



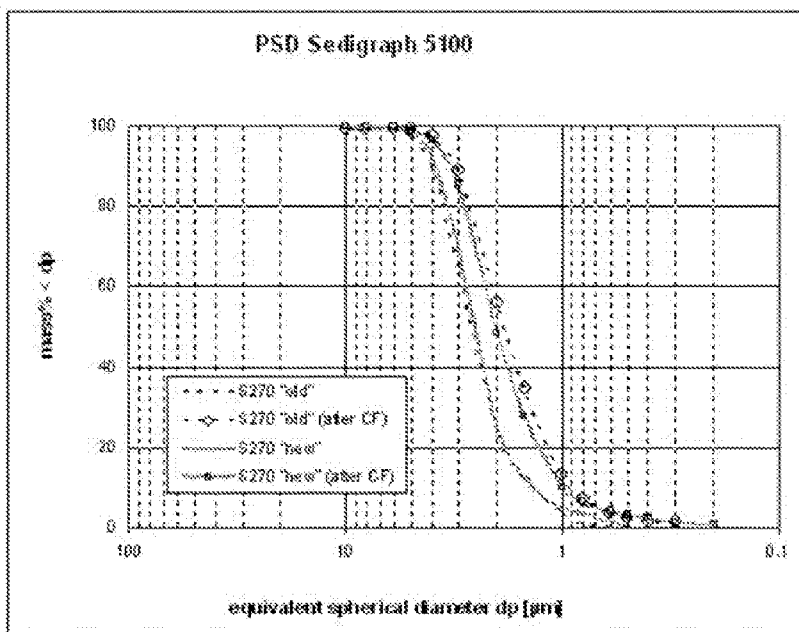
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- (71) Applicant: **OMYA DEVELOPMENT AG** [CH/CH];
Baslerstrasse, CH-4665 Oftringen (CH).
- (72) Inventors; and
- (71) Applicants (for US only): **WENK, Joe** [US/US]; 388
Hunters Crossing Lane, Kingsport, TN 37664 (US).
SAUNDERS, George [US/US]; 1946 Forest Dale Road,
Brandon, VT 05733 (US). **MAURER, Marc** [FR/FR]; 8
Rue De La Pyramide, F-68128 Village-neuf (FR).
SKRZYPCZAK, Mathieu [FR/FR]; 92 A Avenue De
Bale, F-68300 Saint-louis (FR).

- (74) Agent: **ARNOLD, Craig, J.**; Amster, Rothstein & Eben-
stein LLP, 90 Park Avenue, New York, NY 10016 (US).
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[Continued on next page]

(54) Title: PROCESS FOR PREPARING SCALENOHEDRAL PRECIPITATED CALCIUM CARBONATE

Figure 1



(57) Abstract: The present invention provides a process for preparing a precipitated calcium carbonate product. The process comprises the steps of preparing slaking quick lime to obtain slaked lime; and subjecting the slaked lime, without agitation, without prior cooling in a heat exchanger, and in the absence of any additives, to carbonation with carbon dioxide gas to produce PCC. The newly prepared product develops better performance thanks to improved resistance during processing.

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PROCESS FOR PREPARING SCALENOHEDRAL
PRECIPITATED CALCIUM CARBONATE

FIELD OF THE INVENTION

[0001] The present invention relates to a method for producing a precipitated calcium carbonate and, in particular, a precipitated calcium carbonate product in substantially scalenohedral form.

BACKGROUND OF THE INVENTION

[0002] In recent years calcium carbonate has found a wide array of uses across many fields. For example, calcium carbonate is one of the most widely used minerals in the paper, plastic, paint and coating industries both as a filler and, due to its white color, as a coating pigment. In the paper industry calcium carbonate is valued for its high brightness, opacity and gloss and is commonly used as a filler to make bright opaque paper. In addition, calcium carbonate is frequently used as an extender in paints and is also used as a filler in adhesives, sealants and plastics. High grade calcium carbonate has also found uses in formulations of pharmaceuticals.

[0003] Calcium carbonate is known to exist as natural occurring minerals as well as a synthetically produced products.

[0004] "Ground natural calcium carbonate (GNCC)" in the meaning of the present invention is a calcium carbonate obtained from natural sources including marble, chalk or limestone or dolomite. Calcite is a carbonate mineral and the most stable polymorph of calcium carbonate. The other polymorphs of calcium carbonate are the minerals aragonite and vaterite. Aragonite will change to calcite at 380-470°C, and vaterite is even less stable. Ground calcium carbonate is processed through a treatment such as grinding, screening and/or fractionizing by wet and/or dry, for example, by a cyclone. It is known to the skilled person that ground calcium carbonate can inherently contain a defined concentration of magnesium, such as it is the case for dolomitic limestone.

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[0005] "Precipitated calcium carbonate (PCC)" in the meaning of the present invention is a synthesized material, generally obtained by precipitation following the reaction of carbon dioxide and lime in an aqueous environment or by precipitation of a calcium and carbonate source in water or by precipitation of calcium and carbonate ions, for example CaCl_2 and Na_2CO_3 , out of solution. Precipitated calcium carbonate exists in three primary crystalline forms: calcite, aragonite and vaterite, and there are many different polymorphs (crystal habits) for each of these crystalline forms. Calcite has a trigonal structure with typical crystal habits such as scalenohedral (S-PCC), rhombohedral (R-PCC), hexagonal prismatic, pinacoidal, colloidal (C-PCC), cubic, and prismatic (P-PCC). Aragonite is an orthorhombic structure with typical crystal habits of twinned hexagonal prismatic crystals, as well as a diverse assortment of thin elongated prismatic, curved bladed, steep pyramidal, chisel shaped crystals, branching tree, and coral or worm-like forms.

[0006] Among these forms, the scalenohedral form of calcite is particularly desirable for use as a bulking pigment in the paper industry because it is relatively inexpensive to produce and it has desirable light scattering properties.

[0007] Generally, one way to produce calcium carbonate commercially is by calcining crude limestone to obtain quicklime. Water is then added to yield an aqueous suspension of calcium hydroxide ("milk of lime"), and carbon dioxide is reintroduced into this slurry to precipitate the calcium carbonate. The product of this process is known as precipitated calcium carbonate ("PCC"). The resulting aqueous suspension, or slurry, of calcium carbonate may be used as is or further processed (e.g., dewatered, grinded, etc.) to form a dry product. The precipitation reaction is capable of producing each of the three polymorphs (calcite, aragonite and vaterite) depending on the exact reaction conditions used.

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[0008] Prior art processes for producing scalenohedral PCC product typically rely on the use of additives such as monosaccharides (e.g, simple sugars such as fructose, glucose), disaccharides (e.g., sucrose, maltose, lactose), polysaccharides (e.g, starch, cellulose, glycogen), triethanolamine, mannitol, diethanolamine, bicine, morpholine, tri-isopropanolamine, N-ethyl diethanolamine, N,N-diethylethanolamine, sodium boroheptonate, or reagents including a polyhydric alcohol or a polyhydric phenol, during the slaking of the quick lime or prior to carbonation (see, e.g., U.S. Patent Nos. 6,294,143, 5,232,678 and 5,558,850).

[0009] Conventional processes for preparing scalenohedral PCC also typically cool the slaked lime before carbonation (see, e.g., U.S. Patent Nos. 3,320,026 and 6,251,356).

[0010] In addition, conventional processes for preparing scalenohedral PCC utilize agitation during carbonation (see, e.g., U.S. Patent Nos. 3,320,026, 5,232,678, 5,342,600, 5,558,850 and 6,251,356).

[0011] In the manufacture of paper, and particularly woodfree paper, there is a desirability of increasing the filler content to achieve higher bulk, and at the same time, increasing the stiffness of the produced/obtained paper. However, one of the downsides of conventional scalenohedral PCC is that it may not be as strong as required in the manufacture of paper, and particularly uncoated woodfree paper. Accordingly, there exists a need for a low cost process for producing precipitated PCC in the scalenohedral form that is stronger than conventional scalenohedral PCC, that permits an increase in the filler content and density without sacrificing stiffness or bulk of the produced paper.

SUMMARY OF THE INVENTION

[0012] The present invention provides a process for producing low cost precipitated PCC in the scalenohedral form that has a stronger resistance of the PCC clusters/crystals during processing (i.e. lesser tendency to form discrete PCC particles), and leads to

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improved stiffness and/or bulk in woodfree paper applications than conventional scalenohedral PCC. In its general form, the present invention accomplishes these requirements by utilizing a two stage manufacturing process. The first stage includes the step of slaking quick lime to obtain slaked lime. The second stage includes the step of subjecting the slaked lime, without agitation, without prior cooling in a heat exchanger, and in the absence of any additives, to carbonation with carbon dioxide gas to produce PCC.

[0013] As will be discussed in the examples below, the product of this two stage process overcomes the deficiencies of prior PCC production processes and results in a scalenohedral PCC product that has a stronger resistance of the PCC clusters/crystals during processing (i.e. lesser tendency to form discrete PCC particles), and leads to improved stiffness and/or bulk in woodfree paper applications than conventional scalenohedral PCC.

[0014] The present invention also provides a PCC or PCC product prepared by the process of the present invention.

[0015] In addition, the present invention provides a material comprising the PCC or PCC product of the present invention. The material may include, for example, products in which it is desirable to include calcium carbonate as a filler, such as paper, paper coatings, paper products, inks, paints, coatings, plastics, adhesives, building products, foodstuffs, cosmetics and pharmaceutical products.

[0016] The present invention also provides a paper coating comprising the PCC or PCC product of the present invention. The PCC or PCC product of the present invention is believed to result in higher gloss and improved opacity.

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[0017] Finally, the present invention is directed to uses of the PCC or the PCC product of the present invention for the manufacture of a material in which it is desirable to use scalenohedral PCC as a filler.

[0018] Additional objects of the invention will be apparent from the description which follows.

BRIEF DESCRIPTION OF THE FIGURES

[0019] Figure 1 represents a graph of the particle size distribution comparing the PCC prepared in accordance with the conventional process (old) with the PCC prepared in accordance with the present invention (new) both before and after centrifugation (after CF).

[0020] Figure 2 represents an SEM photograph taken of the PCC prepared in accordance with the present invention before centrifugation.

[0021] Figure 3 represents an SEM photograph taken of the PCC prepared in accordance with the present invention after centrifugation.

DETAILED DESCRIPTION OF THE INVENTION

[0022] In accordance with the present invention, a precipitated calcium carbonate product is prepared in a two-stage process. In the first stage, quick lime (CaO) is slaked in water to obtain a calcium hydroxide (Ca(OH)₂) slurry, or milk of lime. This reaction is shown in reaction (1) and preferably takes place in a slaker tank:

[0023] (1) $\text{CaO} + \text{H}_2\text{O} \rightarrow \text{Ca(OH)}_2 + \text{heat}$

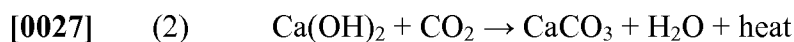
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[0024] The source of quick lime (CaO) used in the slaking reaction is preferably obtained by subjecting crushed limestone to heat (calcination) to form lime (CaO) and carbon dioxide (CO₂). The reaction is preferably performed at an initial temperature of about 85°F to 120°F, and preferably 95°F to 110°F. Since the reaction is exothermic, the temperature typically raises to 180°F to 210°F, and preferably to 195°F to 205°F. The reaction also is desirably performed with mixing or agitation. The duration of the reaction may vary but is typically about 5 to 15 minutes. The solids content of the slurry is typically about 10 to 20 wt.-% solids, and preferably 12 to 18 wt.-% solids. It is within the confines of the present invention that additional water may be introduced during the slaking reaction in order to control and/or maintain and/or achieve the desired solids concentration.

[0025] The calcium hydroxide slurry or slaked lime from the slaking reaction may then be screened if desired in order to remove oversize particles. A suitable screen can include, for example, a screen having an about 30-50 mesh screen size. The calcium hydroxide slurry or slaked lime may then be transferred to an intermediate tank if desired. As a result of air cooling, the temperature of the calcium hydroxide slurry or slaked lime is then reduced by about 40°F to 70°F, and more preferably about 60°F, resulting in slurry temperature of 125°F to 165°F, and preferably 135°F to 155°F. However, contrary to conventional processes for preparing PCC, the calcium hydroxide slurry or slaked lime is not subjected to cooling in a heating exchanger prior to carbonation. In this regard, conventional processes for preparing PCC typically cool the calcium hydroxide slurry or slaked lime to 90°F to 120°F in a heating exchanger prior to carbonation.

[0026] In the second stage, the calcium hydroxide slurry or slaked lime is then subjected to carbonation with carbon dioxide gas to produce PCC. This carbonation step is shown in reaction (2), and takes place in a reactor:

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[0028] Contrary to conventional processes, the calcium hydroxide slurry or slaked lime is not subjected to agitation during the carbonation reaction as is done in conventional processes for preparing PCC. As used herewith, “without agitation” means the agitator of the reactor is turned off. The absence of agitation is believed to slow the reaction and the development of the PCC scalenohedral crystal.

[0029] In addition, contrary to methods for preparing PCC in the prior art, the carbonation is conducted in the absence of any additives. As used herein, the “absence of any additives” means the absence of any additives that may be added prior to or during carbonation, including additives that may be added during the slaking of the quick lime or the resulting calcium hydroxide slurry. Such additives include, for example, a carbohydrate, a monosaccharide, a disaccharide, a polysaccharide, triethanolamine, mannitol, diethanolamine, bicine, morpholine, tri-isopropanolamine, N-ethyl diethanolamine, N,N-diethylethanolamine, sodium boroheptonate, or reagents including a polyhydric alcohol or a polyhydric phenol, or any mixture thereof. Preferably, the absence of any additive means the absence of a monosaccharide or a disaccharide, and most preferably, the absence of any additive means the absence of a disaccharide (e.g., sucrose).

[0030] In accordance with the present invention, the carbon dioxide (CO_2) is selected from gaseous carbon dioxide, liquid carbon dioxide, solid carbon dioxide or a gaseous mixture of carbon dioxide and at least one other gas, and is preferably gaseous carbon dioxide. When the CO_2 is a gaseous mixture of carbon dioxide and at least one other gas, then the gaseous mixture is a carbon dioxide containing flue gas exhausted from industrial processes like combustion processes or calcination processed or alike. CO_2 can also be produced by reacting an alkali- and/or earth alkali carbonate with acid.

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Furthermore, it can be produced by the combustion of organics, such as ethyl alcohol, wood and the like, or by fermentation. When a gaseous mixture of carbon dioxide and at least one other gas is used, then the carbon dioxide is present in the range of 8 to about 99% by volume, and preferably in the range of 10 to 25% by volume, for example 20% by volume. Preferably, the CO₂ is obtained from an external source, and is more preferably captured from the calcination of the crushed calcium carbonate. The carbonation reaction is preferably conducted at an initial temperature of 130°F to 160°F, and more preferably at an initial temperature of 135°F to 145°F. The medium particle size of the calcium carbonate can be controlled by adjusting the starting temperature upwards or downwards 1-2 °F. The reaction desirably precedes until all or substantially all of the calcium hydroxide or slaked lime has been converted into calcium carbonate slurry. In the preferred embodiment, the reaction is stopped when the conductivity of the reaction mixture increases.

[0031] The PCC slurry obtained from the carbonation reaction is then isolated. This is preferably accomplished by transferring the PCC slurry to a holding tank. The PCC slurry may then be subjected to additional processing steps, including, for example, screening, dewatering, dispersion and/or grinding steps to obtain a PCC product having desired characteristics. In the preferred embodiment, the PCC slurry is passed through one or more screens in order to remove larger particles. In the more preferred embodiment, the PCC slurry is passed through a screen to separate particles >45 microns or particles >75 microns.

[0032] The resulting PCC product preferably contains 85% or more scalenohedral particles, and more preferably 90% or more scalenohedral particles, and most preferably 95% or more scalenohedral particles.

[0033] The resulting PCC product also preferably has a medium particle size (d_{50}) of 2.0 to 3.0 microns, and more preferably a medium particle size (d_{50}) of 2.2 to 2.8 microns, and most preferably a medium particle size (d_{50}) of 2.5 microns. Throughout the present application, the "particle size" of a calcium carbonate product is described by its distribution of particle sizes. The value d_x represents the diameter relative to which x % by weight of the particles have diameters less than d_x . This means that the d_{20} value is the particle size at which 20 wt.-% of all particles are smaller, and the d_{75} value is the particle size at which 75 wt.-% of all particles are smaller. The d_{50} value is thus the weight median particle size, i.e. 50 wt.-% of all grains are bigger or smaller than this particle size. For the purpose of the present invention the particle size is specified as weight median particle size d_{50} unless indicated otherwise. For determining the weight median particle size d_{50} value for particles having a d_{50} greater than 0.5 μm , a Sedigraph 5100 device from the company Micromeritics, USA can be used.

[0034] The resulting PCC product also preferably has a BET surface area of 4.0 to 7.0 m^2/g .

[0035] The PCC product obtained in accordance with the process of the present invention has a stronger resistance of the PCC clusters/crystals during processing (i.e. lesser tendency to form discrete PCC particles), and leads to improved stiffness and/or bulk in woodfree paper applications than PCC products prepared using conventional processes.

[0036] If the PCC is subjected to dewatering, dispersion and/or grinding steps, these steps may be accomplished by procedures known in the art. With respect to grinding, the PCC product may be dry ground and/or wet ground. Wet grinding refers to grinding the PCC in a liquid medium (e.g., slurry). Wet grinding may be carried out in the absence of a grinding aid or in the presence of a grinding aid. One or more grinding agents can be

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included, such as, e.g., sodium polyacrylate, a salt of polyacrylate acid, and/or a salt of a copolymer of acrylic acid. Drying may take place using any suitable drying equipment and can, for example, include thermal drying and/or drying at reduced pressure using equipment such as an evaporator, a flash drier, an oven, a spray drier (such as a spray drier sold by Niro and/or Nara), and/or drying in a vacuum chamber. Dispersants also can be included to prepare dispersions if desired.

[0037] The PCC or PCC product produced according to the present invention may be used in various materials in which it is desirable to use calcium carbonate as a filler. For example, the scalenohedral PCC or PCC product may be used in the pharmaceutical field with products such as medicines, in human or animal foodstuffs, in the papermaking field as a filler or in the coating of paper, in water-based or non-water-based paints, in plastics, or in printing inks (e.g., offset printing, rotogravure printing). Preferably, the PCC or PCC product is used as a filler in paper, and more preferably as a filler in uncoated woodfree paper. In this regard, the PCC product of the present invention offers an improvement over conventional PCC in uncoated wood free paper, by allowing better bulk (+ 5-10%), higher opacity and stiffness than conventional PCC.

[0038] When used in the coating of paper, the PCC or PCC product of the present invention is believed to result in higher gloss and improved opacity.

[0039] The present invention is described in the following examples which are set forth to aid in the understanding of the invention, and should not be construed to limit in any way the invention as defined in the claims which follow.

EXAMPLES

[0040] Particle size distribution (mass % particles with a diameter <X) and weight medium diameter (d_{50}) of mineral material. In all of the following examples, the weight

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median diameter and the particle size distribution characteristics of the mineral material were determined via the sedimentation method, i.e. an analysis of sedimentation behavior in a gravimetric field. The measurement was made using a SedigraphTM 5100 of Micromeritics Instrument Corporation.

[0041] The method and the instrument are known to the skilled person and are commonly used to determine grain size of fillers and pigments. The measurement was carried out in an aqueous solution of 0.1 wt.-% $\text{Na}_4\text{P}_2\text{O}_7$. The samples were dispersed using a high speed stirrer and supersonics.

[0042] Specific Surface Area (SSA) of a material. The specific surface area was measured via the BET (Brunauer, Emmett, Teller) method according to ISO 9277 using nitrogen, following conditioning of the sample by heating at 250°C (482°F) for a period of 30 minutes. Prior to such measurements, the sample was filtered, rinsed and dried at 90 to 100°C (194 to 212°F) in an oven for at least 12 hours before being broken down in a mortar with a pestle, and then placed in a mass balance at 130°C (266°F) until a constant weight was observed.

EXAMPLE 1

Preparation of Conventional PCC

[0043] Conventional PCC was prepared as follows. First, burnt lime was reacted with water at a temperature of about 185 to 210°F in a slaker to obtain slaked lime. Next, coarse grits were separated from the slaked lime and dumped to waste. The slaked lime was then collected in a buffer tank and pumped through a heat exchanger to cool the slurry, and then into an intermediate tank. Thereafter, sugar was added to the slaked lime. The cooled slaked lime was then transferred to a reactor set at an initial temperature of >135 °F. Carbon dioxide from the host paper mill's lime kiln was then introduced into the bottom of the reactor with the agitators turned on to convert the slaked lime into

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calcium carbonate slurry. The calcium carbonate slurry was then screened to remove particles >45 microns, and resulting product was then pumped into a storage tank. Two products were prepared using this process by varying the carbonation start temperature. One product had a medium particle size (d_{50}) of a 2.5 micron, a BET specific surface area of 4.9 m²/g, and a d_{75}/d_{25} of 1.49. The other product had a medium particle size (d_{50}) of 2.9 micron, a BET specific surface area of 3.8 m²/g, and a d_{75}/d_{25} of 1.44.

EXAMPLE 2

Preparation of PCC According to the Invention

[0044] The PCC according to the present invention was prepared as in Example 1 with the following differences. First, the slaked lime was not pumped through a heat exchanger to cool the slurry. Second, sugar was not added to the slaked lime. Third, the carbonation reaction was performed with the agitators turned off. The product prepared by this process had a medium particle size (d_{50}) of 2.5 micron, a BET specific surface area of 4.7 m²/g, and a d_{75}/d_{25} of 1.5.

EXAMPLE 3

Handsheets Testing

[0045] The conventional PCC from Example 1 and the PCC according to the present invention from Example 2 were used to prepare handsheets for further testing. More specifically, the handsheets were prepared by first combining 80% hardwood pulp with 20% softwood pulp to achieve a 100% pulp mix. Handsheets were then made using 80% of the pulp and 20% of either the conventional PCC or the PCC according to the present invention. The handsheets were then subjected to the following tests.

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[0046] Gurley porosity. This test measured the time for a 100 cc of air to pass through a paper sample, and used a Gurley-Hill Porosity Meter (Model 4190)(Gurley Precision Instruments, New York) in accordance with Tappi T460 om-96.

[0047] Scott Bond test. This test measured the internal fiber bond strength of paper, and gave an indication of expected performance of the strength in the Z direction. This test was performed with the Scott Internal Bond Tester (Model # B, version AV-2)(Huygen Corporation, Illinois) in accordance with Tappi T569.

[0048] Taber Stiffness. This tests evaluated the stiffness and resiliency of paper, and used a Tabler V-5 Stiffness Tester (Model # 150B) (Teledyne/Taber Inc., New York) in accordance with Tappi T-543 pm-84.

[0049] Tensile Strength. This test measured the maximum tensile strength developed at rupture, and more specifically, the force per unit width required to break a paper sample. This test used the Instron Testing System (Model #1011)(Instron Corporation, Massachusetts) in accordance with Tappi T-498 om-88.

[0050] The results of the testing are presented in Table 1. As can be seen, a handsheet prepared from the PCC according to the present invention had improved stiffness (as determined using the Scott Bond test, the Tabor stiffness test, and tensile strength test) at a higher buck density than handsheets prepared from the conventional PCC products.

Table 1 - PCC Handsheet Testing

		Comparative Example 1 (2.5 mps)	Comparative Example 1 (2.9 mps)	PCC according to invention Example 2
Basis weight				
Basis weight	g/m ²	72.0	71.9	72.2
Basis weight	lb/3300 ft ²	48.8	48.6	48.8
Brightness				
R457 TAPPI	%	88.5	89.5	89.4
Standard deviation		0.2	0.3	0.2
Caliper				
Thickness	Thousandths of inch	5.00	4.70	4.60
Standard deviation		0.20	0.10	0.10
Specific Volume	cm ³ /g	1.76	1.66	1.62
Bulk density	g/cm ³	0.57	0.60	0.62
Filler				
Filler content	%	21.30	21.50	19.90
Gurley Porosity				
Porosity	s	3.9	5.1	4.7
Standard deviation		0.2	0.6	0.5
Opacity				
Opacity	%	88.3	89.6	88.4
Standard deviation		0.7	0.3	0.3
Corrected opacity	%	88.7	90.0	88.8
Scott Bond				
Scott Bond	ft-lb/in ²	64	61	78
Standard deviation		5	7	3
Taber Stiffness				
Bending resist 15°	TU	1.91	2.23	2.33
Standard deviation		0.31	0.28	0.26
Tensile strength				
Tensile strength	lbs/in	8.0	8.4	9.8
Standard deviation		0.3	0.2	0.4
Breaking length	km	1.98	2.09	2.42
Tensile index	Nm/g	19.4	20.5	23.7

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EXAMPLE 4

Resistance Testing

[0051] The PCC prepared by the conventional process (“old PCC”) and the PCC prepared by the process of the present invention (“new PCC”) were subjected to a resistance test involving centrifugation, which subjects the PCC to stress forces due to centrifugal effect and the shear effect generated by the differential speed of the rotor. The parameters of the testing were as follows:

Batch size:	500 Liter
Time operation	~ 60 minutes
centrifuge type, model:	KHD Humboldt SC01
cone angle:	10°
drum diameter:	268 mm
pool depth:	168 mm
rot. speed:	4450 min ⁻¹
diff. rot speed:	41 min ⁻¹
feed rate:	400 l/h
motor nominal current:	28 A
motor nominal power:	15 kW

[0052] The particle size distribution was determined for the old PCC and the new PCC, both before and after centrifugation. The results are shown in Table 2 below and in Figure 1. As shown in Table 2 and Figure 1, the new PCC generated less fines than the old PCC after being subjected to centrifugation. For example, as a result of centrifugation, the old PCC generated an increase of 56% of particles having a $d_p < 2\mu\text{m}$, while the new PCC generated an increase of 48.9% of particles having a $d_p < 2\mu\text{m}$. For $d_p < 1.5\mu\text{m}$, the old PCC generated an increase of 34.6% of particles having a $d_p < 1.5\mu\text{m}$, while the new PCC generated an increase of 27.8% of particles having a $d_p < 1.5\mu\text{m}$. For $d_p < 1.0\mu\text{m}$, the old PCC generated an increase of 13% of particles having a

having a $dp < 1\mu m$, while the new PCC generated an increase of 10.1% particles having a $dp < 1\mu m$. The reduction in fines for the new PCC in comparison to the old PCC as a result of centrifugation demonstrates that the new PCC has a stronger resistance of the PCC clusters/crystals during processing than the old PCC.

Table 2 - PSD Measurements

Mass% < dp	0.2	0.3	0.4	0.5	0.6	0.8	1	1.5	2	3	4	5	6	8	10
S270 "old"				0.3	0.1	0.9	4	12.2	24.2	64.4	89.9	97.4	99.1	99.6	99.5
S 270 "old" (after CF)		1.2	1.6	2.6	3.6	7.1	13	34.6	56	88.7	97.4	99.1	99.3	99.4	99.5
S270 "new"				0.5	1.6	3.4	4.9	12.2	24.9	69.2	91.9	98	99.3	99.2	99.1
S270 "new" (after CF)	0.6	1.2	2.5	3.2	4	6.2	10.1	27.8	48.2	85.5	96.6	98.9	99.6	99.8	99.9

[0053] In addition, SEM photographs of the new PCC before and after centrifugation are shown in Figures 2 and 3, respectively. Samples before and after centrifugation look qualitatively the same, i.e. no observable reduction of the particle size. Therefore, it can be concluded that the inventive PCC has a stronger resistance of the PCC clusters/crystals to the conditions experienced during processing.

[0054] All publications mentioned herein above are hereby incorporated in their entirety. While the foregoing invention has been described in detail for the purposed of clarity and understanding, it will be appreciated by one skilled in the art from a reading of the disclosure that various changes in form and detail can be made without departing from the true scope of the invention in the appended claims. All changes that come within the meaning and range of equivalency of the claims are therefore intended to be embraced therein.

Claims

1. A process for preparing precipitated calcium carbonate (PCC) comprising the steps of:
 - (a) slaking quick lime to obtain slaked lime; and
 - (b) subjecting the slaked lime, without agitation, without prior cooling in a heat exchanger, and in the absence of any additives, to carbonation with carbon dioxide gas to produce PCC.
2. The process according to Claim 1, wherein step (a) is performed at an initial temperature of 85°F to 120°F, preferably at an initial temperature of 95°F to 110°F.
3. The process according to any one of Claims 1-2, wherein the temperature of the reaction in step (a) raises to 180°F to 210°F, preferably to 195°F to 205°F.
4. The process according to any one of Claim 1-3, wherein (a) is performed with mixing or agitation.
5. The process according to any one of Claims 1-4, wherein slaked lime obtained in step (a) has a solids content of 10 to 20% solids, preferably has a solids content of 12 to 18% solids.
6. The process according to any one of Claims 1-5, which further comprises subjecting the slaked lime obtained in step (a) to screening.
7. The process according to any one of Claims 1-6, wherein as a result of air cooling, the temperature of the slaked lime obtained in step (a) is reduced by 40°F to 70°F, prior to carbonation in step (b).

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8. The process according to any one of Claims 1-7, wherein the slaked lime obtained in step (a) is not subjected to cooling in a heating exchanger prior to carbonation in in step (b).

9. The process according to any one of Claims 1-8, wherein the carbonation reaction in step (b) is conducted at an initial temperature of 130°F to 160°F, preferably at an initial temperature of 135°F to 145°F.

10. The process according to any one of Claims 1-9, wherein the PCC obtained in step (b) is isolated.

11. The process according to any one of Claims 1-10, wherein the PCC obtained in step (b) is subjected to screening, dewatering, dispersion and/or grinding steps to obtain a PCC product.

12. The process according to any one of Claims 1-11, wherein the PCC obtained in step (b) is passed through one or more screens to obtain a PCC product.

13. The process according to Claim 11 or 12, wherein the PCC product contains 85% or more scalenohedral particles, preferably contains 90% or more scalenohedral particles, more preferably contains 95% or more scalenohedral particles.

14. The process according to Claim 11 or 12, wherein the PCC product has a medium particle size (d_{50}) of 2.0 to 3.0 microns, preferably of 2.2 to 2.8 microns.

15. The process according to Claim 11 or 12, wherein PCC product has a BET surface area of 4.0 to 7.0 m²/g.

16. A PCC produced by the process according to any one of Claims 1-10.

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17. A PCC product produced by the process according to any one of Claims 11-15.

18. A material comprising the PCC according to Claim 16 or the PCC product according to Claim 17.

19. The material according to Claim 18, wherein the material is a paper, a paper coating, a paper product, an ink, a paint, a coating, a plastic, an adhesive, a building product, a foodstuff or a pharmaceutical product, preferably is paper and more preferably is uncoated woodfree paper.

20. The use of the PCC according to Claim 16 or the PCC product according to Claim 17, for the manufacture of a material selected from a paper, a paper coating, a paper product, an ink, a paint, a coating, a plastic, an adhesive, a building product, a foodstuff or a pharmaceutical product, preferably for the manufacture of paper, more preferably for the manufacture of paper as a paper coating and most preferably for the manufacture of uncoated woodfree paper.

Figure 1

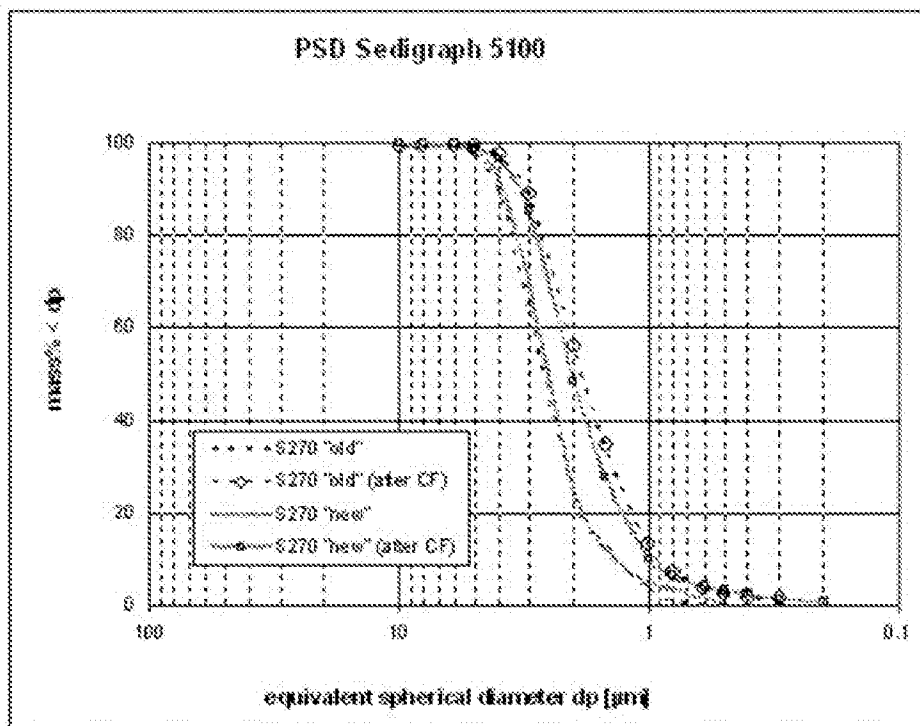


Figure 2

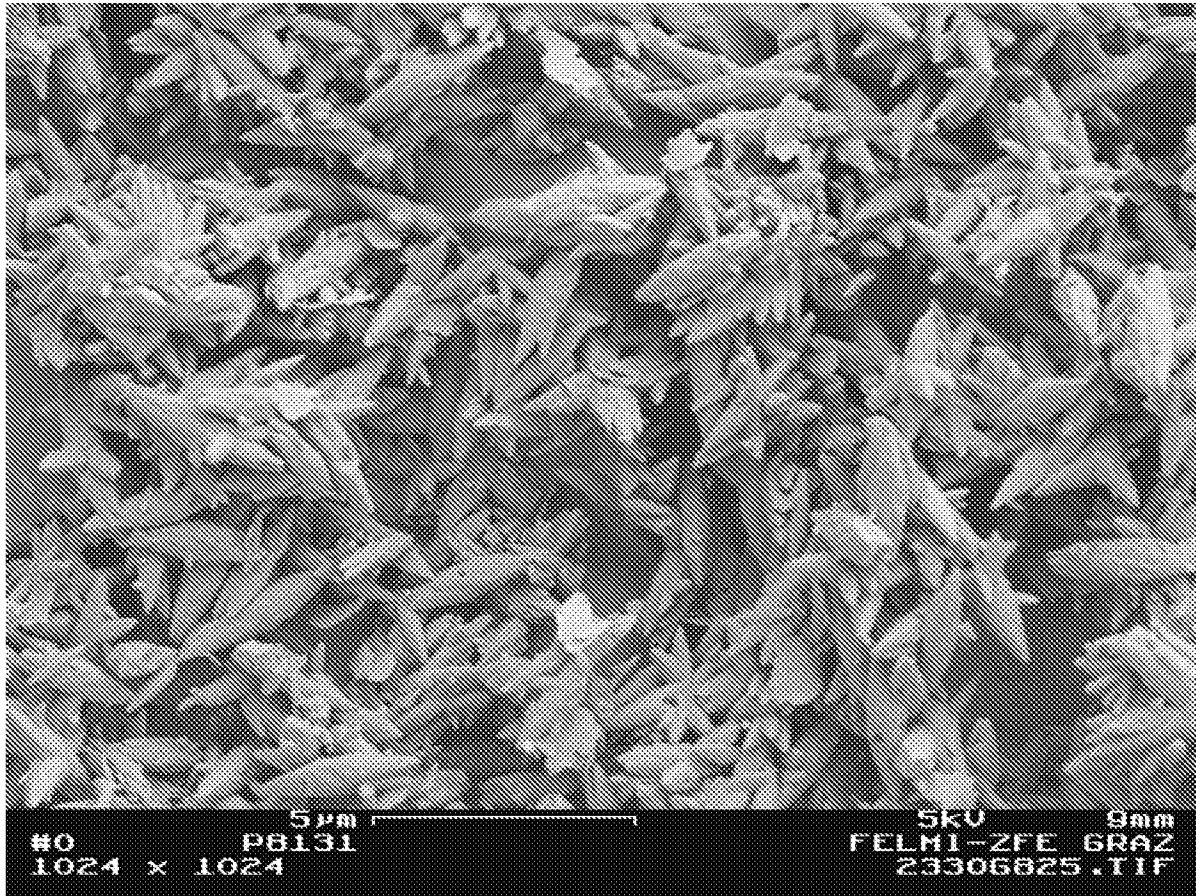
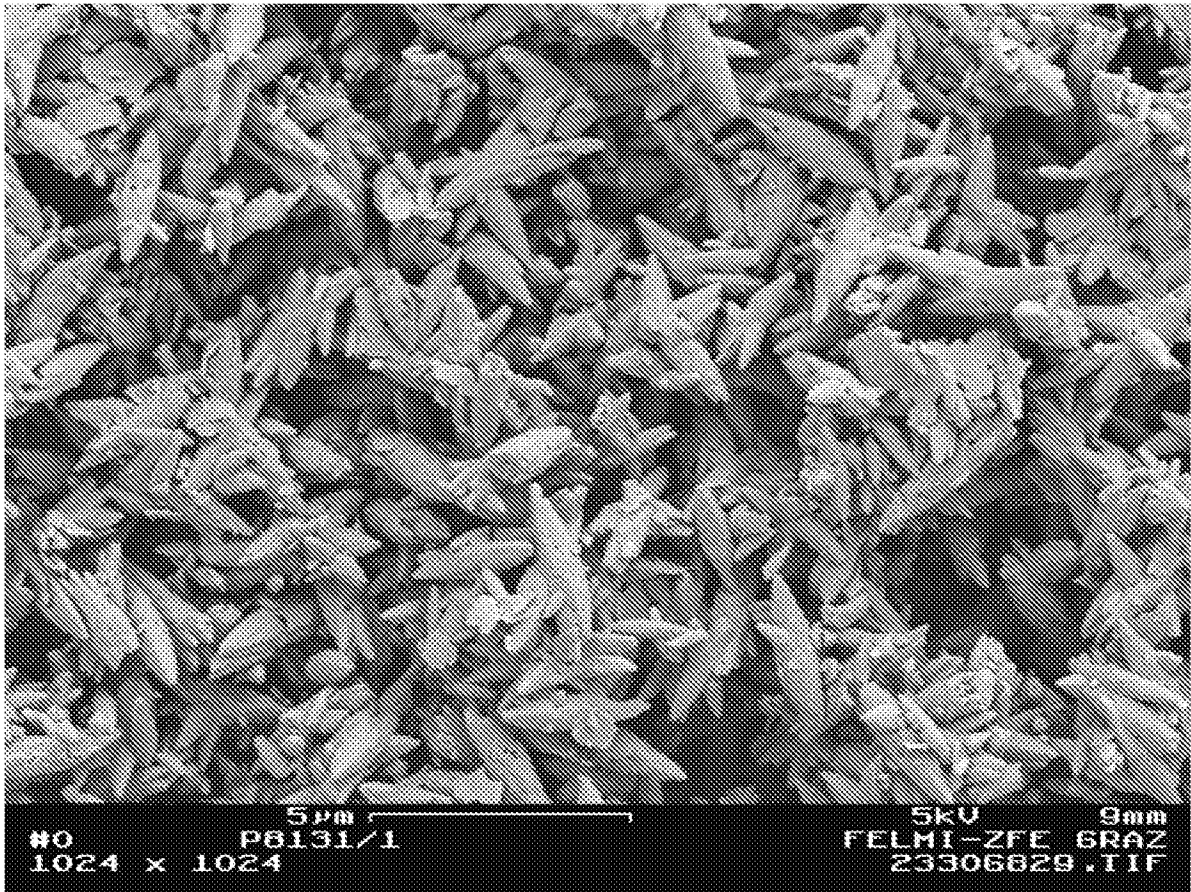


Figure 3



INTERNATIONAL SEARCH REPORT

PCT/US2013/032923 17.06.2013

International application No.

PCT/US 13/32923

A. CLASSIFICATION OF SUBJECT MATTER

IPC(8) - D21H 17/67; C01F 11/02 (2013.01)

USPC - 423/432

According to International Patent Classification (IPC) or to both national classification and IPC

B. FIELDS SEARCHED

Minimum documentation searched (classification system followed by classification symbols)

USPC - 423/432

Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched

USPC - all classes; NPL (key word limited)

Electronic data base consulted during the international search (name of data base and, where practicable, search terms used)

PatBase; Google Scholar

Search Terms: Precipitated, calcium carbonate, quicklime, cooling, exchanger, additives, "without agitation", "without mixing", Wenk w2 Jo*, SAUNDERS w2 George, MAURER w2 Marc, carbonation, carbon w2 dioxide, CO2

C. DOCUMENTS CONSIDERED TO BE RELEVANT

Category*	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
Y	WO 2006/134080 A1 (Cervellati et al.) 21 December 2006 (21.12.2006); pg. 3, ln 12-17	1, 2, 3/1, 3/2
Y	US 6,699,318 B1 (Virtanen) 02 March 2004 (02.03.2004); col 1, ln 33-36	1, 2, 3/1, 3/2
Y	US 2005/0089466 A1 (DeGenova et al.) 28 April 2005 (28.04.2005); para [0017]	2, 3/2

 Further documents are listed in the continuation of Box C.


* Special categories of cited documents:

"A" document defining the general state of the art which is not considered to be of particular relevance

"E" earlier application or patent but published on or after the international filing date

"L" document which may throw doubts on priority claim(s) or which is cited to establish the publication date of another citation or other special reason (as specified)

"O" document referring to an oral disclosure, use, exhibition or other means

"P" document published prior to the international filing date but later than the priority date claimed

"T" later document published after the international filing date or priority date and not in conflict with the application but cited to understand the principle or theory underlying the invention

"X" document of particular relevance; the claimed invention cannot be considered novel or cannot be considered to involve an inventive step when the document is taken alone

"Y" document of particular relevance; the claimed invention cannot be considered to involve an inventive step when the document is combined with one or more other such documents, such combination being obvious to a person skilled in the art

"&" document member of the same patent family

Date of the actual completion of the international search

14 May 2013 (14.05.2013)

Date of mailing of the international search report

17 JUN 2013

Name and mailing address of the ISA/US

Mail Stop PCT, Attn: ISA/US, Commissioner for Patents
P.O. Box 1450, Alexandria, Virginia 22313-1450

Facsimile No. 571-273-3201

Authorized officer:

Lee W. Young

PCT Helpdesk: 571-272-4300

PCT OSP: 571-272-7774

Box No. II Observations where certain claims were found unsearchable (Continuation of item 2 of first sheet)

This international search report has not been established in respect of certain claims under Article 17(2)(a) for the following reasons:

1. Claims Nos.:
because they relate to subject matter not required to be searched by this Authority, namely:

2. Claims Nos.:
because they relate to parts of the international application that do not comply with the prescribed requirements to such an extent that no meaningful international search can be carried out, specifically:

3. Claims Nos.: 4-20
because they are dependent claims and are not drafted in accordance with the second and third sentences of Rule 6.4(a).

Box No. III Observations where unity of invention is lacking (Continuation of item 3 of first sheet)

This International Searching Authority found multiple inventions in this international application, as follows:

1. As all required additional search fees were timely paid by the applicant, this international search report covers all searchable claims.
2. As all searchable claims could be searched without effort justifying additional fees, this Authority did not invite payment of additional fees.
3. As only some of the required additional search fees were timely paid by the applicant, this international search report covers only those claims for which fees were paid, specifically claims Nos.:

4. No required additional search fees were timely paid by the applicant. Consequently, this international search report is restricted to the invention first mentioned in the claims; it is covered by claims Nos.:

Remark on Protest

- The additional search fees were accompanied by the applicant's protest and, where applicable, the payment of a protest fee.
- The additional search fees were accompanied by the applicant's protest but the applicable protest fee was not paid within the time limit specified in the invitation.
- No protest accompanied the payment of additional search fees.