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(54) **Title:** METHODS FOR MAKING EPOXIDIZED FATTY ACID ALKYL ESTERS

(57) **Abstract:** Methods for making epoxidized fatty acid alkyl esters. Such epoxidized fatty acid alkyl esters can be prepared by epoxidizing a natural oil with an acid and a peroxide. Residual acid in the epoxidized natural oil is not neutralized, such as with a base, prior to esterification to produce the epoxidized fatty acid alkyl esters. Epoxidized fatty acid alkyl esters can be employed in plasticizers, either alone or in combination with other plasticizers, such as epoxidized natural oils. Such plasticizers in turn may be used in the formation of polymeric compositions.

METHODS FOR MAKING EPOXIDIZED FATTY ACID ALKYL ESTERS

FIELD

[0001] Various embodiments of the present invention relate to methods for making epoxidized fatty acid alkyl esters. Such epoxidized fatty acid alkyl esters may be employed as plasticizers or in plasticizer compositions.

INTRODUCTION

[0002] Plasticizers are compounds or mixtures of compounds that are added to polymer resins that can lower the modulus and tensile strength, and increase flexibility, elongation, impact strength, and tear strength of the resin (typically a thermoplastic polymer) to which they are added. A plasticizer may also lower the melting point of the polymer resin, which lowers the glass transition temperature and enhances processability of the polymer resin.

[0003] Phthalic acid diesters (also known as “phthalates”) are commonly used as plasticizers in many flexible polymer products, such as polymer products formed from polyvinyl chloride (“PVC”) and other vinyl polymers. Examples of phthalate plasticizers include diisononyl phthalate, diallyl phthalate, di-2-ethylhexyl-phthalate, dioctyl phthalate, and diisodecyl phthalate. Other plasticizers used for high temperature applications are trimellitates and adipic polyesters.

[0004] Phthalate plasticizers have recently come under intense scrutiny by public interest groups concerned about the negative environmental impact of phthalates and potential adverse health effects in humans (especially children) exposed to phthalates.

[0005] An epoxidized alkyl ester of soybean oil (e.g., epoxidized fatty acid alkyl ester, or “eFAAE”) can be used as a plasticizer for polyvinyl chloride (“PVC”) and other polymers (natural rubber, acrylate, etc.) or alternately, it can be used as a primary or secondary plasticizer in a plasticizer blend (such as with epoxidized soybean oil (“eSO”)). Although advancements have been made, improvements in such plasticizers are still desired.

SUMMARY

[0006] One embodiment is a process for producing epoxidized fatty acid alkyl esters, said process comprising, consisting essentially of, or consisting of:

- (a) epoxidizing a natural oil by contacting said natural oil with an acid and a peroxide to thereby produce an epoxidized reaction mixture comprising epoxidized natural oil, residual acid, residual peroxide, and water;

- (b) removing at least a portion of said residual acid, at least a portion of said residual peroxide, and at least a portion of said water from said epoxidized reaction mixture to thereby produce an intermediate reaction mixture; and
- (c) esterifying at least a portion of said epoxidized natural oil in said intermediate reaction mixture, thereby forming said epoxidized fatty acid alkyl esters, wherein said residual acid is not neutralized prior to said esterifying of step (c).

DETAILED DESCRIPTION

[0007] Various embodiments of the present invention concern methods for preparing eFAAE from natural oils. Such eFAAEs can be employed as a plasticizer alone or in combination with an epoxidized natural oil (“eNO”). Plasticizers comprising eFAAE and optionally eNO can be employed with a variety of polymeric resins and in making various articles of manufacture.

Preparing Epoxidized Fatty Acid Alkyl Esters

[0008] The eFAAE can be prepared by first epoxidizing a natural oil. A “natural oil,” as used herein, is an oil comprising fatty acid triglycerides and derived from a microbe (algae, bacteria), a plant/vegetable, and/or a seed. In an embodiment, natural oil includes genetically-modified natural oil. In another embodiment, the natural oil excludes petroleum-derived oil. Non-limiting examples of suitable natural oils include algae oil, beef tallow oil, canola oil, castor oil, corn oil, fish oil, linseed oil, palm oil, rapeseed oil, safflower oil, soybean oil, sunflower oil, tall oil, tung oil, and any combination thereof.

[0009] In an embodiment, the natural oil is soybean oil.

[0010] The term “epoxidized natural oil,” as used herein, is a natural oil wherein at least one fatty acid moiety contains at least one epoxide group. Non-limiting examples of suitable eNO include epoxidized algae oil, epoxidized beef tallow oil, epoxidized canola oil, epoxidized castor oil, epoxidized corn oil, epoxidized fish oil, epoxidized linseed oil, epoxidized palm oil, epoxidized rapeseed oil, epoxidized safflower oil, epoxidized soybean oil, epoxidized sunflower oil, epoxidized tall oil, epoxidized tung oil, and any combination thereof.

[0011] In an embodiment, the epoxidized natural oil is an epoxidized soybean oil (“eSO”).

[0012] In various embodiments, the natural oil is epoxidized by contacting it with an acid and a peroxide to thereby produce an epoxidized reaction mixture comprising an eNO, residual acid, residual peroxide, and water. Thereafter, a portion or at least a portion of the residual acid,

residual peroxide, and water is removed from the epoxidized reaction mixture prior to esterifying the eNO to produce the eFAAE, as discussed below.

[0013] Suitable acids for use in epoxidizing the natural oil include carboxylic acids, such as formic acid and acetic acid; and peroxy-carboxylic acids, such as performic acid and peracetic acid. Catalysts such as mineral acids (e.g., sulfuric acid) and heterogeneous acid resins (e.g., Amberlite™ IR 120H, available from Rohm & Haas) may optionally be employed in the presence of the acid. In an embodiment, the acid employed for epoxidation is formic acid. In an embodiment, the formic acid is employed in the absence of any catalyst.

[0014] Suitable peroxides for use in epoxidizing the natural oil include aqueous solutions of hydrogen peroxide, peroxy-carboxylic acids, alkyl hydroperoxides, and tertiary hydroperoxides. In an embodiment, the peroxide employed is an aqueous solution of hydrogen peroxide. In various embodiments, the aqueous solution can be a 30 to 50 volume percent (“vol%”) solution.

[0015] Techniques suitable for removing residual acid, peroxide, and water can comprise layer separation. Layer separation involves separation of an aqueous layer, which contains water, acids, peroxide, and possible traces of oil and esters, from an organic layer containing eNO and eFAME. Following epoxidation, the reaction mixture is allowed to settle and separate into two layers by density difference, and the bottom aqueous layer is disposed of while the top organic layer is processed further to obtain the desired product, as described below.

[0016] Removal of residual acid, peroxide, and water can also include vacuum distillation of the epoxidized reaction mixture. In an embodiment, vacuum distillation can be performed on all or some of the organic layer resulting from the above-described layer separation process. Vacuum distillation can be performed employing any known or hereafter discovered distillation techniques and equipment. In this distillation process, the peroxide, acid, and water are removed as the distillate, while eNO is recovered as the bottom fraction. In an embodiment, vacuum distillation can be performed at a temperature ranging from 40 to 80 degrees Celsius (“°C”), from 50 to 70 °C, or at 60 °C. Additionally, vacuum distillation can be performed under a reduced pressure ranging from 1 to 50 millibar (“mbar”) (100 to 5,000 pascals (“Pa”)), from 2 to 40 mbar (200 to 4,000 Pa), from 5 to 20 mbar (500 to 2,000 Pa), or at 10 mbar (1,000 Pa). Distillation can be performed for a time ranging from 1 to 5 hours, or from 2 to 3 hours. Additionally, single stage or multi stage distillation may be employed.

[0017] Following distillation, the resulting distilled epoxidized reaction mixture can have a water content of less than 0.4 weight percent (“wt%”), less than 0.35 wt%, less than 0.3 wt%, or less than 0.25 wt%, based on the entire weight of the distilled epoxidized reaction mixture.

[0018] Following distillation, the resulting distilled epoxidized reaction mixture can have an acid value of less than 1, less than 0.98, less than 0.95, or less than 0.9 milligrams of potassium hydroxide per gram of distilled epoxidized reaction mixture (“mg KOH/g”). Acid value is determined by titration-based techniques as described in ASTM D664. In a typical procedure, a known amount of sample is dissolved in organic solvent (e.g., isopropanol) and is titrated with a solution of potassium hydroxide with known concentration along with phenolphthalein as a color indicator.

[0019] In an embodiment, removal of residual acid from the epoxidized reaction mixture does not include neutralization of the residual acid. The terms “neutralization” and “neutralized” denote a chemical reaction between an acid and a base to form a salt. Accordingly, in the instant case, removal of residual acid from the epoxidized reaction mixture does not include reacting the residual acid with a base. In other words, in various embodiments, no base is added to the epoxidized reaction mixture.

[0020] In an embodiment, removal of residual acid from the epoxidized reaction mixture does not include water washing the reaction mixture or any portion thereof (e.g., an organic layer formed by layer separation, as described above).

[0021] In an embodiment, removal of residual acid from the epoxidized reaction mixture does not include azeotropic distillation.

[0022] Following removal of a portion or at least a portion of the residual acid, residual peroxide, and water, the epoxidized natural oil can be transesterified by contact with an alcohol. Alcohols suitable for use in transesterification include C₁ to C₈ monohydric linear alcohols, such as methanol, ethanol, propanol, and butanol, or C₃ to C₈ branched alcohols, such as isopropanol, isobutanol, and 2-ethylhexanol. In an embodiment, the alcohol employed for transesterification is methanol. A catalyst may also be employed for transesterification. Catalysts suitable for use in transesterification include homogeneous alkali catalysts, including metal alkoxides such as sodium methoxide, potassium methoxide, and sodium ethoxide, or metal hydroxides such as potassium hydroxide (“KOH”), sodium hydroxide (“NaOH”), or supported solid alkali catalysts. Other classes of catalysts that may also be employed include acids, acidic resins, double metal

cyanide (“DMC”) catalysts, enzymes, super acids, super bases, metal salts. The catalyst can be in homogeneous or heterogeneous form. In an embodiment, the catalyst employed for transesterification is sodium methoxide solution in methanol.

[0023] Depending on the alcohol employed for transesterification, the alkyl moiety of the resulting eFAAE ester may be, for example, a methyl group, an ethyl group, a propyl group, or a 2-ethylhexyl group. As used herein, an “epoxidized fatty acid alkyl ester” is a C₄-C₂₄ (saturated or unsaturated) carboxylic acid alkyl ester with at least one epoxide group. An “epoxide group” is a three-member cyclic ether (also called oxirane or an alkylene oxide) in which an oxygen atom is joined to each of two carbon atoms that are already bonded to each other. In an embodiment, the eFAAE is an epoxidized fatty acid methyl ester (“eFAME”).

[0024] In various embodiments, the eFAAE has an American Public Health Association (“APHA”) color index value of less than 100, less than 90, less than 80, less than 70, less than 60, or less than 55. APHA color is determined according to ASTM standards E1209 and E313.

Plasticizer

[0025] The present disclosure provides a plasticizer comprising an eFAAE, prepared as described above, and optionally an eNO. In an embodiment, the present plasticizer is a phthalate-free plasticizer, or is otherwise void or substantially void of phthalate.

[0026] When both eNO and eFAAE are present, the plasticizer can contain relative amounts of eNO (e.g., eSO) to eFAAE (e.g., eFAME) in a weight ratio in the range of from greater than (“>”) 0 : less than (“<”) 100 to <100 : >0, more typically from 10:90 to 90:10, more typically from 20:80 to 80:20, and even more typically from 30:70 to 70:30. Weight ratios are based on total weight of the plasticizer.

Polymeric Composition

[0027] The present disclosure provides a polymeric composition. In an embodiment, a polymeric composition is provided which includes a polymeric resin and the present plasticizer as disclosed above.

[0028] Non-limiting examples of suitable polymeric resins include polysulfides, polyurethanes, acrylics, epichlorohydrins, nitrile rubber, chlorosulfonated polyethylene, chlorinated polyethylene, polychloroprene, styrene butadiene rubber, natural rubber, synthetic rubber, EPDM rubber, propylene-based polymers, ethylene-based polymers, and vinyl chloride resins. The term, “propylene-based polymer,” as used herein, is a polymer that comprises a

majority weight percent polymerized propylene monomer (based on the total amount of polymerizable monomers), and optionally may comprise at least one polymerized comonomer. The term, "ethylene-based polymer," as used herein, is a polymer that comprises a majority weight percent polymerized ethylene monomer (based on the total weight of polymerizable monomers), and optionally may comprise at least one polymerized comonomer.

[0029] The term "vinyl chloride resin," as used herein, is a vinyl chloride polymer, such as polyvinyl chloride ("PVC"), or a vinyl chloride copolymer such as vinyl chloride/vinyl acetate copolymer, vinyl chloride/vinylidene chloride copolymer, vinyl chloride/ethylene copolymer or a copolymer prepared by grafting vinyl chloride onto ethylene/vinyl acetate copolymer. The vinyl chloride resin can also include a polymer blend of the above-mentioned vinyl chloride polymer or vinyl chloride copolymer with other miscible or compatible polymers including, but not limited to, chlorinated polyethylene, thermoplastic polyurethane, olefin polymers such as a methacryl polymer or acrylonitrile-butadiene-styrene polymer.

[0030] In an embodiment, the polymeric resin is PVC.

[0031] In an embodiment, the polymeric composition includes from 25 wt% to 90 wt% PVC, from 5 wt% to 20 wt% eFAAE, from 5 wt% to 20 wt% eNO, and from 0 wt% to 35 wt% filler.

Additives

[0032] The polymeric composition may include one or more of the following optional additives: a filler, a flame retardant, a heat stabilizer, an anti-drip agent, a colorant, a lubricant, a low molecular weight polyethylene, a hindered amine light stabilizer, a UV light absorber, a curing agent, a booster, a retardant, a processing aid, a coupling agent, an antistatic agent, a nucleating agent, a slip agent, a viscosity control agent, a tackifier, an anti-blocking agent, a surfactant, an extender oil, an acid scavenger, a metal deactivator, and any combination thereof.

[0033] In an embodiment, the polymeric composition includes PVC, the present plasticizer, a filler (calcium carbonate, clays, silica, and any combination thereof), metal soap stabilizers (zinc stearate or mixed metal stabilizers containing Ca, Zn, Mg, Sn, and any combination thereof), a phenolic or related antioxidant, and a processing aid.

Coated Conductor

[0034] In an embodiment, the above-described polymeric composition can be employed in forming a coating on a conductor. A "conductor," as used herein, is one or more wire(s) or fiber(s) for conducting heat, light, and/or electricity. The conductor may be a single-wire/fiber

or a multi-wire/fiber and may be in strand form or in tubular form. Non-limiting examples of conductors include metals such as silver, gold, copper, carbon, and aluminum. The conductor may also be optical fiber made from either glass or plastic. The coated conductor may be flexible, semi-rigid, or rigid. The coating (also referred to as a “jacket,” “sheath,” or “insulation”) can be on the conductor or on another polymeric layer around the conductor.

TEST METHODS

APHA Color Measurement

[0035] Measure liquid color according to ASTM standards E1209 and E313 using a BYK Gardner LCS IIITM instrument and measure in APHA units. Set up the bench-top instrument and perform calibration check to insure the instrument is working within specifications. Measure sample color using the protocol listed below:

- Set LCS III to measure Hazen/Alpha indices;
- Measure each sample via syringe (10 mL) into individual calibrated cuvettes;
- Place each loaded cuvette into the LCS III and press the test button; a Hazen/Alpha number is generated. Record this number, remove the sample and place back into the LCS III to measure a second time (record data). Repeat for a third time (record data).
- Remove the loaded cuvette and set aside; reset the LCS III to measure Yellowness Index, measure the same cuvette for Yellowness Index (record three measurements).

EXAMPLES

Comparative Example 1: Neutralization, Washing, and Vacuum Drying

[0036] Charge 100 g of soybean oil (GEMINITM, available from Cargill) to a reactor along with 13.2 g of formic acid (90% purity, available from S. D. Fine Chemicals). The reaction vessel is a 500-ml three-neck round-bottom flask with variable speed overhead stirrer having a suitable Teflon blade. Immerse the reactor in an oil bath having temperature control for heating / cooling the reactor. The reactor further includes a reflux condenser and a feeding pump for controlled addition of one or more reactants. The reaction can be carried out in batch or semi-batch mode. Preheat the reaction mass to 27-30 °C, by maintaining the oil bath temperature at 30 °C. Ensure proper mixing in the reactor by mixing the reaction mixture with an overhead stirrer operated at 400 rpm. Add 82.5 g of 50 wt% hydrogen peroxide (“H₂O₂” 48-52 wt% aqueous solution, available from MERCK) to the reactor at a flow rate of 50 ml/hr with a peristaltic pump. The pump can be operated at constant speed / variable speed to control the

reaction exotherm. Maintain temperature of the reaction mixture below 60 °C during addition by controlling the addition rate of the H₂O₂. Once addition of the H₂O₂ is complete, heat the reaction mass to 60 °C and allow the reaction to proceed for five hours. At the end of the reaction, subject the reaction mass to layer separation for two hours. During layer separation, the product eNO and unreacted NO are allowed to separate in the form of an upper organic layer while acids, water, and unreacted peroxide separate as a lower aqueous layer. Drain the resulting aqueous layer to separate most of the water and formic acid. Neutralize the organic layer using dilute bicarbonate solution to remove residual formic acid. Prepare a saturated sodium bicarbonate solution by dissolving sodium bicarbonate powder (99% pure, available from Sigma Aldrich) in distilled water which is further diluted in 5 volumes of distilled water to prepare dilute alkali solution for neutralization. 50 mL of this dilute bicarbonate solution is used for neutralization. Thereafter, wash the organic layer with water several times until it becomes neutral. To determine neutrality, the pH of the wash water is measured after each washing using litmus paper and washing is continued until it reaches ~7. A total 150 mL of wash water is required in five washing steps. For each washing step, 30 mL of distilled water is added in the separating funnel containing the organic layer. The mixture is shaken to ensure adequate contact and allowed to settle. Once clear separation is achieved, the bottom aqueous layer is drained and the top organic layer is washed further. The resulting product contains 0.93 wt% water and has an acid value of 0.85 mg KOH/g. Acid value is determined by titrating the product against 0.1 N KOH in presence of solvent using phenolphthalein as color indicator (ASTM D974). Water content is determined by standard Karl Fischer Titration based method (ASTM D789). Remove residual water under vacuum at ~10 mbar (1,000 Pascals ("Pa")) and 60 °C for two hours, reducing the water content to 0.31%, while the acid value remains nearly the same (0.82).

[0037] Transesterify this epoxidized product using methanol with sodium methoxide as a catalyst. Mix 44.2 g of epoxidized product with 15 g of methanol (>99% pure, available from Sigma Aldrich) and 1.78 g of 25% sodium methoxide solution in methanol (commercial catalyst solution available from Sigma Aldrich). Perform the reaction at 50 °C for two hours. Wash the end product with water after separating glycerol layer from the bottom. Five water washes with 30 mL each are employed to remove the residual catalyst. Wash water is added in the separating funnel containing crude product and shaken. The mixture is allowed to settle into two distinct layers. The bottom aqueous wash water layer is drained while the top organic layer containing

eFAME is subjected to further washing steps. Remove traces of water and methanol under vacuum (~10 mbar (1,000 Pa) vacuum at 60 °C) to obtain the purified product eFAME. The final product properties are provided in Table 1, below.

Comparative Example 2: Azeotropic Distillation

[0038] Epoxidize 100 g of soybean oil using the protocol described in Comparative Example 1 up to and including the initial layer separation step. Subject the organic layer containing residual formic acid and water to azeotropic distillation. Water forms an azeotrope with methyl ethyl ketone ("MEK") at 73.5 °C with 89% MEK by weight. Perform azeotropic distillation by adding excess (50 g) MEK (>99% purity, available from Sigma Aldrich) and then distilling off the water-MEK azeotrope at 75 to 80 °C with ambient pressure. Analyze product after azeotropic distillation for moisture content and acid value as described above in Comparative Example 1 and compare with the water content and acid value before azeotropic distillation to determine extent of removal. Water content is reduced from 1.82% to 0.4%, while acid value is reduced from 10.32 to 3.6 after azeotropic distillation. This indicates that water removal is 78.01%, while acid removal is 65.12%.

[0039] Transesterify 44.2 g of this mixture using methanol with sodium methoxide as a catalyst as described in Comparative Example 1. Additional 0.5% catalyst is required for this reaction because of high acid value, and excessive foaming is observed during reaction. The final product properties are provided in Table 1, below.

Example 1: Vacuum Distillation (100 g)

[0040] Epoxidize 100 g of soybean oil using the protocol described in Comparative Example 1 up to and including the layer separation step. Thereafter, subject the organic layer directly to vacuum distillation to remove residual formic acid and water from the reaction mixture. Perform vacuum distillation at 60 °C and 10 mbar (1,000 Pa) vacuum for two hours. Analyze bottom product after vacuum distillation for moisture content and acid value, and compare with the moisture content and acid value before distillation to determine extent of removal. Moisture content is reduced from 1.77% to 0.24%, while acid value is reduced from 9.51 to 0.88 after vacuum distillation. This indicates that water removal is 87.2% while acid removal was 91.14%. Transesterify 44.2 g of this mixture as described in Comparative Example 1. The final product properties are provided in Table 1, below.

Example 2: Vacuum Distillation (200 g)

[0041] Epoxidize 200 g of soybean oil in the same manner as described in Example 1 using 26.4 g of formic acid and 165 g of 50% H₂O₂. Maintain addition time, temperature, and reaction time as described in Example 1. Subject the product at the end of epoxidation to vacuum distillation as described in Example 1 for three hours, and analyze for water content and acid value. Water content is reduced from 1.89% to 0.22%, while acid value is reduced from 11.3 to 0.9 after vacuum distillation. This indicates that water removal is 88.86%, while acid removal is 92.38%. Transesterify 44.2 g of this mixture as described in Comparative Example 1. The final product properties are noted in Table 1, below.

Table 1: Final eFAME Properties

	Comparative Example 1	Comparative Example 2	Example 1	Example 2
Oxirane oxygen	7.11	7.08	7.12	7.06
Iodine value	1.3	1.1	1.2	1.32
% Yield (eFAME)	92.2%	85.28%	95.2%	94.48%
% moisture	0.33%	0.4%	0.24%	0.22%
Acid value	0.51	0.92	0.46	0.48

Example 3 – Comparison of Vacuum Distillation with Conventional / Other Processes

[0042] Epoxidized soybean oil (“eSO”) samples (prior to esterification) from Examples 1 and 2 are compared to those obtained in Comparative Examples 1 and 2. Key product specifications, such as percent oxirane oxygen and iodine value, are measured to assess the product quality. Oxirane oxygen content is determined according to ASTM D1652. Iodine value is determined according to ASTM D5768. In addition, water content and acid value are obtained to compare the extent of separation achieved by vacuum distillation process as well as for the conventional / other processes. A summary of these product analyses is noted in Table 2, below.

Table 2: eSO Properties (comparison of various downstream processes)

	Oxirane oxygen (%)	Iodine value	Moisture content (%)	Acid value
Target Final Product Specification for eSO	> 6.5	< 5	< 0.4%	< 1
Comparative Example 1: eSO after neutralization & washing + vacuum drying	7.11	1.3	0.31	0.82

	Oxirane oxygen (%)	Iodine value	Moisture content (%)	Acid value
Comparative Example 2: eSO after azeotropic distillation	7.08	1.1	0.4	3.6
Example 1: eSO after vacuum distillation (100 g scale)	7.12	1.2	0.24	0.88
Example 2: eSO after vacuum distillation (200 g scale)	7.06	1.32	0.22	0.9

Example 4 – Color Analysis and Comparison

[0043] Analyze each of the samples described above in Comparative Examples 1 and 2, and Examples 1 and 2, for color both at the ESO stage (i.e., prior to transesterification) and following transesterification. Color analyses are performed according to the test method described above. The results of the color analyses for the ESO stage samples are provided in Table 3, below; results from the color analyses for the transesterified samples are provided in Table 4, below.

Table 3: eSO Color Properties

	Color Value (APHA)
Target Final Product Specification	175 max
Comparative Example 1 Neutralization & washing + vacuum drying	130
Comparative Example 2 Azeotropic distillation	126
Example 1 Vacuum distillation (100 g scale)	128
Example 2 Vacuum distillation (200 g scale)	131

Table 4: eFAME Color Properties

	Color Value (APHA)
Target Final Product Specification	175 max
Comparative Example 1: Neutralization & washing + vacuum drying + transesterification	154
Comparative Example 2: Azeotropic distillation + transesterification	132
Example 1:	

Vacuum distillation + transesterification (100 g scale)	40
Example 2: Vacuum distillation + transesterification (200 g scale)	51

[0044] Although no color value improvement was noted in the eSO samples, the final eFAME samples of Examples 1 and 2 exhibited substantially decreased color values compared to Comparative Examples 1 and 2.

CLAIMS

1. A process for producing epoxidized fatty acid alkyl esters, said process comprising:
 - (a) epoxidizing a natural oil by contacting said natural oil with an acid and a peroxide to thereby produce an epoxidized reaction mixture comprising epoxidized natural oil, residual acid, residual peroxide, and water;
 - (b) removing a portion of said residual acid, at least a portion of said residual peroxide, and at least a portion of said water from said epoxidized reaction mixture to thereby produce an intermediate reaction mixture; and
 - (c) esterifying at least a portion of said epoxidized natural oil in said intermediate reaction mixture, thereby forming said epoxidized fatty acid alkyl esters, wherein said residual acid is not neutralized prior to said esterifying of step (c).

2. A process for producing epoxidized fatty acid alkyl esters, said process consisting essentially of:
 - (a) epoxidizing a natural oil by contacting said natural oil with an acid and a peroxide to thereby produce an epoxidized reaction mixture comprising epoxidized natural oil, residual acid, residual peroxide, and water;
 - (b) removing a portion of said residual acid, at least a portion of said residual peroxide, and at least a portion of said water from said epoxidized reaction mixture to thereby produce an intermediate reaction mixture; and
 - (c) esterifying at least a portion of said epoxidized natural oil in said intermediate reaction mixture, thereby forming said epoxidized fatty acid alkyl esters.

3. The process of either claim 1 or claim 2, wherein said removing of step (b) comprises subjecting said epoxidized reaction mixture to layer separation, thereby forming an organic phase and an aqueous phase, and further comprising subjecting at least a portion of said organic phase to vacuum distillation, thereby forming said intermediate reaction mixture.

4. The process of any of the foregoing claims, wherein said intermediate reaction mixture has an acid value of less than 1 mg KOH/g.
5. The process of any of the foregoing claims, wherein said epoxidized fatty acid alkyl esters have an APHA color value of less than 100.
6. The process of any of the foregoing claims, wherein said peroxide comprises hydrogen peroxide, wherein said acid comprises formic acid, wherein said epoxidized fatty acid alkyl esters comprise epoxidized fatty acid methyl esters.
7. The process of any of the foregoing claims, wherein said removing of step (b) does not comprise azeotropic distillation, wherein said removing of step (b) does not comprise washing said epoxidized reaction mixture with water.
8. A plasticizer comprising at least a portion of said fatty acid alkyl esters of any of the foregoing claims.
9. A polymeric composition comprising a polymeric resin and at least a portion of said fatty acid alkyl esters of any of the foregoing claims.
10. The composition of claim 9, wherein said polymeric resin is polyvinyl chloride.

INTERNATIONAL SEARCH REPORT

International application No PCT/IN2012/000745
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A. CLASSIFICATION OF SUBJECT MATTER
 INV. C08K5/1515 C07D303/42 C07D301/12
 ADD.

According to International Patent Classification (IPC) or to both national classification and IPC

B. FIELDS SEARCHED

Minimum documentation searched (classification system followed by classification symbols)
 C08K C07D

Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched

Electronic data base consulted during the international search (name of data base and, where practicable, search terms used)

EPO-Internal, COMPENDEX, INSPEC, WPI Data

C. DOCUMENTS CONSIDERED TO BE RELEVANT

Category*	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
X	GB 1 382 853 A (DEGUSSA) 5 February 1975 (1975-02-05) the whole document -----	1-10
X	WO 2010/114746 A1 (CARGILL INC [US]; ABRAHAM TIMOTHY WALTER [US]; ZHANG WEI [US]) 7 October 2010 (2010-10-07) paragraphs [0010], [0012] - [0013], [0018], [0024] paragraphs [0034], [0040] - [0041], [0046]; example 1A -----	6

Further documents are listed in the continuation of Box C.

See patent family annex.

* Special categories of cited documents :

- "A" document defining the general state of the art which is not considered to be of particular relevance
- "E" earlier application or patent but published on or after the international filing date
- "L" document which may throw doubts on priority claim(s) or which is cited to establish the publication date of another citation or other special reason (as specified)
- "O" document referring to an oral disclosure, use, exhibition or other means
- "P" document published prior to the international filing date but later than the priority date claimed

"T" later document published after the international filing date or priority date and not in conflict with the application but cited to understand the principle or theory underlying the invention

"X" document of particular relevance; the claimed invention cannot be considered novel or cannot be considered to involve an inventive step when the document is taken alone

"Y" document of particular relevance; the claimed invention cannot be considered to involve an inventive step when the document is combined with one or more other such documents, such combination being obvious to a person skilled in the art

"&" document member of the same patent family

Date of the actual completion of the international search

20 August 2013

Date of mailing of the international search report

29/08/2013

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INTERNATIONAL SEARCH REPORT

Information on patent family members

International application No
PCT/IN2012/000745

Patent document cited in search report		Publication date		Patent family member(s)	Publication date
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			DE	2123929 A1	23-11-1972
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