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(71) Applicant(s)
BASF SE

(72) Inventor(s)
Lehenmeier, Maximilian;Skupin, Gabriel;Bussmann, Martin

(74) Agent / Attorney
Watermark Intellectual Property Pty Ltd, Level 1 109 Burwood Road, Hawthorn, VIC, 3122, AU

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(71) Anmelder: **BASF SE** [DE/DE]; 67056 Ludwigshafen
(DE).

(72) Erfinder: **LEHENMEIER, Maximilian**; Dreikönigstraße
6, 69117 Heidelberg (DE). **SKUPIN, Gabriel**;
Schwerdstr.46, 67346 Speyer (DE). **BUSSMANN,**
Martin; Oppelner Str. 4, 67259 Beindersheim (DE).

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(54) Title: INJECTION-MOULDED ARTICLE

(54) Bezeichnung : SPRITZGUSSARTIKEL

(57) Abstract: The present invention relates to an injection-moulded article having a DIN EN ISO 75-2:2004-09 HDT-B of 80 to 105°C, comprising: i) 47 to 59 wt%, relative to the total weight of components i to iv, of a biodegradable aliphatic polyester; ii) 3 to 14 wt%, relative to the total weight of components i to iv, of an aliphatic-aromatic polyester; iii) 15 to 24 wt%, relative to the total weight of components i to iv, of polylactic acid; iv) 10 to 35 wt%, relative to the total weight of components i to iv, of at least one mineral filler; for components i to iv in compounded form, the ratio of component i to component iii in the compound is 2.2 to 3.2 and the DIN EN 1133-1 (01.03.2012) MVR (190°C, 2.16 kg) of the compound is 8 to 50 cm³/10 min.

(57) Zusammenfassung: Die vorliegende Erfindung betrifft einen Spritzgussartikel mit einer HDT-B nach DIN EN ISO 75-2:2004-09 von 80 bis 105°C enthaltend: i) 47 bis 59 Gew.-%, bezogen auf das Gesamtgewicht der Komponenten i bis iv, eines biologisch abbaubaren aliphatischen Polyesters; ii) 3 bis 14 Gew.-%, bezogen auf das Gesamtgewicht der Komponenten i bis iv, eines aliphatisch-aromatischen Polyesters; iii) 15 bis 24 Gew.-%, bezogen auf das Gesamtgewicht der Komponenten i bis iv, Polymilchsäure; iv) 10 bis 35 Gew.-%, bezogen auf das Gesamtgewicht der Komponenten i bis iv, mindestens eines mineralischen Füllstoffs; wobei für den Compound der Komponenten i bis iv gilt, dass das Verhältnis der Komponente i zur Komponente iii im Compound 2,2 bis 3,2 beträgt und dass der MVR nach DIN EN 1133-1 vom 01.03.2012 (190°C, 2,16 kg) des Compounds 8 bis 50 cm³/10 min beträgt.



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Injection-moulded article

Description

5 The present invention relates to an injection-molded item with HDT-B temperature of from 80 to 105°C in accordance with DIN EN ISO 75-2:2004-09, comprising:

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- i) from 47 to 59% by weight, based on the total weight of components i to iv, of a biodegradable polyester comprising:
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- i-a) from 90 to 100 mol%, based on components i-a to i-b, of succinic acid;
- i-b) from 0 to 10 mol%, based on components i-a to i-b, of one or more C₆-C₂₀ dicarboxylic acids;
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- i-c) from 98 to 102 mol%, based on components i-a to i-b, of 1,3-propanediol or 1,4-butanediol;
- i-d) from 0 to 1% by weight, based on components i-a to i-c, of a chain extender or branching agent;
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- ii) from 3 to 14% by weight, based on the total weight of components i to iv, of an aliphatic-aromatic polyester comprising:
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- ii-a) from 30 to 70 mol%, based on components ii-a to ii-b, of a C₆-C₁₈ dicarboxylic acid;
- ii-b) from 30 to 70 mol%, based on components ii-a to ii-b, of terephthalic acid;
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- ii-c) from 98 to 100 mol%, based on components ii-a to ii-b, of 1,3-propanediol or 1,4-butanediol;
- ii-d) from 0 to 1% by weight, based on components ii-a to ii-c, of a chain extender or branching agent;
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- iii) from 15 to 24% by weight, based on the total weight of components i to iv, of polylactic acid;
- iv) from 10 to 35% by weight, based on the total weight of components i to iv, of at least one mineral filler;

where the following applies to the compounded material comprising components i to iv: the ratio of component i to component iii in the compounded material is from 2.2 to 3.2, and the MVR of

the compounded material is from 8 to 50 cm³/10 min in accordance with DIN EN 1133-1 of March 1, 2012 (190°C, 2.16 kg).

Heat-resistant items of this type are suitable for the production of coffee capsules, lids for hot drinks, cutlery, containers for hot contents, and microwave tableware.

US 6,573,340 and WO 2005/063881 disclose filled biodegradable polymer mixtures which comprise a soft polymer, for example an aliphatic-aromatic polyester (PBAT) and a rigid polymer such as polylactic acid (PLA). WO 2013/000847 moreover discloses filled polymer mixtures made of polybutylene succinate (PBS) and PLA, and EP 1561785 discloses filled polymer mixtures made of PBAT, PBS, and PLA. Although the polymer mixtures disclosed in the last two documents are suitable for injection molding, they are not suitable for applications such as coffee capsules, lids for hot drinks, or microwave tableware, because they have limited heat resistance and only moderate impact resistance.

The present invention therefore attempts to provide injection-molded items which do not have the abovementioned disadvantages. A particular desire was to provide a plastic with heat resistance adequate for applications in the field of hot food and drink. A further intention was that the items have sufficiently high impact resistance to comply with the mechanical requirements applicable thereto.

Surprisingly, this property profile is possessed by an injection-molded item comprising:

- i) from 47 to 59% by weight, preferably from 48 to 55% by weight, based on the total weight of components i to iv, of a biodegradable polyester comprising:
 - i-a) from 90 to 100 mol%, based on components i-a to i-b, of succinic acid;
 - i-b) from 0 to 10 mol%, based on components i-a to i-b, of one or more C₆-C₂₀ dicarboxylic acids;
 - i-c) from 98 to 102 mol%, based on components i-a to i-b, of 1,3-propanediol or 1,4-butanediol;
 - i-d) from 0 to 1% by weight, based on components i-a to i-c, of a chain extender or branching agent;
- ii) from 3 to 14% by weight, preferably from 5 to 11% by weight, based on the total weight of components i to iv, of an aliphatic-aromatic polyester comprising:
 - ii-a) from 30 to 70 mol%, based on components ii-a to ii-b, of a C₆-C₁₈ dicarboxylic acid;
 - ii-b) from 30 to 70 mol%, based on components ii-a to ii-b, of terephthalic acid;

ii-c) from 98 to 100 mol%, based on components ii-a to ii-b, of 1,3-propanediol or 1,4-butanediol;

5 ii-d) from 0 to 1% by weight, based on components ii-a to ii-c, of a chain extender or branching agent;

iii) from 15 to 24% by weight, preferably from 15 to 20% by weight, based on the total weight of components i to iv, of polylactic acid;

10 iv) from 10 to 35% by weight, preferably from 18 to 30% by weight, based on the total weight of components i to iv, of at least one mineral filler;

where the following applies to the compounded material comprising components i to iv: the ratio of component i to component iii in the compounded material is from 2.2 to 3.2, and the MVR of
15 the compounded material is from 8 to 50 cm³/10 min and preferably from 14 to 40 cm³/10 min in accordance with DIN EN 1133-1 of March 1, 2012 (190°C, 2.16 kg). The HDT-B temperature of the items produced from these compounded materials is moreover from 80 to 105°C, preferably from 85 to 100°C, in accordance with DIN EN ISO 75-2:2004-09, and at the same time the Charpy impact resistance of these items is preferably more than 80 kJ/m², in particular from 90
20 to 250 kJ/m², in accordance with DIN EN 179-1/1eU:2000+Amd.A (Non-instrumented impact resistance test of June 1, 2001 at 23°C, 50% relative humidity).

The invention is described in more detail below.

25 The aliphatic polyesters i suitable for the invention are described in more detail in WO 2010/034711, which is expressly incorporated herein by way of reference.

The structure of polyesters i is generally as follows:

30 i-a) from 90 to 100 mol%, based on components i-a to i-b, of succinic acid;

i-b) from 0 to 10 mol%, based on components i-a to i-b, of one or more C₆-C₂₀ dicarboxylic acids;

35 i-c) from 98 to 102 mol%, based on components i-a to i-b, of 1,3-propanediol or 1,4-butanediol;

i-d) from 0 to 1% by weight, based on components i-a to i-c, of a chain extender or branching agent.

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The polyesters i described are preferably synthesized in a direct polycondensation reaction of the individual components. The dicarboxylic acid derivatives here are reacted together with the diol in the presence of a transesterification catalyst directly to give the high-molecular-weight

polycondensate. On the other hand, it is also possible to obtain the copolyester i via transesterification of polybutylene succinate (PBS) with C₆-C₂₀ dicarboxylic acids in the presence of diol. Catalysts usually used are zinc catalysts, aluminum catalysts, and in particular titanium catalysts. An advantage of titanium catalysts such as tetra(isopropyl) orthotitanate and in particular tetrakisobutoxy titanate (TBOT) over the tin catalysts, antimony catalysts, cobalt catalysts, and lead catalysts often used in the literature, for example tin dioctanoate, is that any residual quantities of the catalyst or downstream product from the catalyst that remain within the product are less toxic. This is a particularly important factor in biodegradable polyesters because they pass directly into the environment.

The succinic acid, or a mixture of the dicarboxylic acids, is generally first heated to an internal temperature of from 170 to 230°C over a period of about 60-180 min in the presence of an excess of diol, together with the catalyst, resultant water being removed by distillation. The melt of the prepolyester thus obtained is usually condensed at an internal temperature of from 200 to 250°C within a period of from 3 to 6 hours at reduced pressure, while the diol liberated is removed by distillation, until the desired viscosity is reached at intrinsic viscosity (IV) of from 100 to 450 mL/g, and preferably from 120 to 250 mL/g.

The polyesters i of the invention can moreover be produced by the processes described in JP 2008-45117 and EP-A 488 617. It has proven advantageous to begin by reacting components a to c to give a prepolyester with IV of from 50 to 100 mL/g, preferably from 60 to 80 mL/g, and then to react this with a chain extender i-d, for example with diisocyanates, or with epoxy-containing polymethacrylates, in a chain extension reaction to give a polyester i with IV of from 100 to 450 mL/g, preferably from 150 to 300 mL/g.

Acid component i-a used comprises from 90 to 100 mol%, based on acid components a and b, preferably from 91 to 99 mol%, and with particular preference from 92 to 98 mol%, of succinic acid. Succinic acid is accessible by a petrochemical route, or else preferably from renewable raw materials, for example as described in EPA 2185682. EPA 2185682 discloses a biotechnology process for the production of succinic acid and 1,4-butanediol starting from different carbohydrates, using microorganisms from the Pasteurellaceae class.

The quantity used of acid component i-b, based on acid components i-a and i-b, is from 0 to 10 mol%, preferably from 1 to 9 mol%, and with particular preference from 2 to 8 mol%.

The expression C₆-C₂₀ dicarboxylic acids b means in particular adipic acid, suberic acid, azelaic acid, sebacic acid, brassylic acid, and/or arachidonic acid. Preference is given to suberic acid, azelaic acid, sebacic acid, and/or brassylic acid. The abovementioned acids are accessible from removal raw materials. By way of example, sebacic acid is accessible from castor oil. Polyesters of this type feature excellent biodegradation performance [reference: Polym. Degr. Stab. 2004, 85, 855-863].

The dicarboxylic acids i-a and i-b can be used either in the form of free acid or in the form of ester-forming derivatives. Particular ester-forming derivatives that may be mentioned are the di-C₁- to C₆-alkyl esters, such as dimethyl-, diethyl-, di-n-propyl, diisopropyl, di-n-butyl, di-isobutyl, di-tert-butyl, di-n-pentyl-, diisopentyl or di-n-hexyl esters. It is likewise possible to use anhydrides of the dicarboxylic acids. The dicarboxylic acids or ester-forming derivatives thereof can be used here individually or in the form of a mixture.

The diols 1,3-propanediol and 1,4-butanediol are likewise accessible from renewable raw materials. It is also possible to use mixtures of the diols. 1,4-Butanediol is preferred as diol because the melting points of the resultant copolymer are higher and said copolymer exhibits better crystallization.

The ratio of the diol (component i-c) to the acids (components i-a and i-b) established at the start of the polymerization reaction is generally from 1.0:1 to 2.5:1 and preferably from 1.3:1 to 2.2:1 (diol:diacids). Excess quantities of diol are drawn off during the polymerization reaction, and the ratio obtained at the end of the polymerization reaction is therefore approximately equimolar. The expression approximately equimolar means that the diacid/diol ratio is from 0.98 to 1.00.

One embodiment uses from 0 to 1% by weight, preferably from 0.1 to 0.9% by weight, and with particular preference from 0.1 to 0.8% by weight, based on the total weight of components i-a to i-b, of a branching agent i-d and/or chain extender i-d' selected from the group consisting of: a polyfunctional isocyanate, isocyanurate, oxazoline, carboxylic anhydride such as maleic anhydride, epoxide (in particular an epoxy-containing poly(meth)acrylate), an at least trihydric alcohol, and an at least tribasic carboxylic acid. The general procedure uses no branching agents, but only chain extenders.

Examples of suitable bifunctional chain extenders are tolylene 2,4-diisocyanate, tolylene 2,6-diisocyanate, diphenylmethane 2,2'-diisocyanate, diphenylmethane 2,4'-diisocyanate, diphenylmethane 4,4'-diisocyanate, naphthylene 1,5-diisocyanate, or xylylene diisocyanate, hexamethylene 1,6-diisocyanate, isophorone diisocyanate, or methylenebis(4-isocyanatocyclohexane). Particular preference is given to isophorone diisocyanate and in particular to hexamethylene 1,6-diisocyanate.

The expression aliphatic polyesters i in particular means polyesters such as polybutylene succinate (PBS), polybutylene succinate-co-adipate (PBSA), polybutylene succinate-co-sebacate (PBSSe), polybutylene succinate-co-azelate (PBSAz), or polybutylene succinate-co-brassylate (PBSBr). The aliphatic polyesters PBS and PBSA are marketed by way of example by Showa Highpolymer as Bionolle®, and by Mitsubishi as GSPIa®. WO 2010/034711 describes more recent developments.

The number-average molar mass (M_n) of the polyesters i is generally in the range from 5000 to 100 000 g/mol, in particular in the range from 10 000 to 75 000 g/mol, preferably in the range

from 15 000 to 50 000 g/mol, their weight-average molar mass (M_w) being from 30 000 to 300 000 g/mol, preferably from 60 000 to 200 000 g/mol, and their M_w/M_n ratio being from 1 to 6, preferably from 2 to 4. Intrinsic viscosity is from 30 to 450 g/mL, preferably from 100 to 400 g/mL (measured in *o*-dichlorobenzene/phenol (ratio by weight 50/50)). Melting point is in the range from 85 to 130°C, preferably in the range from 95 to 120°C. The MVR range is in the range of from 8 to 50 and in particular from 15 to 40 cm³/10 min (190°C, 2.16 kg) in accordance with DIN EN 1133-1.

The expression aliphatic-aromatic polyesters ii means linear, chain-extended and optionally branched and chain-extended polyesters, as described by way of example in WO 96/15173 to 15176, or in WO 98/12242, expressly incorporated herein by way of reference. Mixtures of different semiaromatic polyesters can likewise be used. More recent developments of interest are based on renewable raw materials (see WO 2010/034689). The expression polyesters ii in particular means products such as ecoflex® (BASF SE).

Among the preferred polyesters ii are polyesters comprising, as essential components:

- ii-a) from 30 to 70 mol%, preferably from 40 to 60 mol%, and with particular preference from 50 to 60 mol%, based on components ii-a) to ii-b), of an aliphatic dicarboxylic acid or a mixture thereof, preferably as follows: adipic acid, azelaic acid, sebacic acid, and brassylic acid,
- ii-b) from 30 to 70 mol%, preferably from 40 to 60 mol%, and with particular preference from 40 to 50 mol%, based on components ii-a) and ii-b), of an aromatic dicarboxylic acid or a mixture thereof, preferably as follows: terephthalic acid,
- ii-c) from 98.5 to 100 mol%, based on components ii-a) to ii-b), of 1,4-butanediol and 1,3-propanediol; and
- ii-d) from 0 to 1% by weight, preferably from 0.1 to 0.2% by weight, based on components ii-a) to ii-c), of a chain extender, in particular of a di- or polyfunctional isocyanate, preferably hexamethylene diisocyanate, and optionally of a branching agent, preferably: trimethylolpropane, pentaerythritol, and in particular glycerol.

Aliphatic diacids and the corresponding derivatives ii-a that can be used are generally those having from 6 to 20 carbon atoms, preferably from 6 to 10 carbon atoms. They can be either linear or branched compounds. However, it is also in principle possible to use dicarboxylic acids having a larger number of carbon atoms, by way of example having up to 30 carbon atoms.

Examples that may be mentioned are: 2-methylglutaric acid, 3-methylglutaric acid, α -ketoglutaric acid, adipic acid, pimelic acid, azelaic acid, sebacic acid, brassylic acid, suberic acid, and itaconic acid. The dicarboxylic acids or ester-forming derivatives thereof can be used here individually or in the form of a mixture of two or more thereof.

It is preferable to use adipic acid, azelaic acid, sebacic acid, brassylic acid, or respective ester-forming derivatives of these, or a mixture thereof. It is particularly preferable to use adipic acid or sebacic acid, or respective ester-forming derivatives of these, or a mixture thereof.

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Preference is in particular given to the following aliphatic-aromatic polyesters: polybutylene adipate terephthalate (PBAT) and polybutylene sebacate terephthalate (PBSeT).

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The aromatic dicarboxylic acids ii-b or ester-forming derivatives of these can be used individually or in the form of a mixture of two or more thereof. It is particularly preferable to use terephthalic acid or its ester-forming derivatives such as dimethyl terephthalate.

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The diols ii-c - 1,4-butanediol and 1,3-propanediol - are accessible in the form of renewable raw material. Mixtures of the diols mentioned can also be used.

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A general procedure uses from 0 to 1% by weight, preferably from 0.1 to 1.0% by weight, and with particular preference from 0.1 to 0.3% by weight, based on the total weight of the polyester, of a branching agent and/or from 0.05 to 1% by weight, preferably from 0.1 to 1.0% by weight, based on the total weight of the polyester, of a chain extender (ii-d). Preferred branching agents and chain extenders (ii-d) are the same as the branching agents and chain extenders (i-d) described in detail above.

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The number-average molar mass (M_n) of the polyesters ii is generally in the range from 5000 to 100 000 g/mol, in particular in the range from 10 000 to 75 000 g/mol, preferably in the range from 15 000 to 38 000 g/mol, their weight-average molar mass (M_w) being from 30 000 to 300 000 g/mol, preferably from 60 000 to 200 000 g/mol, and their M_w/M_n ratio being from 1 to 6, preferably from 2 to 4. Intrinsic viscosity is from 50 to 450 g/mL, preferably from 80 to 250 g/mL (measured in o-dichlorobenzene/phenol (ratio by weight 50/50)). Melting point is in the range from 85 to 150°C, preferably in the range from 95 to 140°C.

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MVR (melt volume rate) is generally from 0.5 to 20 cm³/10 min, preferably from 5 to 15 cm³/10 min, in accordance with EN ISO 1133-1 DE (190°C, 2.16 kg weight). Acid numbers are generally from 0.01 to 1.2 mg KOH/g, preferably from 0.01 to 1.0 mg KOH/g, and with particular preference from 0.01 to 0.7 mg KOH/g, in accordance with DIN EN 12634.

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Poly(lactic acid) (PLA) is used as rigid component iii.

It is preferable to use poly(lactic acid) with the following property profile:

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- melt volume rate from 20 to 50 and in particular from 30 to 40 cm³/10 minutes (MVR for 190°C and 2.16 kg in accordance with ISO 1133-1 DE)
- melting point below 240°C
- glass transition temperature (T_g) above 55°C

- water content smaller than 1000 ppm
- residual content of monomers (lactide) smaller than 0.3%
- molecular weight greater than 80 000 daltons.

5 Examples of preferred polylactic acids are NatureWorks® 6201 D, 6202 D, 6251 D, 3051 D, and in particular 3251 D, and also crystalline polylactic acids from NatureWorks.

10 The percentage proportion by weight used of the polylactic acid iii, based on components i and iv, is from 15 to 24%, preferably from 15 to 20%. It is preferable here that the polylactic acid iii forms the dispersed phase and that the polyester i forms the continuous phase or is part of a cocontinuous phase. The heat resistance of polymer mixtures with polyester i in the continuous phase or as part of a cocontinuous phase is higher than that of polymer mixtures in which polylactic acid iii forms the continuous phase. In order to ensure good heat resistance in the injection-molded item (HDT-B temperature from 85 to 105°C in accordance with DIN EN ISO 15 75-2:2004-09) the ratio of component i to component iii in the compounded material from which the items are produced should be from 2.2 to 3.2, and preferably from 2.5 to 3.1.

20 A general procedure uses from 10 to 35% by weight, in particular from 18 to 30% by weight, and particularly preferably from 18 to 25% by weight, based on the total weight of components i to iv, of at least one mineral filler iv selected from the group consisting of: chalk, graphite, gypsum, iron oxide, calcium chloride, dolomite, kaolin, silicon dioxide (quartz), sodium carbonate, titanium dioxide, silicate, wollastonite, mica, montmorillonites, talc powder, mineral fibers, and conductive carbon black.

25 Particular preference is given to chalk and to talc powder as fillers. Interestingly, it has been found that addition of chalk can provide a further improvement in the biodegradability of the items. Use of talc powder can in turn be more effective in increasing modulus of elasticity and in improving heat resistance.

30 The compounded material of the invention comprising components i to iv can moreover comprise other additives known to the person skilled in the art. Examples are the additional substances conventionally used in plastics technology, for example stabilizers; nucleating agents, such as the mineral fillers iv already mentioned above, or else crystalline polylactic acid; lubricants and release agents, such as stearates (in particular calcium stearate); plasticizers, for 35 example citric esters (in particular tributyl acetyl citrate), glycerol esters, such as triacetyl glycerol, or ethylene glycol derivatives, surfactants, such as polysorbates, palmitates, or laurates; waxes, for example erucamide, stearamide, or behenamide, beeswax or beeswax esters; antistatic agents, UV absorbers; UV stabilizers; antifogging agents, or dyes. The concentrations used of the additives are from 0 to 2% by weight, in particular from 0.1 to 2% by weight, based on the 40 compounded material i to iv of the invention. The compounded material i to iv of the invention can comprise from 0.1 to 10% by weight of plasticizers.

Mixtures of chalk and talc have proven to be particularly advantageous. A ratio of from 1 : 5 to 5 : 1 in the mixture, preferably from 1 : 3 to 3 : 1, and in particular from 1 : 2 to 1 : 1, has been found to be advantageous.

- 5 For the purposes of the present invention, a substance or a substance mixture complies with the "biodegradable" feature when said substance or the substance mixture has a percentage degree of biodegradation of at least 90% after 180 days in accordance with DIN EN 13432.

10 Biodegradability generally leads to decomposition of the polyester (mixtures) in an appropriate and demonstrable period of time. The degradation can take place by an enzymatic, hydrolytic, or oxidative route, and/or via exposure to electromagnetic radiation, for example UV radiation, and can mostly be brought about predominantly via exposure to microorganisms, such as bacteria, yeasts, fungi, and algae. Biodegradability can by way of example be quantified by mixing polyester with compost and storing the mixture for a particular time. By way of example, 15 in accordance with DIN EN 13432 (with reference to ISO 14855), CO₂-free air is passed through ripened compost during the composting process, and the compost is subjected to a defined temperature profile. Biodegradability here is defined as a percentage degree of biodegradation, by taking the ratio of the net quantity of CO₂ released from the specimen (after subtraction of the quantity of CO₂ released by the compost without specimen) to the maximum quantity of CO₂ 20 release from the specimen (calculated from the carbon content of the specimen). Biodegradable polyesters or biodegradable polyester mixtures generally exhibit clear signs of degradation after just a few days of composting, examples being fungal growth, cracking, and perforation.

25 Other methods for determining biodegradability are described by way of example in ASTM D5338 and ASTM D6400-4.

Injection molding, also called the injection-molding process, involves a shaping process that is very frequently used in plastics processing. Injection molding can also provide an extremely cost-effective method of producing large numbers of ready-to-use moldings. In simplified terms, 30 the process functions as follows: the respective thermoplastic material ("molding composition") is melted in an injection-molding machine consisting of a heatable cylinder within which there is a rotating screw, and is injected into a metal mold. The mold cavity determines the shape and the surface structure of the finished component. Weights of components that can be produced nowadays are from well below one gram up to tens of kilograms.

35 Injection molding can provide a method of fast, cost-effective production of consumer articles with high precision. The nature of the surface of the respective component here can be selected by the designers with almost no restriction. It is possible to produce a wide variety of surface structures, from smooth surfaces for optical applications by way of grained effects for regions 40 having attractive haptic properties through to engraved effects or other patterns.

For reasons of cost-effectiveness, the injection-molding process is particularly suitable for the production of relative large numbers of units, for example of packaging items.

Items in widespread use are those such as chocolate-box inserts, games-box inserts, folding blister packs for a very wide variety of small items displayed on adjustable racking in retail outlets, and yoghurt pots and margarine tubs. Lids for coffee cups or other cups for hot drinks are a preferred item, as also are packs intended to contain hot foods or drinks.

A particularly preferred injection-molded item is the coffee capsule. The expression coffee capsule means a pack of volume capacity from 1 ml to 80 ml, preferably from 3 to 50 ml. A pulverulent material from the food-or-drink sector, in particular coffee powder, or a mixture of pulverulent materials from the food-or-drink sector, is charged to said pack. The expression material from the food-or-drink sector means not only coffee but also tea, milk, cocoa, and soup extracts. The shape of the pack can be rotationally symmetrical, conical, spherical, or else angular, but preferably rotationally symmetrical and primarily cylindrical. Said pack serves firstly for the storage of the material(s) from the food-or-drink sector, and also for the preparation of a hot water-based drink which is produced via passage of hot water (at from 60 to 100°C) in a subsequent step. When the water passes through the pack it dissolves substances that provide flavor and bitterness, thus forming the hot drink. The pack is intended to be manufactured via injection molding. The wall thickness used here for the flat film from which the pack(s) are produced has a thickness from 100 to 1000 µm, preferably from 250 to 800 µm, and in particular from 155 to 550 µm. The item can be composed of one, and preferably of a plurality of, layer(s). At least one layer comprises the compounded material described in the introduction comprising components i) to iv). Another layer of the final molded pack preferably forms a barrier layer. The multilayer structure can be produced via coextrusion during the flat-film production process or else, after the flat-film production process, can be applied in the form of layer: for example via extrusion, printing, spraying, or sputtering, in principle by applying a dispersion, a coating material, or any other polymer-based or polymer-containing system, or by applying a metallic or oxide-containing layer, but preferably by using a polymer-based or metalized layer. An example of a metalized layer that can be used is aluminum, and layers suitable as polymer-based layer are those comprising polyglycolic acid (PGA), polyhydroxyalkanoates (PHA), for example poly-3-hydroxybutyrate (PHB), poly-3-hydroxybutyrate-co-3-hydroxyvalerate (PHB(V)), poly-3-hydroxybutyrate-co-3-hydroxy hexanoate (PHB(H)), or poly-3-hydroxybutyrate-co-4-hydroxyvalerate; polyvinyl alcohol (PVOH), polyvinylidene chloride (PVDC), or ethylene-vinyl alcohol (EVOH). This barrier layer is characterized by an oxygen transmission rate (OTR) of from 0 to 1000 g/m²/d, measured on the entire film composite after pack production in accordance with ASTM D1434, and also by a water vapor transmission rate of from 0 to 1000 g/m²/d in accordance with ASTM F1249, and also preferably at the same time by an aroma barrier.

The good oxygen barrier and, respectively, aroma barrier can also be achieved by means of overlap packaging for one or more coffee capsules. Suitable overlap packaging can be barrier-film-coated plastics films or paper films.

Compounded materials comprising components i to iv that are suitable for the injection-molding process are in particular those with MVR (190°C, 2.16 kg) of from 8 to 50 cm³/10 min in accordance with ISO 1133-1 of March 1, 2012, with particular preference from 14 to 40 cm³/10 min.

5

Performance-related tests:

10 The molecular weights M_n and M_w of the semiaromatic polyesters were determined by means of SEC in accordance with DIN 55672-1: eluent hexafluoroisopropanol (HFIP) + 0.05% by weight calcium trifluoroacetate; narrowly distributed polymethyl methacrylate standards were used for calibration.

15 Intrinsic viscosities were determined in accordance with DIN 53728 part 3, January 3, 1985, Capillary viscosimetry. An M-II micro-Ubbelohde viscosimeter was used. Solvent used was the mixture: phenol/*o*-dichlorobenzene in a ratio of 50/50 by weight.

The modulus of elasticity was determined by means of a tensile test on tensile specimens of thickness about 420 μm in accordance with ISO 527-3: 2003.

20

Charpy impact resistance was determined in accordance with DIN EN 179-1/1eU:2000+Amd.A (at 23°C, 50% rel. humidity). The test sample (80 mm \times 10 mm \times 4 mm), in the form of horizontal bar supported close to its ends, is subjected to a single impact of a pendulum, the impact line being central between the two test sample supports, and the velocity of bending (of the test sample) being high and nominally constant (2.9 or 3.8 m/s).

25

HDT-B heat resistance was determined in accordance with DIN EN ISO 75-2:2004-9. A standard test sample is subjected to three-point bending under constant load so as to produce a flexural stress (HDT/B 0.45 MPa) stated in the relevant part of said international standard. The temperature is increased at uniform rate (120 K/h), and the temperature value measured is that at which a defined standard deflection is reached, corresponding to the defined increased in flexural strain (0.2%).

30

1. Starting materials

35

Polyester i:

i-1 Polybutylene succinate: GS-Pla® FZ71-PD from Mitsubishi Chemical Corporation (MVR 22 cm³/10 min (190°C, 2.16 kg))

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Polyester ii:

ii-1 Polybutylene adipate-co-terephthalate: ecoflex® F A1300 from BASF SE (MVR 8.5 cm³/10 min (190°C, 2.16 kg))

- 5 ii-2 Polybutylene sebacate-co-terephthalate: ecoflex® FS A1300 from BASF SE (MVR 8.5 cm³/10 min (190°C, 2.16 kg))

Component iii:

- 10 iii-1 Polylactic acid: (PLA) Ingeo® 3251 D from NatureWorks (MVR 35 cm³/10 min (190°C, 2.16 kg))

Component iv:

- 15 iv-1 Talc IT extra from Mondo Minerals

2. Compounding

The compounding materials listed in Table 1 were manufactured in a Coperion MC 40 extruder.

- 20 The discharge temperatures were set at 250°C. The extrudate was then pelletized under water. After production of the pellets, they were dried at 60°C.

3. Production of the items (general specification GS)

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The compounded material is passed through a Ferromatik Millacron K65 injection-molding machine with 30.00 mm screw. The injection mold was a single- or multi-cavity mold with open hot runner. CAMPUS was used to manufacture molds for the standards ISO 179/1eU and ISO 527-1/-2. Mold temperature was 30°C. The injection pressure and hold pressure used for

- 30 the molds were 560 bar and, respectively, 800 bar.

Table 1 – Items produced by GS:

Example	Comparative C1	2	3	Comparative C4	Comparative C5
Compounds* (amounts in percent by weight)					
i-1	59.8	56	52.5	48.9	45.2
ii-2	0	5	10	15	20
iii-1	22.2	21	19.5	18.1	16.8
iv-1	18	18	18	18	18
i/iii-ratio	2.69	2.67	2.69	2.70	2.69
Items produced by GS					
HDT/B (° C)	94.3	88.3	83.3	79.0	73.1
Charpy (kJ/m ²)	76.2	94.5	119	150	190
Mod. of elasticity (MPa)	2625	2105	1827	1563	1329
MVR (cm ³ /10min)	20.6	15.3	14.8	14.2	13.8

*the compounds each contained 0.3% by weight of erucamide, based on the compound

- 5 Examples 2 and 3 exhibit much-improved impact resistance as compared with C1, while maintaining a very high level of heat resistance (HDT/B). Larger amounts of aliphatic-aromatic polyester ii-2 (see C4 and C5) give injection-molded items with unsatisfactory distortion resistance (HDT/B).
- 0 The injection-molded items described by EP 2 540 779 have either low impact-resistance (addition of talc) or low heat resistance (addition of chalk). Those with chalk feature a low barrier to oxygen as well.

15 Comprises/comprising and grammatical variations thereof when used in this specification are to be taken to specify the presence of stated features, integers, steps or components or groups thereof, but do not preclude the presence or addition of one or more other features, integers, steps, components or groups thereof.

CLAIMS:

1. An injection-molded item with HDT-B temperature of from 79 to 105°C in accordance with DIN EN ISO 75-2:2004-09, comprising:
 - i) from 47 to 59% by weight, based on the total weight of components i to iv, of a biodegradable polyester comprising:
 - i-a) from 90 to 100 mol%, based on components i-a to i-b, of succinic acid;
 - i-b) from 0 to 10 mol%, based on components i-a to i-b, of one or more C₆-C₂₀ dicarboxylic acids;
 - i-c) from 98 to 102 mol%, based on components i-a to i-b, of 1,3-propanediol or 1,4-butanediol;
 - i-d) from 0 to 1% by weight, based on components i-a to i-c, of a chain extender or branching agent;
 - ii) from 3 to 14% by weight, based on the total weight of components i to iv, of an aliphatic-aromatic polyester comprising:
 - ii-a) from 30 to 70 mol%, based on components ii-a to ii-b, of a C₆-C₁₈-dicarboxylic acid;
 - ii-b) from 30 to 70 mol%, based on components ii-a to ii-b, of terephthalic acid;
 - ii-c) from 98 to 100 mol%, based on components ii-a to ii-b, of 1,3-propanediol or 1,4-butanediol;
 - ii-d) from 0 to 1% by weight, based on components i-a to i-c, of a chain extender or branching agent;
 - iii) from 15 to 24% by weight, based on the total weight of components i to iv, of polylactic acid;
 - iv) from 10 to 35% by weight, based on the total weight of components i to iv, of at least one mineral filler;

where the following applies to the compounded material comprising components i to iv: the mass ratio of component i to component iii in the compounded material is from 2.2 to

- 3.2, and the MVR of the compounded material is from 8 to 50 cm³/10 min in accordance with DIN EN 1133-1 of March 1, 2012 (190°C, 2.16 kg).
2. The item according to claim 1, where the ratio of component i to component iii is from 2.5 to 3.1.
 3. The item according to claim 1 or 2, where the MVR of polyester i is from 15 to 40 cm³/10 min in accordance with DIN EN 1133-1 of March 1, 2012 (190°C, 2.16 kg).
 4. The item according any one of claims 1 to 3, where the MVR of polyester ii is from 5 to 15 cm³/10 min in accordance with DIN EN 1133-1 of March 1, 2012 (190°C, 2.16 kg).
 5. The item according any one of claims 1 to 4, where the MVR of polyester iii is from 30 to 40 cm³/10 min in accordance with DIN EN 1133-1 of March 1, 2012 (190°C, 2.16 kg).
 6. The item according any one of claims 1 to 5, which comprises at least 20% by weight of a mineral filler iv, based on the total weight of components i to iv.
 7. The item according to claim 5, where the filler iv is talc powder.
 8. The item according to any one of claims 1 to 7 with Charpy impact resistance greater than 80 kJ/m² in accordance with DIN EN 179-1/1eU:2000.
 9. The item according to any one of claims 1 to 8 further comprising a barrier layer, with volume capacity of from 1 to 80 ml, with oxygen transmission rate of from 0 to 1000 g/m²/d in accordance with ASTM D1434, suitable for the production of coffee capsules.
 10. The use of an item according to any one of claims 1 to 8 as microwave tableware or lids of cups for hot drinks.

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