to a reduction station. The reduction station reduces the height of the product stream and increasing the width of the product stream as the product stream is conveyed through the reduction station.

[0010] While multiple embodiments are disclosed, still other embodiments of the invention will become apparent to those skilled in the art from the following detailed description, which shows and describes illustrative embodiments of the invention. As will be realized, the invention is capable of modifications in various obvious aspects, all without departing from the spirit and scope of the invention. Accordingly, the drawings and detailed description are to be regarded as illustrative in nature and not restrictive.

BRIEF DESCRIPTION OF THE DRAWINGS

[0011] FIG. 1 is a schematic side view of a product cooling system incorporating a cooling belt conveyor and a series of squeeze rollers that reduce a product stream in height and increase the product stream in width, thereby increasing the surface contact between the product stream and the cooling belt.

[0012] FIG. 2 is a schematic plan view of the system shown in FIG. 1.

[0013] FIG. **3** is a schematic side view of product cooling system incorporating a squeeze belt conveyor reducing a product stream in height and increasing the product stream in width before the product stream reaches the cooling belt conveyor.

[0014] FIG. 4 is a schematic side view of the product cooling system incorporating an inclined squeeze belt conveyor reducing a product stream in height and increasing the product stream in width before the product stream reaches the cooling belt conveyor.

[0015] FIG. 5*a* is a block diagram illustrating a method of increasing the surface area contact between a product stream and a conveyor belt.

[0016] FIG. 5*b* is a block diagram illustrating a method of automatically adjusting the surface area contact between a product stream and a conveyor belt based on a temperature reading taken from the product stream.

[0017] FIG. 6 is a schematic plan view of the system shown in FIG. 1 employing chilled squeeze rollers.

DETAILED DESCRIPTION

[0018] FIG. 1 is a schematic side view of a product cooling system 5 according to one embodiment of the invention. As shown in FIG. 1, the system 5 includes a cooling belt conveyor 10, a reduction station 15, a product barrel 20, and a hopper 25 with an orifice 26. The hopper 25 is located above one end of the cooling belt conveyor 10 and the product barrel 20 is located below the other end of the cooling belt conveyor 10. The reduction station 15 is located at a point along the cooling belt conveyor 10 between the hopper 25 and the barrel 20.

[0019] A product stream 27, the product being a fully dehydrated molasses-based feed supplement or other similar animal feed product, emanates from the orifice 26 of the hopper 25 onto the cooling belt conveyor 10. The cooling belt conveyor 10 transports the product stream 27 through the reduction station 15 where the product stream 27 is reduced in depth and increased in width. This facilitates cooling of the product stream 27 because the surface contact between the cooling belt conveyor 10 and the product stream 27 is increased. After leaving the reduction station 15, the product stream 27 travels along the cooling belt conveyor 10 to the product barrel 20 or form.

[0020] The cooling belt conveyor 10 includes a cooling belt 30, conveyor wheels 35 and a cooling water spray system 40. The cooling belt 30 travels about the conveyor wheels 35. The cooling belt 30 is stainless steel or another material also having good heat transfer and product release capabilities.

[0021] As shown in FIG. 2, the cooling belt is powered by one or more electric motors 42. As further indicated in FIG. 2, in one embodiment of the invention, the electric motor 42 has a variable frequency drive (VFD) 44 that allows the cooling belt 30 to travel at different speeds. For example, in one embodiment, the VFD 44 causes the cooling belt 30 to travel at approximately 1 to approximately 30 feet per minute. In another embodiment, the cooling belt 30 travels at a speed of approximately 30 to approximately 60 feet per minute. In another embodiment, the cooling belt 30 travels at a speed of approximately 60 to approximately 100 feet per minute. In another embodiment, the cooling belt 30 travels at a speed of approximately 100 feet per minute or greater. In another embodiment, the cooling belt 30 travels at a speed of approximately 100 feet per minute or greater. In another embodiment, the cooling belt 30 travels at a speed of approximately 60 feet per minute.

[0022] The length of the cooling belt conveyor 10 may vary depending on the desired temperature drop of the product being cooled, the temperature of the water in the cooling water spray system 40, and the travel speed of the cooling belt 30. For example, in one embodiment of the invention, the cooling belt conveyor 10 is between about 10 and about 150 feet long or longer. In another embodiment, the cooling belt conveyor 10 is approximately 50 feet long. In other embodiments of the invention, the conveyor will be greater than or less than 50 feet long.

[0023] The width of the cooling belt 30 may vary depending on the width of the product stream 27 emanating from the orifice 26 of the hopper 25. For example, in one embodiment of the invention, the cooling belt 30 is between about 4 and about 48 inches wide or wider. In another embodiment, the cooling belt 30 is between about 12 and about 36 inches wide. In another embodiment, the cooling belt **30** is between about 18 and about 30 inches wide. In another embodiment, the cooling belt **30** is about 24 inches wide. Finally, in another embodiment, the cooling belt **30** is about 30 inches wide.

[0024] As shown in FIG. 1, the cooling water spray system 40 is located within the cooling belt conveyor 10 and has water piping 45 terminating in spray heads 50. To cool the cooling belt 30, water spray 55 emanates from the spray heads 50 and contacts the bottom surface of the cooling belt 30. In one embodiment of the invention, the water used in the cooling water spray system 40 is water pumped from underground aquifers. This ground water exits the spray heads at approximately 50 to approximately 65 degrees Fahrenheit. In another embodiment, the ground water would be approximately 58 to approximately 62 degrees Fahrenheit.

[0025] In one embodiment, the water used in the cooling water spray system 40 is chilled water from a chiller. The chilled water may exit the spray heads 50 at approximately 40 to approximately 55 degrees Fahrenheit. In other embodiments, the water temperature may be higher or lower than these values. In one embodiment, other cooling mediums are applied against the bottom of the cooling belt 30, for example brine solutions or cooled air. In one embodiment of the invention, jets of cooled air blow down on the top of the product stream 27 as it travels along the cooling belt conveyor 10.

[0026] In one embodiment of the invention, the cooling belt conveyor 10 utilizes about 0.01 to about 10.0 gallons per minute (gpm) of cooling water per linear foot of the cooling belt conveyor 10. In another embodiment, the cooling belt conveyor 10 utilizes about 0.05 to about 2.0 gpm of cooling water per linear foot of the cooling belt conveyor 10. In another embodiment, the cooling belt conveyor 10. In another embodiment, the cooling belt conveyor 10. In another embodiment, the cooling belt conveyor 10 utilizes about 1.2 to about 1.8 gpm of cooling water per linear foot of the cooling belt conveyor 10.

[0027] The reduction station 15, in the embodiment shown in FIG. 1, has a first stage squeeze roller 60, a second stage squeeze roller 65, a first support roller 70, and a second support roller 75. The squeeze rollers 60, 65 are located above the cooling belt 30. The contact surfaces of the squeeze rollers 60, 65 are stainless steel, TEFLON®, or another material known in the art as possessing good product release characteristics. The support rollers 70, 75 are located below the cooling belt 30 and their corresponding squeeze rollers 60, 65. The support rollers 70, 75 support the cooling belt 30.

[0028] In the embodiment shown in FIG. 3, the reduction station 15 is located on a squeeze belt conveyor 80 and has a first stage squeeze roller 60, a second stage squeeze roller 65, and a low-friction board 85. The squeeze rollers 60, 65 are located above the squeeze belt 90 and the low-friction board 85 is located below the squeeze belt 90. The low-friction board 85 supports the squeeze belt 90. The squeeze belt 90 is stainless steel, TEFLON®, or another material known in the art as possessing good product release characteristics. The squeeze belt 90 travels about conveyor wheels 35.

[0029] In one embodiment, whether the reduction station 15 is located on the cooling belt conveyor 10 or on the squeeze belt conveyor 80, the reduction station 15 includes

only one squeeze roller **60**. In other embodiments, the reduction station **15** has more than two squeeze rollers **60**, **65**. Also, there may be more than or less than two support rollers **70** per reduction station **15**. Furthermore, in other embodiments, the low-friction board **85** may be substituted for support rollers **70**, **75**, or vice versa.

[0030] As shown in FIG. 3, in one embodiment, the reduction station 15 is separate from the cooling belt conveyor 10. Specifically, the squeeze belt conveyor 80 has a reduction station 15 and is installed in a horizontal configuration, terminating above the cooling belt conveyor 10. In the embodiment shown in FIG. 4, the squeeze belt conveyor 80 is installed in an inclined manner, sloping up from the orifice 26 of the hopper 25 to the cooling belt conveyor 80 is installed in an inclined manner sloping down from the orifice 26 of the hopper 25 to the cooling belt conveyor 80 is installed in an inclined manner sloping down from the orifice 26 of the hopper 25 to the cooling belt conveyor 10.

[0031] Operation of the invention will now be explained by referring to FIGS. 1, 2 and 5. This explanation is equally applicable to the embodiments illustrated in FIGS. 3 and 4, except the product streams 27 in FIGS. 3 and 4 are reduced on the squeeze belt conveyors 80 before being routed to the cooling belt conveyors 10. FIG. 5a is a block diagram showing the steps of a method for increasing the surface area contact between a product stream 27 and a conveyor belt.

[0032] Referring to FIGS. 1, 2 and 5, a product stream 27, the product being a fully dehydrated molasses-based feed supplement or other similar animal feed product, exits the orifice 26 of the hopper 25 onto the cooling belt 30 as an unreduced product stream 95 (block 200 in FIG. 5*a*). As shown in FIGS. 1 and 2, the height and width of the unreduced product stream 95 are approximately equal to the dimensions of the orifice 26.

[0033] In one embodiment of the invention, the height of the unreduced product stream 95 is approximately 2.0 to approximately 6.0 inches and the width is approximately 1.0 to approximately 12.0 inches. In one embodiment, the height of the unreduced product stream 95 is approximately 1.25 to approximately 1.50 inches and the width is approximately 4.0 to approximately 4.5 inches. In other embodiments, the height and width of the unreduced product stream 95 may be other sizes.

[0034] The unreduced product stream 95 is carried along the cooling belt 30 to the reduction station 15 (block 210 in FIG. 5*a*). The reduction station 15 converts the unreduced product stream 95 into a fully reduced product stream 100 by decreasing the height of the product stream 27 and increasing the width of the product stream 27 (block 220 in FIG. 5*a*).

[0035] In one embodiment of the invention, the reduction station 15 will have decreased the height of the product stream 27 by about 10 to about 98 percent or more. In another embodiment, the reduction station 15 will have decreased the height of the product stream 27 by about 25 to about 75 percent.

[0036] In one embodiment of the invention, the reduction station 15 will have increased the width of the product stream 27 by about 10 to about 500 percent. In another embodiment, the reduction station 15 will have increased the width of the product stream 27 by about 50 to about 200 percent.

[0037] In one embodiment of the invention, the height of the fully reduced product stream 100 is approximately 0.25 to approximately 3.0 inches and the width is approximately 2.0 to approximately 24.0 inches. In one embodiment, the height of the fully reduced product stream 100 is approximately 0.5 to approximately 0.75 and the width is approximately 8.0 to approximately 9.0 inches. In other embodiments, the height and width of the fully reduced product stream 100 may be other sizes.

[0038] In the embodiment illustrated in FIGS. 1 and 2, the reduction station 15 converts the unreduced product stream 95 into the fully reduced product stream 100 as follows. As the unreduced product stream 95 reaches the reduction station 15, the unreduced product stream 95 is drawn between the rotating first stage squeeze roller 60 and the traveling cooling belt 30. The height of the unreduced product stream 95 is reduced to the height of the partially reduced product stream 105 (see FIG. 1). The width of the partially reduced product stream 105 (see FIG. 2).

[0039] The partially reduced product stream 105 is carried along the cooling belt 30 to the rotating second stage squeeze roller 65. The partially reduced product stream 105 is drawn between the rotating second stage squeeze roller 65 and the traveling cooling belt 30. The height of the partially reduced product stream 105 is reduced to the height of the fully reduced product stream 100 (see FIG. 1). The width of the partially reduced product stream 105 is increased to the width of the fully reduced product stream 100 (see FIG. 2). The cooling belt 30 carries the fully reduced product stream 100 from the reduction station 15 (block 230 in FIG. 5*a*).

[0040] In one embodiment, the width of the fully reduced product stream 100 is now nearly equivalent to the width of the cooling belt 30. As a result, the heat transfer rate from the product stream 27 to the cooling belt 30 is maximized because the contact area between the product stream 27 and the cooling belt 30 is maximized and because the surface area to volume ratio of the product stream 27 is maximized. Thus, the temperature of the product stream 27 can be quickly reduced, preventing further degradation of the product.

[0041] Upon exiting the reduction station 15, the fully reduced product stream 100 travels along the cooling belt 30 to a product barrel 20 or form. Once a barrel 20 or form is filled with product, the barrel 20 or form is taken to a storage area where the product is allowed to harden.

[0042] The space between each squeeze roller 60, 65 and the cooling belt 30 or squeeze belt 90, as the case may be, can be adjusted via a thickness adjustor 110 as shown in FIG. 3. Thus, the rate of heat transfer from a product stream 27 to a cooling belt 30 may be controlled by adjusting the thickness adjustor 110 to modify the width of the product stream 27 as it leaves the reduction station 15.

[0043] In one embodiment, the axle 115 of a squeeze roller 60, 65 is supported on each end by a thickness adjustor 110. The thickness adjustor 110 is slidably mounted on a roller frame 120. The thickness adjustor 110 has one or more slots 125 that slidably engage with bolts 130 that protrude through the slots 125 from the side of the roller frame 120. The space between a squeeze roller 60, 65 and a belt 30, 90 may be increased by moving the roller's thickness adjustors

110 up along their roller frames 120. Similarly, the space between a squeeze roller 60, 65 and a belt 30, 90 may be decreased by moving the roller's thickness adjustors 110 down along their roller frames 120. In either case, the bolts 130 are then tightened to secure the thickness adjustors 110 in place.

[0044] In one embodiment, as shown in FIG. 4, the thickness adjustors 110 are automated in that they are moved along a roller frame 120 by a motor 131. In one embodiment, the motor 131 turns a shaft 132 that turns a worm gear 133 that meshes with a gear rack 134. As the worm gear 133 rotates against the gear rack 133, the thickness adjustor 110 is caused to translate along the roller frame 120. In other embodiments, other gear configurations are utilized to allow the motor 131 to translate the thickness adjustor 110. In still other embodiments, the thickness adjustor 110 is translated along the roller frame 120 via a hydraulic piston.

[0045] As indicated in FIG. 4, in one embodiment, a temperature sensor 134 will be located near the end of the cooling belt conveyor 10. In other embodiments, the temperature sensor 134 will be located in other locations along the cooling belt conveyor 10 or the squeeze belt conveyor 80.

[0046] As outlined in FIG. 5*b*, in one embodiment, a temperature sensor 134 reads the temperature of the product stream 27 at some point before the product stream 27 enters the barrel 20 (block 300). The temperature of the product stream 27 is sent to a processor 135 (block 310). The processor 135 compares the temperature of the product stream 27 to an optimal temperature range stored in a memory 136 (block 320).

[0047] As previously explained in this specification, if the product stream 27 is insufficiently cooled, significant thermal degradation of the product may occur. The temperature above which significant thermal degradation will occur is called the thermal degradation temperature. Alternatively, if the product stream 27 is excessively cooled, it will lose its workability and will be unable to conform to the barrel 20. The temperature below which workability is lost is the workability temperature. Consequently, the optimal temperature range is a temperature range where the product stream 27 is warm enough to readily conform to the barrel 20 (i.e., above the workability temperature) but not so warm that unacceptable thermal degradation will occur (i.e., below the thermal degradation temperature). The optimal temperature range may vary from day to day depending on the chemical makeup of the molasses being used and the ambient temperature.

[0048] If the temperature of the product stream 27 is greater than the thermal degradation temperature, the processor 135 will signal the motor 131 to decrease the clearance between the squeeze roller 60 and the belt 30, 90 (block 330a). This will increase the surface contact between the cooling belt 30 and the product stream 27 to lower the temperature of the product stream 27.

[0049] If the temperature of the product stream 27 is less than the workability temperature, the processor 135 will signal the motor 131 to increase the clearance between the squeeze roller 60 and the belt 30, 90 (block 330b). This will decrease the surface contact between the cooling belt 30 and the product stream 27 to raise the temperature of the product stream 27.

[0050] Once the product stream 27 has had time to react to the adjustment and its temperature has stabilized, the temperature sensor 134 will take another temperature reading. If the new temperature reading is still not within the optimum temperature range, the processor 135 will again signal the motor 131 to adjust the thickness adjustors 110 as necessary.

[0051] In another embodiment, where a processor 135 and a memory 136 are not available, an operator uses a temperature sensing device to read the temperature of the product stream 27 at some point before the product stream 27 enters the barrel 20. The operator compares the temperature reading to an optimal temperature range. If the temperature reading is greater than the thermal degradation temperature, the operator adjusts the thickness adjustors 110, either manually or via the motor 131, to decrease the clearance between the squeeze roller 60 and the belt 30, 90. This will increase the surface contact between the cooling belt 30 and the product stream 27 to lower the temperature of the product stream 27.

[0052] If the temperature reading is less than the workability temperature, the operator adjusts the thickness adjustors 110, either manually or via the motor 131, to increase the clearance between the squeeze roller 60 and the belt 30, 90. This will decrease the surface contact between the cooling belt 30 and the product stream 27 to raise the temperature of the product stream 27.

[0053] Once the product stream 27 has had time to react to the adjustment and its temperature has stabilized, the operator will take another temperature reading. If the new temperature reading is still not within the optimum temperature range, the operator will again adjust the thickness adjustors 110 as necessary.

[0054] As illustrated in FIG. 6, to further enhance the removal of heat from a product stream 27, the aforementioned embodiments may have one or more squeeze rollers 60, 65 that are chilled squeeze rollers 140.

[0055] As shown in FIG. 6, the supply piping 142 and return piping 145 connect to the ends of each axle 115. Each axle 115 is hollow and serves as a conduit for a cooling medium to enter or exit the chilled squeeze rollers 140. Candidates for a cooling medium include, but are not limited to, ground water, chilled water, CFCs, HFCs, HCFCs, and ammonia.

[0056] The cooling medium flows through the supply piping 142, into a chilled squeeze roller 140, and into the return piping 145. As the cooling medium flows through a chilled squeeze roller 140, the cooling medium absorbs heat that transfers from the product stream 27 through the surface of the chilled squeeze roller 140.

[0057] Each piping connection to the axle 115 of a chilled squeeze roller 140 has a flexible pipe element 150. The flexible pipe elements 150 allow the chilled squeeze roller 140 to be raised or lowered on its thickness adjustors 110 and prevents vibration from being transmitted from the chilled squeeze roller 140 to the piping 142, 145.

[0058] The amount and rate of heat transfer from a product stream 27 may vary depending on several different variables, such as the material of the cooling belt 30, the temperature and flow rate of the water sprayed against the cooling belt 30, the travel speed of the cooling belt 30, the depth of the

product stream 27, the amount of surface contact between the cooling belt 30 and the fully reduced product stream 100, and the composition of the product stream 27.

[0059] As shown in FIG. 4, in one embodiment of the invention, an unreduced product stream 95 of fully dehydrated molasses-based feed supplement exits the orifice 26 of the hopper 25 onto an inclined squeeze belt conveyor 80. The unreduced product stream 95 has a height of 1.25 to 1.50 inches and a width of 4.0 to 4.5 inches. The unreduced product stream 95 travels up the squeeze belt conveyor 80 where it enters a reduction station 15 having a single squeeze roller 60. In other embodiments, the reduction station 15 will have two or more squeeze rollers 60.

[0060] The product stream exits the reduction station 15 as a fully reduced product stream 100 having a height of 0.5 to 0.75 inch and a width of 8.0 to 9.0 inches. The fully reduced product stream 100 travels from the squeeze belt conveyor 80 onto the cooling belt 30.

[0061] The cooling belt conveyor 10 is approximately 50 feet long and has a stainless steel cooling belt 30 that travels at approximately 60 feet per minute. A VFD 44 allows the cooling belt 30 to travel at lower or higher speeds. Ground water having a temperature of approximately 58 to 62 degrees Fahrenheit is sprayed against the bottom of the cooling belt 30. By the time the product stream 27 has traveled from the orifice 26 of the hopper 25 to the product barrel 20, the product stream will have experienced a temperature decrease of approximately 8.0 to approximately 12.0 degrees Fahrenheit.

[0062] Although the invention has been described with reference to preferred embodiments, persons skilled in the art will recognize that changes may be made in form and detail without departing from the spirit and scope of the invention.

I claim:

1. A system for enhancing the cooling of a product stream wherein the product stream is a livestock feed product, the system comprising:

a conveyor system including a conveyor belt; and

a squeeze roller located above the conveyor belt and positioned to reduce the height and increase the width of the product stream.

2. The system of claim 1 wherein the conveyor belt is a cooling belt.

3. The system of claim 1 wherein the conveyor belt is a squeeze belt.

4. The system of claim 3 further comprising a cooling belt, wherein the product stream, having been reduced in height and increased in width on the squeeze belt, travels from the squeeze belt to the cooling belt.

5. The system of claim 1 wherein the squeeze roller has a thickness adjustor that allows the space between the squeeze roller and the conveyor belt to be increased or decreased.

6. The system of claim 1 further comprising a piping system circulating a cooling medium and wherein the squeeze roller is connected to the piping system and is a chilled squeeze roller.

7. The system of claim 1 further comprising a second squeeze roller positioned to further reduce the height and increase the width of the product stream.

8. The system of claim 1 further comprising a support roller, the support roller positioned to support a portion of the conveyor belt near the location of the squeeze roller.

9. The system of claim 1 further comprising a low-friction board positioned to support a portion of the conveyor belt.

10. A system for enhancing the cooling of a product stream wherein the product stream is a livestock feed product, the system comprising:

- a reduction station configured to increase the surface area to volume ratio of the product stream; and
- a conveyor system having a conveyor belt routed through the reduction station, the conveyor belt configured to transport the product stream through the reduction station.

11. The system of claim 10 wherein the conveyor belt is a cooling belt.

12. The system of claim 10 wherein the conveyor belt is a squeeze belt.

13. The system of claim 12 further comprising a cooling belt located near a distal end of the squeeze belt, wherein the product stream, after traversing the reduction station, travels from the squeeze belt to the cooling belt.

14. The system of claim 10 wherein the reduction station comprises a first reduction stage.

15. The reduction station of claim 14 further comprising a second reduction stage.

16. The system of claim 10 wherein the reduction station comprises a squeeze roller.

17. The system of claim 16 wherein the squeeze roller has a thickness adjustor that allows the space between the squeeze roller and the conveyor belt to be increased or decreased.

18. The system of claim 16 further comprising a piping system circulating a cooling medium and wherein the squeeze roller is connected to the piping system and is a chilled squeeze roller.

19. The reduction station of claim 16 further comprising a support roller, the support roller positioned to support a portion of the conveyor belt near the location of the squeeze roller.

20. The reduction station of claim 16 further comprising a low-friction board positioned to support a portion of the conveyor belt.

21. A method for enhancing the cooling of a product stream wherein the product stream is a livestock feed product, the method comprising:

directing the product stream onto a conveyor belt;

conveying the product stream to a reduction station; and

increasing the surface area to volume ratio of the product stream.

22. The method of claim 21 wherein the surface area to volume ratio of the product stream is increased by applying a squeeze roller to reduce the height and to increase the width of the product stream as the product stream is conveyed through the reduction station.

23. The method of claim 22 wherein the height of the product stream is decreased to approximately 0.25 to approximately 1.0 inch.

24. The method of claim 22 wherein the height of the product stream is decreased by approximately 10 to approximately 98 percent.

25. The method of claim 24 wherein the height of the product stream is decreased by approximately 25 to approximately 75 percent.

26. The method of claim 22 wherein the width of the product stream is increased by approximately 10 to approximately 500 percent.

27. The method of claim 26 wherein the width of the product stream is increased by approximately 50 to approximately 200 percent.

28. The method of claim 21 further comprising cooling the product stream with a cooling conveyor belt.

29. The method of claim 28 wherein the step of cooling the product stream comprises spraying water against the bottom of the cooling conveyor belt.

30. The method of claim 29 wherein the water is ground water having a temperature of approximately 50 to approximately 65 degrees Fahrenheit.

31. The method of claim 29 wherein the water is chilled water having a temperature of approximately 40 to approximately 55 degrees Fahrenheit.

32. The method of claim 28 wherein the cooling conveyor belt travels at approximately 30 to approximately 90 feet per minute.

33. The method of claim 21 wherein the conveyor belt is a squeeze belt and the method further comprises conveying the product from the reduction station to a cooling conveyor belt.

34. The method of claim 21 wherein the reduction station comprises a chilled squeeze roller and the method further comprises circulating a cooling medium through the chilled squeeze roller.

35. The method of claim 21 further comprising monitoring a product stream temperature and adjusting the surface area to volume ratio of the product stream to maintain the product stream temperature above a workability temperature and below a thermal degradation temperature.

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