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(54) **VAPOR CYCLE SYSTEM WITH DE-SUPERHEATER**

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(57) **ABSTRACT**

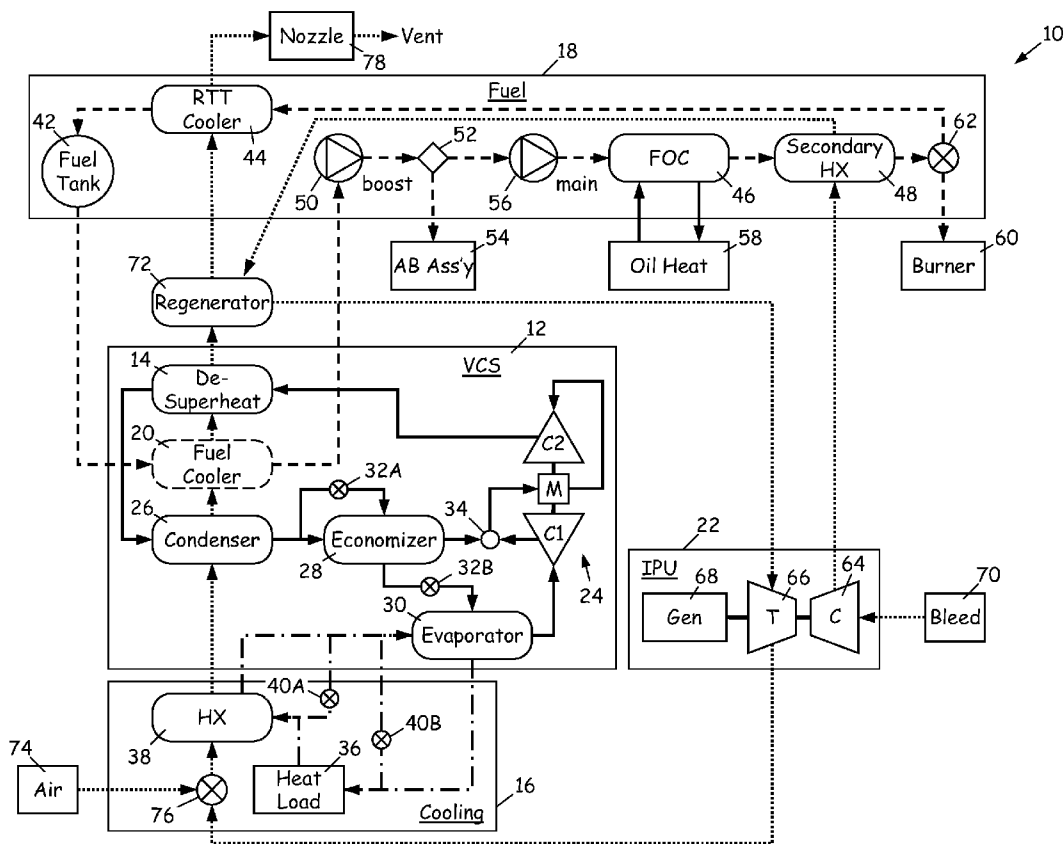
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A vapor cycle system comprises a compressor for compressing a coolant to form a superheated vapor, a de-superheater for cooling the superheated vapor to form a reduced temperature vapor by exchanging heat with a cooling fluid flow, a condenser for condensing the reduced temperature vapor to form a condensed liquid by exchanging heat with the cooling fluid flow, and an evaporator for evaporating the condensed liquid. The de-superheater is located downstream of the condenser in the cooling fluid flow, and a temperature of the cooling fluid flow is higher at the de-superheater than at the condenser.



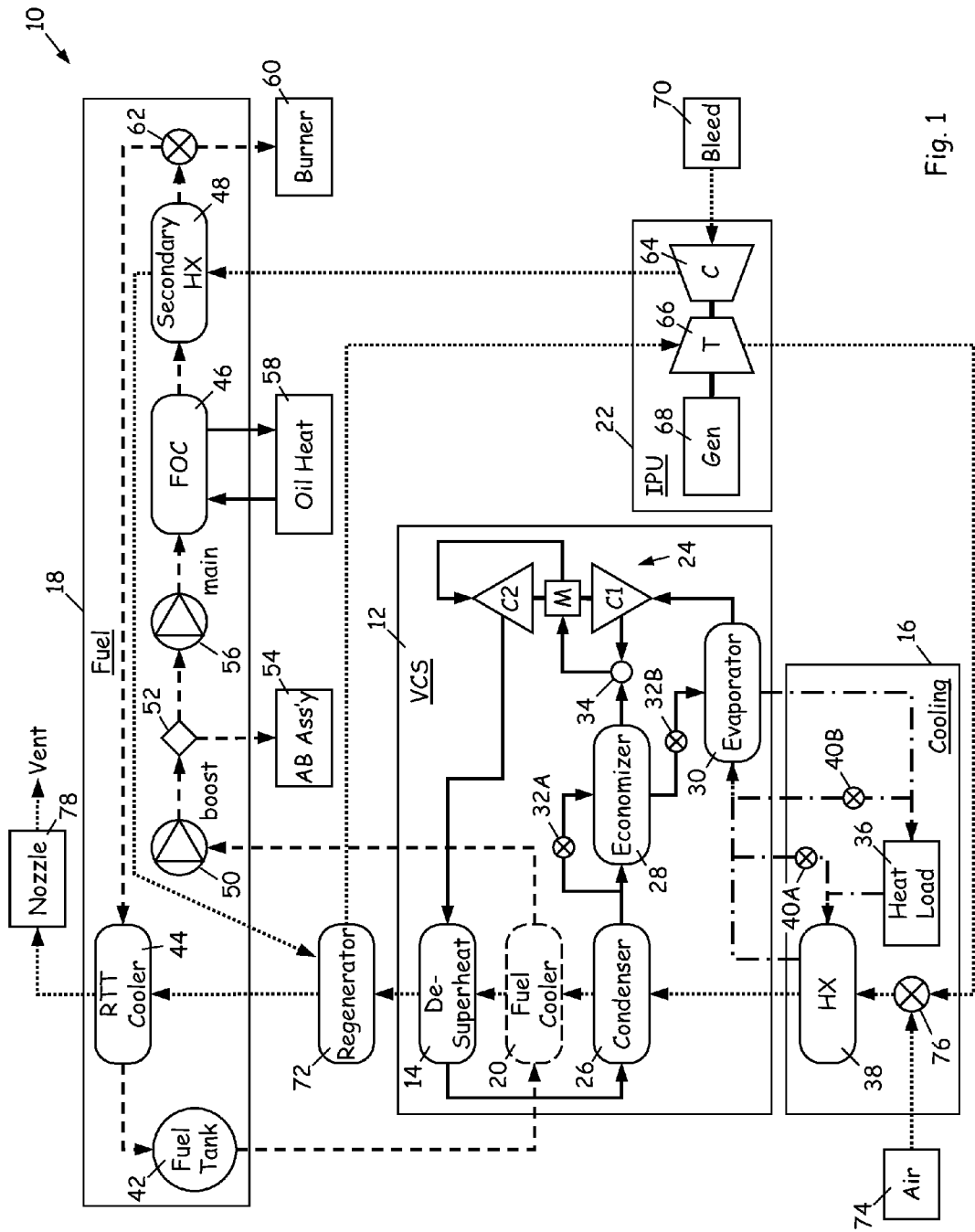


Fig. 1

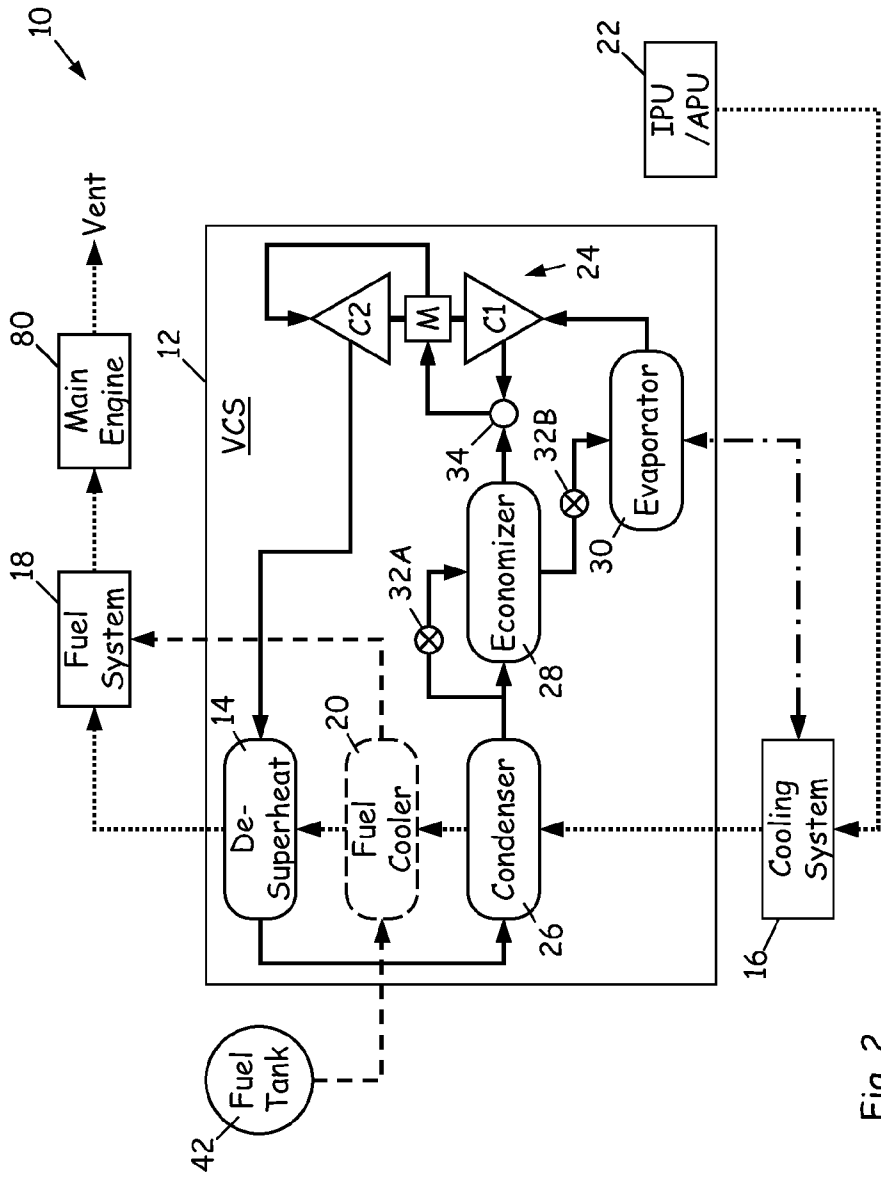


Fig. 2

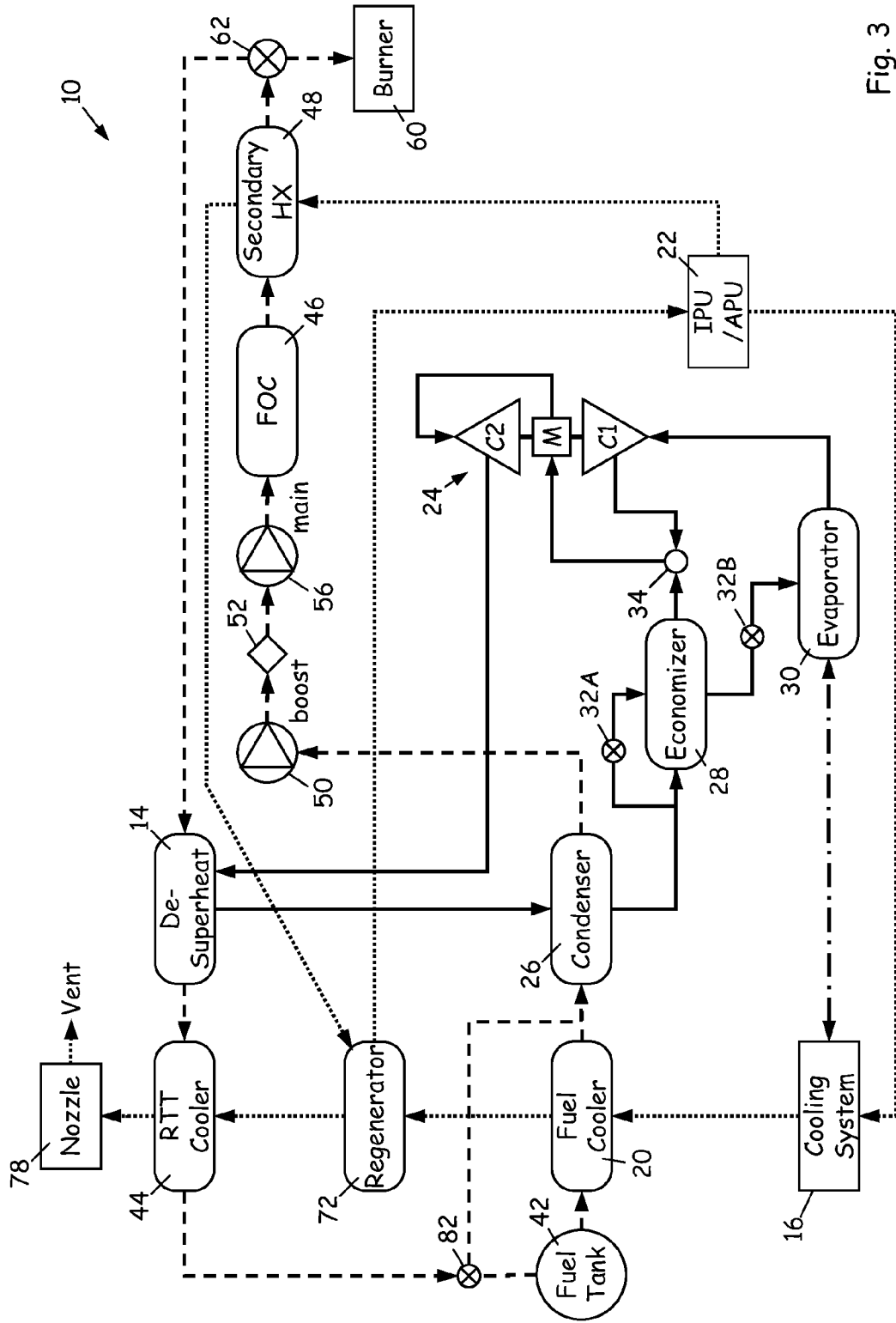


Fig. 3

## VAPOR CYCLE SYSTEM WITH DE-SUPERHEATER

### BACKGROUND

[0001] This invention relates generally to thermal management, and particularly to vapor cycle systems. In particular, the invention concerns thermal management for an aircraft-based vapor cycle system.

[0002] Modern commercial aircraft typically include a number of different heating and cooling systems for the cabin and cargo bay areas, galley facilities, power electronics, and avionics and radar systems. Each of these components has different thermal requirements and power constraints, making overall efficiency an important design criterion.

[0003] Most aircraft cooling systems utilize at least one vapor cycle system or VCS unit. The vapor cycle system includes a compressor for compressing the coolant, and a condenser for condensing the compressed fluid, with heat dispersed to different cooling fluid streams. The coolant then flows through an expansion valve to an evaporator, where the fluid expands and cools.

[0004] In some configurations, cold VCS fluid is cycled through an AC pack for cooling cabin air. Alternatively, a number of independent cooling loops can be used to cycle specialized coolants to heat loads distributed throughout the aircraft, cooling the coolant by exchanging heat with the vapor cycle system at the evaporator.

[0005] In either configuration, weight and efficiency are always at a premium. This makes thermal management an important design consideration, with particular respect to increasing efficiency, reducing the overall weight and size envelope, and maintaining system reliability and service life.

### SUMMARY

[0006] A vapor cycle system comprises a compressor, a de-superheater, a condenser, and an evaporator. The compressor compresses a coolant to form a superheated vapor, and the de-superheater cools the superheated vapor by heat exchange with a cooling fluid flow, forming a reduced temperature vapor. The condenser condenses the reduced temperature vapor by exchanging additional heat with a cooling fluid flow, forming a condensed liquid.

[0007] The condensed liquid is expanded then evaporated in the evaporator, absorbing thermal energy and starting the cycle again. The de-superheater is located downstream of the condenser in the cooling fluid flow, so that the cooling fluid temperature is higher at the de-superheater than at the condenser.

### BRIEF DESCRIPTION OF THE DRAWINGS

[0008] FIG. 1 is a schematic illustration of a thermal management system for an aircraft, with a vapor cycle system having a de-superheater.

[0009] FIG. 2 is a schematic illustration of the vapor cycle system and de-superheater, in an air-cooled embodiment.

[0010] FIG. 3 is a schematic illustration of the vapor cycle system and de-superheater, in a fuel-cooled embodiment.

### DETAILED DESCRIPTION

[0011] FIG. 1 is a schematic illustration of thermal management system 10 for an aircraft. System 10 includes vapor cycle system (VCS) 12 with de-superheater 14, cooling system 16, fuel circulation system 18 with fuel cooler 20 (dashed

lines), and integrated power unit (IPU) 22. Integrated power unit 22 generates electrical power and regenerates cooling air flow (dotted lines) for thermal management system 10. De-superheater 14 reduces losses in vapor cycle system 12 (solid lines), raising the coefficient of performance (COP) for thermal transfer to cooling system 16 (dot-dashed lines), and increasing the overall efficiency of thermal management system 10.

[0012] Vapor cycle system 12 includes de-superheater 14, compressor 24, condenser 26, economizer 28 and evaporator 30. In one embodiment, vapor cycle system 12 operates on a two-phase coolant or refrigerant fluid such as 1,1,1,2-tetrafluoroethane or R-134a (hydrofluorocarbon HFC-134a). Vapor cycle system 12 is also operable on older refrigerants such as R-12 (chlorofluorocarbon CFC-12) or R-22 (hydrochlorofluorocarbon HCFC-22), but in modern applications “green” fluids are typically used, including R-134a and other HFC, haloalkane and halocarbon-based refrigerant fluids with relatively short environmental lifetimes and reduced potential for ozone depletion.

[0013] The VCS loop is driven by compressor 24, which compresses the refrigerant to a superheated phase. The superheated phase is a gaseous or vapor state, at a temperature and pressure above the saturation and condensation points. De-superheater 14 cools the superheated vapor by exchanging heat with the cooling fluid stream, “de-superheating” the fluid to improve efficiency or decrease weight for the vapor/liquid phase transition in condenser 26.

[0014] In particular, de-superheater 14 improves the performance of condenser 26 by delivering fluid in a cooler vapor state, as compared to the superheated vapor output of compressor 24. Cooler vapor condenses more quickly, because less heat must be removed to reach the condensation temperature, increasing the efficiency of vapor cycle system 12.

[0015] De-superheater 14 also utilizes a higher-temperature (hotter) flow, downstream of condenser 26 and fuel cooler 20, while condenser 26 use a cooler fluid flow, upstream of fuel cooler 20 and de-superheater 14. Because the de-superheat temperature is higher than the condensation temperature, temperature differential  $\Delta T$  is less at both de-superheater 14 and condenser 26. This reduces the change in entropy and improves the coefficient of performance, as described below.

[0016] Refrigerant exits condenser 26 in a two-phase (liquid/vapor) state, at approximately the condensation temperature. Upstream expansion valve 32A provides a minor expansion into economizer 28, further reducing the temperature before entering evaporator 30 through downstream (major) expansion valve 32B.

[0017] The refrigerant fluid enters evaporator 30 as a sub-cooled liquid or compressed fluid, or in a two-phase liquid/vapor state. The refrigerant evaporates and expands in evaporator 30 to produce a gas or vapor phase, absorbing heat from cooling system 16 as described below.

[0018] Fluid from evaporator 30 enters compressor 24 in a substantially gaseous or vapor state. In two-stage compressor embodiments, as shown in FIG. 1, economizer 28 also delivers cooled fluid to mixer 34, which reduces the temperature of fluid exiting first compressor stage C1. This improves heat transfer for cooling motor M, and eases second-stage compression by reducing the energy required to compress the refrigerant to a superheated vapor state in second compressor stage C2. Along with de-superheater 14, these additional VCS components further increase the coefficient of performance

by reducing temperature differentials, and lowering the total entropy of vapor cycle system 12.

[0019] Cooling system 16 absorbs heat from load 36, and disperses the heat through thermal transfer to evaporator 30 of vapor cycle system 12. In some cooling systems 16, heat is also dispersed to the cooling air flow via heat exchanger (HX) 38.

[0020] Heat load 36 includes one or more aircraft systems that require heating or cooling, for example a cabin, cockpit, cargo bay or galley chiller, or electronics components for radar, weapons control, avionics and cabin-based electronics or display systems. In power electronics cooling system (PECS) embodiments, heat load 36 may include power electronics for flight control actuators and other flight-critical systems.

[0021] Cooling system (or cooling loop) 16 operates on a refrigerant fluid with high heat transfer capability over a wide temperature range, for example polyalphaolefin (PAO) or hydrogenated PAO. Alternatively, cooling system 16 operates on a silicate ester or oil-based coolant fluid such as Coolanol®, as available from Exxon Mobile of Fairfax, Va., or another fluid such as water, glycol, etc.

[0022] The relative flows of cooling system refrigerant through heat exchanger 38 and evaporator 30 are controlled via bypass valves 40A and 40B, based on cooling demands, ambient temperature, flight conditions and the available cooling air flow. For example, bypass valves 40A and 40B can be adjusted to regulate higher levels of air cooling in heat exchanger 38 during cruise flight conditions, and higher levels of evaporator cooling in evaporator 30 during takeoff and landing, or during ground operations.

[0023] Fuel circulation system 18 comprises fuel-air cooler 20, fuel tank 42, return-to tank (RTT) cooler 44, fuel-oil cooler (FOC) 46, and secondary (fuel-air) heat exchanger 48. Fuel system 18 typically operates on a kerosene-type jet fuel such as Jet A or Jet A-1, or a naphtha-type fuel such as Jet B for low-temperature performance. In military applications, fuel system 18 operates on a modified kerosene-based fuel such as JP-5 or JP-8, or a modified naphtha or “wide-cut” fuel such as JP-4.

[0024] Heat transfer in fuel circulation system 18 is determined according to the temperature requirements of the various fuel subsystems, and based on the different performance demands and fuel system capabilities of military-type aircraft, as compared to commercial designs. In the particular embodiment of FIG. 1, for example, flow from fuel tank 42 circulates through fuel cooler 20 to reduce downstream operating temperatures, with fuel cooler 20 located between condenser 26 and de-superheater 14 in the cooling fluid flow. The fuel-air exchange temperature at fuel cooler 20 is thus higher than the condensation temperature at condenser 26, and lower than the de-superheat temperature at de-superheater 14.

[0025] On afterburning turbofan engines, boost pump 50 supplies fuel to inlet valve 52 for afterburner (AB assembly) 54, in order to provide thrust augmentation during short periods of peak operational demand. Boost pump 50 also provides a downstream pressure drop through fuel cooler 20, and generates an overpressure to limit cavity formation at the inlet to main fuel pump 56.

[0026] Main fuel pump 56 drives flow through fuel-oil-cooler 46 and secondary heat exchanger 48. Fuel-oil-cooler 46 accepts heat from oil heat load 58, including rotor bearings and other elements of a combustion turbine or turbofan engine (e.g., the main engines for a jet aircraft). Alternatively,

oil heat load 58 represents a gearbox or other differential rotation system for a turboprop, turboshaft or geared turbofan engine. Secondary heat-exchanger 48 comprises a fuel-air heat exchanger to cool the compressed air flow from integrated power unit 22, and to pre-heat the fuel before combustion in burner 60.

[0027] Valve 62 regulates the recirculation of fuel flow back through RTT cooler 44 to fuel tank 42. As opposed to secondary heat-exchanger 48, which raises the fuel temperature by exchanging heat with compressed air flow from integrated power unit 22, RTT cooler 44 exchanges heat with the expanded cooling air flow to reduce fuel temperatures for storage in fuel tank 42.

[0028] Integrated power unit 22 includes an air-cycle machine with compressor 64 and turbine 66, or an auxiliary power unit (APU) comprising compressor 64 and turbine 66 in flow series with a combustor or burner. In some embodiments, generator 68 is rotationally coupled to turbine 64 and compressor 66, for example using a coaxial shaft and clutch mechanism to swap generator 68 in and out during ground operations, or based on flight conditions and real-time electrical demand.

[0029] Source 70 of bleed air comprises a compressed air supply such as a first-stage compressor bleed or fan air bleed from the main engine, or a third-stream air source such as an independently modulated bleed flow from a downstream compressor section. Alternatively, bleed air is provided by a ram air intake. In further embodiments, source 70 comprises a static inlet for use during ground operations, or a compressed air supply generated by an APU.

[0030] Incoming air is compressed and heated by compressor 64, then cooled by heat transfer to fuel circulation system 18 in secondary (fuel-air) heat exchanger 48. In some embodiments, a primary heat exchanger may also be included, typically upstream of compressor 64.

[0031] The compressed air exchanges heat with the downstream cooling air flow in regenerator (air-air heat exchanger) 72, then expands in turbine 66 to produce a low temperature, relatively low-pressure cooling air flow for thermal management system 10. In air-cycle machine embodiments, there is an overall pressure drop from source 70 to the outlet of expansion turbine 66 or energy input from a motor/generator, providing the energy required to turn compressor 64 and generator 68.

[0032] Depending on embodiment, cooling air from integrated power unit 22 may be mixed with additional cooling fluid from air source 74. Air source 74 includes an additional fan or compressor bleed air supply, a ram air intake or a third-stream compressed air source providing a supply of relatively cool compressed air. Valve 76 regulates or switches the source between integrated power unit 22 and air source 74, depending on flight conditions, ambient pressure and temperature, and cooling demands.

[0033] Downstream of mixer valve 76, the cooling air flow exchanges heat with vapor cycle system 12, cooling system 16 and fuel circulation system 18. Generally, temperatures increase in the downstream direction, as heat is transferred to the cooling air from different components of thermal management system 10. The order of the flow series thus depends on the individual cooling needs of each component, as well as the temperature differential and corresponding entropy and efficiency considerations.

[0034] There is an advantage in using the hottest available sink of thermal energy, as compared to the source tempera-

ture; that is, with small temperature differential  $\Delta T$ , because this allows more heat to be rejected from the system. To promote rapid heat transfer, however, larger differentials are desired, because the heat transfer ( $Q$ ) is proportional to temperature differential  $\Delta T$ . That is,

$$Q = hAA\Delta T, \quad [1]$$

where  $h$  is the heat transfer coefficient and  $A$  is the heat transfer surface area.

[0035] Thermal management also depends on other critical design factors including condensation points and other phase transition temperatures, thermal loading, and environmental (ambient) temperatures and pressures, as compared to the desired cabin and cargo bay conditions across a full range of different flight conditions, and the operating temperature ranges for heat loads including galley chillers, avionics, radar systems and power electronics. Thermal management thus requires constant tradeoffs among different air, fuel, oil, cooling system and VCS components, presenting an almost unlimited number of possible system configurations and corresponding design choices, and making the net results of any particular change or modification difficult to predict.

[0036] In the embodiment of FIG. 1, cooling flow passes first through heat exchanger 38 of cooling system 16. This provides the coldest available cooling fluid at relatively high  $\Delta T$ , to provide rapid chilling of low-temperature galley and cabin air systems, and for flight control and other mission-critical systems including radar, avionics and power electronics.

[0037] Within vapor cycle system 12, cooling air flows through condenser 26 first, in order to effect a vapor/liquid phase transition at a temperature at or below the condensation point. De-superheater 14 is downstream of condenser 26 in the cooling flow series, so that the de-superheat temperature is above the condensation temperature. The superheated vapor phase is hotter than the condensate, so heat can be transferred at higher temperature (lower  $\Delta T$ ), thereby reserving the cooler air for heat sources that required a lower temperature sink.

[0038] As shown in FIG. 1, the cooling air flow also exchanges heat with fuel circulation system 18, reducing the fuel temperature in fuel cooler 20. This puts vapor cycle system 12 in thermal contact with fuel circulation system 18, via the cooling air flow over condenser 26, fuel cooler 20 and de-superheater 14. Downstream of vapor cycle system 12, cooling air also passes through regenerator (air-air heat exchanger) 72 and RTT cooler 44, as described above.

[0039] Depending on embodiment, downstream air may be used to cool thrust nozzle 78, or other main engine components such as blade or vane airfoils for the compressor and turbine section, or hot components of afterburner assembly 54 and burner 60. After core engine or nozzle cooling, cooling air is typically vented to the outside atmosphere.

[0040] FIG. 2 is a schematic illustration of vapor cycle system 12 for thermal management system 10, with air-cooled de-superheater 14 and condenser 26. Cooling system 16 is shown in generic form, exchanging thermal energy with evaporator 30 of vapor cycle system 12. Integrated power unit 22 utilizes an air cycle machine or an APU to produce a regenerating cooling air flow from one or more sources of compressed air, as described above with respect to FIG. 1. Fuel system 18 is also shown in generic form, and thrust nozzle 78 is replaced by a generic cooling load 80.

[0041] As shown in FIG. 2, de-superheater 14 is located between compressor 24 and condenser 26 in the vapor cycle flow series, and between fuel cooler 20 and regenerator 72 in the cooling air flow series. In particular, de-superheater 14 is downstream of condenser 26, where the air is hotter, so the de-superheat temperature is higher than the condensation temperature. Condenser 26 is located downstream of cooling system 16, so the cooling air temperature is higher at condenser 26 than cooling system 16.

[0042] Air-cooled de-superheater 14 include a vapor-air heat exchanger to cool the superheated VCS fluid by exchanging heat with the cooling air flow, lowering the superheated VCS fluid temperature before entering condenser 26. The air temperature is increased downstream of condenser 26, reducing  $\Delta T$  (and the change in entropy) at de-superheater 14. This increases efficiency and raises the system coefficient of performance, as described above.

[0043] De-superheater 14 exchanges thermal energy with fuel circulation system 18 via the cooling air flow through fuel cooler (air-fuel heat exchanger) 20, in flow series between condenser 26 and de-superheater 14. In particular, fuel cooler 20 raises the cooling air temperature above the condensation point, at which condenser 26 operates. De-superheater 14 exchanges additional thermal energy with the fuel flow via downstream components of fuel circulation system 18, as shown FIG. 1, above.

[0044] Condenser 26 is also air cooled, and is located between cooling system 16 and fuel cooler 20 in the cooling air flow series. Condenser 26 exchanges additional thermal energy with the cooling air flow through the cycling of VCS refrigerant through economizer 28, evaporator 30, compressor 24 and back to de-superheater 14, where de-superheater 14 is located downstream of fuel cooler 20 in the cooling air flow. Condenser 26 exchanges thermal energy with fuel circulation system 18 via air flow over fuel cooler 20, and via downstream components as described above for de-superheater 14.

[0045] FIG. 3 is a schematic illustration of vapor cycle system 12 for thermal management system 10, with fuel-cooled de-superheater 14. In this embodiment, de-superheater 14 is located between compressor 24 and condenser 26 in the vapor cycle flow series, and between secondary (fuel-air) heat exchanger 48 and RTT cooler 44 in the fuel flow series.

[0046] Fuel-cooled de-superheater 14 comprises a fuel-vapor heat exchanger to cool the superheated VCS fluid by direct heat exchange with the fuel flow, lowering the superheated refrigerant temperature before entering condenser 26. The fuel temperature is increased downstream of secondary heat exchanger 48, lowering  $\Delta T$  for de-superheater 14 and reducing the change in entropy to improve the coefficient of performance and overall operating efficiency, as described above.

[0047] Condenser 26 is also fuel-cooled, and is located downstream of fuel cooler 20 and upstream of boost pump 50 in the fuel flow series. In this embodiment, condenser 26 condenses the cooled, superheated VCS fluid by direct heat exchange with the fuel flow. Bypass valve 82 regulates the relative fuel flow through fuel tank 42 and fuel cooler 20, maintaining the fuel temperature below the condensation point to encourage a vapor/liquid phase transition in condenser 26.

[0048] While this invention has been described with reference to exemplary embodiments, it will be understood by

those skilled in the art that various changes may be made and equivalents may be substituted for elements thereof without departing from the spirit and scope of the invention. In addition, modifications may be made to adapt a particular situation or material to the teachings of the invention, without departing from the essential scope thereof. Therefore, the invention is not limited to the particular embodiments disclosed herein, but includes all embodiments falling within the scope of the appended claims.

- 1. A vapor cycle system comprising:
  - a compressor for compressing a refrigerant to form a superheated vapor;
  - a de-superheater for cooling the superheated vapor to form a reduced temperature vapor by exchanging heat with a cooling fluid flow;
  - a condenser for condensing the reduced temperature vapor to form a condensed liquid by exchanging heat with the cooling fluid flow; and
  - an evaporator for evaporating the condensed liquid;
 wherein the de-superheater is located downstream of the condenser in the cooling fluid flow, such that a temperature of the cooling fluid flow is higher at the de-superheater than at the condenser.
- 2. The system of claim 1, wherein the cooling fluid flow comprises an air flow.
- 3. The system of claim 2, further comprising an air cycle system for generating the air flow from at least one source selected from the group consisting of a ram air supply, a bleed air supply, or a third-stream air supply from an aircraft engine.
- 4. The system of claim 2, wherein the de-superheater comprises an air-vapor heat exchanger to cool the superheated vapor by heat exchange with the air flow.
- 5. The system of claim 2, further comprising a heat load located between the condenser and the de-superheater in the cooling air flow; wherein the heat load comprises a heat exchanger to cool a fluid by heat exchange with the air flow.
- 6. The system of claim 1, wherein the cooling fluid flow comprises a fuel flow.
- 7. The system of claim 6, wherein the de-superheater comprises a fuel-vapor heat exchanger to cool the superheated vapor by direct heat exchange with the fuel flow.
- 8. The system of claim 1, further comprising a cooling loop for exchanging heat between a heat load and the evaporator.
- 9. The system of claim 8, wherein the cooling loop comprises a heat exchanger located upstream of the condenser in the cooling fluid flow, such that the temperature of the cooling fluid flow is lower at the heat exchanger than at the condenser.
- 10. The system of claim 9, wherein the heat load comprises at least one selected from the group consisting of a passenger cabin, a cargo bay, a galley, an avionics system, a radar system and power electronics for actuating a flight control surface.
- 11. A thermal management system for an aircraft, the system comprising:
  - a cooling loop, wherein the cooling loop circulates coolant inside the aircraft; and
  - a vapor cycle unit, wherein the vapor cycle unit operates on a fluid to cool the coolant, the vapor cycle unit comprising:

- a compressor, configured to compress the fluid to a superheated vapor phase;
  - a de-superheater, configured to cool the fluid from the superheated vapor phase to a cooled vapor phase by exchanging heat with a cooling flow;
  - a condenser, configured to condense the fluid from the cooled vapor phase to a condensed liquid phase by exchanging heat with the cooling flow;
  - an expansion device, configured to expand the fluid from the condensed liquid phase to an expanded phase; and
  - an evaporator, configured to cool the coolant by evaporation of the fluid from the expanded phase to the vapor phase;
- wherein the de-superheater is located downstream of the condenser in the cooling flow, such that the cooling flow is hotter at the de-superheater than at the condenser.
- 12. The system of claim 11, wherein the cooling flow comprises a fuel flow for the aircraft, and wherein the de-superheater comprises a vapor-fuel heat exchanger for cooling the superheated vapor phase by direct heat exchange with the fuel flow.
  - 13. The system of claim 11, wherein the cooling flow comprises a cooling air flow.
  - 14. The system of claim 13, further comprising a fuel cooler located downstream of the condenser and upstream of the de-superheater in the cooling air flow, such that the cooling flow is hotter at the de-superheater than at the fuel cooler.
  - 15. The system of claim 13, wherein the cooling loop comprises a heat exchanger located upstream of the condenser in the cooling air flow, such that the cooling air flow is colder at the heat exchanger than at the condenser.
  - 16. A method for cooling an aircraft system, the method comprising:
    - circulating a coolant through the aircraft system;
    - cooling the coolant by exchanging heat with an evaporating fluid;
    - compressing the evaporating fluid to form a superheated vapor;
    - de-superheating the superheated vapor by exchanging heat with a cooling flow at a de-superheat temperature; and
    - condensing the superheated vapor by exchanging heat with the cooling flow at a condensation temperature, wherein the condensation temperature is lower than the de-superheat temperature.
  - 17. The method of claim 16, further comprising generating the cooling flow as a fuel flow for the aircraft by pumping fuel from a fuel tank.
  - 18. The method of claim 16, further comprising generating the cooling flow as a stream of cooling air by expansion of a compressed air source.
  - 19. The method of claim 16, further comprising cooling the coolant by exchanging heat with the cooling flow at a temperature lower than the condensation temperature.
  - 20. The method of claim 16, further comprising cooling a fuel flow for the aircraft by exchanging heat with the cooling flow at a temperature higher than the condensation temperature and lower than the de-superheat temperature.

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