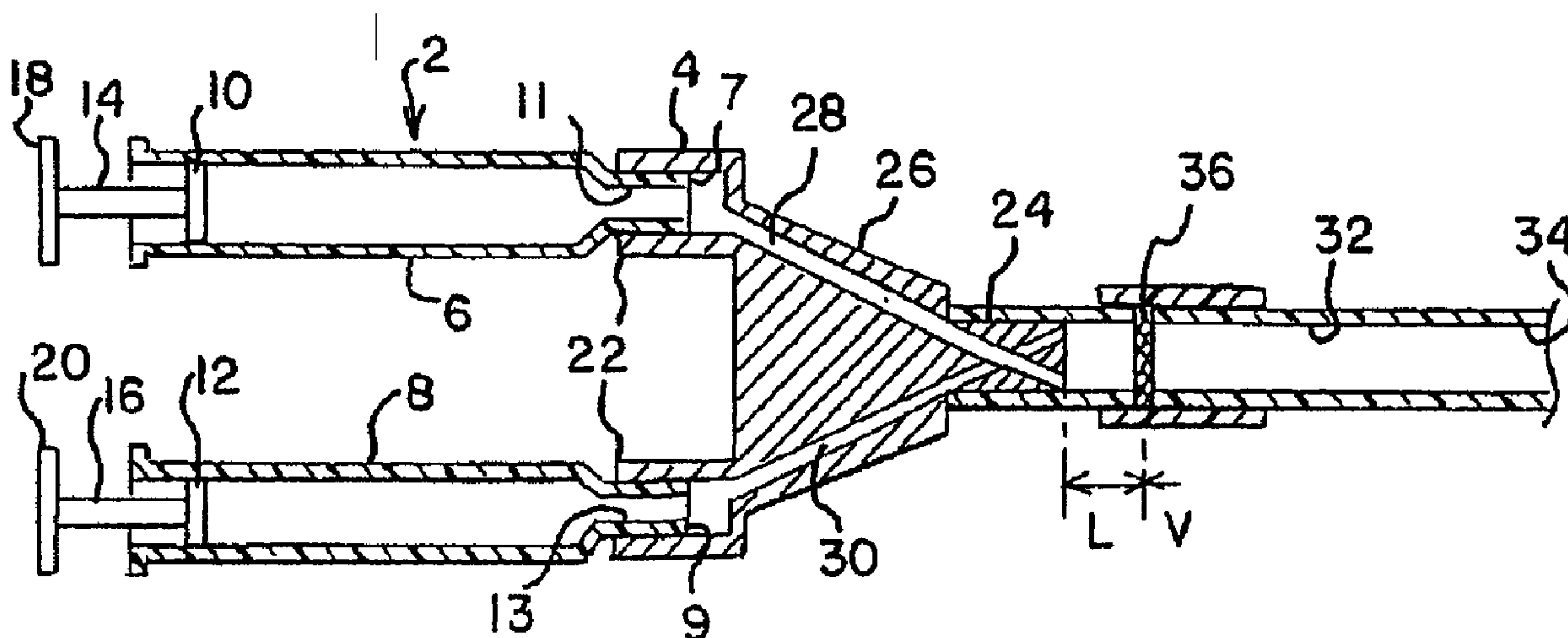




(86) Date de dépôt PCT/PCT Filing Date: 2007/01/17
 (87) Date publication PCT/PCT Publication Date: 2007/07/26
 (45) Date de délivrance/Issue Date: 2013/08/06
 (85) Entrée phase nationale/National Entry: 2008/06/05
 (86) N° demande PCT/PCT Application No.: US 2007/060639
 (87) N° publication PCT/PCT Publication No.: 2007/084919
 (30) Priorité/Priority: 2006/01/17 (US60/759,695)

(51) Cl.Int./Int.Cl. *A61B 17/00* (2006.01),
B01F 5/06 (2006.01)
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(54) Titre : DISPOSITIF, SYSTEME ET PROCEDE DE MELANGE
 (54) Title: DEVICE, SYSTEM AND METHOD FOR MIXING



(57) Abrégé/Abstract:

The present invention includes various compositions, devices, systems and methods for mixing at least two separate streams of components. In one aspect of the invention, a device is provided for mixing at least two separate streams of components which, when mixed, form a combined fluid stream. The device comprises a first passageway adapted to communicate with one of the at least two separate streams, and a second passageway adapted to communicate with another of the at least two separate streams. The device further comprises a mixer communicating with each of the first and second passageways comprising a three-dimensional lattice defining a plurality of tortuous, interconnecting passages therethrough. The mixer has physical characteristics which include a selected one or more of mean flow pore size, thickness and porosity is positioned upstream of the dispensing end of the third passageway to mix the component streams of the combined fluid stream.



(12) INTERNATIONAL APPLICATION PUBLISHED UNDER THE PATENT COOPERATION TREATY (PCT)

(19) World Intellectual Property Organization
International Bureau



(43) International Publication Date
26 July 2007 (26.07.2007)

PCT

(10) International Publication Number
WO 2007/084919 A1

(51) International Patent Classification:

A61B 17/00 (2006.01) B01F 5/06 (2006.01)

(21) International Application Number:

PCT/US2007/060639

(22) International Filing Date: 17 January 2007 (17.01.2007)

(25) Filing Language:

English

(26) Publication Language:

English

(30) Priority Data:

60/759,695 17 January 2006 (17.01.2006) US

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(81) Designated States (unless otherwise indicated, for every kind of national protection available): AE, AG, AL, AM, AT, AU, AZ, BA, BB, BG, BR, BW, BY, BZ, CA, CH, CN, CO, CR, CU, CZ, DE, DK, DM, DZ, EC, EE, EG, ES, FI, GB, GD, GE, GH, GM, GT, HN, HR, HU, ID, IL, IN, IS, JP, KE, KG, KM, KN, KP, KR, KZ, LA, LC, LK, LR, LS, LT, LU, LV, LY, MA, MD, MG, MK, MN, MW, MX, MY, MZ, NA, NG, NI, NO, NZ, OM, PG, PH, PL, PT, RO, RS, RU, SC, SD, SE, SG, SK, SL, SM, SV, SY, TJ, TM, TN, TR, TT, TZ, UA, UG, US, UZ, VC, VN, ZA, ZM, ZW.

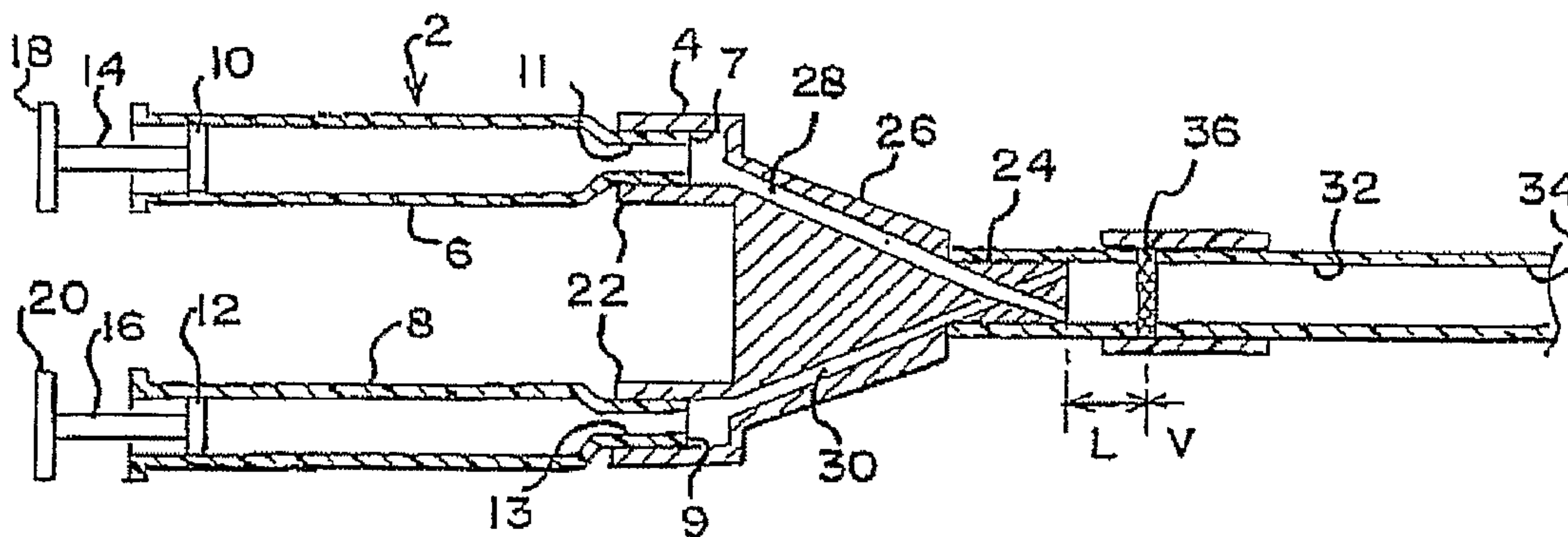
(84) Designated States (unless otherwise indicated, for every kind of regional protection available): ARIPO (BW, GH, GM, KE, LS, MW, MZ, NA, SD, SL, SZ, TZ, UG, ZM, ZW), Eurasian (AM, AZ, BY, KG, KZ, MD, RU, TJ, TM), European (AT, BE, BG, CH, CY, CZ, DE, DK, EE, ES, FI, FR, GB, GR, HU, IE, IS, IT, LT, LU, LV, MC, NL, PL, PT, RO, SE, SI, SK, TR), OAPI (BF, BJ, CF, CG, CI, CM, GA, GN, GQ, GW, ML, MR, NE, SN, TD, TG).

Published:

- with international search report
- before the expiration of the time limit for amending the claims and to be republished in the event of receipt of amendments

For two-letter codes and other abbreviations, refer to the "Guidance Notes on Codes and Abbreviations" appearing at the beginning of each regular issue of the PCT Gazette.

(54) Title: DEVICE, SYSTEM AND METHOD FOR MIXING



(57) Abstract: The present invention includes various compositions, devices, systems and methods for mixing at least two separate streams of components. In one aspect of the invention, a device is provided for mixing at least two separate streams of components which, when mixed, form a combined fluid stream. The device comprises a first passageway adapted to communicate with one of the at least two separate streams, and a second passageway adapted to communicate with another of the at least two separate streams. The device further comprises a mixer communicating with each of the first and second passageways comprising a three-dimensional lattice defining a plurality of tortuous, interconnecting passages therethrough. The mixer has physical characteristics which include a selected one or more of mean flow pore size, thickness and porosity is positioned upstream of the dispensing end of the third passageway to mix the component streams of the combined fluid stream.

WO 2007/084919 A1

DEVICE, SYSTEM AND METHOD FOR MIXING**INVENTOR**

Yves Delmotte

BACKGROUND

[0001-2]. This disclosure generally relates to an inline mixer for mixing multiple components of a combined fluid stream, such as a sealant or other combined fluid stream made of multiple components. More particularly, this disclosure relates to such inline mixers, systems utilizing such inline mixers and methods of inline mixing in the field of wound and tissue sealing with, for example fibrin. Even more particularly, the present invention relates to fibrin compositions prepared by such inline mixing.

[0003]. Inline mixing of combined fluid streams, including fluid streams of different viscosities, may be useful in a wide variety of settings including the medical field, the food industry, electronics, automotive, energy, petroleum, pharmaceutical, chemical industries, manufacturing and others. In one example of an application in the medical field, inline mixing of two or more combined fluid streams is employed to form a sealant, such as a tissue sealant, that is applied to human and animal tissue. Such sealant may be employed to seal or repair tissue at a surgical or wound site, to stop bleeding, seal wounds, treat burns or skin grafts and a variety of other purposes. In the food industry, inline mixing of two or more components are useful for blending of food and beverage compositions. In the electronics and/or manufacturing industries, the combination of two or more components may be

employed to create coatings or sealants as desired for particular applications. This may include coating or sealants that are optically clear, electrically conductive or insulative, thermally conductive or high temperature resistant or useful in very low temperature or cryogenic applications. In the ophthalmologic field, inline mixing of two or more components may be desirable to provide relatively small quantities or low flow rates of a treating agent for treatment of the eye. In the fuel or energy industries, inline mixing of air, water or other components with fuel may be helpful to create environmentally safer or cleaner fuels. Inline mixing may also be helpful in the manufacture of nano or micro sized particles and particle suspensions for use in the medical (such as drug delivery) field.

[0004]. In the medical field, and more particularly in the field of tissue sealants used to seal or repair biological tissue, such sealant is typically formed from two or more components that, when mixed, form a sealant having sufficient adhesion for a desired application, such as to seal or repair skin or other tissue. Such sealant components are preferably biocompatible, and can be absorbed by the body, or are otherwise harmless to the body, so that they do not require later removal. For example, fibrin is a well known tissue sealant that is made from a combination of at least two primary components -- fibrinogen and thrombin, which have, depending on the temperature, different viscosities of about 200 cps and 15 cps, respectively. Upon coming into contact with each other, the fibrinogen and thrombin components interact to form a tissue sealant, fibrin, which is extremely viscous.

[0005]. Sealant components may be kept in separate containers and are combined prior to application. However, because sealant components such as fibrinogen and thrombin have different viscosities, complete and thorough mixing is often difficult to achieve. If the components are inadequately mixed, then the efficacy of the sealant to seal or bind tissue at the working surface is compromised.

[0006]. Inadequate mixing of the type described above is also a problem present in other medical and/or non-medical fields, where two or more components having relatively different viscosities are required to be mixed together. Such components may tend to separate from each other prior to use or be dispensed in a less than thoroughly mixed stream, due at least in part to their different viscosities, flow rates and depending on the temperature and amount of time such mixture may be stored prior to use.

[0007]. To overcome the difficulties of the formation of the highly viscous fibrin in the medical field, in providing tissue sealant, it has become common to provide inline mixing of two or more components – in lieu of batch or tank mixing of the components--to form a tissue sealant, just prior to its application on a work surface. Such sealant may be applied by a dispenser that ejects sealant directly onto the tissue or other substrate or working surface. Examples of tissue sealant dispensers are shown in U.S. Patent Nos. 4,631,055, 4,846,405, 5,116,315, 5,582,596, 5,665,067, 5,989,215, 6,461,361 and 6,585,696, 6,620,125 and 6,802,822 and PCT Publication No. WO 96/39212. Further examples of such dispensers also are sold under the Tissomat® and Duploject® trademarks, which are marketed by Baxter AG. Typically, in these prior art devices, two individual streams of the components fibrinogen and thrombin are combined and the combined stream is dispensed to the work surface. Combining the streams of fibrinogen and thrombin initiates the reaction that results in the formation of the fibrin sealant. While thorough mixing is important to fibrin formation, fouling or clogging of the dispenser tip can interfere with proper dispensing of fibrin. Such clogging or fouling may result from contact or mixing of the sealant components in a dispenser for an extended period of time prior to ejection of the sealant components from the dispensing tip.

[0008]. In current mixing systems, the quality of mixing of two or more components having different viscosities may vary depending on the flow rate. For example, under certain flow conditions, the components may be dispensed as a less than thoroughly mixed stream. Accordingly, there is a desire to provide a mixing system which is not dependent on the flow rate to achieve sufficient mixing.

[0009]. Although prior devices have functioned to various degrees in forming and dispensing mixtures, there is a continuing need to provide a mixer and dispensing system that provides reliable and thorough mixing of at least two components (such as, for example, for a tissue sealant) for application to a desired work surface or other use applications in other fields. Such a mixing system could be provided to dispense the mixture just prior to or at least in close proximity to its intended use or application. Preferably, such a mixer and dispensing system would also avoid undue fouling or clogging of the dispenser.

Summary

[00010]. In one aspect, the present disclosure is directed to a device for mixing at least two separate streams of components which, when mixed, form a combined fluid stream, the device comprising a first passageway adapted to communicate with one of the at least two separate streams; a second passageway adapted to communicate with another of the at least two separate streams; and a porous mixing member communicating with each of the first and second passageways comprising a three-dimensional lattice defining a plurality of tortuous, interconnecting passages therethrough, the porous mixing member having physical characteristics to sufficiently mix the component streams of the combined fluid stream, which characteristics include a selected one or more of mean flow pore size, thickness and porosity, the porous mixing member comprising a porous sintered material selected from the group consisting of glass, ceramic, metal and polymer.

[00011]. In one particular example, the mean flow pore size may be between about 5 and 300 microns. In another particular example, the mixer has a mean flow pore size within the range of about 15 and 100 microns. In a further example, the mixer has a porosity between about 20% and 60% and more particularly a porosity within the range of about 20% and 40%. In another example, the mixer has a thickness within the range of about 1.5 to 3.0 millimeters. In another example, the product of the mean flow pore size thickness and porosity of the mixer is within the range of about 0.016 to 0.055.

[00012]. The device described above may further have a K value within the range of about 5 to 17 as determined by Darcy's Law described in further detail below.

[00013]. In another aspect, the present disclosure is directed to a device that provides a combined fluid stream that is fibrin from a mixture of selected amounts of fibrinogen and thrombin. The fibrin mixture may be characterized by the degree or rate of crosslinking, as measured by a ratio of an amount of a constituent chain in the fibrin mixture to an amount of the same constituent chain present in fibrinogen. The constituent chain may include an alpha monomer chain. Furthermore, the fibrinogen and the fibrin mixture include at least an alpha monomer chain, albumin and beta monomer chain and a rate of crosslinking that is measured by a Q value which is the quotient of X_n / X_i where X_i and X_n each represent the ratio of the alpha

chain to the combined amount of albumin and beta chain respectively for the fibrinogen and the mixture. The amount of the constituent chain, such as where the constituent chain is an alpha monomer chain, in the fibrinogen may be greater than the amount of the constituent chain in the fibrin mixture. In another example, where the combined fluid stream is a fibrin mixture of selected amounts of fibrinogen and thrombin, the fibrin and/or the degree of mixing of components may be characterized by a first optical characteristic. The combined fluid stream provides a relatively uniform optical characteristic indicating that the first and second components are sufficiently mixed to form a fibrin mixture. One of the first and second optical characteristics may be fluorescence.

[00014]. In another aspect, the present disclosure is directed to the device including two mixers located in series. In a further example, the mixer may be a porous member, and in a further example a plurality of mixers may be spaced in a spaced apart relation to each other. In another example, the mixers may be adjacent to each other. In a further example, the mixer may be downstream from a location where at least two separate streams are first combined. In another example, the mixer may comprise a porous material selected from the group consisting of glass, ceramic, metal or polymer. In a further example, the mixer may be a sintered material selected from the group consisting of glass, ceramic, metal or polymer. The mixer may be a sintered polymer and more particularly the mixer may be made of centered polypropylene or polyethylene.

[00015]. In another aspect, the present disclosure is directed to a fibrin composition. The fibrin composition is a mixture of selected amounts of fibrinogen and thrombin wherein the mixture comprises a selected amount of the constituent chain which constituent chain is also present in fibrinogen. The mixture has a rate of crosslinking as measured by Q value that is measured by the quotient of X_n / X_1 where X_n is at least in part based on the amount of the constituent chain in the mixture and X_1 is at least in part based on the amount of the constituent chain present in fibrinogen. The Q value is at least less than about 0.91.

[00016]. In another aspect, the fibrinogen and the mixture include at least a alpha monomer chain, albumin and a beta monomer chain and X_1 and X_n , each represent the ratio of the alpha chain to the combined amount of albumin and the beta chain respectively for the fibrinogen and the mixture. In a further aspect, the constituent chain is an alpha monomer. In another aspect, the amount of alpha

monomer chain of fibrinogen is greater than the amount of the alpha monomer chain in the fibrin mixture. In a particular example, the Q value is less than about 0.9 and may be less than about 0.8.

[00017]. In a further aspect, the present disclosure is directed to a fibrin composition including a first component of fibrinogen having a first optical characteristic and a second component of thrombin having a second optical characteristic. The first and second components when mixed form a combined fluid stream that provides a relatively uniform optical characteristic to indicate when the first and second components are sufficiently mixed. In one example, the first and second optical characteristics may be fluorescence. In a more particular example of the fibrin composition described above, the thrombin has a high fluorescence and the fibrinogen has a low fluorescence. In the fibrin composition, the fibrinogen may lack fluorescence. In a further example, the fluorescence of the fibrin may be distributed across the combined fluid stream with a larger degree of fluorescence being observed at a selected intermediate location of the stream.

[00018]. The present disclosure is also directed to a method for combining at least two separate components of a tissue sealant composition. The method includes providing a mixer comprising a three dimensional lattice defining a plurality of tortuous interconnecting passages therethrough. The method includes selecting a material for the mixer that is based on the physical characteristics of the material. The characteristics include a selected one or more of mean flow pore size, thickness and porosity volume.

[00019]. In a further aspect, the method includes selecting a porosity of mean pore size sufficient to form a generally homogenous mixed stream. In one example, the method includes selecting the mean flow pore size that is between about 5 and 300 microns and more particularly a pore size within the range of about 15 and 100 microns.

[00020]. In another aspect, the method includes selecting a porosity between about 20% and 60% and more particularly a porosity within the range of about 20% and 40%. Finally, the method may include selecting a thickness within the range of about 1.5 to 3.0 millimeters. In another aspect, the method includes selecting the mixer having a product of the mean flow pore size thickness and porosity of the mixer within the range of about 0.016 to 0.055.

[00021]. In a further aspect, the method includes that at least one of the two components includes a liquid, solid or gas, and each component may further be some combination of a solid, liquid or gas. In another aspect, the two components may include fibrinogen and thrombin. In a further aspect, the method includes at least two mixers located in series and further comprises flowing the two components through the mixers to mix the first and second components. In yet a further aspect, the method provides selecting of the mixer by determining the K value, as described in further detail below, or by determining the product of the mean flow pore size, thickness and porosity of the mixer. Further, the method may include selecting the mixer by determining the degree of crosslinking of the tissue sealant, where the tissue sealant is a fibrin mixture and a Q value may be measured, in accordance with other aspects previously described below. In addition, another aspect of the method may include sequentially passing the two components through the mixer, as described in further detail below, one or more times but not limited to a plurality of times. In yet another aspect, the method may include combining the two components in the vicinity of the mixer at a selected location upstream of the mixer.

[00022]. In another aspect, the present disclosure is directed to a tissue sealant system for combining and dispensing a combined fluid stream comprising at least two containers each separately containing one or more components. The system includes a first passageway communicating with one of at least two containers and a second passageway communicating with another of at least the two containers. The mixer communicating with each of the first and second passageway comprises or includes a three dimensional lattice defining a plurality of tortuous interconnecting passages therethrough. The mixture has a K value within the range of about 5 to 17 as defined by Darcy's Law which is $K = Q * \eta * L / (S * \Delta P)$.

[00023]. In another aspect, the present disclosure is directed to a device for mixing at least two separate streams of components which when mixed form a combined fluid stream. The device includes a first passageway in fluid communication with one of the at least two separate streams and a second passageway in fluid communication with another of the at least two separate streams. The device includes at least two mixers and spaced apart relation to each other, one mixer being located upstream of the other and communicating with each of the first and second passageways. Each mixer has a three dimensional lattice defining a plurality of tortuous interconnecting passages therethrough. A third

passageway downstream of the at least two mixers allows flow of the combined fluid stream. In a further aspect, at least one of the mixers comprises a porous member. In another aspect, at least one of the mixers is downstream from a location where the at least two separate streams are first combined. The mixers may be made of a porous material selected from the group consisting of glass, ceramic, metal or polymer and more particularly at least one of the mixers may be sintered material selected from the group consisting of glass, ceramic, metal or polymer. In a more specific example, at least one of the mixers is made of a sintered polymer such as, for example, sintered polypropylene or polyethylene.

[00024]. In another aspect, the present disclosure is directed to a method for combining one or more components. The method includes providing at least two mixers in a spaced apart relation to each other one mixer being located upstream of the other and each mixer comprising a three dimensional lattice defining a plurality of tortuous interconnecting passages therethrough. The method further includes simultaneously flowing a first component and a second component through the mixers to mix the first and second components.

[00025]. In a further aspect, the present disclosure is directed to a device for mixing at least two separate components which when mixed form a combined fluid stream. The device includes at least one mixer having a first and second sides and comprising a three dimensional lattice defining a plurality of tortuous interconnecting passages therethrough. The device includes a first port in fluid communication with the first side of the mixer and adapted to communicate with the source of a first component. The device further includes a second port in fluid communication with the second side of the mixer that is adapted to communicate with the source of the second component. Each port is in fluid communication with the other port through the mixer to allow one of the first and second components to flow from a selected one of the first and second sides of the mixer to the other side and to allow return flow of both the first and second components from the other side to the mixer. The device may further include a dispenser or container for dispensing or collecting the combined fluid stream. In one aspect, at least one of the two components includes a liquid, solid or gas, and each component may further be some combination of a solid, liquid or gas. In another aspect, the two components may include at least selected one of diesel, oil, gasoline, water and air. In a further aspect, the two components

may include egg white and air. In yet a further aspect, the two component may include fibrinogen and thrombin.

[00026]. In another aspect, the present disclosure is directed to a method for combining two or more components. The method includes providing at least one mixer positioned intermediate the first and second passageway and in fluid communication therewith. The first and second passageways are in respective fluid communication with the first and second components. The method includes sequentially passing the first component through the mixer from the first passageway to the second passageway and passing both the first and second components through the mixer from the second passageway to the first passageway. In accordance with this method, the first and second components may pass through a mixture of plurality of times such as, but not limited to, at least three times. In a further aspect, of the method, the combined first and second components are stored in one of the first and second passageways which is adapted for connection to an outlet port for dispensing the combined components. In one aspect, at least one of the first and second components is a liquid, solid or gas. In another aspect, the first and second components are both liquids, solids or gases. In a further aspect, at least one of the components may be a combination of a liquid, solid or gas and the other of the first and second components may be a liquid, solid or gas or a combination thereof.

[00027]. In a further aspect, the present disclosure is directed to a device for combining at least two separate streams of components which when mixed, form a combined fluid stream. The device includes a first passageway in fluid communication with one of the at least two separate streams. The device further includes a second passageway in fluid communication with another of the at least two separate streams. The device may further include a third passageway in fluid communication with and downstream of the first and second passageways for joining at least two separate streams at a selected location. The device includes at least one mixer downstream of and in the vicinity of the selected location. The mixer comprises a three dimensional lattice defining the plurality of tortuous interconnecting passages therethrough and an outlet downstream of the mixer to allow the flow of the combined fluid stream. In one aspect, at least one of the two components includes a liquid, solid or gas, and each component may further be some combination of a solid, liquid or gas. In another aspect, the two components

may include at least selected one of diesel, oil, gasoline, water and air. In a further aspect, the two components may include egg white and air. In yet a further aspect, the two component may include fibrinogen and thrombin.

[00028]. In another aspect, the present disclosure is directed to a method of mixing at least two separate streams of components to form a combined fluid stream comprising the steps of conveying a first component stream through a first passageway; conveying a second component stream through a second passageway; and passing the first and second component streams from the first and second passageways through a porous mixing member comprising a three-dimensional lattice defining a plurality of tortuous, interconnecting passages therethrough, the porous mixing member having physical characteristics to sufficiently mix the component streams, which characteristics include a selected one or more of mean flow pore size, thickness and porosity, the porous mixing member comprising a porous sintered material selected from the group consisting of glass, ceramic, metal and polymer.

[00029]. In another aspect, the method includes applying the combined at least two fluid streams to a desired working surface. The mixer may be a porous member having a plurality of pores in a mean pore size between about 5 and 300 microns. The mixer may also be porous member having a porosity between about 20% and 40%. The method described above may also include stopping the at least two streams of components through the mixer and subsequently repeating passing the at least two streams of components through the mixer.

[00030]. A more detailed description of these and other aspects of the devices, systems, methods and compositions of the present disclosure is set forth below.

[00031]. Although described later in terms of certain structures, it should be understood that the device, system and method of the present invention are not limited to the identical structures shown, and that the scope of the present invention is defined by the claims as now or hereafter filed.

Brief Description of the Drawings

[00032]. Figure 1 is a partial cross-sectional view of one embodiment of a tissue sealant dispenser set forth in the present disclosure.

[00033]. Figure 2 is an enlarged cross-sectional view of the distal end portion of the dispenser of Figure 1, showing portions of the dispenser removed.

- [00034]. Figure 3 is an enlarged distal end view of the distal end portion of Figure 2.
- [00035]. Figure 4 is a perspective view of the distal end portion shown in Figure 2.
- [00036]. Figure 5 is a top view of an alternative dispenser, similar to Figure 1 with a mixing portion removed, showing portions in cross section to illustrate the fluid stream passageways defined in a distal end portion of the dispenser.
- [00037]. Figure 6 is a top view of the dispenser of Figure 1 with a mixing portion removed, showing portions in cross section to illustrate the fluid stream passageways defined in a distal end portion of the dispenser.
- [00038]. Figure 7 is a top view of another alternative dispenser, similar to Figure 1, with a mixing portion removed, showing portions in cross section to illustrate the fluid stream passageways defined in a distal end portion of the dispenser.
- [00039]. Figure 8 is a distal end view of the dispenser of Figure 5.
- [00040]. Figure 9 is a scanning electron picture showing a lateral cross section of a sintered polypropylene material having a width of approximately 8.0 millimeters (mm) and a thickness of about 1.0 mm at about x30 magnification.
- [00041]. Figure 10 is a scanning electron picture showing a lateral cross section of a sintered polypropylene material having a width of approximately 8.0 millimeters (mm) and a thickness of about 1.0 mm at about x100 magnification.
- [00042]. Figure 11 is a scanning electron picture showing a lateral cross section of a sintered polypropylene material having a width of approximately 8.0 millimeters (mm) and a thickness of about 1.0 mm at about x350 magnification.
- [00043]. Figure 12 is a scanning electron picture showing a lateral cross section of a sintered polypropylene material having a width of approximately 8.0 millimeters (mm) and a thickness of about 1.0 mm at about x200 magnification.
- [00044]. Figure 13 is a scanning electron picture showing a longitudinal cross section of a sintered polypropylene material having a width of approximately 8.0 millimeters (mm) and a thickness of about 1.0 mm at about x30 magnification.
- [00045]. Figure 14 is a scanning electron picture showing a longitudinal cross section of a sintered polypropylene material having a width of approximately 8.0 millimeters (mm) and a thickness of about 1.0 mm at about x100 magnification.

[00046]. Figure 15 is a scanning electron picture showing a longitudinal cross section of a sintered polypropylene material having a width of approximately 8.0 millimeters (mm) and a thickness of about 1.0 mm at about x250 magnification.

[00047]. Figure 16 is a scanning electron picture showing a longitudinal cross section of a sintered polypropylene material having a width of approximately 8.0 millimeters (mm) and a thickness of about 1.0 mm at about x350 magnification.

[00048]. Figure 17 shows porosity measurements of a selected material, of sintered polypropylene, obtained using a mercury porosity test.

[00049]. Figure 18 is a partial cross-section view of a tissue sealant dispenser employing a modified distal end portion.

[00050]. Figure 19 is a partial cross-sectional view of another embodiment of a tissue sealant dispenser set forth in the present disclosure.

[00051]. Figure 20 is an enlarged cross-sectional view of the distal portion of the dispenser shown in Figure 19.

[00052]. Figure 21 is a cross section taken along line 21-21 of Figure 20 with a mixing portion removed.

[00053]. Figure 22 is an enlarged side view, similar to Figure 2, but two mixers with no spacing between the mixers.

[00054]. Figures 23-27 are enlarged side views, similar to Figure 2, except showing a different mixer arrangement having two mixers with different relative spacing between the mixers.

[00055]. Figures 28-29 are side views, similar to Figure 20, except showing several different dispenser tips with two-mixer arrangements having different relative spacing between the mixers.

[00056]. Figures 30-32 are side views, similar to Figure 20, except showing several different dispenser tips with mixer arrangements having one, two or three mixers with no spacing between the mixers.

[00057]. Figure 33 is a partial cross-sectional view of another embodiment of a dispenser set forth in the present disclosure.

[00058]. Figure 34 is a partial cross-sectional view of a further embodiment of a tissue sealant dispenser set forth in the present disclosure.

[00059]. Figure 35 is a top view of a yet further embodiment of a tissue sealant dispenser set forth in the present disclosure.

[00060]. Figure 36 is a cross section taken along line 36-36 of Figure 35.

- [00061]. Figure 37 is a top view of a modified embodiment of a tissue sealant dispenser having a single mixing device connected to a dispensing device with a single container set forth in the disclosure.
- [00062]. Figure 38 is a cross section of the tissue sealant dispenser of Figure 37.
- [00063]. Figure 39 is an enlarged cross section of a portion of the dispenser in Figure 37, showing other portions removed.
- [00064]. Figure 40 is a side view of a portion of the dispenser in Figure 39 showing additional portions removed.
- [00065]. Figure 41 is an side view of a modified mixing device shown disconnected from a dispensing apparatus.
- [00066]. Figure 42 is a cross section taken along 42-42 of Figure 41.
- [00067]. Figure 43 is a side view of another mixing device shown disconnected from a dispensing apparatus.
- [00068]. Figure 44 is a cross section taken along 44-44 of Figure 43.
- [00069]. Figure 45 is a side view of a portion of the dispenser in Figure 44 showing additional portions removed.
- [00070]. Figure 46 is a right end view of Figure 45.
- [00071]. Figure 47 is a top view of an arrangement that includes two dispensing devices connected by one of the mixing devices shown in Figures 39-46.
- [00072]. Figure 48 is a top view of an alternate arrangement that includes two dispensing devices connected by one of the mixing devices shown in Figures 39-46.
- [00073]. Figure 49 is a top view of yet another arrangement that includes two dispensing devices connected by a different mixing device.
- [00074]. Figure 50 is a schematic view of a modified embodiment, similar to Figure 48, further including a reservoir for receiving or storing the combined fluid stream for various applications.
- [00075]. Figure 51 is a plan view of a further embodiment set forth in the present disclosure showing an infusion system employing a mixing device.
- [00076]. Figure 52 is an enlarged cross section of a portion of the system of Figure 50 with other portions shown removed.
- [00077]. Figures 53-54 graphically show the turbidimetry measurements of different fibrin matrices employing different dispensing apparatus.

[00078]. Figure 55 shows the % crosslinking of alpha (α) monomer chains in different fibrin mixtures for three different groups, each group employing a different flow rate, 2ml/min, 4ml/min and 6 ml/min, and each group consisting of results based on three different dispensing devices.

[00079]. Figure 56 shows electrophoretic patterns for ten different samples of fibrinogen or fibrin mixtures, which identifies the presence or absence of different constituent components according to the molecular weight of such components.

[00080]. Figure 57-60 are graphs showing the amount of constituent components present in respective samples of fibrinogen and three different fibrin mixtures each employing a different dispensing apparatus.

[00081]. Figure 61 shows the % crosslinking of alpha (α) monomer chains in different fibrin mixtures at different temperatures--4°C, 18°C, 22°C, 37°C.

[00082]. Figures 62-63 are graphs showing the degree of fluorescence along a cross-section of tubing for a fibrin mixture, respectively, of an apparatus without a mixer (in Figure 62) and an apparatus with at least one mixer (in Figure 63).

[00083]. Figures 64-65 are graphs showing a plot of permeability K values, pressure values and viscosity values relative to one another, based on Darcy's Law, with the remaining variable being held constant.

Description of the Preferred Embodiments

[00084]. In accordance with one embodiment of the present invention, Figure 1 illustrates a dispenser, generally indicated at 2, for mixing at least two components of a combined fluid stream, such as a sealant, or tissue sealant or other combined fluid stream. Although the dispensers, systems and methods are generally illustrated and described in the context of a tissue sealant dispenser, it is understood that the present invention is not limited to such a dispenser or to the mixing of tissue sealant components, and that the present invention has applications in a variety of settings where mixing of component fluid streams is desired.

[00085]. As shown in Figure 1, dispenser 2 includes at least two fluid component sources, illustrated in the form of hollow cylinders or barrels 6 and 8, although other source containers from which fluid components are provided may be used. In the embodiment of Figure 1, each barrel has a generally cylindrical interior or bore in which one of the fluid components such as fibrinogen or thrombin for forming fibrin tissue sealant is stored. The distal end 7, 9, respectively, of each

barrel has an outlet port 11, 13, respectively, for communicating with a dispensing tip structure, generally at 4.

[00086]. In Figure 1, the bore of each barrel 6, 8 preferably slidably receives a piston or plunger 10, 12, respectively, for ejecting the sealant component from the respective bore. A plunger or pusher 14, 16 is associated with each piston and extends proximally from each respective bore. A thumb-rest 18, 20 is preferably associated with each plunger 14, 16 and may be actuated or pushed manually or automatically to eject the component. The thumb-rests 18, 20 may be actuated either independently or simultaneously, such as by a common actuator or yoke that couples the plungers together for simultaneous movement.

[00087]. As shown in Figure 1, the illustrated tip assembly or structure is a multi-part assembly and includes a flow director 26. The flow director 26 has a proximal end 22 and a distal end 24 and defines respective first and second passageways 28 and 30. Each passageway 28, 30 communicates with a respective bore of the barrels 6, 8 to allow the respective component to exit the distal end 24. As shown in Figure 1, the inlet to each passageway 28 and 30 is suitable for attachment to one of the outlets from barrels to 6, 8 such as, for example, by a luer fitting or other attachments as will be apparent to persons of skill in the relevant field.

[00088]. Although manually actuated plungers are illustrated for dispensing the fluid components, other types of devices may be used in connection with the present invention including manually or electrically actuated dispensers. Further, as noted above, it is contemplated that the present invention is not limited to dispensers for sealant and may be used to combine two or more components for other combined fluid streams for other applications within or outside of the medical field.

[00089]. In Figure 1, each of the first and second passageways 28, 30 communicates with one of the components as a separate fluid stream until such streams approach or are at the distal end 24. As shown in Figure 1, the first and second passageways 28, 30 may be non-parallel and non-intersecting relative to one another such that they direct each component stream into a combined third passageway 32 at an angle that may assist combination of the two streams. For example, as shown in Figure 1, the passageways are separate (with one passageway 28 or 30 being located offset and non-intersecting to the other) until the streams exit their respective passageways. In Figure 1, the exiting streams are initially directed away from each other, towards opposed inner surfaces of the third

passageway 32 which will deflect the separate stream and cause them to converge. The flow of the fluid component streams in the third passageway 32 downstream of the distal end 24 may be turbulent or otherwise provide fluid flow conditions which result in some mixing of the exiting streams of fluid components in this region.

[00090]. In Figures 5-8, each figure includes an alternative orientation for the component passageways of the flow director, although other orientations may be used. The alternative dispensing devices 50, 60 and 70, respectively in Figures 5 and 8, show a straight and parallel orientation, where the fluid component streams exit the flow director along generally parallel paths. Figure 6 shows non-parallel and non-intersecting flow paths similar to that of Figure 1. Figure 7 shows right-angled parallel flow paths at the distal end of the device (with one passageway located in front of the other and only one passageway being shown in Figure 7). Other orientations are also possible.

[00091]. As described above, and further shown in Figures 1-4, a third passageway 32 communicates with the first and second passageways 28, 30. A distal-most dispensing end 34 of the third passageway 32 provides for exiting of the mixed component stream and may include an orifice of any desired shape or a dispensing structure such as a tubing segment, cannula, spraying device, spray head or other types of dispensing devices, depending on the desired form in which the combined mixture is to be applied and/or the work surface.

[00092]. In accordance with the present invention, a mixer, generally indicated at 36, is positioned upstream of the dispensing end 34 of the third passageway 32 for mixing of the component streams. As the component streams flow through the mixer 36, they are mixed together to provide a thorough mixing of two or more components to create a substantially homogeneous combined fluid stream that is dispensed from the dispensing end 34.

[00093]. The mixer 36 described herein is preferably formed of a three-dimensional lattice or matrix that defines a plurality of tortuous interconnected passageways through the mixer. As a result of this structure, the component fluid streams are intimately mixed together as they pass through the mixer. The mixer 36 may provide for a laminar flow of the fluid component streams to enhance mixing between the fluid component streams, or otherwise provide fluid flow conditions which preferably promote significant mixing of the fluid component streams.

[00094]. One preferred material for the mixer is illustrated in cross-sections in Figures 9-16. The material shown there is polymeric material formed by sintering to define an integral porous structure. The lattice or matrix of polymeric material forms a plurality of essentially randomly-shaped, tortuous interconnected passageways through the mixer. The material of the mixer 36 may be selected, for example, from one or more of the following: Polyethylene (PE), High Density Polyethylene (HDPE), Polypropylene (PP), Ultra High Molecular Weight Polyethylene (UHMWPE), Nylon, Polytetra Fluoro Ethylene (PTFE), PVdF, Polyester, Cyclic Olefin Copolymer (COC), Thermoplastic Elastomers (TPE) including EVA, Polyethyl Ether Ketone (PEEK), glass, ceramic, metal, polymer materials other than polyethylene or polypropylene or other similar materials. The mixer 36 may also be made of a polymer material that contains an active powdered material such as carbon granules or calcium phosphate granules with absorbed molecules. Other types of materials are also possible. A sintered polypropylene material suitable for the present invention may be available from commercial sources, such as from Bio-Rad Laboratories, Richmond, California, United States, Porex Porous Products Group of Porex Manufacturing, Fairburn, Georgia, United States, Porvair Technology, a Division of Porvair Filtration Group Ltd., of Wrexham, United Kingdom, including Porvair Vyon Porvent, PPF or PPHP materials, or MicroPore Plastics, Inc., of 5357 Royal Woods, Parkway, Tucker, GA 30084, <http://www.microporeplastics.com/>.

[00095]. It is also possible that the mixer 36 may be made of one or more materials having one or more characteristics that may assist mixing of the component streams. By way of example and not limitation, the material may be hydrophilic, which is material that essentially absorbs or binds with water, hydrophobic, a material which is essentially incapable of dissolving in water, oleophobic, a material which is essentially resistance to absorption of oils and the like, and/or have other characteristics that may be desired to enhance mixing of the components.

[00096]. As noted above, the mixer 36 preferably is made in whole or in part of a three-dimensional lattice or matrix that defines a plurality of tortuous, interconnecting passages therethrough. In Figures 9-16, the streams of the components may pass through the illustrated three-dimensional lattice or matrix that defines a plurality of tortuous, interconnecting passages so that the component streams are thoroughly mixed to create an essentially homogeneous combined fluid

stream. At Figures 9-12, scanning electron pictures show lateral sections respectively at about X30, X100, X350 and X200 magnifications for a sintered polypropylene material having a width of approximately 8.0 millimeters (mm) and a thickness of about 1.0 mm. At Figures 13-16, scanning electron pictures show a longitudinal section respectively at about X30, X100, X250 and X350 magnifications for the same material shown in Figures 9-12, illustrating other views of the three-dimensional lattice. As shown in Figures 9-16, the illustrated passages preferably intersect at one or more random locations throughout the mixer such that the two component streams are randomly combined at such locations as such streams flow through the mixer. It should be understood that the three-dimensional lattice or matrix may be formed in a variety of ways and is not limited to the random structure of a sintered polymeric material as shown in Figures 9-16.

[00097]. The illustrated mixer 36 in Figures 1-4 is made of a porous material and may have varying porosity depending on the application,. Such porous material preferably has a porosity that allows the streams of the components to pass through to create a thoroughly-mixed combined fluid stream. The porosity of a material may be expressed as a percentage ratio of the void volume to the total volume of the material. The porosity of a material may be selected depending on several factors including but not limited to the material employed and its resistance to fluid flow (creation of excessive back pressure due to flow resistance should normally be avoided), the viscosity and other characteristics and number of mixing components employed, the quality of mixing that is desired, and the desired application and/or work surface. By way of example and not limitation, the porosity of a material that may be employed for mixing fibrin components may be between about 20% and 60%, preferably between about 20% to 50% and more preferably between about 20% and 40%.

[00098]. At Figure 17, porosity measurements of a selected material, manufactured by Bio-Rad Laboratories, are shown as obtained using a mercury porosity test on an Autopore III apparatus, a product manufactured by Micromeritics of Norcross, GA. It may also be possible to determine the porosity of a selected material in other ways or using other tests. At Figure 17, such porosity measurements show the total volume of mercury intrusion into a material sample to provide a porosity of about 33%, an apparent density of about 0.66 and an average pore diameter of about 64.75 microns. Materials with other porosities also may be

employed for mixing fibrin or for mixing combined fluid streams other than fibrin, as depending on the desired application.

[00099]. Also, the mean pore size range of the mixer may vary. In the three-dimensional lattice shown in Figures 9-16, the mixer 36 may define a plurality a pores that define at least a portion of the flow paths through which the streams of the components flow. The range of mean pore sizes may be selected to avoid undue resistance to fluid flow of such component streams. Further, the mean pore size range may vary depending on several factors including those discussed above relative to porosity. Several mean pore size ranges for different materials for the mixer are shown in Table 1, except at no. 16 which includes a "control" example that lacks a mixer.

TABLE 1

PART III: Evaluation of single porous disks
Materials from Porvent and Porex

Sample ID	Type	Form	Property	Mean Pore Size	Thickness	Mixing
2		PE sheet	Hydrophobic	5—55 μm	2.0 mm	good
21		PP sheet	Hydrophobic	15—>300 μm	2.0 mm	good
6		PE sheet	Hydrophobic	20—60 μm	3.0 mm	good
19		PP sheet	Hydrophobic	70—210 μm	1.5 mm	good
22		PP sheet	Hydrophobic	70—140 μm	3.0 mm	good
24		PP sheet	Hydrophobic	125—175 μm	3.0 mm	good
1			Hydrophobic	7—12 μm	1.5 mm	no fibrin extrusion
8		PE sheet	Hydrophobic	40—90 μm	1.5 mm	good
7		PE sheet	Hydrophobic	20—60 μm	1.5 mm	good
9		PE sheet	Hydrophobic	20—60 μm	3.0 mm	good
16		PE sheet	Hydrophobic	40—100 μm	1.5 mm	good
18		PE sheet	Hydrophobic	40—100 μm	3.0 mm	good
20		PE sheet	Hydrophobic	80—130 μm	3.0 mm	good
14		PE sheet	Hydrophobic	20—60 μm	1.5 mm	good
17		PE sheet	Hydrophobic	80—130 μm	1.5 mm	good
26	Control	--	-----	-----		
27		PP sheet	Hydrophobic	7—145 μm	1.5 mm	good

[000100]. Table 1 includes several commercial sintered polyethylene (PE) or polypropylene (PP) materials manufactured by Porex or by Porvair under the tradename Porvent or Vyon. The table summarizes the mixing results achieved from each material based on quality of fibrin obtained after fibrinogen and thrombin (4

International Units (IU)/ml) passed through a device having a single mixer such as shown in Figure 1, except for one experiment (at ID 26) which is the control and lacks any mixer. The indicated mean pore size ranges vary between about 5 and 300 microns. In Table 1, the ranges for materials nos. 2, 21, 6, 19, 22, 24, 8-9, 16, 18, 20, 14, 17, and 27 each generally indicate good mixing quality for fibrin. In Table 1, such mean pore size ranges are not intended to be exhaustive and other mean pore size ranges are also possible and useful for mixing. The mean pore size ranges indicated in Table 1 were obtained from the technical data sheets of the listed materials provided by the suppliers Porvair and Porex.

[000101]. The mixer may be further configured and sized so as to provide sufficiently thorough mixing of the streams of the components. The size of the mixer may vary depending on such factors which include the size and/or configuration of the dispenser, the mixer porosity and mean pore size, the mixer material employed, the desired degree of mixing, the mixing components, and/or the desired application. For a mixer having the above discussed example ranges for porosity and mean pore sizes, the mixer thickness may range between about 1.5 mm and 3.0 mm, as indicated in Table 1. Other thicknesses are also possible including a variable or non-uniform thickness.

[000102]. Also, the shape and configuration of the mixer may vary from the generally circular cross section or disk shape that is shown in Figures 1-4. It is possible that the mixer may have other shapes or configurations including but not limited to elliptical, oblong, quadrilateral or other shapes. In the embodiment shown in Figure 1-4, the mixer radius may range between about 3 mm and 5 mm although other dimensions are also possible.

[000103]. As shown in Figure 1, the mixer 36 is preferably positioned downstream of the distal end 24, at about a length L from where the separate component streams are initially allowed to flow together, although it may also be positioned where the streams join. It is contemplated that the distance L may vary depending on the design requirements and extent of mixing that is required. By way of example, in a handheld dispenser of type shown in Figures 1-4 for use in fibrin delivery, the distance L may range between about 0 and 6 mm or more, preferably, between about 1 and 6 mm. Generally speaking, the homogeneity of fibrin created by the illustrated mixer decreases with a decrease in the distance L, such as 4 mm and less by employing the dispenser type shown in Figures 1-4. More preferably, a

distance L of between about 5 and 6 mm is preferred for the embodiment shown in Figure 1-4 although other distances are also possible. It is contemplated that other designs may be employed than the described Y-shaped passageway structure that is shown and/or other physical parameters may be employed for such structure such as, other diameters, lengths, number of passageways and/or passageway orientations, such as shown in Figures 5-8, so that the value of distance L may have a different range than described above and is not limited to the above ranges.

[000104]. Also, the mixer may be manufactured in various ways which may depend on the desired shape, thickness and/or other characteristics of the material or materials that is employed for the mixer. By way of example and not limitation, the mixer may be fabricated or sectioned from one or more pieces of material having a desired size, thickness and/or other characteristics for the mixer. Alternatively, the mixer may be prefabricated including one or more molding processes to form a mixer having a desired size, thickness and/or other characteristics. It is also possible that the mixer may be manufactured in other ways. The mixer may be preassembled as part of a cannula, luer, spray tip, tube, or other device, such as by molding ultrasonic welding, mechanical fittings or other attachment techniques. By way of example and not limitation, Figure 18 shows a mixer 80, similar to the mixer 36 of Figure 1 that is located within a cannula-type device 82. Alternatively, the mixer may be assembled by the user as part of a suitable device prior to use although other uses may also be employed.

[000105]. The material for the mixer may be characterized and selected for a given application based on one or more physical characteristics so as to provide a sufficiently and relatively homogeneous combined fluid stream downstream of the mixer and upon passing the component streams through the mixer. By way of example, Table 2 illustrates various sintered polymer materials for the mixers suitable for use in the dispensers systems and methods described herein, and their physical characteristics. The specific materials identified in Table 2 are manufactured by, for example, Porvair Filtration Group Ltd. (Hampshire, United Kingdom) or Porex Corporation (Fairburn, Georgia, USA). The data represented in this table includes the K value from Darcy's Law, as indicated in the following equation:

[000106].
$$Q = \frac{K * S * \Delta P}{\eta * L}$$

[000107]. where Q is the Flow rate of fluid flow through the material;

[000108]. S is the surface area of the material;

[000109]. ΔP is the change in pressure between the upstream and downstream locations of the material;

[000110]. L is the thickness of the material; and

[000111]. η is the viscosity of the fluid flowing through the material, or if more than one fluid is flowing the viscosity of the more viscous component.

[000112]. The K values typically represent a permeability value and are represented in Table 2 based on increasing K value, expressed in units of $\mu\text{m}^2\text{s}$ which represents increasing values of permeability. Table 2 also summarizes several physical characteristics of the material including the relative values for minimum pore size (min.) mean flow pore size, maximum pore size (max.), average bubble point (or pressure that causes the liquid to create air bubbles), thickness, and porosity. The physical characteristics of each of the materials in Table 2 were obtained based on testing using methods known to those of skill in the art.

[000113]. By way of example and not limitation, the K values in Table 2 were obtained by permeability testing using water passed through the listed materials having the indicated physical characteristics. The permeability test was helpful to characterize materials based on their K value and, these materials are listed in order of increasing K value in Table 2. For the measurement of permeability, the materials employed included sintered porous material sheet supplied by Porvair and Porex. The permeability test was performed on a syringe that was filled with water. The pressure reducer was turned off and all connections downstream of the syringe were opened. Then water was allowed to flow through the syringe until the pressure drop between top and bottom of the syringe was about zero. The pressure reducer was then switched on and compressed air was injected to push water from the syringe at a constant flow rate. The volume of injected air was determined based on monitoring the flow of water between upper and lower volumetric markings on the syringe. As soon as the water meniscus crossed the upper mark, the time and pressure were recorded (P1). When the water meniscus crossed the lower mark on the syringe body, the total time (t), pressure (P2) and volume of water (V) were recorded. In addition to the known values of P1, P2, t and V, the remaining parameters for the calculation of permeability that were known include: Diameter of sintered material disc is about 10mm, the thickness is about 1.5mm, the surface of

sintered material disc is about 78.54 mm², the Dynamic viscosity of water 10⁻³ Pascal second (Pa.s). This test was used to determine the K values in Table 2.

[000114]. As described herein, it is contemplated that other liquids, gases and solids may be used to determine a K value from Darcy's Law for these materials or other materials. It is realized that different liquids, gases and solids will change the viscosity value (η) of Darcy's Law and, as such, will provide different K values or ranges for a given set of physical properties (thickness L and surface area S) of the material, flow rate Q and pressure difference ΔP that may be employed. Further, even where the same liquid, gas or solid is used, such that the viscosity is held constant, other parameters may be varied to achieve different K values. By way of example and not limitation, any one or more of the flow rate, surface area, thickness, and/or pressure difference may be varied and, as such, vary the resulting K value that is determined.

[000115]. Turning briefly to Figures 64-65, a three-dimensional curve shows the permeability or K values along one axis, pressure values along a second axis and viscosity values along a third axis (with Figure 65 identical to Figure 64, except the axes of permeability and pressure have been rotated clockwise to better show the curve). Generally speaking, the illustrated curve is applicable to any liquid, gas or solid that may be employed for permeability testing of a given material. By way of example, Figures 64-65 show the variation in permeability or K values, pressure values and viscosity, assuming other parameters of Darcy's Law, such as surface area S, flow rate Q and material thickness L are held constant. As indicated in Figures 64-65, for a given viscosity and pressure value, the permeability or K value may known according to the illustrated curve. Even if only one of the permeability, pressure or viscosity value is constant, the curve provides an indication of the other two values, which may vary along the illustrated curve, due to their relationship to each other based on Darcy's Law, described above.

TABLE 2

Permeability		Porosity					
Sample	K" μm^2 "	Min.	Mean Flow Pore	Max	Avg. Bubble Pt.	Thick	Porosity
1	0.55	3	5	7	13	1.5	45
2	1.41	4.0-7.0	17-22	50-60	50-70	2	27
3	1.93	5.0-8.0	8.0-12	12.0-18.0	15-25	2	44
4	3.41	4.0-7.0	17-22	50-60	50-70	2	27
5	3.76	4.0-7.0	17-22	50-60	50-70	2	27
6	4.72	6	16	36	47	3	42
7	5.08	9	23	49	57	1.5	48
8	5.81	10	36	88	101	1.5	39
9	6.18	7	21	45	52	3	45
10	6.48	6.0-9.0	35-45	130-160	101-130	1.5	39
11	6.55	6.0-9.0	35-45	130-160	101-130	1.5	39
12	6.67	7.0-11	30-40	85-105	60-80	1.68	39
13	7.14	6.0-9.0	35-45	130-160	101-130	1.5	39
14	7.14	9	28	64	67	1.5	49
15	7.32	7.0-11	25-35	68-88	55-75	2	35
16	7.89	14	43	119	108	1.5	51
17	10.90	13	65	300	183	1.5	56
18	10.99	9	32	70	85	3	46
19	12.30	11	80	300	207	1.5	50
20	12.57	10	51	140	129	3	48
21	14.09	13-17	80-100	300	180-210	2	51
22	15.02	10	61	217	163	3	46
23	15.64						
24	16.49	12	81	300	227	1.5	42
25	25.23	15	298	300	TP	3	49

TABLE 3

Sample	MFP*thick*PV*1000	K
1	3.375	0.55
3	8.8	1.93
2	10.53	1.41
4	10.53	3.41
5	10.53	3.76
7	16.56	5.08
6	20.16	4.72
14	20.58	7.14
15	21	7.32
8	21.06	5.81
12	22.932	6.67
10	23.4	6.48
11	23.4	6.55
13	23.4	7.14
9	28.35	6.18
16	32.895	7.89
18	44.16	10.99
24	51.03	16.49
17	54.6	10.9
19	60	12.3

20	73.44	12.57
22	84.18	15.02
21	91.8	14.09
25	438.06	25.23

[000116]. At Table 3, the K values of the materials listed at Table are represented. By way of example and not limitation, good, homogeneous mixing of a combined fibrinogen and thrombin mixture has been observed using mixer or disk made of a material having a K value from Tables 2-3 between approximately 5 and 17. In addition, Table 3 includes a numerical product of the mean flow pore size (MFP), thickness and porosity volume (PV) multiplied by 1000 (based on increasing value of this product). It has also been observed that using a mixer having a MFP * thickness * PV * 1000 value, within the range of about 16 to 55 achieves good, homogeneous mixing of fibrin. The mixer material may also be selected based on one or more of the above physical characteristics or other characteristics. As discussed above, the permeability or K values may vary from those discussed above in Tables 2-3, for example, where a liquid other than water is used, or where a gas and solid may be employed for the permeability testing or where different physical characteristics or parameters are employed. In such instances, it is contemplated that an appropriate range of K values will be determined and the material of the mixer may be appropriately selected based on a range of K values that is determined to provide sufficient quality of mixing.

[000117]. Figures 19-21 illustrate another embodiment of the present invention which includes a tissue sealant dispenser, generally indicated at 102. Similar to the dispenser 2 shown in Figures 1-4, the dispenser 102 in Figures 19-21 includes a pair of hollow barrel or tubes 106, 108, pistons 110, 112, plungers 114, 116 and thumb rests 118, 120, and flow director 126. The flow director 124 has a distal end 124, and first, second and third passageways 128, 130 and 132. As shown in Figure 21, the respective openings A, B of the first and second passageways 128, 130 are positioned so as to assist combination of the two separate streams as they exit the distal end 124, as described above. More specifically, in Figures 19-21, the outlets are located in offset relationship and direct fluid flow outwardly toward the wall of tubing 132, although other locations and/or orientations may be used.

[000118]. Referring to Figure 19, the dispenser preferably has two or more mixers for enhanced mixing and preferably two, or first and second mixers 136A and 136B. In Figure 19, such mixers 136A and 136B are located upstream of a dispensing end 134 and in spaced-apart series relationship, spaced from each other at a distance V along the passageway 132. Generally speaking, the homogeneity or quality of mixing of fibrin increases with an increase in the number of mixers, such as for two mixers, although any number of mixer may be used.

[000119]. The passageway 132 may be of one-piece construction or comprised of separate portions or tubing segments 132A, 132B and 132C, with the mixers 136A, 136B located between the segments 132A, 132B and 132C, as shown in Figure 19, so as to ensure the desired spacing between the mixers 136A, 136B, between the upstream mixer 136A and the distal end 124, and between the downstream mixer 136B and the dispensing end 134. An outer housing 138 may be sized to tightly overfit the tubing segments 132A, 132B and 132C and the mixers 136A and 136B for supporting and aligning the mixers 136A, 136B and tubing segments 132A, 132B, 132C.

[000120]. The distance V between the mixers 136A, 136B may be varied between about 0 mm, in which the mixers are adjacent to each other, and 6 mm or more. Figures 22-27 illustrates some different possible spacing distances between the mixers 136A, 136B. The distance V between two mixers 136A, 136B is shown at about 0 mm, 1 mm, 2 mm, 3 mm, 4 mm and 5 mm (as respectively indicated by Figures 22-27). Generally speaking, when employed in a tissue sealant application, it has been found that the presence of fibrin between the two mixers increases when the distance V between them increases. A distance V of about 3 mm and above in the illustrated embodiment has resulted in good fibrin formation to form a combined fluid stream having sufficient homogeneity. As discussed above, the length L upstream of the first mixer may also be selected between about 0 mm to 6mm or more. For example, if two mixers are used having the above discussed size range, one combination may include a distance V between the mixers 136A, 136B of about 4 mm or less and a length L between the upstream mixer 136A and the distal end 124 of about 6 mm or less, so as to minimize fibrin formation on either side of the mixers 136A, 136B and/or clogging of the pores of the mixers 136A, 136B. Other variations or combinations of distances V and lengths L are also possible. As previously discussed above for the value L , the value V may also vary based on

different designs and/or the different parameters that are employed in such design and so the value V is not limited to the above discussed values or ranges.

[000121]. The mixing and dispensing systems described herein may provide for a "Stop and Go" device or process, in which the flow of fluid component streams are intermittently started and stopped. For such "Stop and Go" device or process, the length L and/or the distance V preferably should not generate significant fibrin formation on the mixer or mixers or between the mixers if more than one mixer is employed. For a "Stop and Go" device employing at least two mixers, the length L and the distance V may vary. By way of example and not limitation, for a two mixer device, a length L of about 3 mm and a distance V of about 4 mm may achieve sufficiently thorough mixing as well as avoid significant generation of fibrin on or between the two mixers. Other variations of the length L and the distance V are also possible from those discussed and may be employed, depending on the desired application and/or other designs and parameters that may be employed.

[000122]. Figures 28-29, show two mixers, with a distance V at about 2 mm and 3 mm, respectively, therebetween, and a length L at about 6 mm. Any reasonable number of mixers is also possible to enhance mixing provided flow is not unduly restricted. Also Figures 30-32, respectively show mixer arrangements with one mixer 136A, two mixers 136A and 136B and three mixers 136A, 136B and 136C without any distance or spacing (V) therebetween and with a length L of about 6 mm. Where more than one mixer is used, the mixers do not have to have the same characteristics, such as porosity, mean pore size or length as describe above. It may be desirable to varying the characteristics of the mixers to increase the thoroughness of mixing as the fluid streams pass through the dispenser.

[000123]. In Figure 33, a further embodiment of the present invention includes a dispenser, generally indicated at 202. Similar to previously described embodiments, the dispenser 202 includes a pair of hollow barrels or tubes 206, 208, pistons 210 and 212, plungers 214 and 216, thumb rests 218, 220 and a flow director 226. A proximal end 222 of the dispenser 202 provides a common actuator, which joins the proximal ends of the plungers 214 and 216 together at the end 222, for simultaneously ejecting the components from a distal end 224. The distal end 224 defines separate passageways 228 and 230 for separately ejecting the respective components into a third passageway 232 in which a single mixer 236 is located upstream of a dispensing end 234 and is positioned downstream of the distal end

224 at a length L. As noted above, other variations are possible including variations in the number of mixers and the length L.

[000124]. In Figure 33, a fourth passageway 240 is defined in the distal end 224 and is adapted for fluid communication with a source of sterile gas, such as air which communicates with the distal end via tubing (such as tubing as shown in Figure 10 at 342). The source of gas may be actuated by pneumatic, mechanical, electrical and/or some combination thereof, such as described and shown in U.S. Patent No. 7,537,174 filed January 12, 2006.

[000125]. In Figure 33, such dispenser 202 operates similarly to the dispenser 2 as described in Figures 1-4 except that the two components may be ejected from the device with the assistance of gas to provide a mixed gas and component fluid stream from the distal end 234 of the dispenser 202. It is also possible for the passageway 240 to introduce gas or water for cleaning the passageways of the mixer and/or the dispensing end 234 and/or other tubing or cannula structures located downstream, which may facilitate operation of a stop & go device during intermittent starting and stopping of fluid flow.

[000126]. In Figure 34, a modified dispenser, generally indicated at 302, includes identical parts as discussed above with respect to Figure 33, except that the third passageway 332 includes two mixing devices 336A, 336B positioned in spaced-apart series upstream of a dispensing end 334. In accordance with aspects of the invention previously described, variations are possible for a length L between the upstream mixer 336A and the distal end 324 and a distance V between the upstream and downstream mixers 336A and 336B.

[000127]. Other modifications are also possible. For example, the gas-assisted spray dispensers shown in Figures 33-34, or any of the above embodiments, may be modified to include various alternative orientations for the component passageways, such as and not limited to the orientations shown in Figures 5-8. For example, a modified dispenser may provide parallel component passageways for separate components fluid streams, such as using a catheter or other similar structure, having a desired length, such as for use as part of a laparoscopic spray device or other minimally invasive surgical instrument and/or procedure. If gas-assist is employed, the gas fluid stream may be located either upstream or downstream of the mixer, and/or upstream or downstream of the location where the fluid component stream

are joined. Other variations from the above discussed modifications are also possible.

[000128]. Figures 35-36 shows another dispenser, generally indicated at 402, which includes similar parts as discussed above with respect to Figures 1, 19, 33 or 34 except that the device may employ a spray head 438, which includes a mechanical break up unit known as MBU that allows the components (such as fibrinogen and thrombin), to be sprayed with air and/or water and which is shown and described in U.S. Patent 6,835,186. As discussed above with respect to other embodiments, the connector 438 in Figure 35 may employ one or more mixing devices 436 located in the passageway 432 in which the fibrinogen or thrombin are combined. The air and/or water may be introduced into the combined stream either upstream or downstream of such mixing.

[000129]. In accordance with another aspect of the present invention, Figures 37-40 show a connector, generally indicated at 500, that includes a mixing device 502 located therein. In Figure 37, the connector 500 may be located in fluid communication with a dispensing device, such as a single or multi-barrel dispensing device, as previously described herein although other devices are also possible. As shown in Figure 37, the connector is provided at the distal end of a collecting/dispensing device 504 having a single container, which device may, for example, be located downstream of the dispensing device in Figures 1-4 for storing or collecting the sufficiently mixed components after they have passed through the mixer. Other arrangements are also possible and are not limited to the devices shown and described.

[000130]. As indicated in previous embodiments, the mixing devices 502 may be located in spaced relation to each other and located in series. The connector 500 also includes first and second ends, 506 and 508, respectively, which, as shown in Figures 39-40, may be respectively associated with a male and/or female luer locking feature for connection to the dispensing device 504, as shown, and/or other dispensing devices. In Figures 39-40, the connector in 500 includes a sleeve 510 which defines a fluid passageway 512 defined therein that receives the mixing devices. The sleeve 510 may include grooves 514 defined on the interior surface of the sleeve to receive a portion of an extension 516 that defines a channel or tubing in fluid communication with the device 504. The grooves may, for example, receive projections 518 defined in the extension 516 which may be inserted by rotating the

projections along the curved profile of the grooves 514 (as shown in Figure 514) to provide a luer lock type connection. It is possible that either end of the connector 500 may provide other shapes, configurations and/or types of connections that may prevent inadvertent disconnect of the fluid passageways, as may be desired, and, as such, are not limited to the connections shown and described.

[000131]. Figures 41 and 42 show an alternate connector 600 having a single mixing device 602 located in a fluid passageway 604 defined in the connector 600. The connector 600 includes first and second ends 606 and 608, respectively, which may provide two female luer locks that may be attached to a dispensing device, such as a syringe or other device at each side of the connector.

[000132]. Figures 43-46 show yet another modified connector 700, which employs two mixing devices 702 that are positioned in series within a fluid passageway 704 defined in the connector. As shown in Figure 44, the connector 700 includes a first and second ends 706 and 708, which may respectively be associated with a female and male luer locking feature. The connector may be comprised of one or more tubing sections 710, 712, and 714, as shown in Figure 44-46, which are attached together, for example, by mechanical connection or by ultrasonic welding. For example, the interior surface of the tubing section 710 includes a lock system to attach to the tubing section 706 and a respective end 714 of the tubing section 710 may allow for a locking connection between the tubing section 706 with a cannula, needle, syringe or other device. Generally speaking, it is preferred for the connector to have a luer lock feature where employed in medical applications although other connections are possible for other applications.

[000133]. In accordance with a further aspect of the present invention, a method provides for mixing at least two separate streams of components, such as for example, sealant components. The method may be performed by providing a mixer such as at least one mixer 36, 236 or more than one mixer 136A, 136B, 336A, 336B, which includes a three-dimensional lattice or matrix that defines a plurality of tortuous, interconnecting passages therethrough, such as in any of the above-described embodiments. The method further provides for passing the at least two separate streams of components such as sealant components through the mixer.

[000134]. As noted above, the method may be performed with at least one mixer or a plurality of mixers, such as two or more mixers positioned in series, either adjacent or spaced from one another. The method may also be repeated a plurality

of times such that the flow of the two streams may be stopped and then the flow of the streams may be restarted so that the streams pass through the mixer with minimal clogging of such mixer.

[000135]. During operation of the dispensers 2, 102, 202, 302, 402 in Figures 1-21, 33-35 two separate streams flow through the respective first and second passageways 28, 30, 128, 130, 228, 230 (only one passageway 330 being shown in Figure 34) to the third passageway 32, 132, 232, 332, 432. As the streams flow through the three-dimensional lattice that defines the tortuous, interconnecting passages in the single mixer 36, 236, 436 or the mixers in series 136A, 136B, 336A, 336B the streams are mixed into an essentially homogeneous combined fluid stream.

[000136]. By way of example, Figure 47 shows a method for providing mixing of at least two separate components employing a connector 800, such as any of those described above having at least one mixer, which connector may be attached at one end to a device 802 having two separate containers 806 and 808, respectively, and attached at its other end to a dispenser 804. As noted above, the components may be allowed to flow from the separate containers 806 and 808 through corresponding separate passageways 810 and 812 to a combined passageway 814 which extends to the connector 800. The mixture of the components flows through the connector 800 having at least mixer positioned therein to a passageway 816 of the dispenser attached to the opposite side of the connector 800 for dispensing as desired.

[000137]. Turning to Figure 48, another embodiment of a mixing/dispensing system is shown. As seen in Figure 48, a mixing device 900 is located between two containers, (e.g., dispensers) each holding a fluid (liquid or gas). The portion of the combined device that holds mixing device 900 can be integrated with one of the dispensers or be a connector, with at least one mixer 901 located therein. Such connector is shown having first and second ends 902 and 904, each connected to a dispenser 906 and 908, respectively, having a single container 910 and 912. By way of example and not limitation, the present invention provides a method for mixing at least two separate streams of fluid components, where each component, is separately located in one of the dispensers 906 and 908. Each container includes a distal passageway 914 and 916, respectively, which each fluidly communicate with one side of the mixing device 900, which as shown in Figure 48 provide two female luer attachments, although the mixing device 900 may also be provided with two

male luer on its ends 902 and 904 and/or some combination thereof, as desired for other attachments. When it is desired to mix the components, one component, such as fibrinogen, which, for example is located in the left dispenser is allowed to flow from one (or first) side of the mixer to another (or second) side of the mixer thereby allowing flow into the other container 908 on the right side of the mixer, where, for example, thrombin is located. It is contemplated that either one or both of the containers may be partially filled prior to mixing to accommodate the additional volume of the other component. The two components are preferably allowed to flow from the container 908 through the mixer to the left side of the mixer. Each time the components pass through the mixing device 900 further mixing between the components is provided. It is contemplated that the components may pass through the mixing device 900 at least once, but more preferably several times, as desired or necessary to achieve sufficient mixing.

[000138]. For example, where fibrinogen and thrombin are employed, it may be desired to allow the components to pass through the mixing device back and forth between the two containers at least two or three times to achieve sufficient mixing. The mixture may then be stored in one of the containers 906, 908 and detached from the other to permit dispensing at a desired location. Alternately, a device, as shown and described below at Figures 50A-50C, may include a separate nozzle or exit port transfer through which the mixed fluid may be dispensed. It may further be desired to employ the mixing device of Figure 48 to mix fibrinogen and thrombin and air. For example, one of the containers 910, 912 may contain 1ml of fibrinogen having about a 100mg/ml concentration and the other may contain 1 ml of thrombin, for example, of a 4IU thrombin concentration, and 2.5 ml of air with the mixing device located between the two containers for transferring the components back and forth between the two containers at least once, and preferably, several times, and, more preferably, at least four times, to create a "fibrin mousse" that is a fibrin mixture having a relatively higher volume of air (such as 125% by air volume in the above example), and a lower density than fibrin mixed without air. The fibrin mousse may, for example, allow application to the underside of a patient's body, such as for treatment of acute or chronic injuries such as a foot ulcer injury. Other volumes of fibrinogen and thrombin, and having different relative amounts, may be combined with different volumes of air to increase or decrease the percentage of air contained in the combined fibrin mixture. The fibrin mousse obtained may also be lyophilized to form

a sponge or grinded to obtain a hemaostatic powder (dry fibrin glue), as described in U.S. Patent 7,135,027. Other variations are also possible, including mixing of different liquid components for other fields of application, such as egg whites and oil and/or water for the food industry, oil and water or diesel and water for the automotive industry, as well as other applications described further below. Alternatively, it is also possible to mix two or more gases employing the mixing device of Figure 48.

[000139]. As previously described devices and systems described herein are not limited to mixing liquid components. One or both of the components may in fact be a gas such as air or other gases. The embodiment shown in Figure 48 is particularly well suited for mixing a liquid with a gas. In an example involving fibrin formulation, one of the fibrin forming components may include a selected amount of air and some are discussed further below, although other liquid-gas mixtures are also possible. It is also possible for one or more of the components to be a solid that may be passed through a mixer in any one of the devices and systems described herein. The solid is comprised of particles having a size or diameter that is relatively smaller than the minimum pore size of the mixer so that such solid may pass through the mixer. For example, one or more solids may be mixed with another solid, a liquid or a gas as, for example, in methods for making nano or micro sized particles and suspensions thereof.

[000140]. In accordance with another aspect of the present invention, three or more components may be mixed together using any of the above described embodiments or the like. For example, In Figure 49 shows first and second devices 1002 and 1004 connected to one another via a mixing device 1006 that employs at least one mixer 1008 located therein. The first device 1002, which may be similar to the dispensers 2, 102, 202, and 302, as described above, may employ at least two containers each separately containing a component, such as one of fibrinogen or thrombin, for mixing. The second device 1004 may contain biphasic calcium phosphate granules. When mixing is desired, the fibrinogen and thrombin may be allowed to flow from the first device 1002 through the mixing device of the mixing device 1006, to provide mixing between the two components into a fibrin mixture, which then is allowed to flow into the second device 1004 to fill the porous spaces around the granules. The second device 1004 may be disconnected for application,

for example, to aid bone growth for a patient. Other methods for mixing of the present invention are also possible.

[000141]. Turning to Figures 50A-50C, a modified mixing device 1050 is provided between two containers, 1052 and 1054, and, as such, is similar to the mixing device shown in Figure 48, and further includes a third container 1056. Each of the containers 1052, 1054 and 1056 are connected by way of a valve 1058 (with the mixing device 1050 being shown at the left side of the valve), such as a three-way valve, stop cock or other suitable valve structure which allows selected communication between at least two containers at a selected time. Other variations to the illustrated arrangement are also possible. For example, it is possible to employ one or more mixing devices at either side of the valve and/or to employ two or more mixing devices at any one side of the valve.

[000142]. By way of example, Figure 50A shows the first container 1052 and the second container 1054 in fluid communication with each other across the valve 1058 via a fluid passageway 1060. In Figure 50A, the valve is open to allow for fluid flow between the two containers while fluid flow to the third container 1056 across the valve 1058 is closed. Each container 1052 and 1054 contains at least one component, respectively identified as A and B for mixing into a combined mixture.

[000143]. As shown in Figures 50A and 50B, the component A from container 1054 is allowed to flow across the valve 1058 through the open fluid passageway 1060 and the mixing device 1050 to the container 1052 on the other side of the mixing device 1050 such that both components A + B reside in the same container. In Figures 50A-50C, the components A + B may be allowed to flow between the first and second containers 1052 and 1054 at least once (i.e., to container 1054) as a combined mixture and perhaps several times (i.e., back and forth between containers 1052 and 1054) to achieve the desired number of changes in flow direction that provides sufficient mixing of such components using the mixing device. In Figures 50A-50C, which employs a single mixing device, it may be desirable to switch the direction of flow several times, although the number of changes in flow direction may be reduced as the number of mixing devices that may be employed is increased. When the desired number of changes in flow direction has occurred, the components A+B preferably reside in one of the containers 1052 and 1054, such as shown in Figure 50B, which shows components A + B in the same container 1052.

[000144]. In Figure 50C, the position of the valve 1058 is rotated to provide a fluid passageway 1062 between one of the containers 1052 and the third container 1056. The flow of the combined mixture A + B is then allowed to flow into the third container 1056, which may be a reservoir or other structure that utilizes the combined mixture. By way of example and not limitation, the third container 1056 may be cylinder of an engine or a reservoir that is in fluid communication with the engine and each component A, B selected from one of a liquid or gas or a mixture of liquid or gas, such as water, air, alcohol, gasoline oil and/or diesel oil or some combination thereof. Such application may be beneficial to provide inline mixing of biodiesel fuel, super oxygenated fuel, fuel additives or other desired automotive mixtures. An example of forming biodiesel fuel employing the device in Figures 50A-50C may include 0.13 ml of water and 0.77 ml gasoline oil or diesel that is "swooshed" back and forth between containers A and B and then allowed to collect in the third container for immediate use or be stored for later use. An example of super oxygenated fuel employing on the device in Figure 50A-50C may include 2.0 ml of air and 1.0 ml diesel that is similarly allowed to "swoosh" back and forth between the two containers, in a desired number of times, before passing into the third container for use. Other fields of application are also possible. It is further contemplated that the water may be obtained from a water reservoir located in the automobile and that may be filled by the driver at home or at a gasoline station and/or may be collected from the air conditioning system, rain and/or other methods.

[000145]. It may be preferable to have the above described mixing system available at a service or fuel station where the fuel components are mixed just prior to dispensing by a user into an automobile for use. Alternatively, it may be more preferable to have the mixing system as part of automobile fuel system where the fuel components are mixed just prior to use by the automobile (e.g., just prior to when the fuel mixture is introduced into the cylinder or other combustion device).

[000146]. In addition to the medical and automotive applications already described above, any of the inline mixing devices, as described herein, may be employed in other applications. Examples of such other applications include aerospace (e.g., space propulsion), chemical (e.g., mixtures of cosmetics, paint, detergents), food (e.g., drink mixtures, food additives), PVC or polymer emulsions cosmetics, dental, health or pharmaceutical, adhesives and water treatment (water additives), oil drilling fluids (mixing pressurized water). In addition, such inline mixing

devices may be employed in ophthalmologic applications such as to mix and dispense relatively small quantities such as, at about 50 microliters, which may typically require dispensing to a patient at a relatively slow flow rate. As described and shown below, dispensers using one or two mixers, as described herein, achieved relatively good quality of mixing, that is independent of the flow rate employed. In this regard, it is contemplated that the mixers described herein may be employed in other medical and non-medical applications to achieve sufficiently good quality of mixing regardless of the relatively high or low flow rates that may be employed.

[000147]. For example, the mixing device such as in Figure 48 or 50A-50C may be used to mix an egg white with air to create an egg white mousse. In such example, one of the containers A and B may contain 2.5 ml of air and the other may contain 0.5 ml of egg white. Alternatively, the mixing device may be used for other food mixtures such as egg yolk with olive oil to create a mayonnaise mixture, vegetable oil and vinegar to create vinaigrette or other food mixtures.

[000148]. Figures 51-52 show yet another connector 1100 which, for example, may be employed in an in-line tubing apparatus or method to mix two or more liquids during an infusion delivery to a patient. In Figure 51, two containers or bags 1102 and 1104 each separately contain a different fluid, for delivery or infusion to a patient. By way of example and not limitation, the fluids may include dextrose and bicarbonate although other fluid is possible. Infusion may be aided by gravity, pump and/or other convention methods. Each container fluidly communicates with a respective passageway 1106 and 1108 which extends downstream to the connector 1100. As previously described with the above embodiments, the connector 1100 may include at least one mixing device or more, with two mixing devices 1110 being shown in Figure 52 by way of example. The separate passageways 1106 and 1108 are preferably allowed to join together at a selected location 1112 upstream of the connector 1100. The fluid streams pass through the mixing devices 1110 to a passageway 1114 located downstream of the connector 1100 for delivery of the mixture to the patient.

[000149]. Any of the devices and systems described herein may be employed as part of a disposable kit, such as a sterile disposable kit for medical applications. The kit may comprise, for example, any one or more of the dispensing/collecting devices or containers shown in Figures 1-8 and 18-52, packaged together with a mixer

arrangement, as shown in any of Figures 1-4 or 18-52. The mixer may be already connected together with the dispensing/collecting device or may be a separately packaged or stand alone article that may be assembled to such device.

[000150]. Where the devices and systems described above are used to prepare a fibrin tissue sealant, a high quality of mixing of a combined fibrin fluid stream, may be characterized by an essentially homogeneous quality (which may be a white color for fibrin obtained with a low thrombin concentration or may be a more transparent appearance for fibrin having a relatively higher thrombin concentration) and a minimum amount of transparent, free liquid, which occurs when the fibrinogen component is essentially homogeneously polymerized with the thrombin component. Accordingly, as shown in Figure 53, the quality of mixing of fibrin may be estimated by turbidimetry measurements which graphically show the absorbance of light of a fibrin matrix. In Figure 52 the abscissa represents the change in turbidity based on the optical density (OD) of a dispensed component, such as fibrin, that is monitored at 405 nanometers (nm) with a spectrophotometer, and where the ordinate represents time in minutes. Further explanation of turbidimetry measurements for a fibrin combined fluid stream is provided in "Alteration of Fibrin Network by Activated Protein C", by András Gruber, et al. *Blood*, Vol. 83, No. 9 (May 1, 1994); pp. 2541-2548.

[000151]. As shown in Figure 53, such turbidimetry measurements were performed based on a fibrin matrix made of essentially similar concentrations, such as, for example, 4 International Units (IU), of fibrinogen and thrombin, although other concentrations or different combinations of concentrations may be employed for each component. Mixing was performed essentially at room temperature, such as, for example, between about 15 and 25 degrees Celsius. At Figure 53, curve no. 1 represents a control dispenser which lacks any mixer i.e. or mixing device. Curves nos. 2-4 represent three dispensers which include a mixer 36, such as shown in Figures 1-4, where the mixer is comprised of three different materials, respectively, Sample 2, PE, a product sold by Porvair (at curve no. 2); another PP product, as sold by Porvair (at curve no. 3); and Sample 7, a product sold by Porex (at curve no. 4). The graph at Figure 53, essentially shows a correlation between the use of a mixer (at curves nos. 2-4) and a reduction in the time required for essentially homogeneous mixing. At Figure 53, curves nos. 2, 3 and 4 show that the time required to reach a plateau representing consistent optical density, and thus,

essentially homogeneous mixing is achieved is less time (2-3 minutes) for dispensers having a mixer as compared to the time required (> 10 minutes) for a control dispenser which lacks such mixer.

[000152]. At Figure 54, the quality of mixing of fibrin is characterized and determined by turbidimetry curve representing two mixers spaced about 4 mm apart and a length L of about 6 mm between the upstream mixer 136A and the distal end 124, such as shown in Figures 19-21 and as previously described. The turbidimetry curve of Figure 53 indicates that the absorbance of light of the combined fibrin fluid stream, reaches a plateau indicative of essentially homogeneous mixing at about 2-3 minutes, similar to above discussed single mixer embodiments

[000153]. The present invention also may provide a combined fluid stream which preferably has a consistent viscosity regardless of temperature. Generally, an increase in temperature improves mixing of components, such as fibrinogen and thrombin. It is noted that the viscosity of fibrinogen varies between about 150 and 250 centipoises (cps) or about 1.5 and 2.5 g/ (cm * sec), depending on temperature, which is significantly different, by approximately an order of magnitude, from the viscosity of thrombin, which is between about 10 and 20 centipoises (cps) or about 0.1 and 0.2 g/ (cm * sec), also depending on temperature. The present invention may provide for essentially homogeneous mixing at about room temperature without requiring any heating of the components, such as by employing of the above described embodiments.

[000154]. The quality of mixing of a combined fluid stream, such as fibrin, may also be characterized and determined by adding a contrast or radiopaque agent, such as, for example, Iohexol to the thrombin concentration, prior to mixing of the components. For example, 50, 100, 200, 300, 400, 500 and 600 mg/mL concentrations of Iohexol were separately added to essentially similar thrombin concentrations, such as 75IU, the concentration of a contrast or radiopaque agent, such as Iohexol, may range between about 50 and 1200 mg/mL, preferably between about 300 and 400 mg/mL. Each thrombin/Iohexol combination may be mixed with a fibrinogen component using a mixer, such as a two-mixer arrangement having a distance V of about 4 mm and a length L of about 6 mm. After passing the components through such mixer, the fibrin samples with Iohexol, as arranged alongside each other, provide more transparent, homogeneously-mixed fibrin streams as compared to a fibrin sample that was obtained without Iohexol using a

mixer (indicated at "+" or as arranged alongside the 600 mg/mL sample) which is shown having a white color with greater turbidity. The above described samples were also compared to a "control" fibrin sample without Iohexol and without a mixer. The control sample shown provides a fibrin stream having inconsistent turbidity, viscosity and color which is typical of insufficient mixing. It is possible to use other contrast or radiopaque agents, depending on the desired application and the combined fluid stream to be employed.

[000155]. It is also possible to add other additive agents, such as antibiotics, drugs or hormones to one or more of the fluid component streams. For example, additives such as Platelet Derived Growth Factor (PDGF) or Parathyroid Hormone (PTH), such as those manufactured for Kuros Biosurgery AG of Zurich, Switzerland, may be added to one of the fibrin-forming components, such as fibrinogen. Bone morphogenic proteins (BMP) may also be employed. By way of example and not limitation, other agents include hydroxypropylmethylcellulose, carboxymethylcellulose, chitosan, photo-sensitive inhibitors of thrombin and thrombin-like molecules, self assembling amphiphile peptides designed to mimic aggregated collagen fibers (extracellular matrices), factor XIII, cross-linking agents, pigments, fibers, polymers, copolymers, antibody, antimicrobial agent, agents for improving the biocompatibility of the structure, proteins, anticoagulants, anti-inflammatory compounds, compounds reducing graft rejection, living cells, cell growth inhibitors, agents stimulating endothelial cells, antibiotics, antiseptics, analgesics, antineoplastics, polypeptides, protease inhibitors, vitamins, cytokine, cytotoxins, minerals, interferons, hormones, polysaccharides, genetic materials, proteins promoting or stimulating the growth and/or attachment of endothelial cells on the cross-linked fibrin, growth factors, growth factors for heparin bond, substances against cholesterol, pain killers, collagen, osteoblasts, drugs, etc. and mixtures thereof. Further examples of such agents also include, but are not limited to, antimicrobial compositions, including antibiotics, such as tetracycline, ciprofloxacin, and the like; antimycogenic compositions; antivirals, such as gangcyclovir, zidovudine, amantidine, vidarabine, ribaravin, trifluridine, acyclovir, dideoxyuridine, and the like, as well as antibodies to viral components or gene products; antifungals, such as diflucan, ketaconazole, nystatin, and the like; and antiparasitic agents, such as pentamidine, and the like. Other agents may further

include anti-inflammatory agents, such as alpha- or beta- or .gamma-interferon, alpha- or beta-tumor necrosis factor, and the like, and interleukins.

[000156]. It is possible that such agent or agents may be premixed with one or more of the fluid components, such as fibrinogen and/or thrombin in the respective component container. Alternatively, it may be possible for such agent or agents to be stored in a separate container as a liquid or lyophilized for mixing with one or more components during use of the dispenser and/or mixer. For a dispenser or mixer, such as in any of the above described embodiments, in which one or more of agents are employed, the combined fluid stream preferably provides a sufficiently thoroughly mixed sealant, such as fibrin sealant, in which the antibiotic, drug, hormone, or other agents may be essentially well dispersed throughout the sealant. Such antibiotic, drug, hormone, or other agent may allow controlled release over time to the applied working surface, for example, to aid in post-operative or surgical treatment. It is contemplated that various agents may be employed depending on the desired application and the combined fluid stream.

[000157]. Although the present invention has been described as employing at least two separate sources of fluid upstream of the mixer, it is also possible to eliminate one of such sources and provide such source within the formation of one or more mixing devices. For example, for forming a tissue sealant, such as fibrin, thrombin may be adsorbed, either soaked as a liquid or incorporated as a solid, into one or more of the mixers and freeze-dried to provide a source of thrombin. Such a mixing device could be connected or otherwise placed in flow communication with a single source of fibrinogen, such as a single syringe containing fibrinogen at 45 mg/mL, for generating a tissue sealant via the mixing that would occur when the fibrinogen is forced through the mixer. Other wet or dry components may be employed with one or more mixers or different components may be employed on different mixers, where one than one mixer is employed.

[000158]. Another way to determine and characterize the quality of mixing may include mechanical testing of the combined fluid stream. Such testing may include testing the reactivity of the combined fluid stream to forces such as tension or compression forces. Generally speaking, a sufficiently thoroughly mixed, polymerized and homogeneous fibrin stream may withstand tensioning and compression forces to a greater extent than a fibrin stream which is insufficiently mixed, polymerized and homogeneous. For example, for a fibrin stream, tension

may be applied to the fibrin stream along its length to determine the extent of fibrin elongation without separation of the stream. In one example, for two mixers having a distance V of between about 0 and 5 mm, preferably between about 3 and 4 mm, and a length L between about 2 and 6 mm, preferably between about 5 and 6 mm, a resulting fibrin stream may provide a fibrin elongation of about 100% to 130%, although other elongations are also possible. Other types of tests may also be employed for determining the quality of mixing.

[000159]. Figures 55-60 show another way and perhaps preferred way of characterizing and determining the quality of mixing from the mixing device of the present invention, such as for a fibrin mixture. The degree of crosslinking may for example, measure a selected amount of a constituent component chain that is contained in the fibrin mixture to a selected amount of the same constituent component in fibrinogen, prior to mixing. Fibrinogen contains selected amounts of alpha (α) monomer chain, albumin, beta (β) chain and gamma (γ) chain. After mixing with thrombin to form fibrin, the fibrin contains different amounts of such component chains due to the crosslinking that has occurred. Typically, fibrin contains a reduced amount of alpha monomer and gamma monomer chains, which have polymerized into alpha-alpha pairs or polymers and gamma-gamma pairs or polymers (or gamma dimer) chains. By way of example and not limitation, the degree or rate of crosslinking may measure that amount of reduction in the alpha monomer chain that is present in the fibrin mixture as compared to the amount of such alpha monomer that is present in the fibrinogen prior to mixing.

[000160]. At Figure 55, the rate of crosslinking is shown for three flow rates of fibrin, at 2ml/min for Group 1, at 4ml/min for Group 2, and at 6ml/min for Group 3. At each flow rate, at least one fibrin sample was separately analyzed for each of the following devices: a control device, which lacked a mixing device; a single mixing device made of polyethylene (PE), having a thickness of 1.5mm and placed 2 mm from the distal end (such as a dispensing housing having a distal end overmolded on a needle or cannula having a single mixer); and a double mixing device made of polyethylene (PE), having thickness of 1.5mm, and having a distance between the mixing devices of about 4mm and a distance between the end of the dispensing distal end and the first mixing device of about 4mm. As shown in Figure 55, the rate of crosslinking of the non-mixing device ranges between about 0-2%. The rate of crosslinking for the single mixing device ranges between about 10-20%, preferably

10-16%. The rate of crosslinking for the double mixing device ranges between about 20-30%, preferably 23-36%. As shown in Figure 55, the rate of crosslinking of fibrin obtained using one or two mixing devices at each flow rate is generally consistent regardless of the flow rate employed.

[000161]. The degree of alpha- α -chain cross-linking is determined by measuring the reduction overtime of the alpha- α -chain-band in comparison to the band containing the fibrin- β -chain and albumin. An electrophoresis method was performed based on an UREA/SDS electrophoresis technique on a DESAGA electrophoresis system (Sarstedt-Gruppe) loaded with a 5% acryl amid separation gel to identify the different chains of fibrinogen. After mixing fibrinogen and thrombin components at a ratio 1:1, the mixture was incubated at 37 C. The fibrinogen component employed for each of the samples described contained about 3IU of Factor X III (FXIII) although it is realized that other concentrations of FXIII may be employed, which will achieve difference rates of crosslinking. Generally, crosslinking increases as the amount of FXIII is increased. After an incubation time of 0 and 120 min, the reaction was stopped by addition of a denaturant sample buffer and heated at 70 C for 5 min. The clots were left overnight for dissolution in the sample buffer at room temperature. The samples were loaded on a 5 % polyacrylamide/urea gel. The gel was stained with Coomassie Brilliant Blue R250 and destained according to the method of Furlan, as shown on Figure 56. The amounts of alpha- α -chain, beta- β -chain, gamma- γ -chain, fibronectin and albumin of samples in Figures 55-60 were then determined by densitometry and plotted on drawings represented by Figures 57, 58, 59 and 60.

[000162]. In Figure 56, 12 lanes of horizontal bands are shown that were prepared according to the electrophoresis procedure described above including a marker or baseline at lane 12 for purposes of quality control for such procedure. In Figure 56, the "zero sample 1" and "zero sample 2" indicate the presence of constituent components, according to molecular weight, in fibrinogen at an incubation time zero, and thus before any crosslinking with thrombin has occurred. Samples 10-18 show the presence of the constituent components in a fibrin mixture after an incubation time of 120 minutes, according to the different devices represented in Group 2 of Figure 55. More particularly, samples 10-12 correspond to the results obtained without employing a mixing device (corresponding to "ctrl" at

4ml/min in Figure 55), samples 13-15 show the results obtained by employing one mixing device (corresponding to "1 disc" at 4ml/min in Figure 55), and samples 16-18 show the results obtained by employing two mixing devices (corresponding "2 disc" at 4ml/min in Figure 55). As shown in Figure 56, each of the "zero samples" and samples 10-18 contains selected amounts of alpha (α) monomer chain, a combined albumin + beta (β) chain and gamma (γ) chain, as indicated by the respective bands illustrated for each sample. Also in Figure 56, each of samples 10-18 alpha (α) polymer chain, as indicated at the top of samples 10-18, and gamma (γ) polymer (or gamma dimer) chain, located above the alpha monomer chain are present. Such chains are typically present after crosslinking has occurred due to mixing of the fibrinogen and thrombin components, and thus are generally absent or negligible in the "zero samples" shown in Figure 56. Typically, a darker band indicates a greater amount of a constituent chain. In Figure 56, samples 13-18, which employ at least one more mixing devices, have darker alpha (α) polymer and gamma (γ) polymer (or gamma dimer) chains, which correspond to the greater crosslinking values shown in Figure 55.

[000163]. Turning to Figure 57, the relative amounts of the constituent chains contained in the "zero samples" are shown which include 3 peaks along the graph, labeled at 1, 2 and 3. Respectively, such peaks correspond to the amount of the gamma (γ) monomer chain at peak 1, the amount of the albumin + beta (β)-chain at peak 2, and the amount of the alpha- (α) - chain at peak 3. If present, the amount of the gamma polymer or gamma dimer chain would be represented above the label at peak 4 and the amount of alpha polymer chain would be represented above the label at peak 5, (although little if any measurable peak can be seen due to mixing with thrombin not yet occurring. Based on the data represented in Figure 57, the relative amounts of alpha - (α) -Monomer chain to beta - (β)-Monomer chain plus albumin can be calculated by integration of the area under each respective peak as follows:

[000164]. TABLE 4

Number	Total
1	19.712
2	84.771
3	26.619
4	24.411

[000165]. Figures 58-60 show the relative amounts of selected constituent components contained in sample 12 – one of the control samples from Figure 56, sample 13 – one of the single mixing device samples—and sample 17 – one of the two mixing device samples – and their respective peaks at 1, 2, 3 and 4 corresponding to the amount of the gamma monomer chain at peak 1, the amount of the albumin + beta-(β)-chain at peak 2, and the amount of the alpha- (α) – monomer chain at peak 3, and the amount of the gamma polymer or gamma dimer chain at peak 4, representing some crosslinking reaction due to the mixing of fibrinogen and thrombin. Based on integrating the area under the respective peaks in Figures 58-60, the relative amounts of such chains are calculated as follows:

[000166]. TABLE 5

Number – chain	Totals from Sample 12	Totals from Sample 13	Totals from Sample 17
1 – γ monomer	12.932	5.486	4.077
2 – albumin + β	82.833	87.718	77.378
3 – α monomer	26.714	24.821	19.444
4 – γ dimer	8.390	14.825	13.044

[000167]. The degree of crosslinking may be represented as a Q value:

[000168]. $Q = X_n / X_1$,

[000169]. where X_1 represents the ratio or quotient of the total alpha α chain (total at peak 3) to the total albumin + β chain (total at peak 2) from Table 4 for an incubation time zero (0) (time) or for fibrinogen prior to mixing with thrombin; and

[000170]. X_n represents the ratio or quotient of the total alpha α chain (total at peak 3) to the total albumin + β chain (total at peak 2) for any one of the samples indicated in Table 5 for an incubation time n or for a fibrin mixture after mixing with thrombin.

[000171]. Based on the above samples, the estimated crosslinking or Q values may be represented as follows:

[000172]. TABLE 6

Value	Sample 0/1 – Fibrinogen	Sample 12	Sample 13	Sample 17
α monomer/ (albumin + β)	26.619/84.771	26.714/82.833	24.821/87.718	19.444/77.378
$X_1 = \alpha$ monomer/ (albumin + β)	0.314	0.314	0.314	0.314
$X_n = \alpha$	--	0.322	0.282	0.251

monomer/ (albumin + β)				
X_n / X_1	0.314	0.322/0.314	0.282/0.314	0.251/0.314
Q	-	1.0	0.89	0.79
% crosslinking		0	11	21

[000173]. Based on the above examples, X_1 may be represented as $X_1 = \alpha \text{ chain} / \text{albumin} + \beta \text{ chain}$ from "Zero Sample" or fibrinogen prior to mixing. For example, X_1 may have a value of about 26.619/84.771 or about 0.314, as indicated above. X_n may be represented as $X_n = \alpha \text{ chain} / \text{albumin} + \beta \text{ chain}$ for any one of the fibrin mixtures of Samples 12, 13 or 17, as indicated above, for example, in sample 17, X_n may have a value of about 19.444/77.378 or about 0.251. The incubation time employed in the above examples is about 120 minutes and were observed at a temperature of 37 degrees Celsius, although other incubation times and temperatures may be employed. The rate of crosslinking further may be represented as a percentage, which is also indicated in the above table and may be calculated as follows:

[000174]. Rate of crosslinking [%] : $100 \times (1 - Q)$

[000175]. As shown in Table 6 above the quality of mixing as determined by the rate of alpha chain crosslinking was improved in devices using at least one mixer and further improved when two mixers are used. As shown in Table 6 the % crosslinking reported was approximately 11% and within a typical range of approximately 10-16%. The % crosslinking in devices using two mixers was approximately 21% and within a range of about 20%-30%.

[000176]. In Figure 61, the data shown indicates the effect of temperature on the quality of fibrin mixing formed with a two mixer device, such as shown in Figures 19-21. For example, the distance between the mixers may be 4mm and the distance from the y piece to the first mixer may be 4mm, with a thickness of 1.5mm. The data represents the rate of crosslinking of a fibrin mixture at each of temperatures 4°C, 18°C, 22°C and 37°C for each of a control device without a mixer as compared to using a mixing device, as described above.

[000177]. As represented in Figure 61, the % crosslinking for fibrin obtained by using the mixing device ranged between about 24-33% with the highest value obtained at 4°C, a temperature at which fibrinogen has an estimated viscosity of between about 500-600 cps. At 18°C and 22°C the viscosity of fibrinogen ranges

between about 160cps to 120cps and at 37°C, the viscosity of fibrinogen is between about 70-80 cps and thrombin is about 5 cps. As shown, the % crosslinking using the described mixing device is relatively consistent at each represented temperature, as compared to the control device which achieves poor crosslinking at the lower temperatures 4-22°C.

[000178]. As represented in Table 6, the quality of mixing is not dependent on the temperature when using a mixing device in contrast to the control device which requires an increase to 37°C to such a value of 21% crosslinking. By way of example, a fibrin mixture using a mixing device in Table 6 would not require heating or warming above typical operating room temperatures of about 18°C to 22°C, as 27%-33% crosslinking is achieved as such temperature ranges. In addition, the above described % crosslinking is generally not affected by gamma irradiation, or sterilization as applied with the medical field.

[000179]. Other ways may also be employed to measure the degree of crosslinking, such as for example, measuring the increase or decrease in other constituent chains. By way of example and not limitation, in addition or as an alternative to the above, it is also possible to measure the degree of crosslinking by measuring the increase in one or both of the gamma (γ) polymer (or gamma (γ) dimer) chain and the alpha (α) polymer chain, as either component generally increases as the degree of crosslinking increases to indicate mixing of the fibrinogen and thrombin. Another way to measure the degree of crosslinking may be measure the decrease in the gamma (γ) monomer chain, which decreases as the degree of crosslinking increases.

[000180]. Figures 62-63 show yet another way to estimate the quality of mixing from the mixing device of the present invention, such as for a fibrin mixture. For example, the degree of mixing may be determined by monitoring an optical characteristic of the fibrinogen and an optical characteristic of thrombin as compared to the presence of such optical characteristics in the fibrin mixture. As shown in Figures 62-63, one such optical characteristic may include the degree of fluorescence emitted from a combined fibrinogen and thrombin fluid stream in the fluid passageway after joining the separated streams of such components.

[000181]. Figure 62 shows the distribution of fluorescence in a cross-section of tubing (represented between the two black lines, between 1.2 and -1.5 mm of the

tubing section height) for a combined fluid stream of thrombin and fibrinogen and the relative grey level, which ranges between about 0-250, for an apparatus without a mixing device. In contrast, Figure 63 shows the distribution of fluorescence in a similar section of tubing that is observed downstream a mixing device, such as employing any of the previously described mixing devices. In Figure 62, the distribution of fluorescence is evaluated after 1, 3 and 20 seconds of flow rate. A relatively high distribution of fluorescence of about 220 to 250 is generally concentrated on one side of the section of tubing between about 0 and 1.2, along the Y-axis, which corresponds to the presence of thrombin that generally has a high degree of fluorescence. A relatively low distribution of fluorescence is indicated on the other side of the section of tubing between about 0 and -1.5, which generally corresponds to the presence of fibrinogen that generally has a low distribution of fluorescence. As represented in Figure 62, the high distribution of fluorescence along one side of the tubing section and the low distribution of fluorescence on the other side of such tubing section generally indicates that relatively little mixing is achieved between the thrombin and fibrinogen fluid streams.

[000182]. In contrast, Figure 63 shows the distribution of fluorescence of a combined fibrinogen and thrombin stream downstream of a mixing device, with respective distribution curves shown for 1, 3 and 20 seconds. As can be seen in Figure 63, each curve is generally well distributed over the entire tubing section between the range of about 1.2 and -1.5 mm of the tubing section height. It is also possible that other ways may be employed to measure the quality of mixing, such as for example, other optical or physical characteristics of the components.

[000183]. As can be seen from the above description, the present invention has several different aspects, which are not limited to the specific structures shown in the attached drawings. Variations of these concepts or structures may be embodied in other structures for carrying out application of tissue sealant or other applications in the medical or other fields without departing from the present invention as set forth in the appended claims.

What is claimed is:

1. A device for mixing at least two separate streams of components which, when mixed, form a combined fluid stream, the device comprising:

a first passageway adapted to communicate with one of the at least two separate streams;

a second passageway adapted to communicate with another of the at least two separate streams; and

a porous mixing member communicating with each of the first and second passageways comprising a three-dimensional lattice defining a plurality of tortuous, interconnecting passages therethrough, the porous mixing member having physical characteristics to sufficiently mix the component streams of the combined fluid stream, which characteristics include a selected one or more of mean flow pore size, thickness and porosity,

the porous mixing member comprising a porous sintered material selected from the group consisting of glass, ceramic, metal and polymer.

2. The device of claim 1 in which the product of the mean flow pore size, thickness and porosity of the porous mixing member is within the range of about 0.016 to 0.055.

3. The device of claim 1 in which the porous mixing member has a K value within the range of about 5 to 17, as measured by Darcy's Law:

$$K = Q * \eta * L / (S * \Delta P)$$

where Q = flow rate of the combined fluid stream,

η = viscosity of the more viscous of the two components,

L = thickness of the porous mixing member,

S = surface area of the porous mixing member, and

ΔP = change in pressure between upstream and downstream locations of the porous mixing member.

4. The device of claim 1, said device being a tissue sealant device.

5. The device of claim 4, further comprising at least two containers separately containing a fibrinogen component and a thrombin component which combine to produce a fibrin mixture having selected amounts of fibrinogen and thrombin, the first passageway communicating with one of the at least two containers and the second passageway communicating with another of the at least two containers, wherein each of the fibrinogen and the fibrin mixture includes at least an alpha monomer chain, albumin and a beta monomer chain and wherein the fibrin mixture has a rate of cross-linking measured by a Q value of X_n/X_1 , where X_1 and X_n each represent the ratio of the alpha chain to the combined amount of albumin and the beta chain, respectively for the fibrinogen and the mixture.
6. The device of claim 4, further comprising at least two containers separately containing a fibrinogen component and a thrombin component, the first passageway communicating with one of the at least two containers and the second passageway communicating with another of the at least two containers, wherein the combined fluid stream is a fibrin mixture of selected amounts of fibrinogen and thrombin respectively having a first and second optical characteristic and the combined fluid stream provides a relatively uniform optical characteristic to indicate when the first and second components are sufficiently mixed to form the fibrin mixture.
7. The device of claim 6, wherein said one of the first and second optical characteristic is fluorescence.
8. The device of any one of claims 1 to 7 comprising at least two of said porous mixing members located in series.
9. The device of claim 8, wherein the porous mixing members are in spaced-apart relation to each other.
10. The device of claim any one of claims 1 to 9, wherein the porous mixing member comprises a material selected from polypropylene or polyethylene.

11. The device of any one of claims 1 to 10, wherein the porous mixing member is downstream from a location where the at least two separate streams are first combined.
12. The device of claim 1, further comprising a third passageway in fluid communication with and downstream of the first and second passageways for joining the at least two separate streams at a selected location and an outlet downstream of the porous mixing member to allow flow of the combined fluid stream, and wherein the porous mixing member is downstream of and in the vicinity of the selected location.
13. The device of claim 12, wherein at least one of the two components includes a liquid.
14. The device of claim 12, wherein at least one of the two components includes a solid.
15. The device of claim 12, wherein at least one of the two components includes a gas.
16. The device of claim 12, wherein the two components include at least two selected from diesel, oil, gasoline, water and air.
17. The device of claim 12, wherein the two components include egg white and air.
18. The device of claim 12, further comprising at least two containers separately containing a fibrinogen component and a thrombin component.
19. The device of any one of claims 12 to 18 comprising at least two of said porous mixing members located in series.

20. The device of claim 1, wherein the porous mixing member has first and second sides and the device further comprises:

a first port in fluid communication with the first side of the porous mixing member and adapted to communicate with a source of a first component; and

a second port in fluid communication with the second side of the porous mixing member and adapted to communicate with a source of a second component,

each port being in fluid communication with the other port through the porous mixing member to allow one of the first and second components to flow from a selected one of the first and second sides of the porous mixing member to the other side and to allow return flow of both the first and second components from the other side through the porous mixing member.

21. The device of claim 20, further comprising a container for collecting said combined fluid stream.

22. A method of mixing at least two separate streams of components to form a combined fluid stream comprising the steps of:

conveying a first component stream through a first passageway;

conveying a second component stream through a second passageway;

and

passing the first and second component streams from the first and second passageways through a porous mixing member comprising a three-dimensional lattice defining a plurality of tortuous, interconnecting passages therethrough, the porous mixing member having physical characteristics to sufficiently mix the component streams, which characteristics include a selected one or more of mean flow pore size, thickness and porosity,

the porous mixing member comprising a porous sintered material selected from the group consisting of glass, ceramic, metal and polymer.

23. The method of claim 22, wherein the product of the mean flow pore size, thickness and porosity of the porous mixing member is within the range of about 0.016 to 0.055.

24. The method of claim 22, wherein the porous mixing member has a K value within the range of about 5 to 17, as measured by Darcy's Law:

$$K = Q * \eta * L / (S * \Delta P)$$

where Q = flow rate of the combined fluid stream,

η = viscosity of the more viscous of the two components,

L = thickness of the porous mixing member,

S = surface area of the porous mixing member, and

ΔP = change in pressure between upstream and downstream locations of the porous mixing member.

25. The method of any one of claims 22 to 24, wherein the first and second component streams are components of a tissue sealant composition.

26. The method of any one of claims 22 to 24, wherein the first and second component streams include fibrinogen and thrombin.

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Unscannable items received with this application
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des dossiers au 10^{ième} étage)

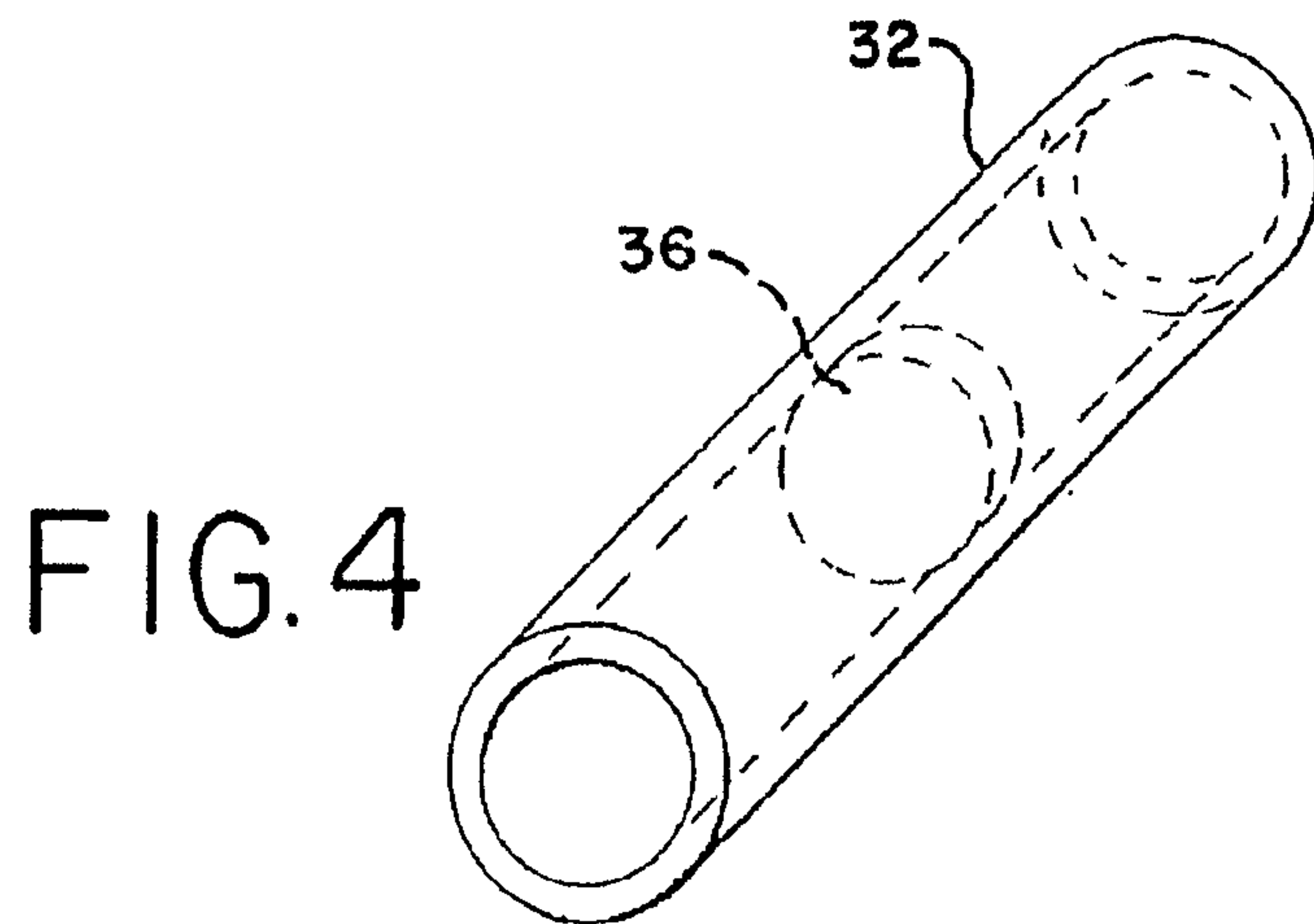
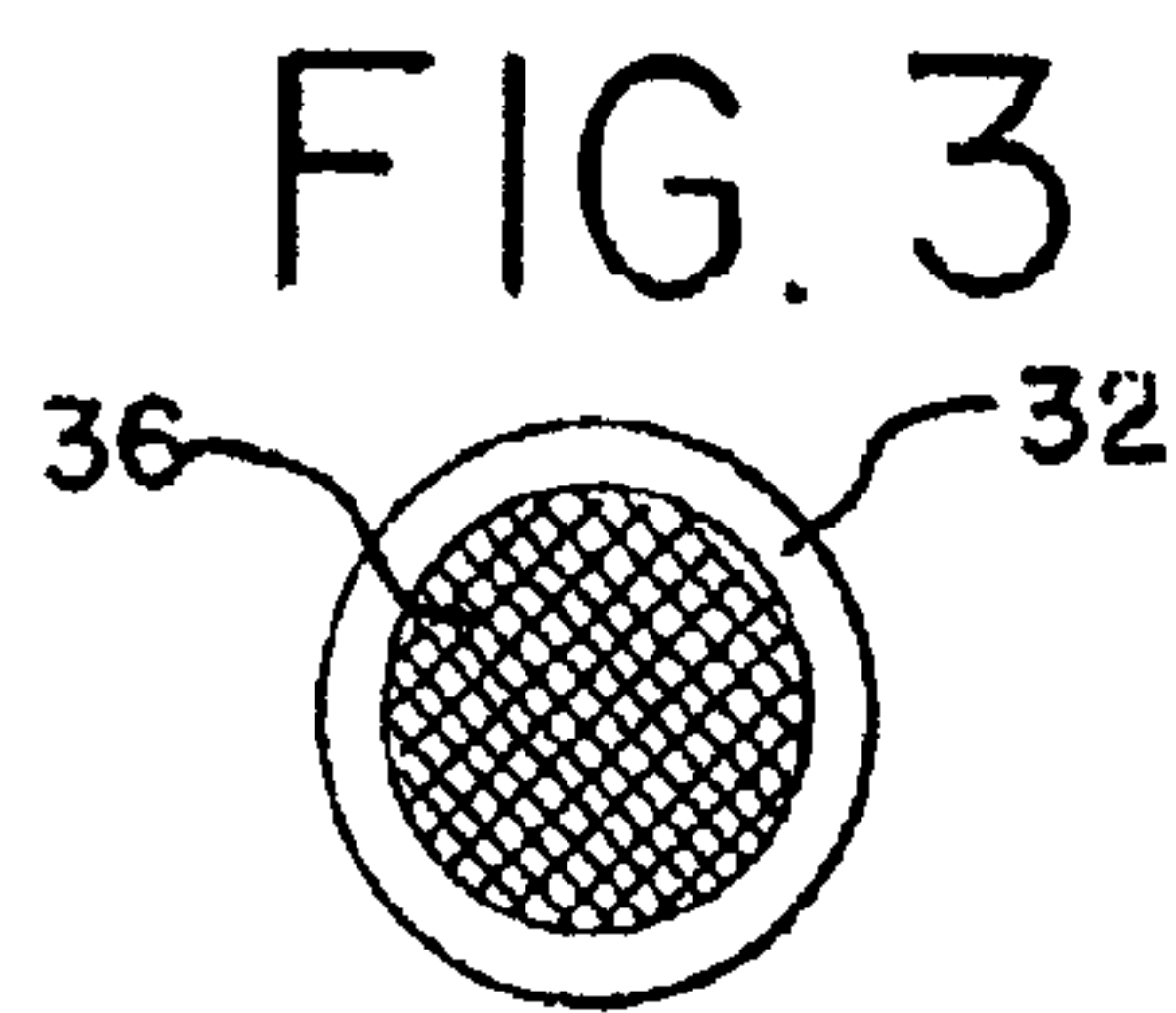
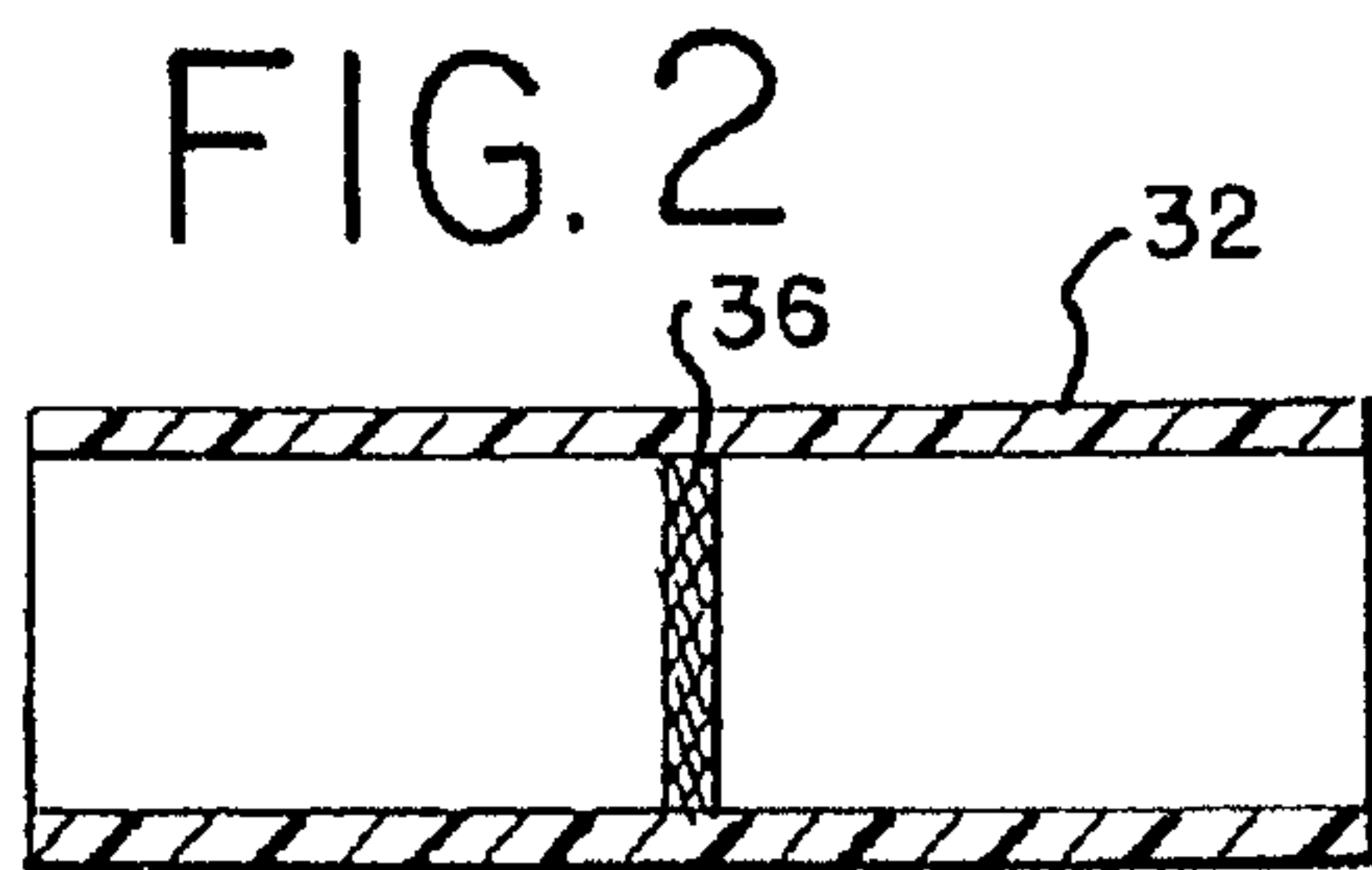
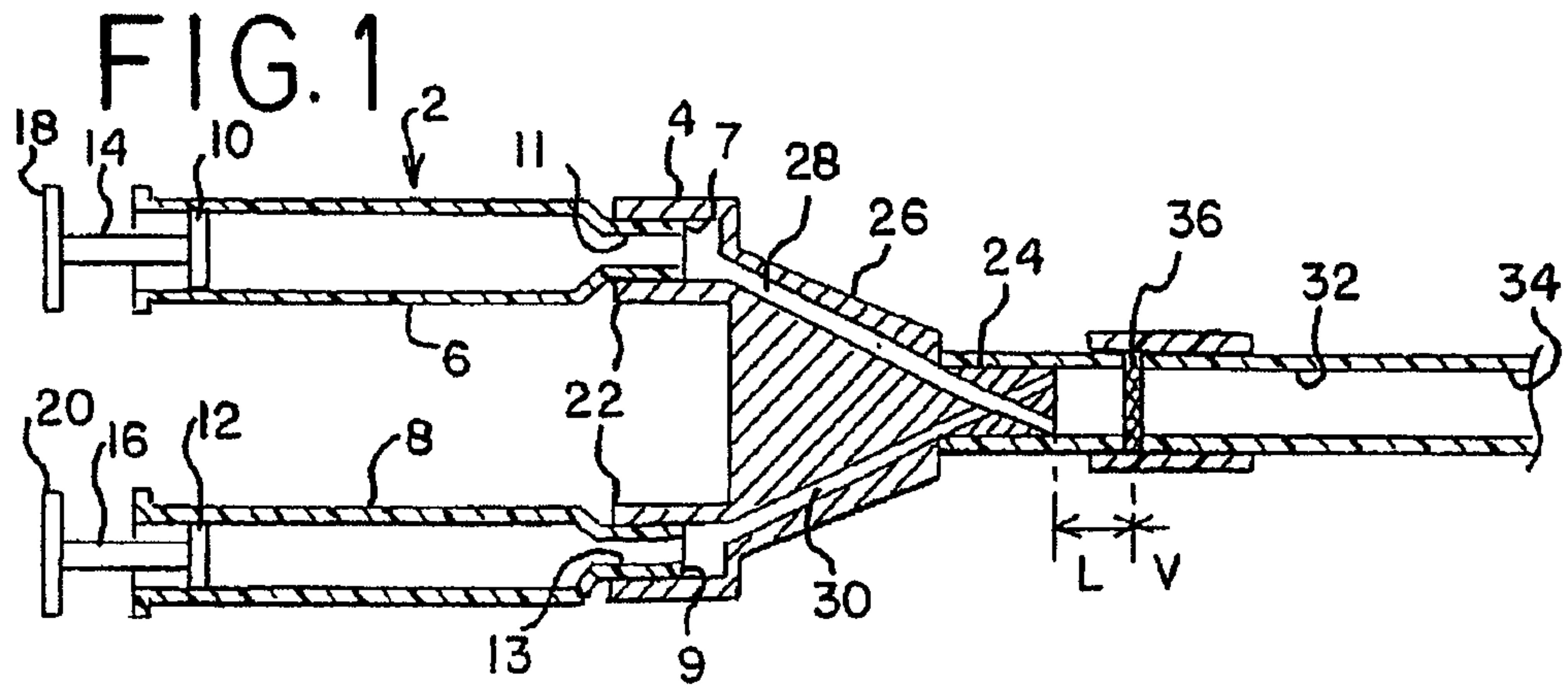


FIG. 5

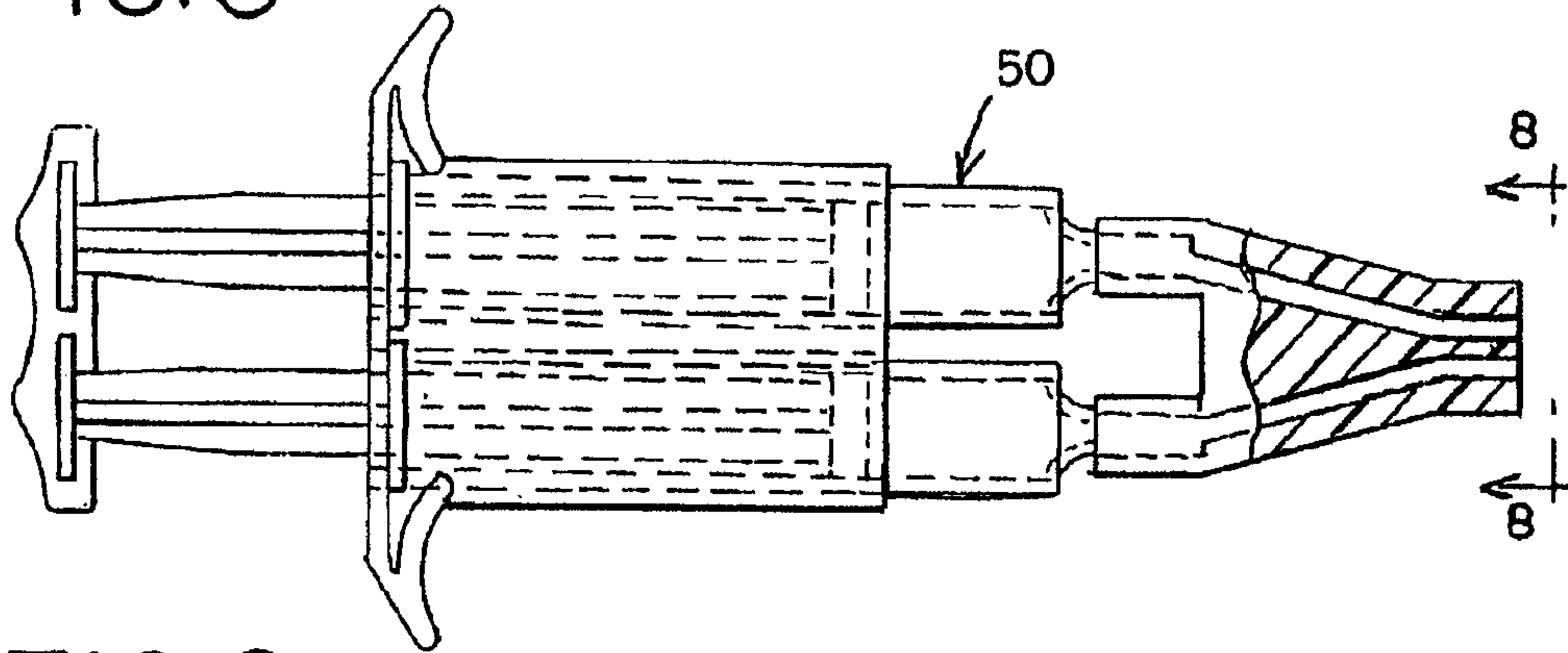


FIG. 6

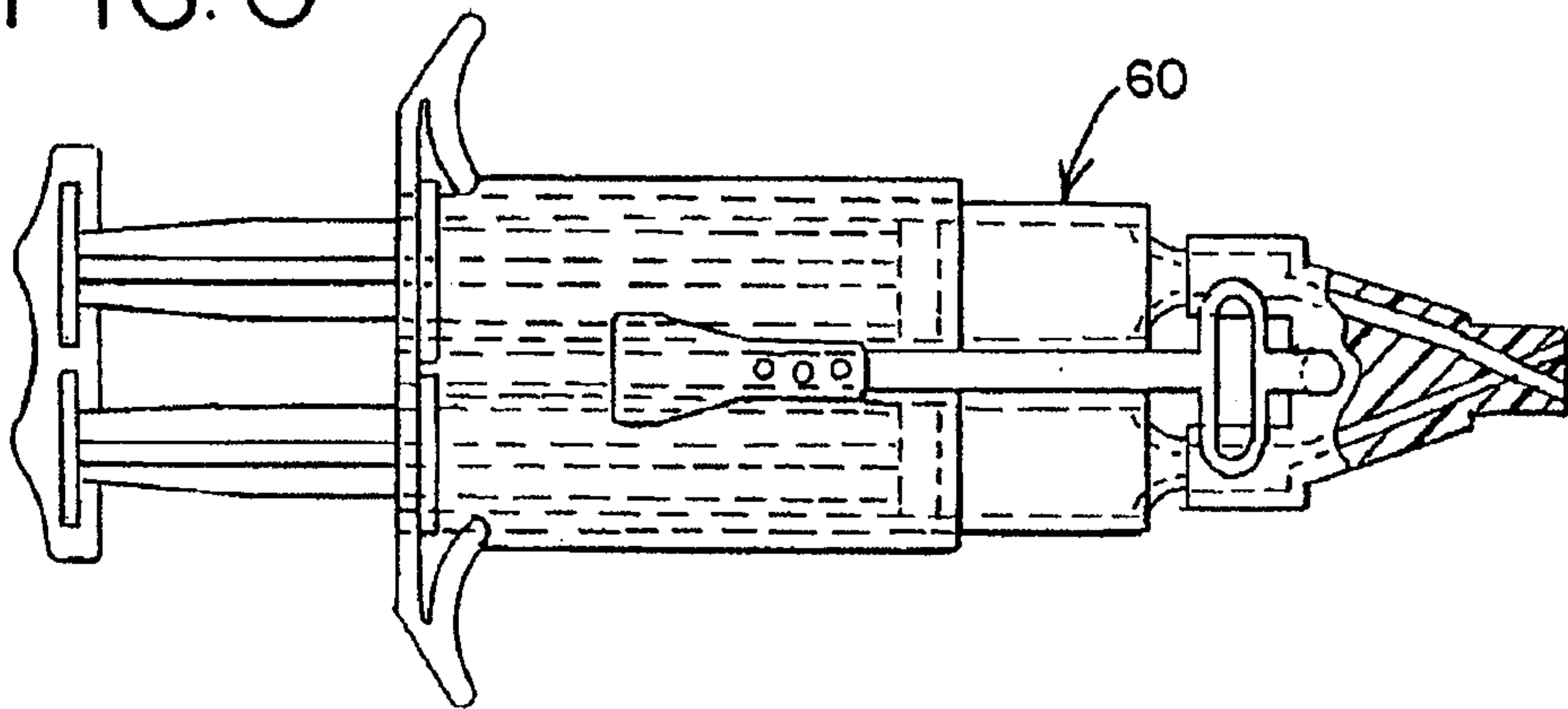


FIG. 7

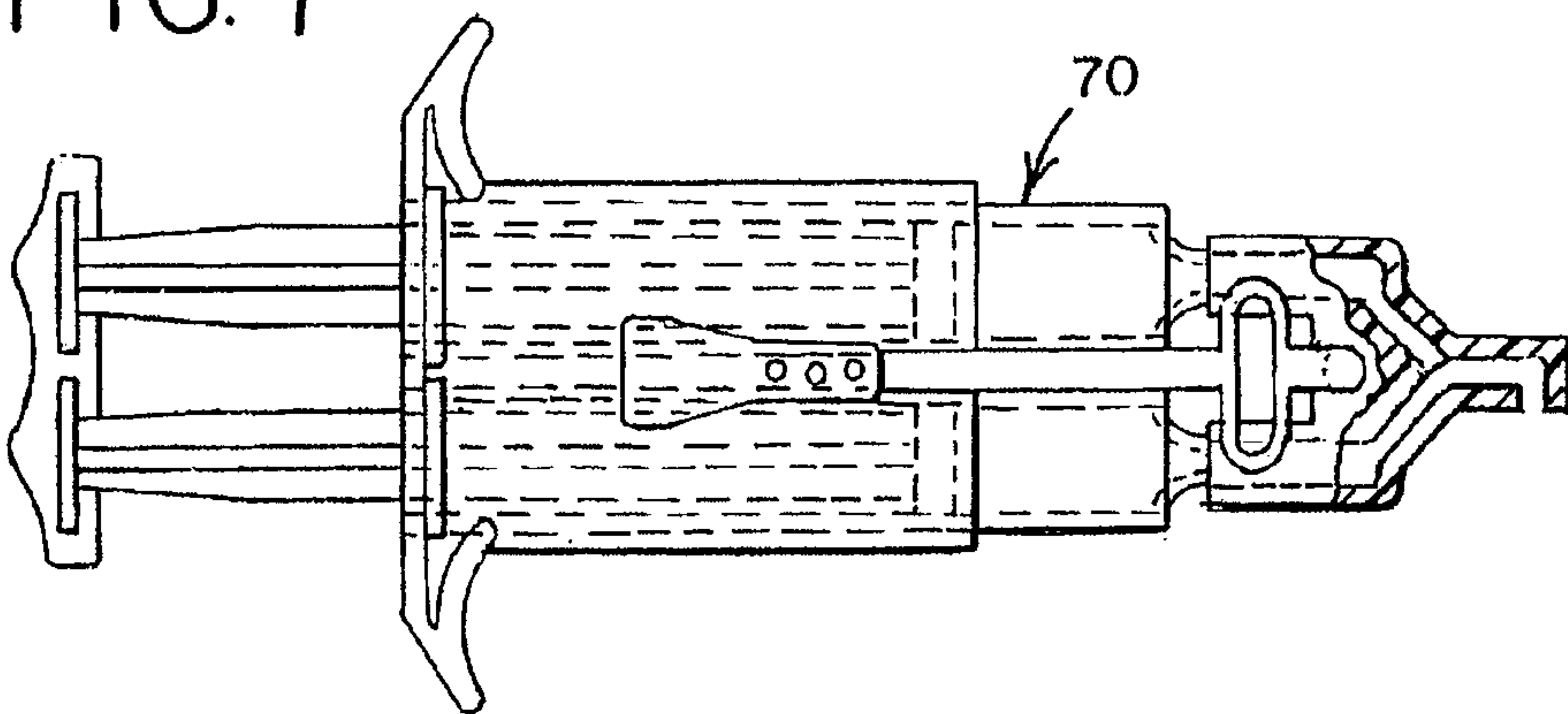
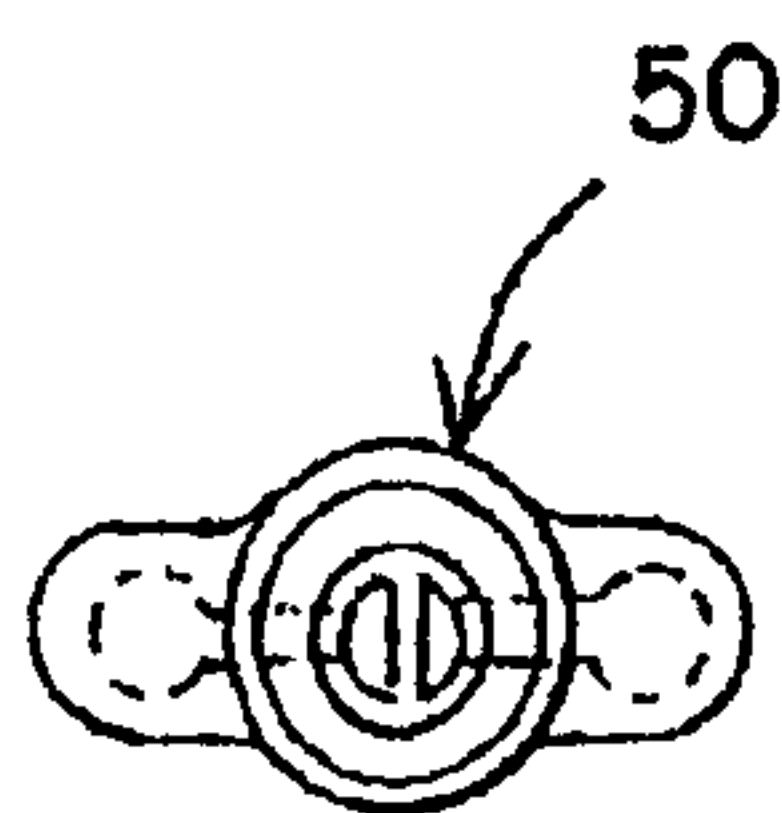


FIG. 8



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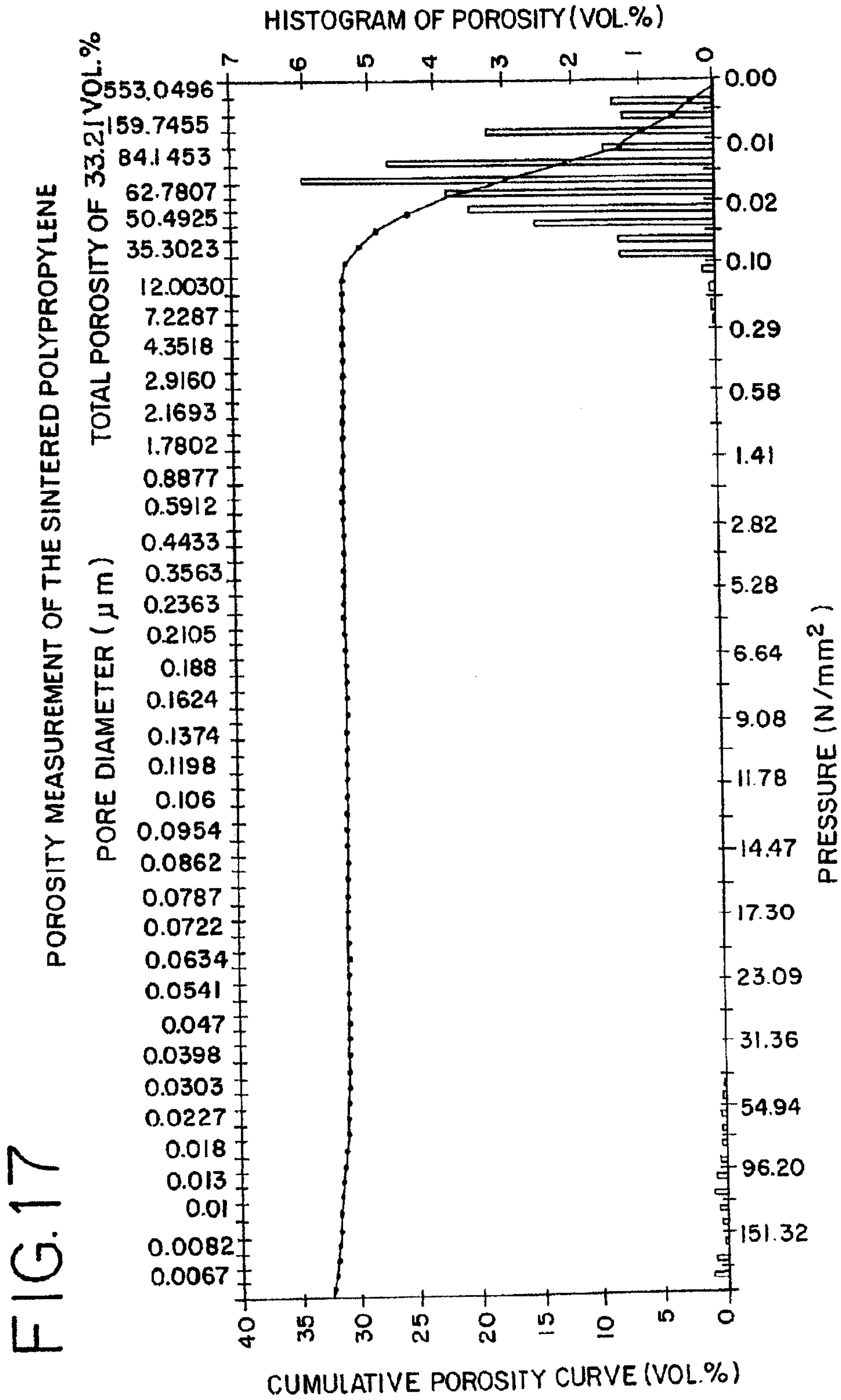


FIG. 17

POROSITY MEASUREMENT OF THE SINTERED POLYPROPYLENE

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FIG. 18

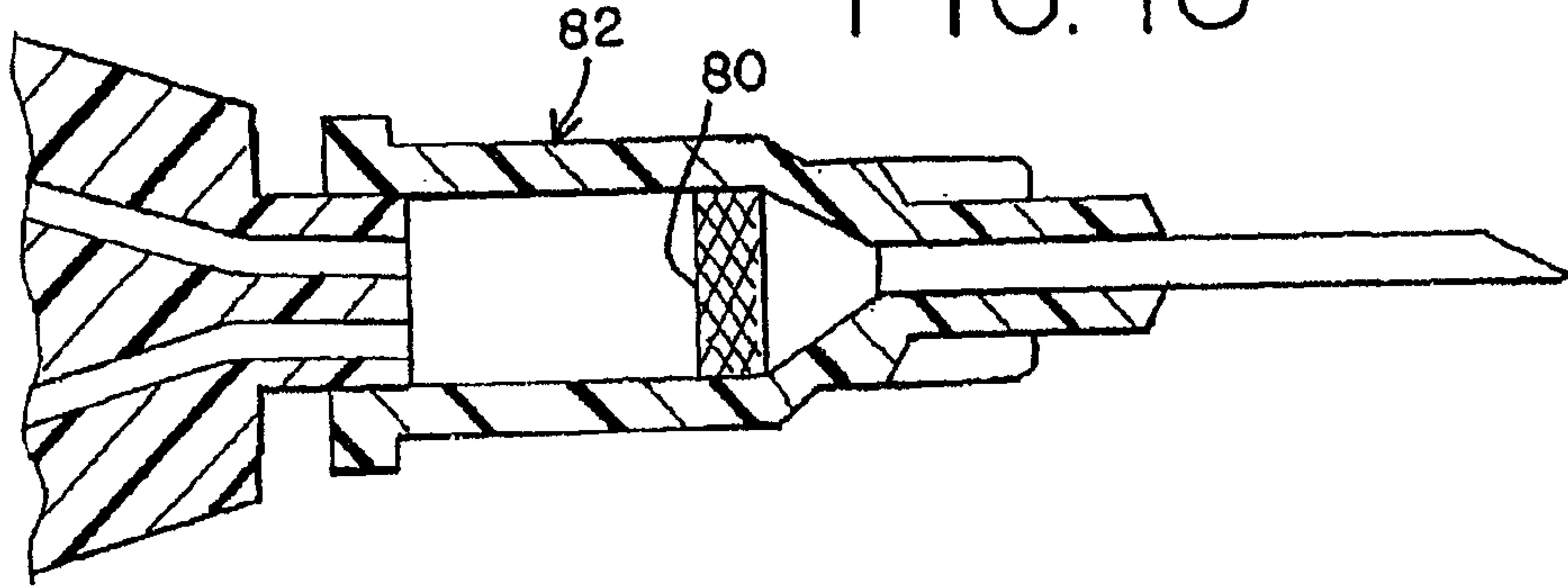


FIG. 19

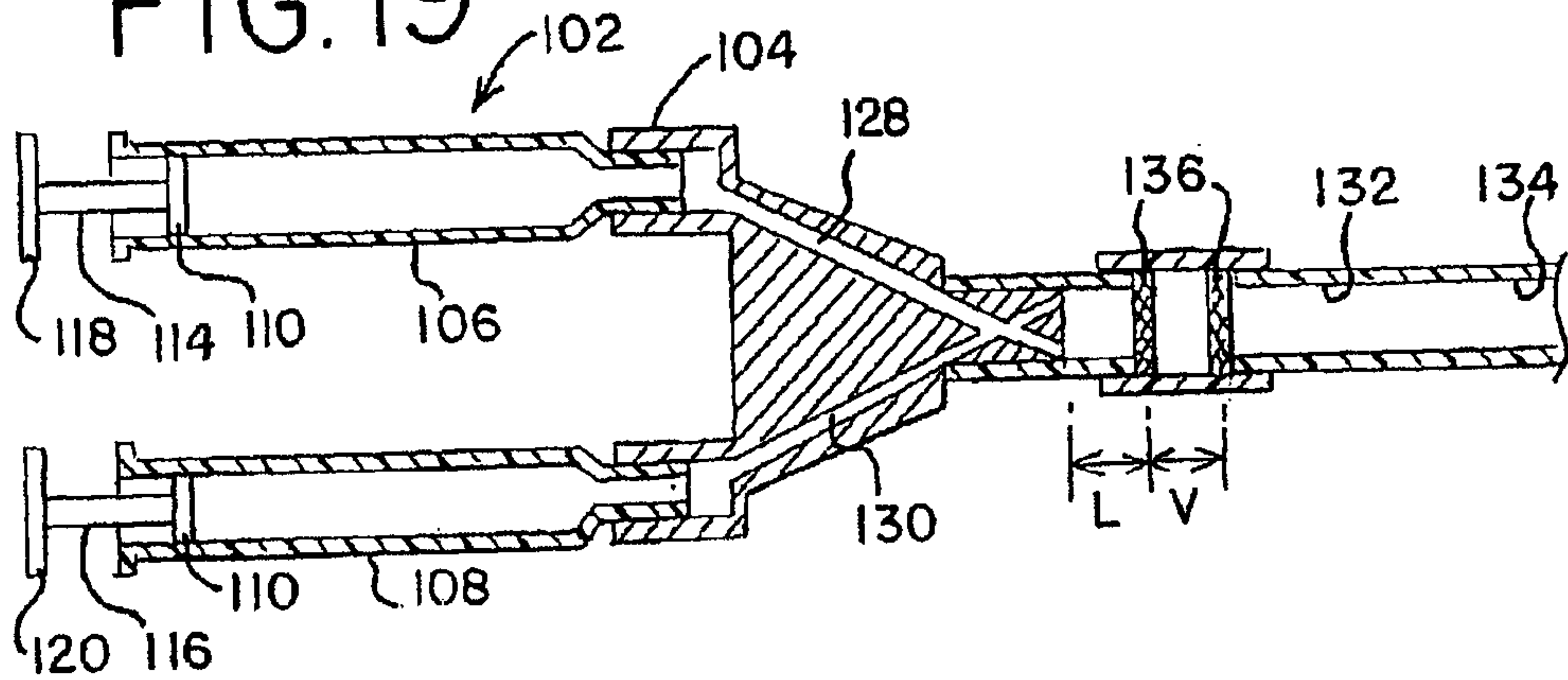


FIG. 20

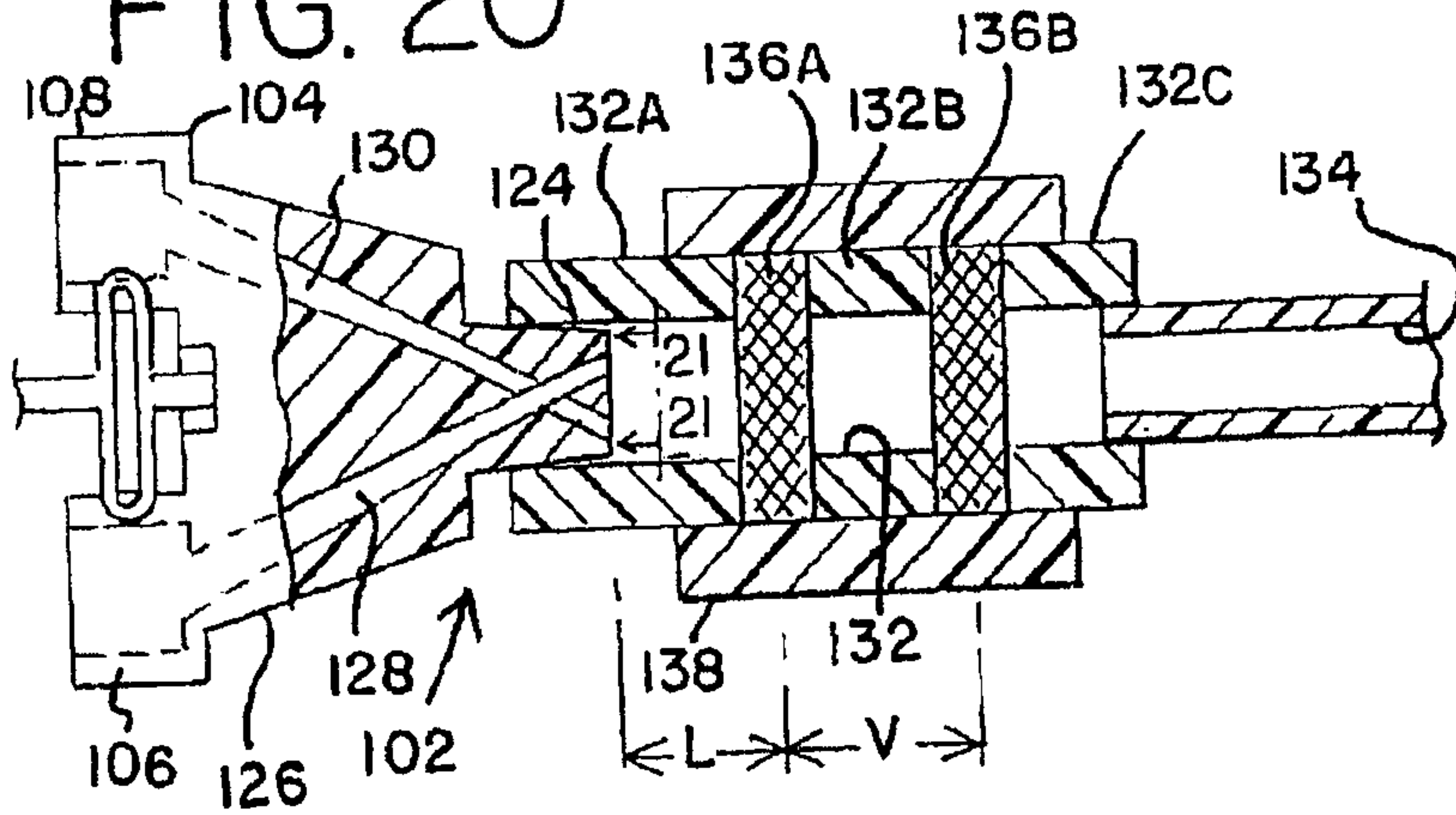
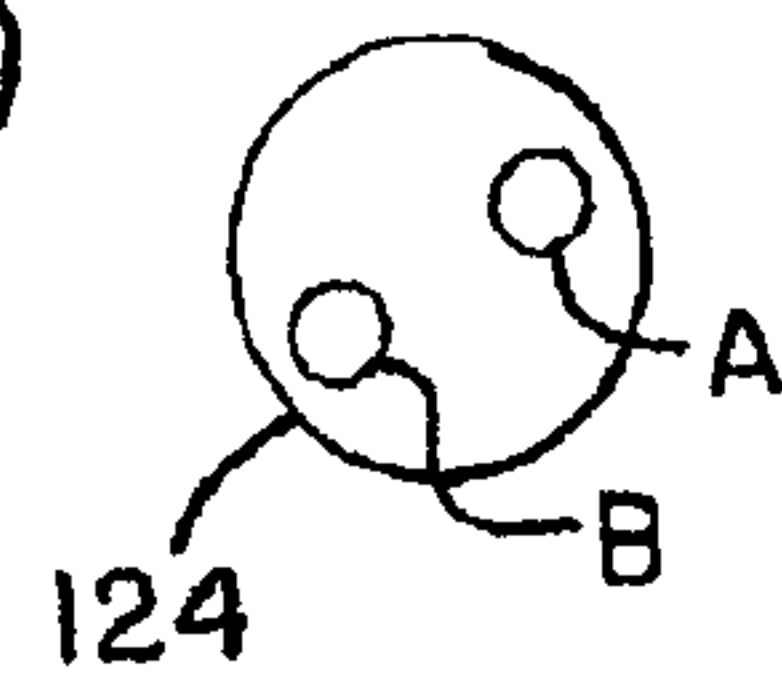


FIG. 21



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FIG. 22

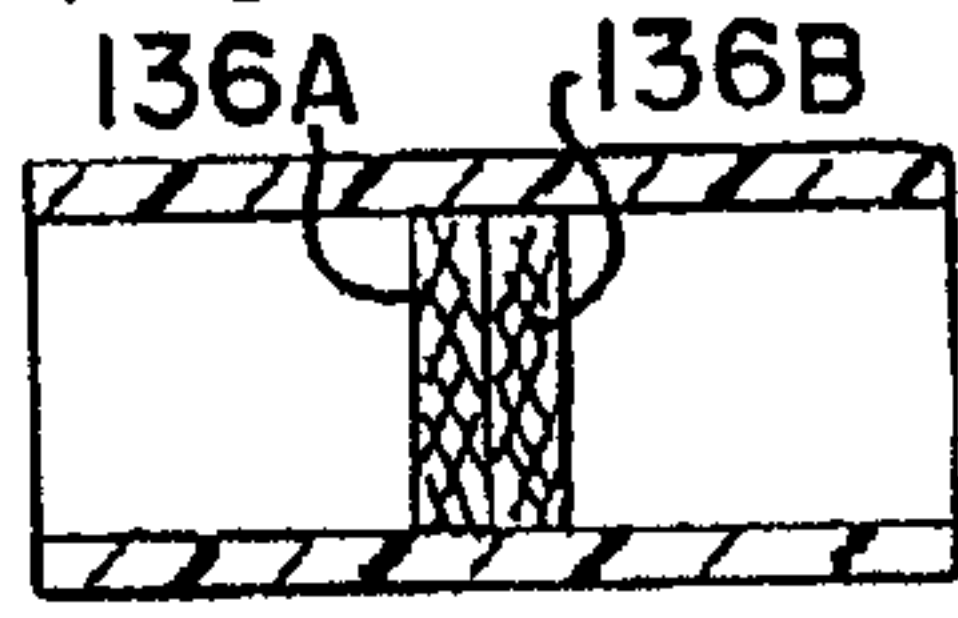


FIG. 25

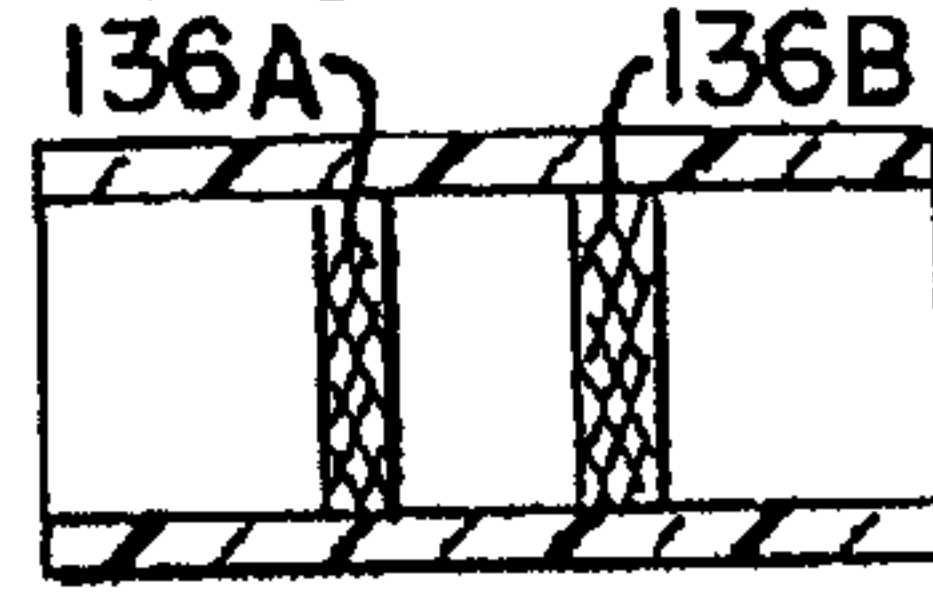


FIG. 23

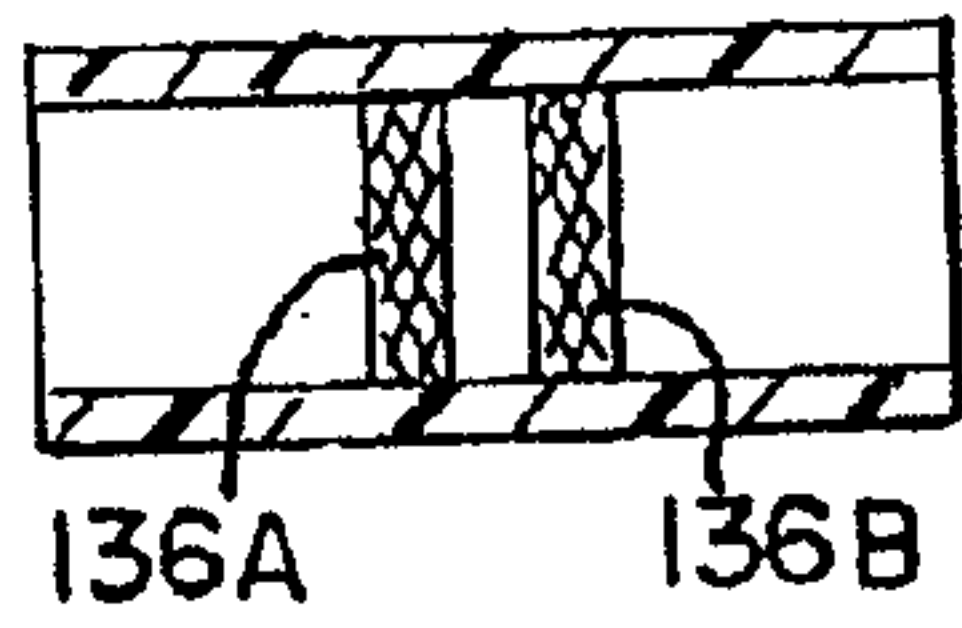


FIG. 26

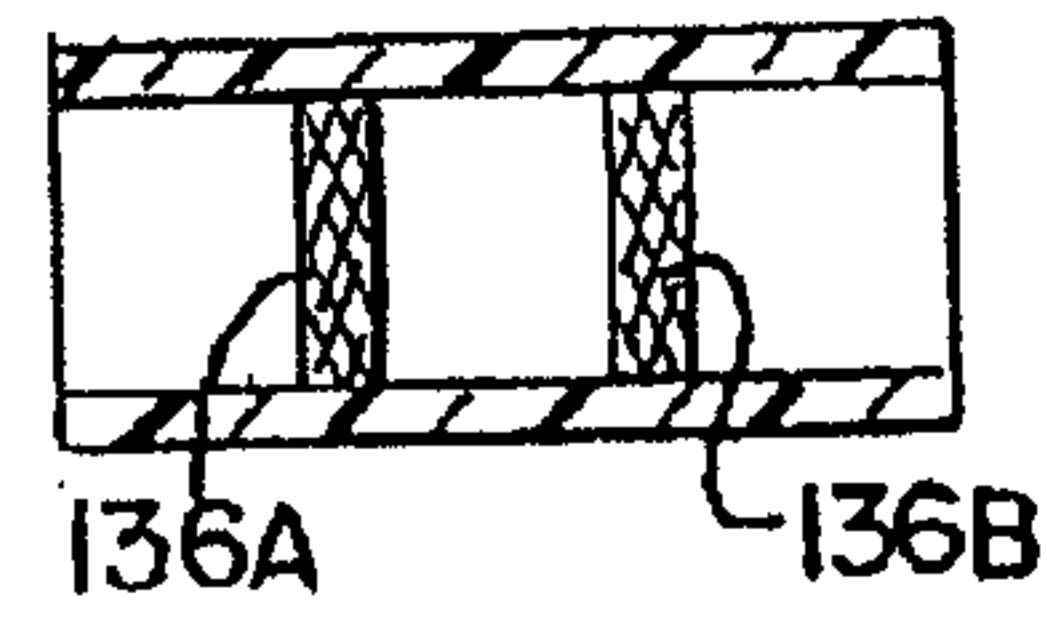


FIG. 24

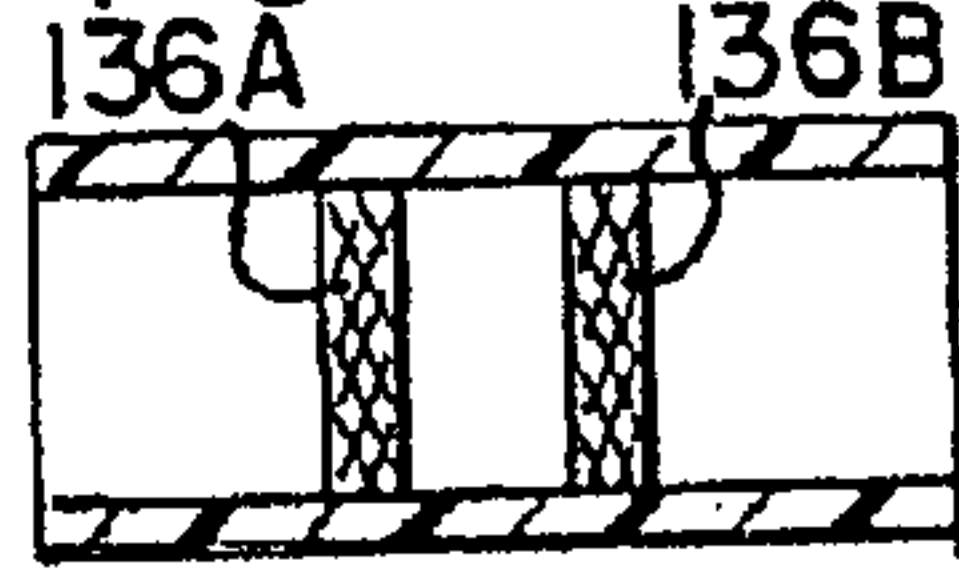


FIG. 27

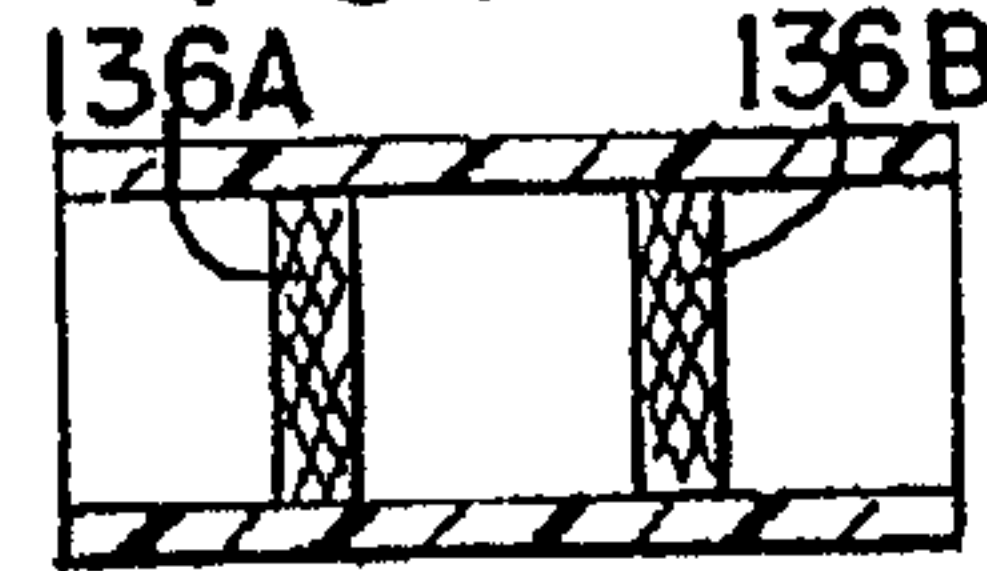


FIG. 30

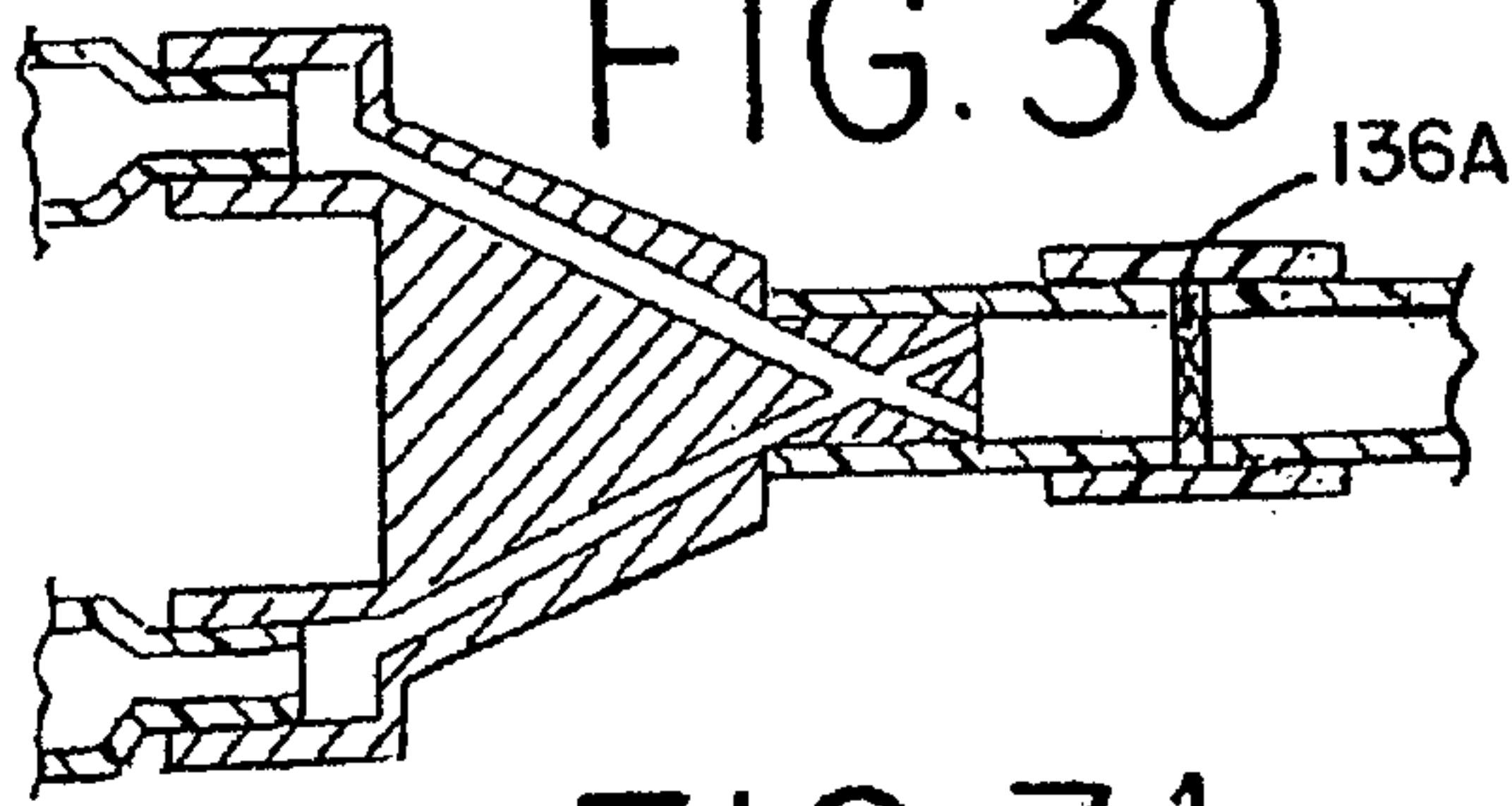


FIG. 28

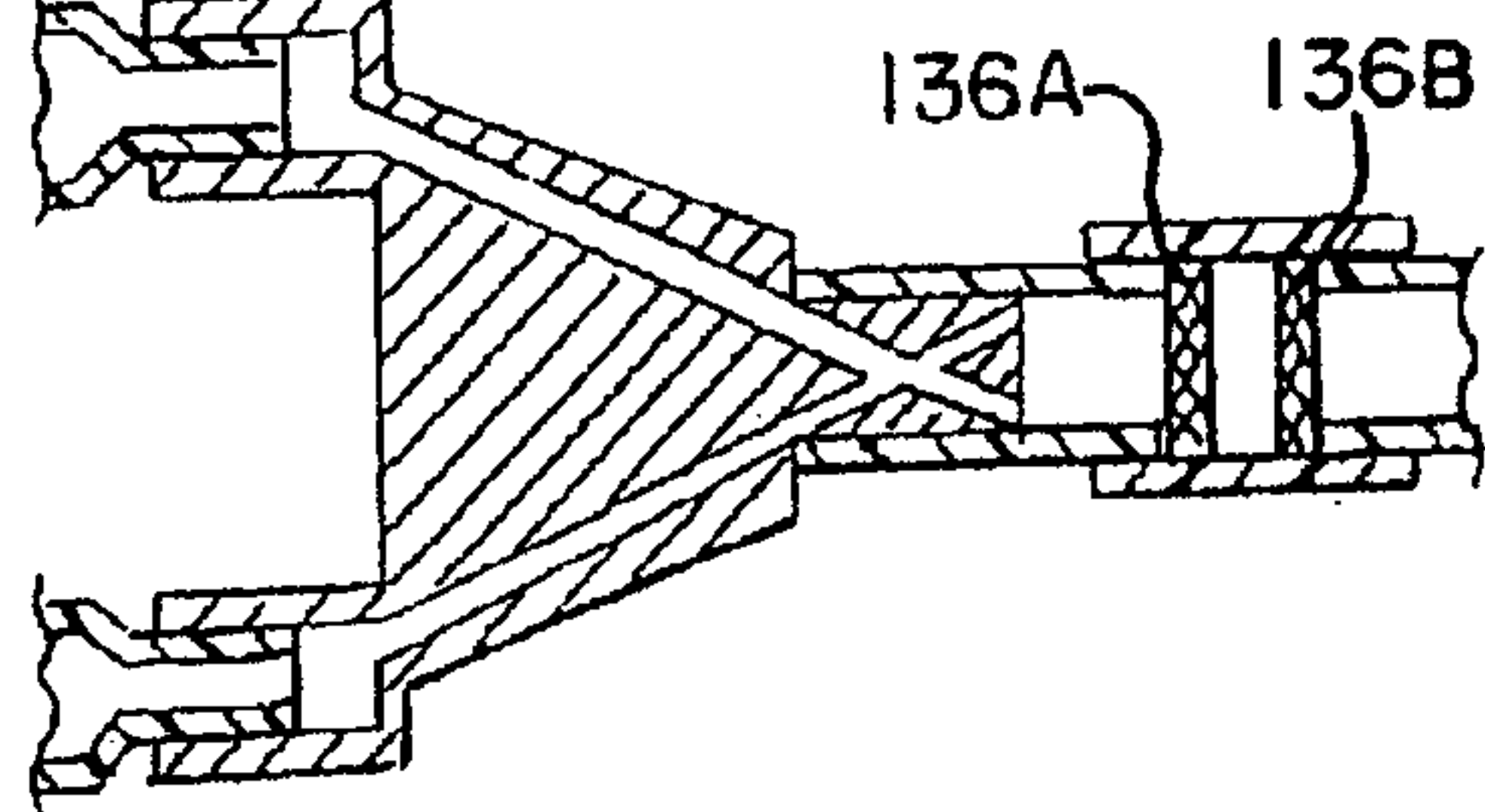


FIG. 31

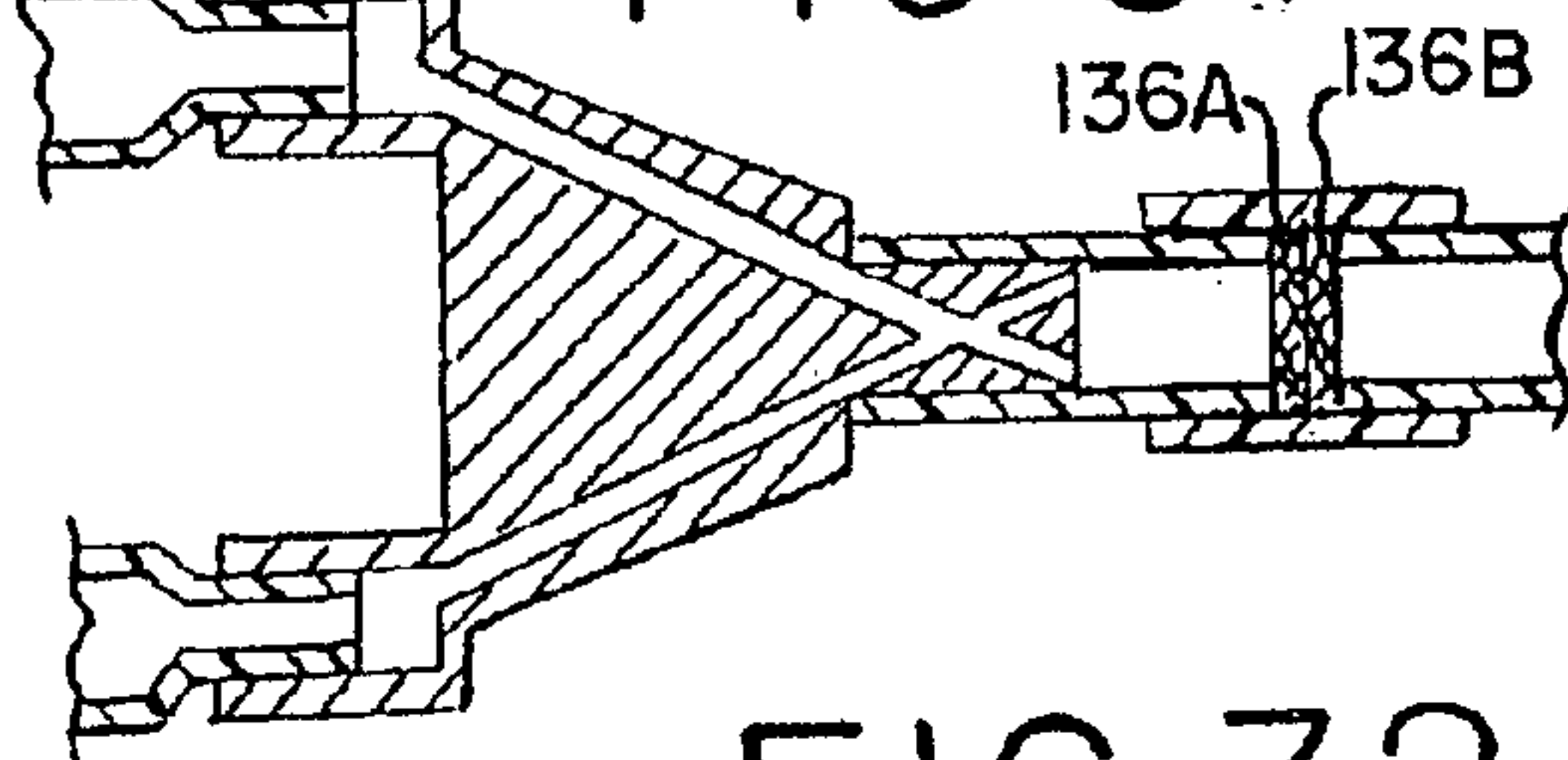


FIG. 29

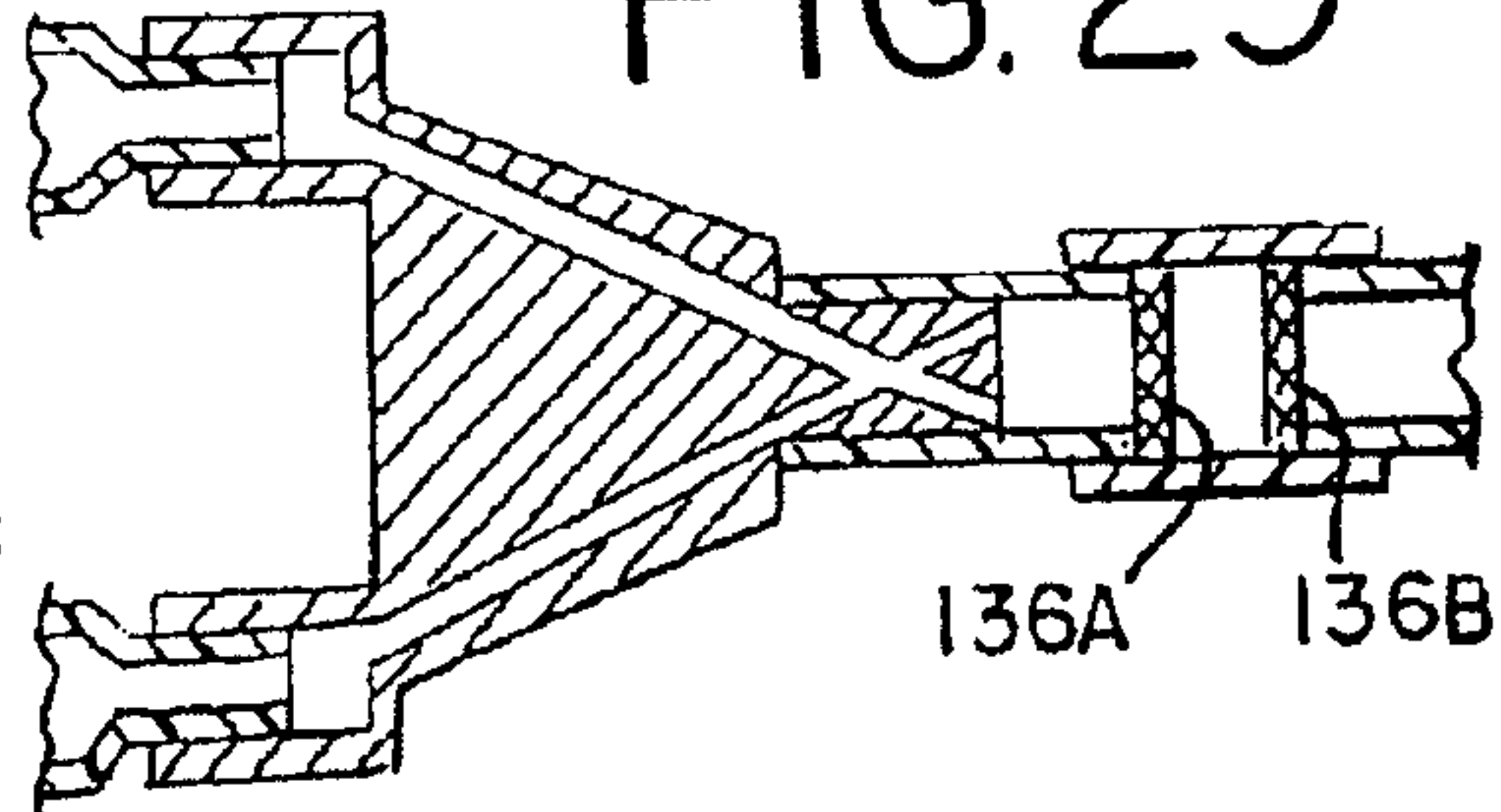
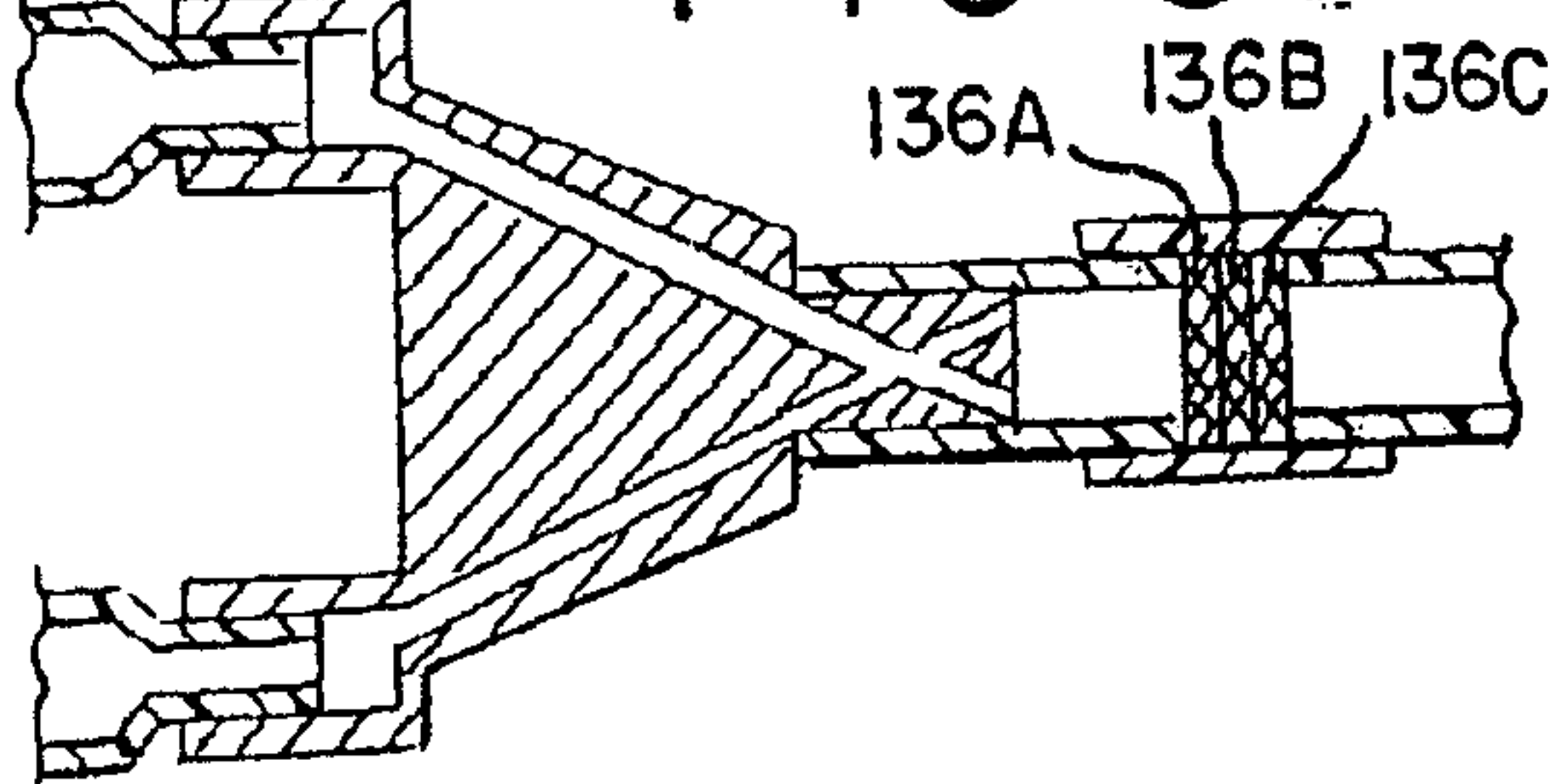
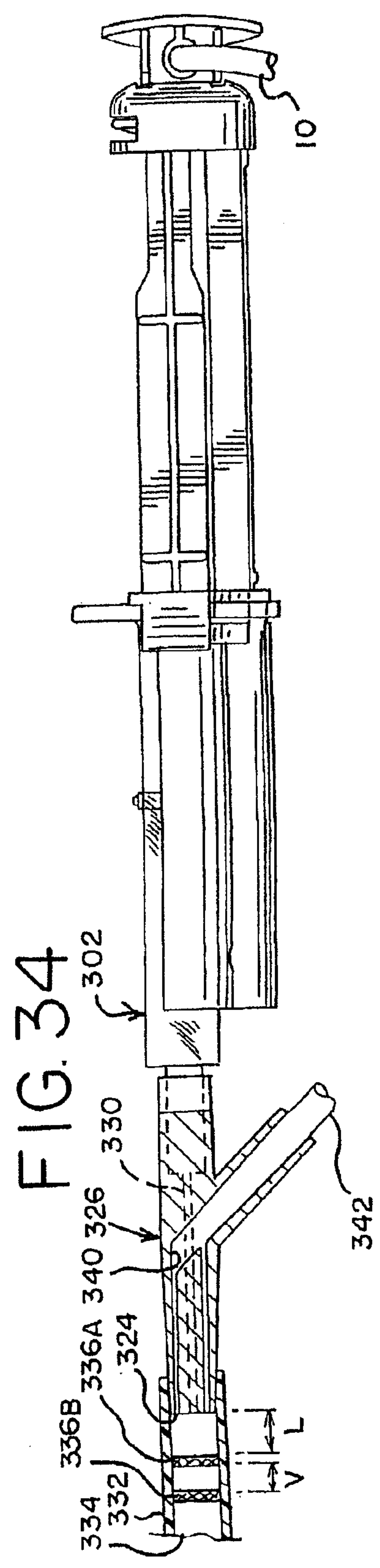
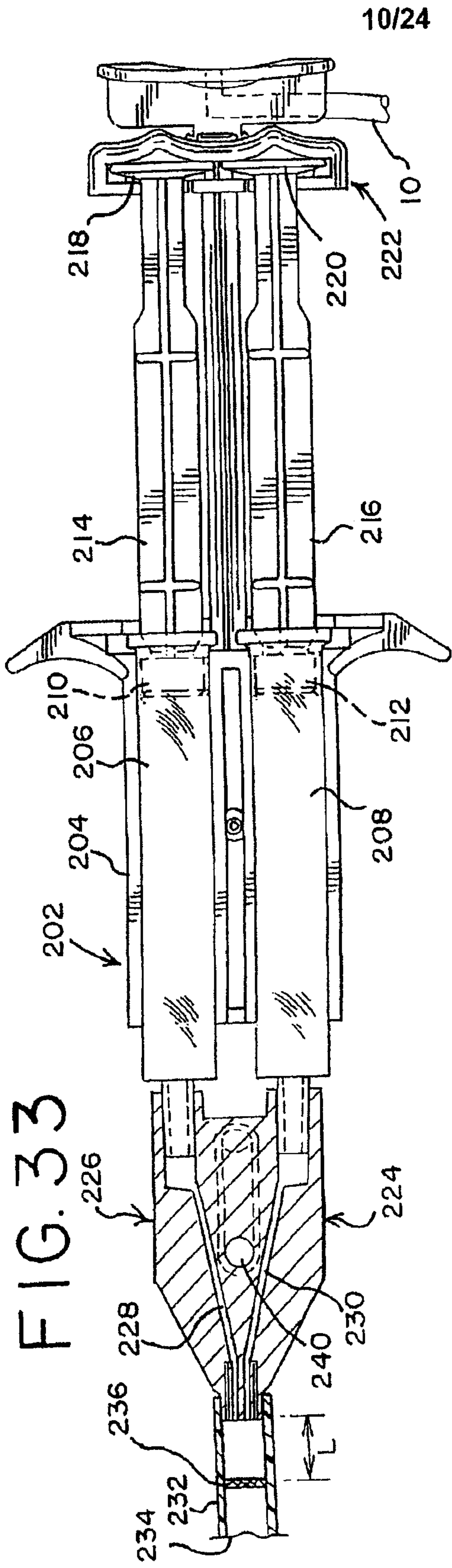


FIG. 32



136A 136B



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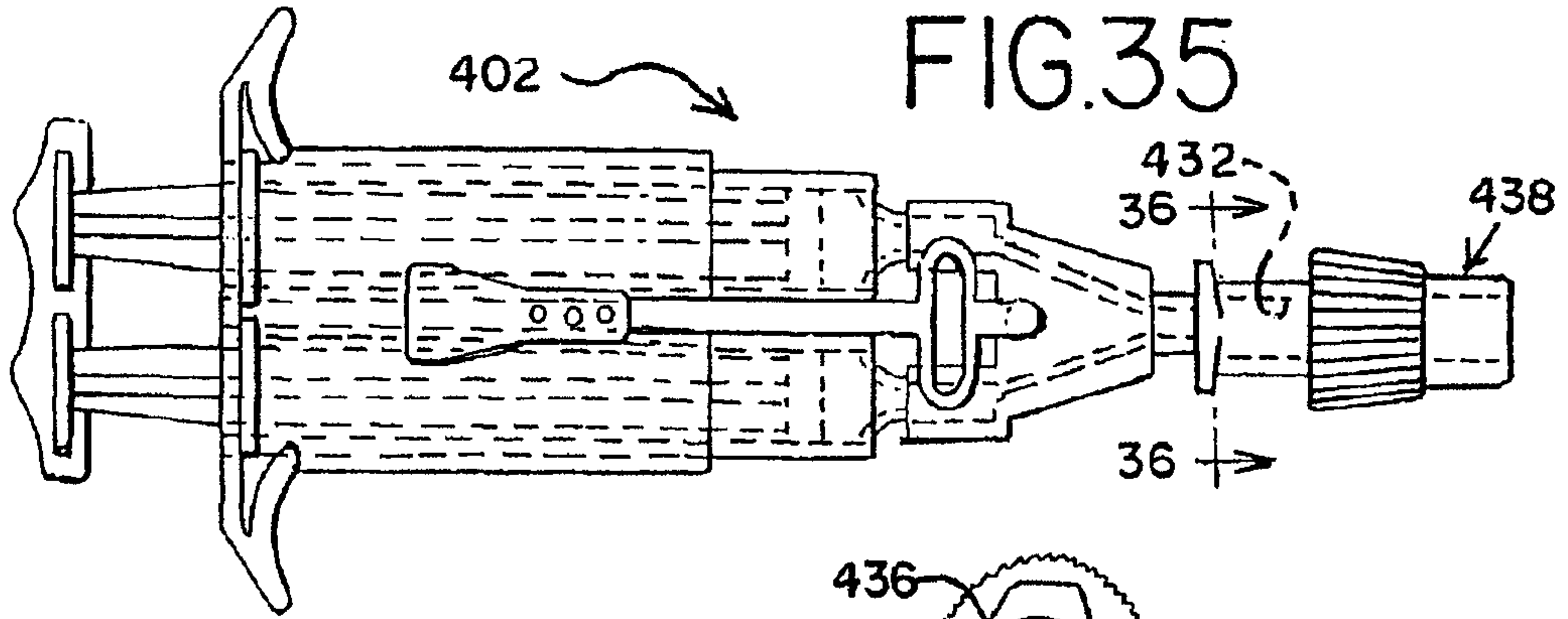


FIG. 36

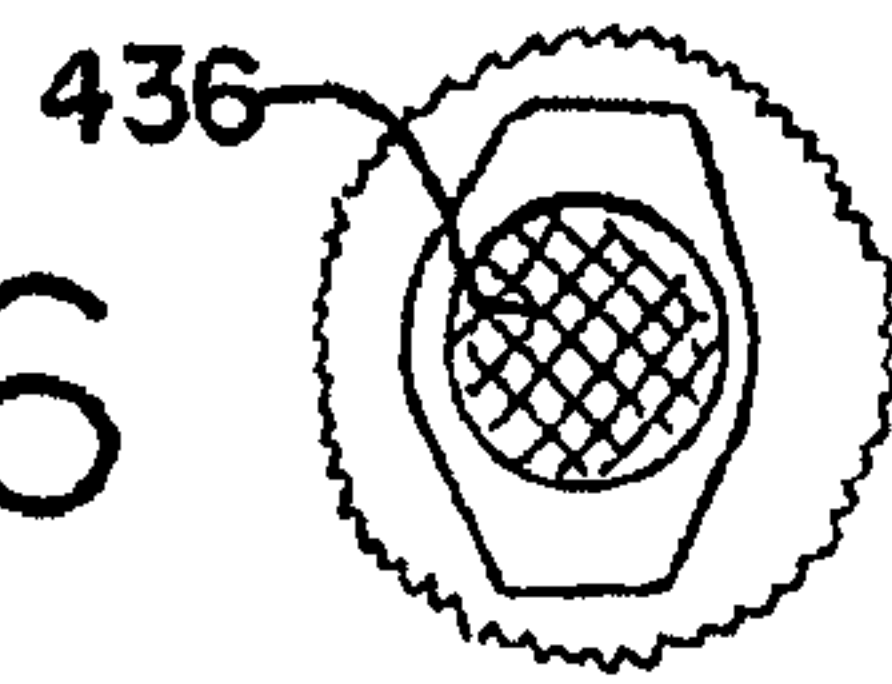


FIG. 37

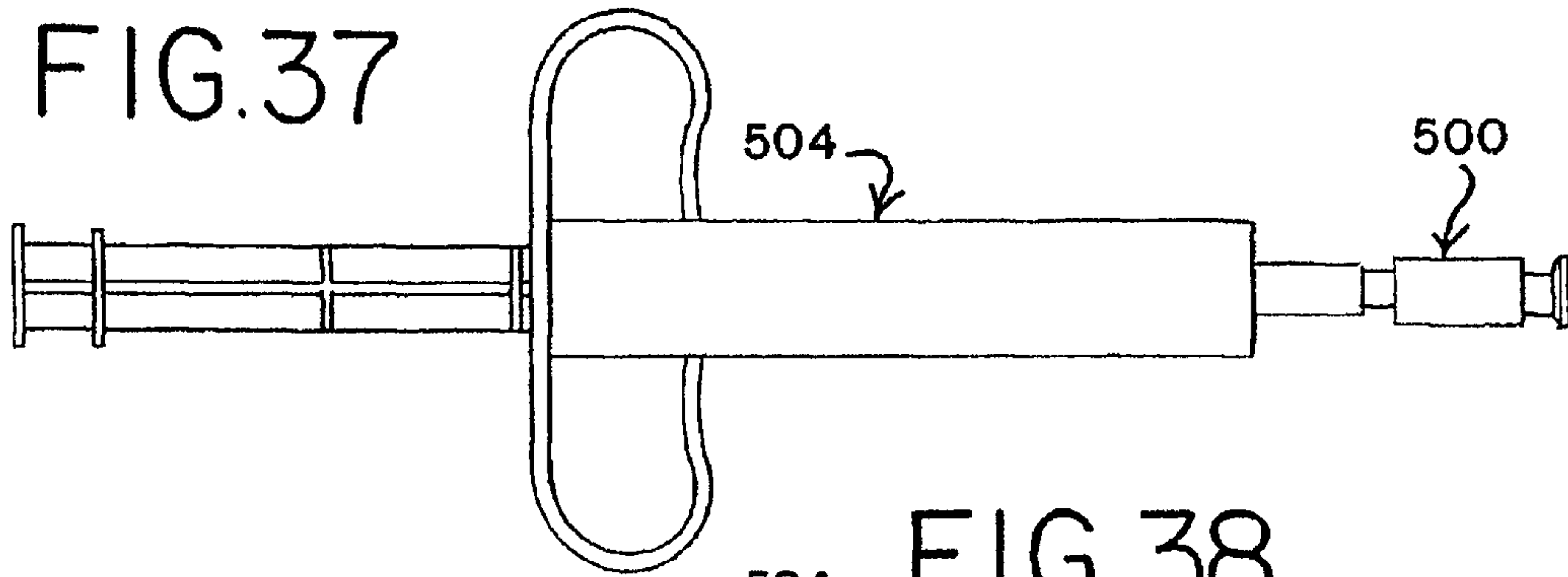


FIG. 38

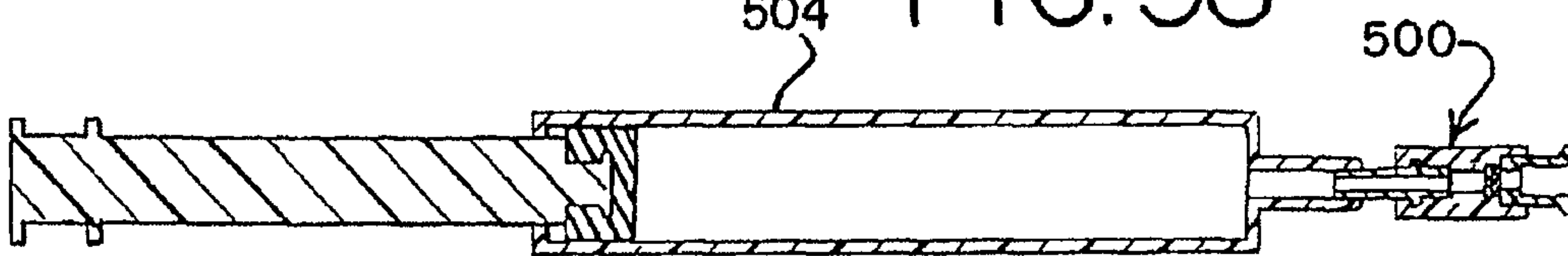


FIG. 39

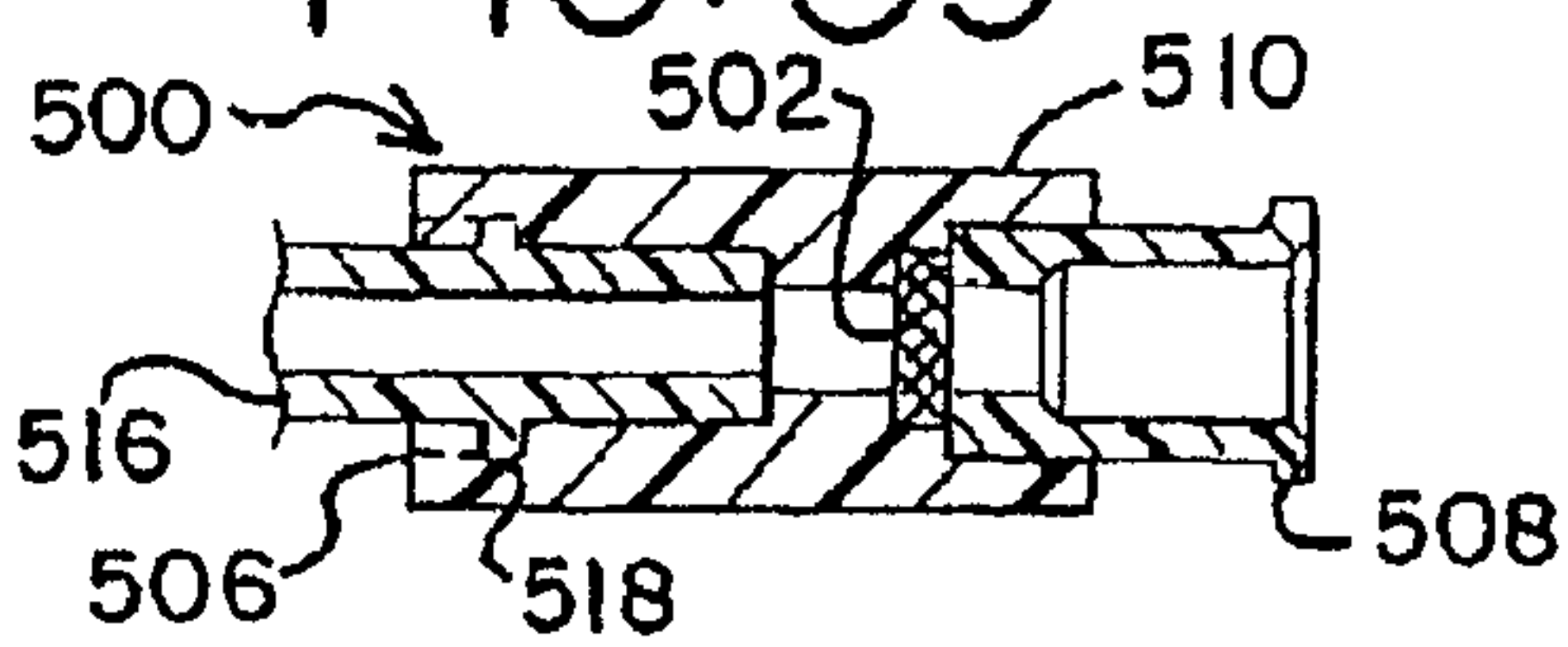


FIG. 41

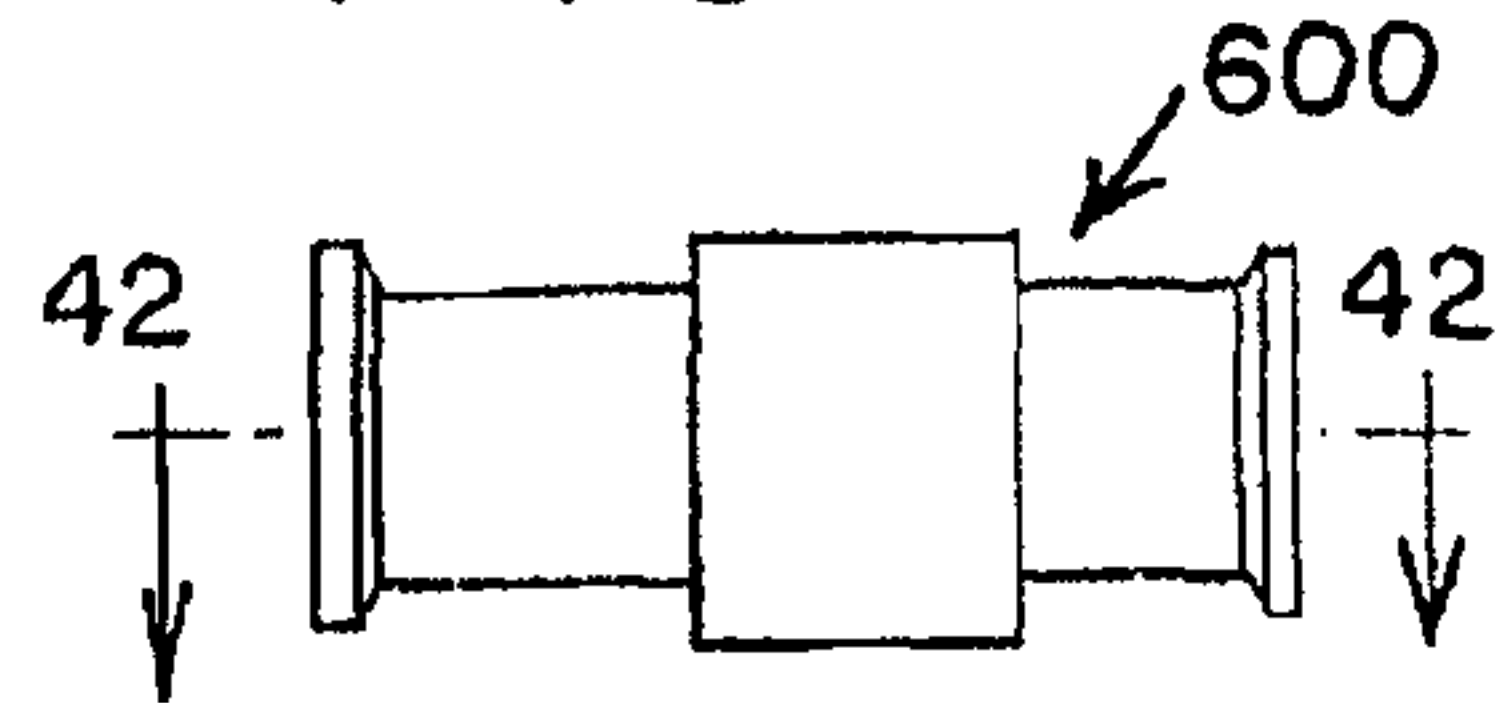


FIG. 40

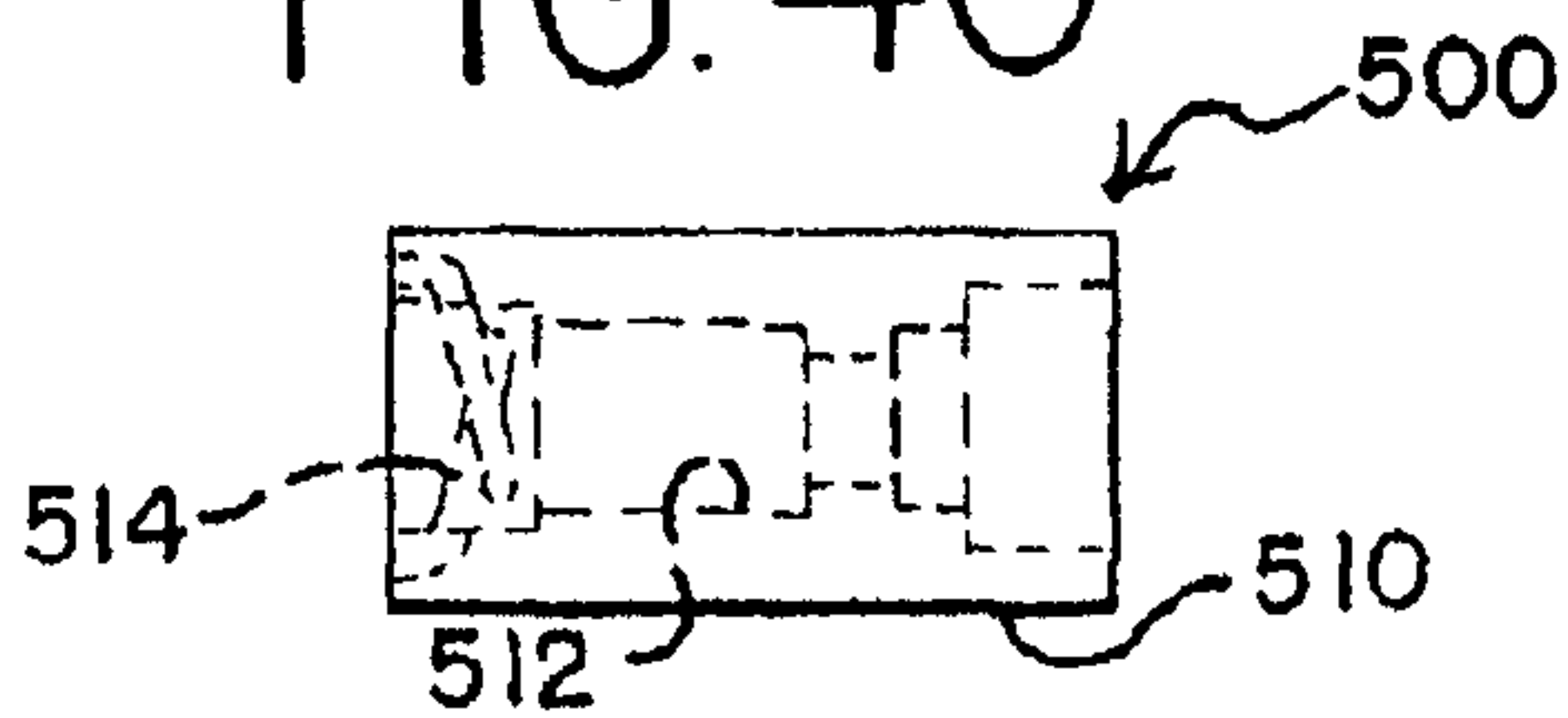
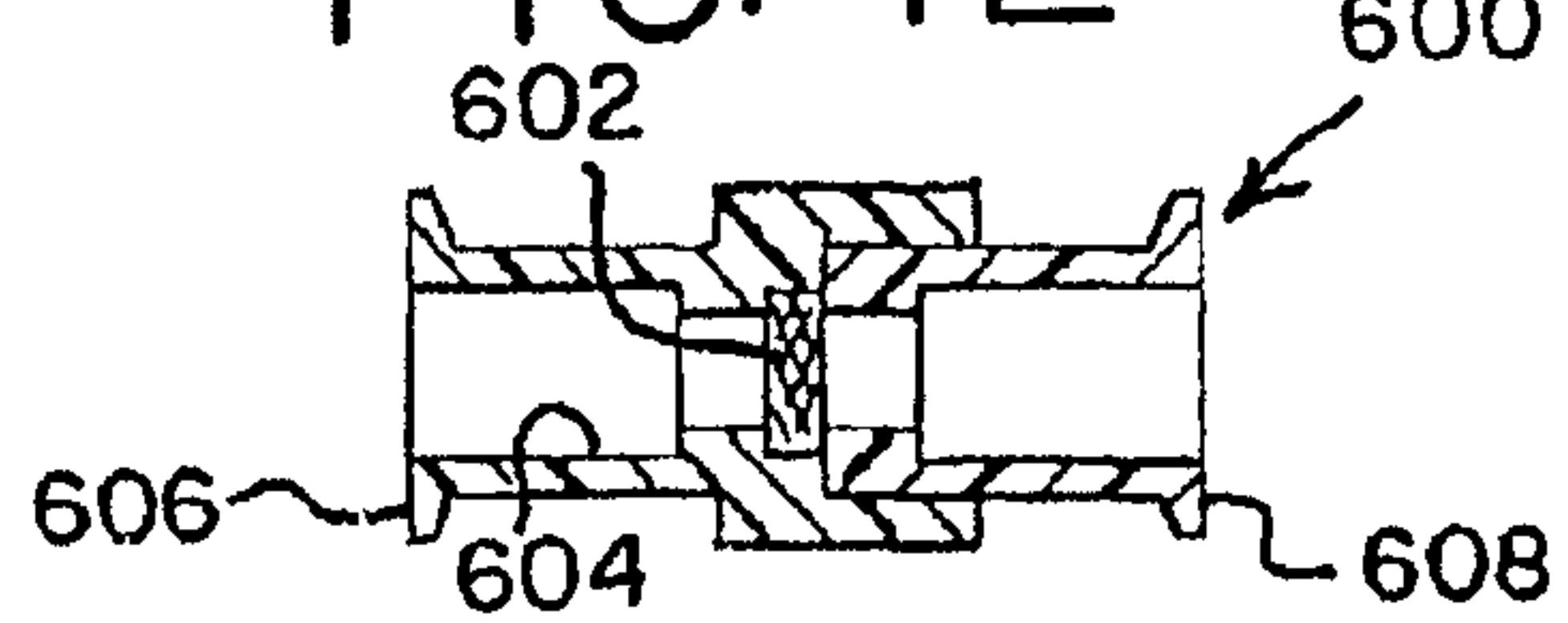


FIG. 42



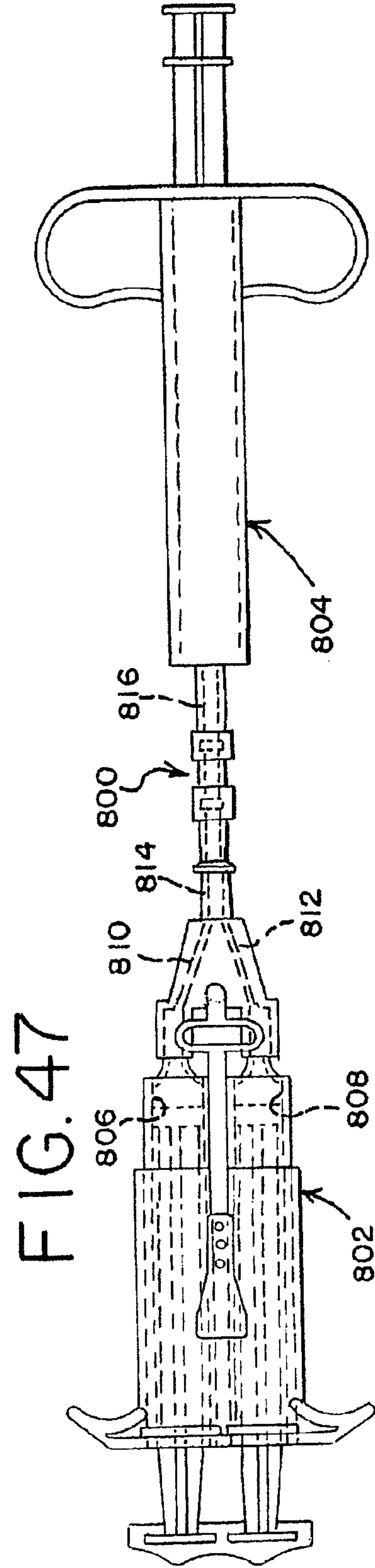
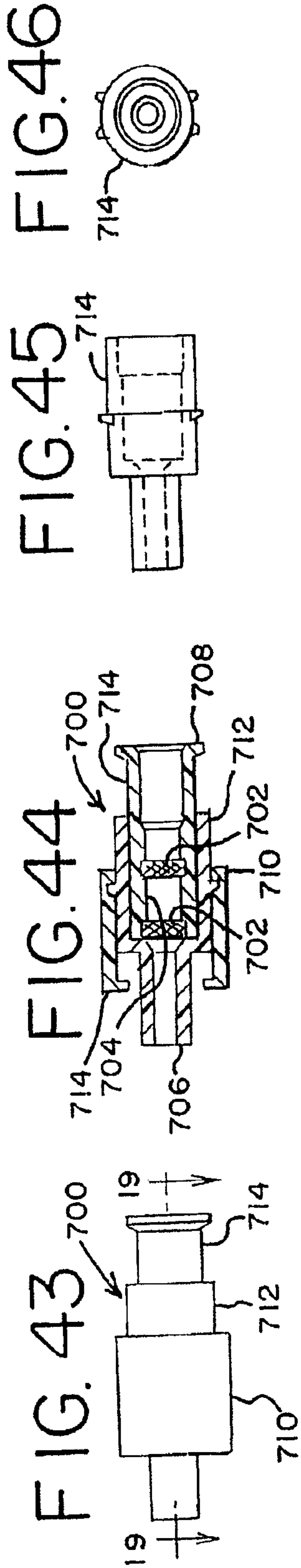


FIG. 48

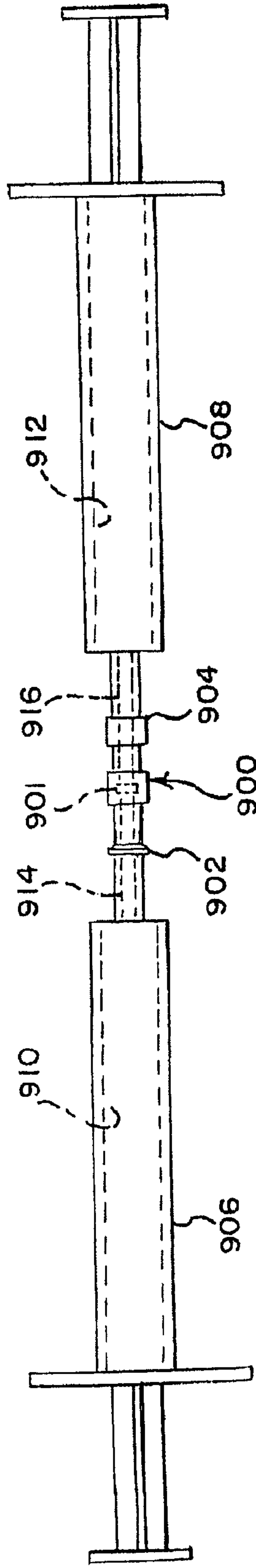
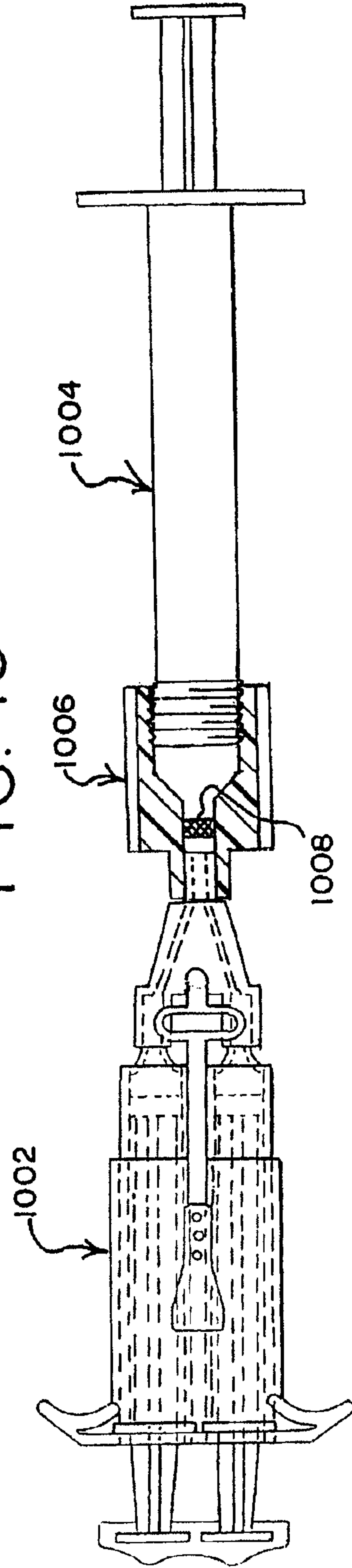


FIG. 49



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FIG. 50A

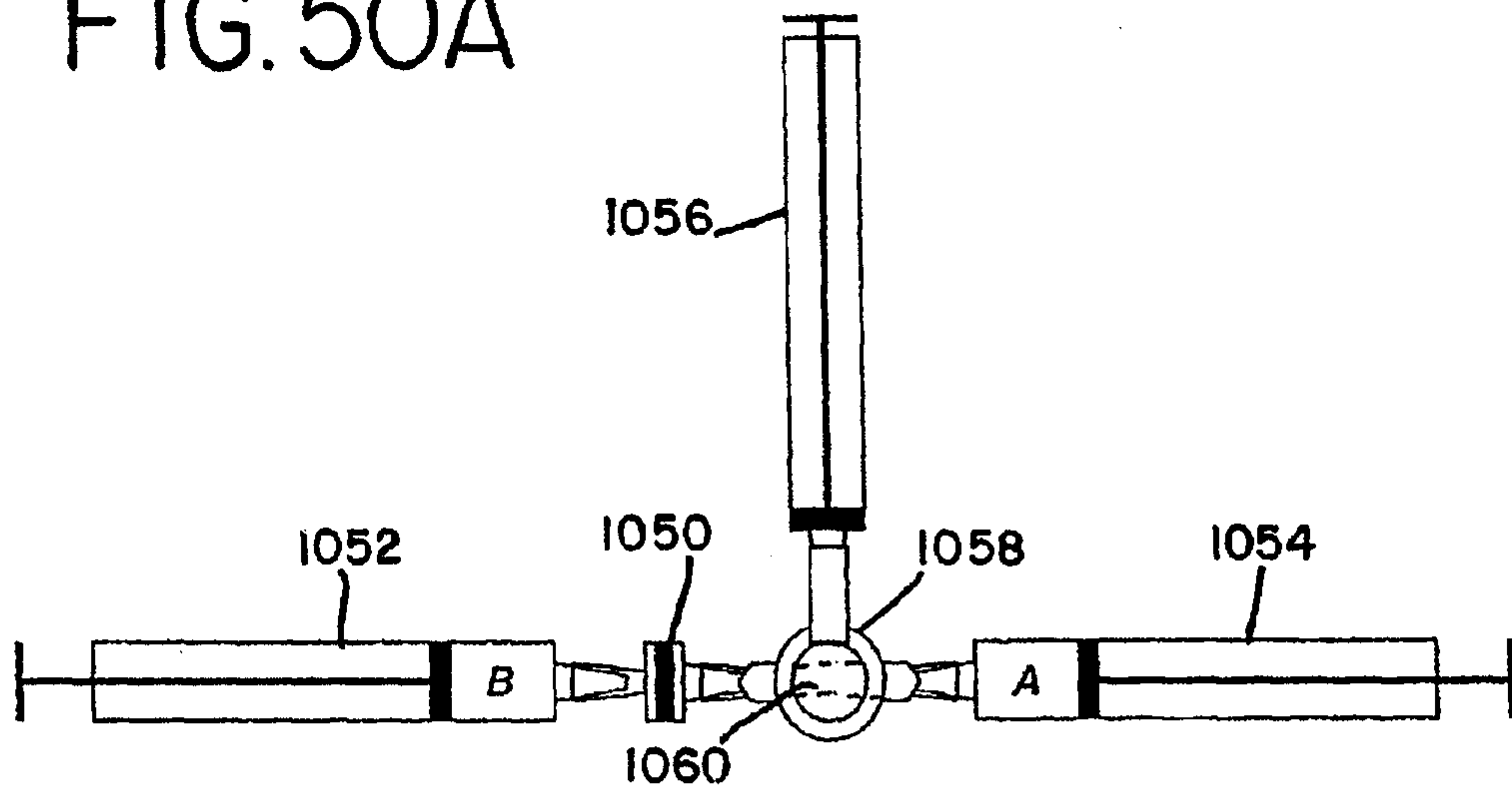


FIG. 50B

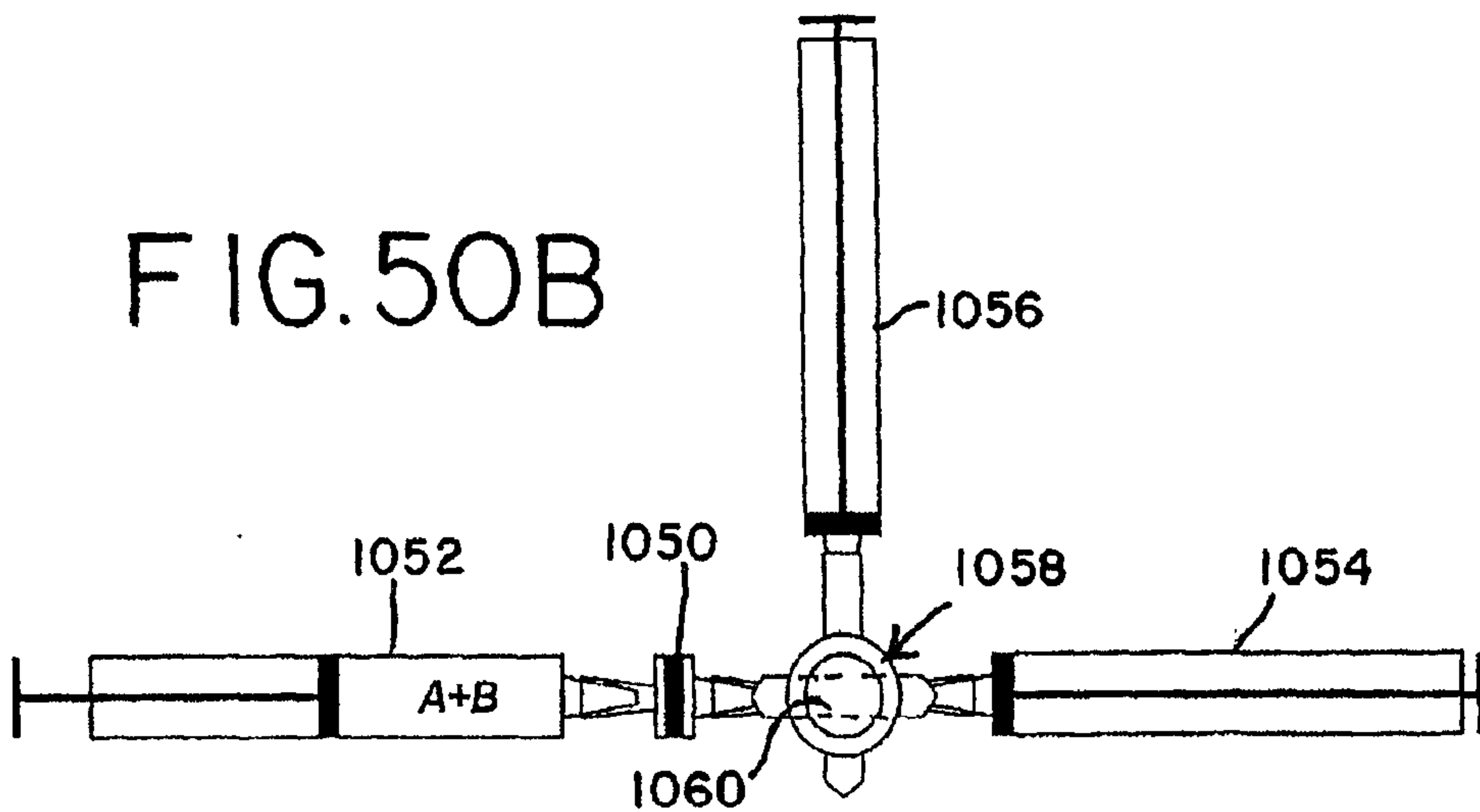


FIG. 50C

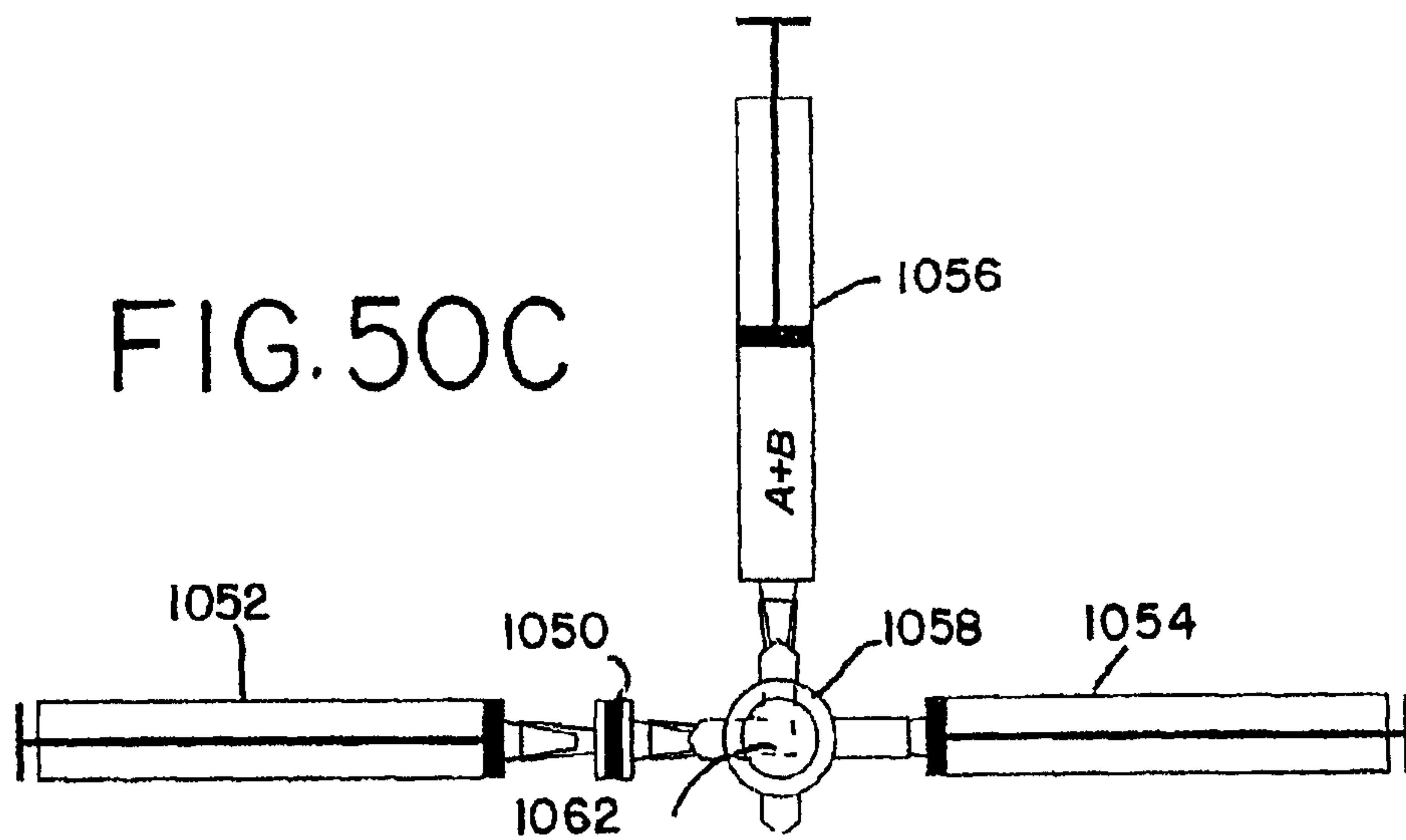


FIG. 51

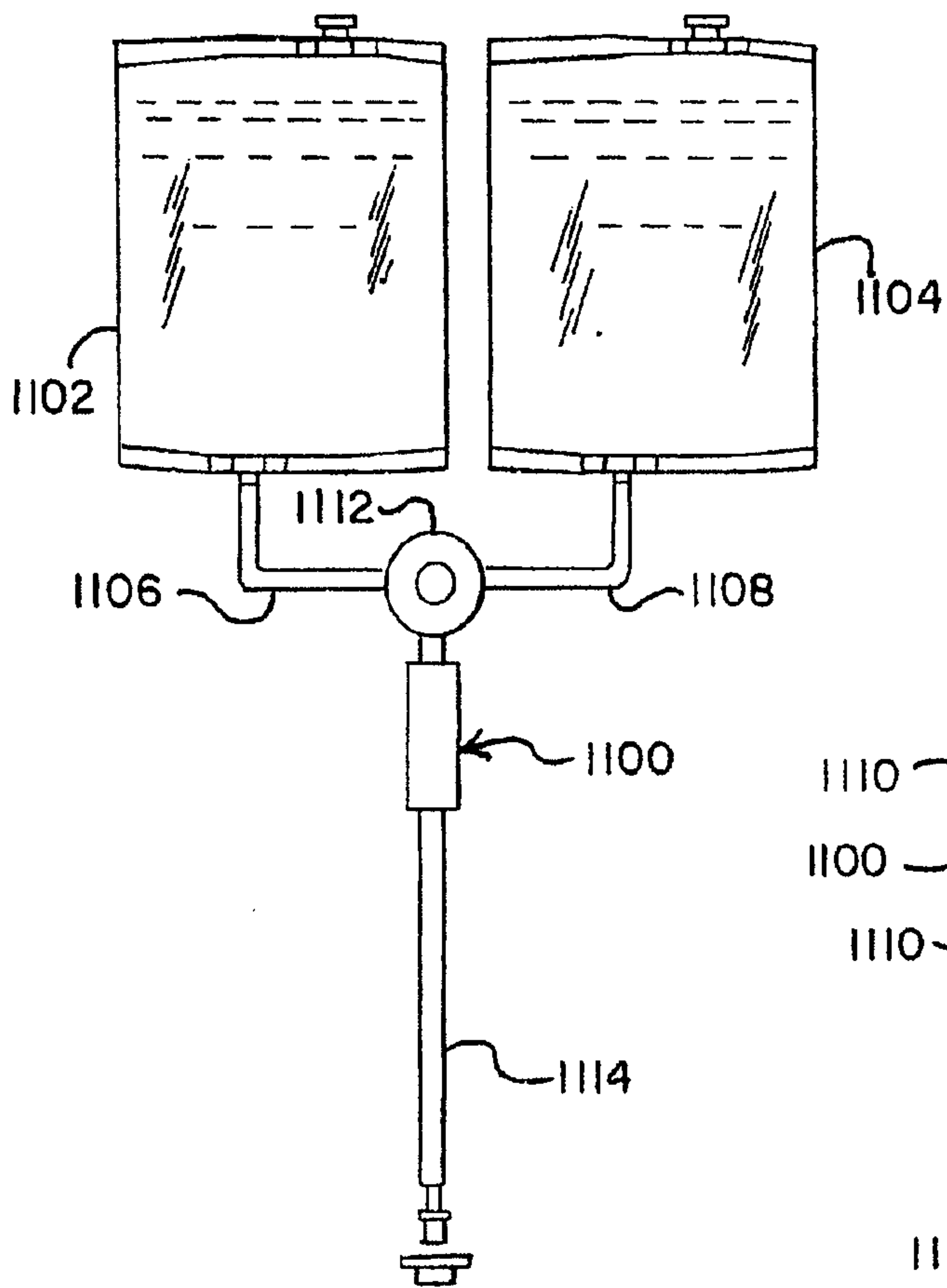


FIG. 52

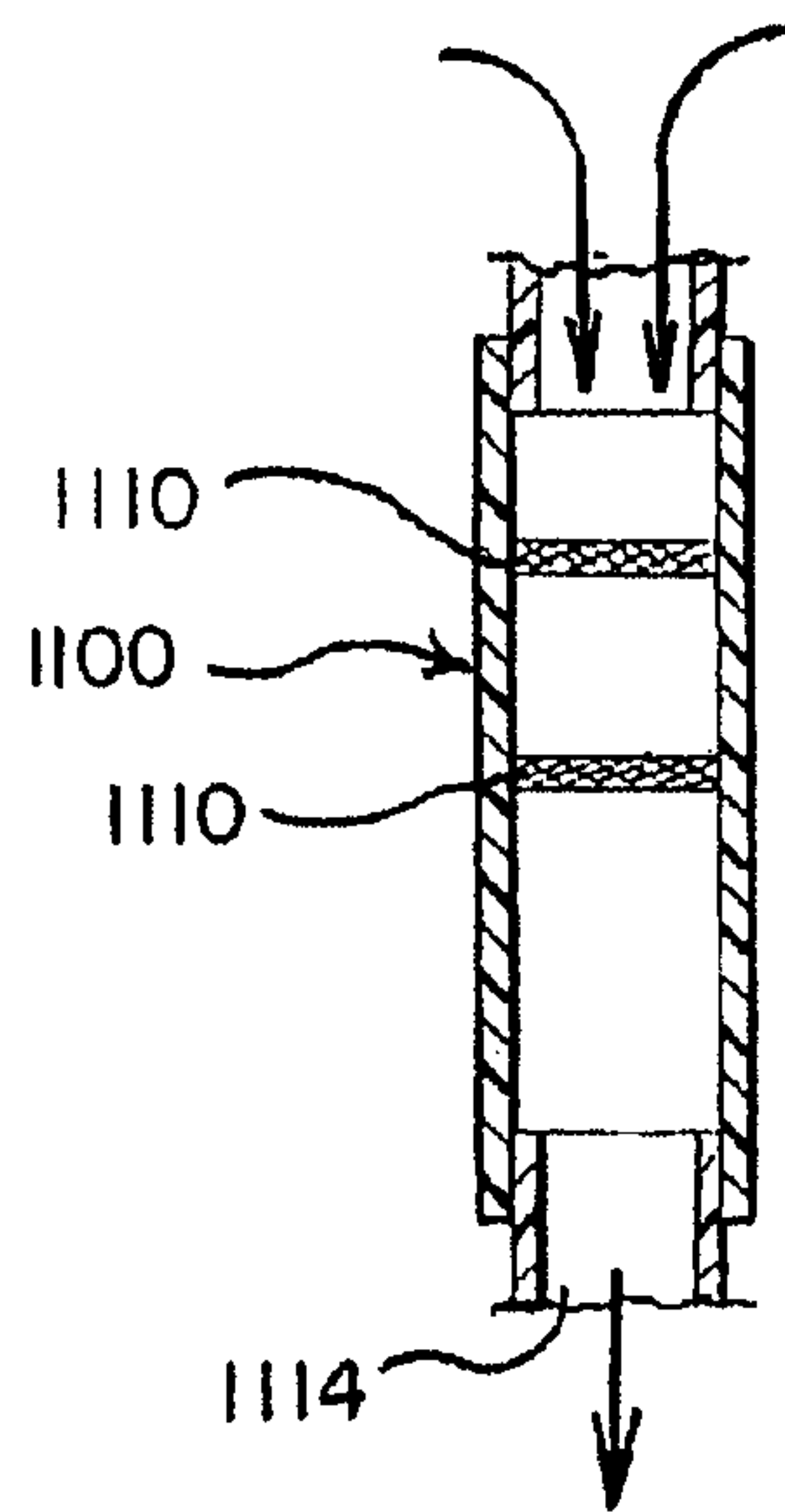
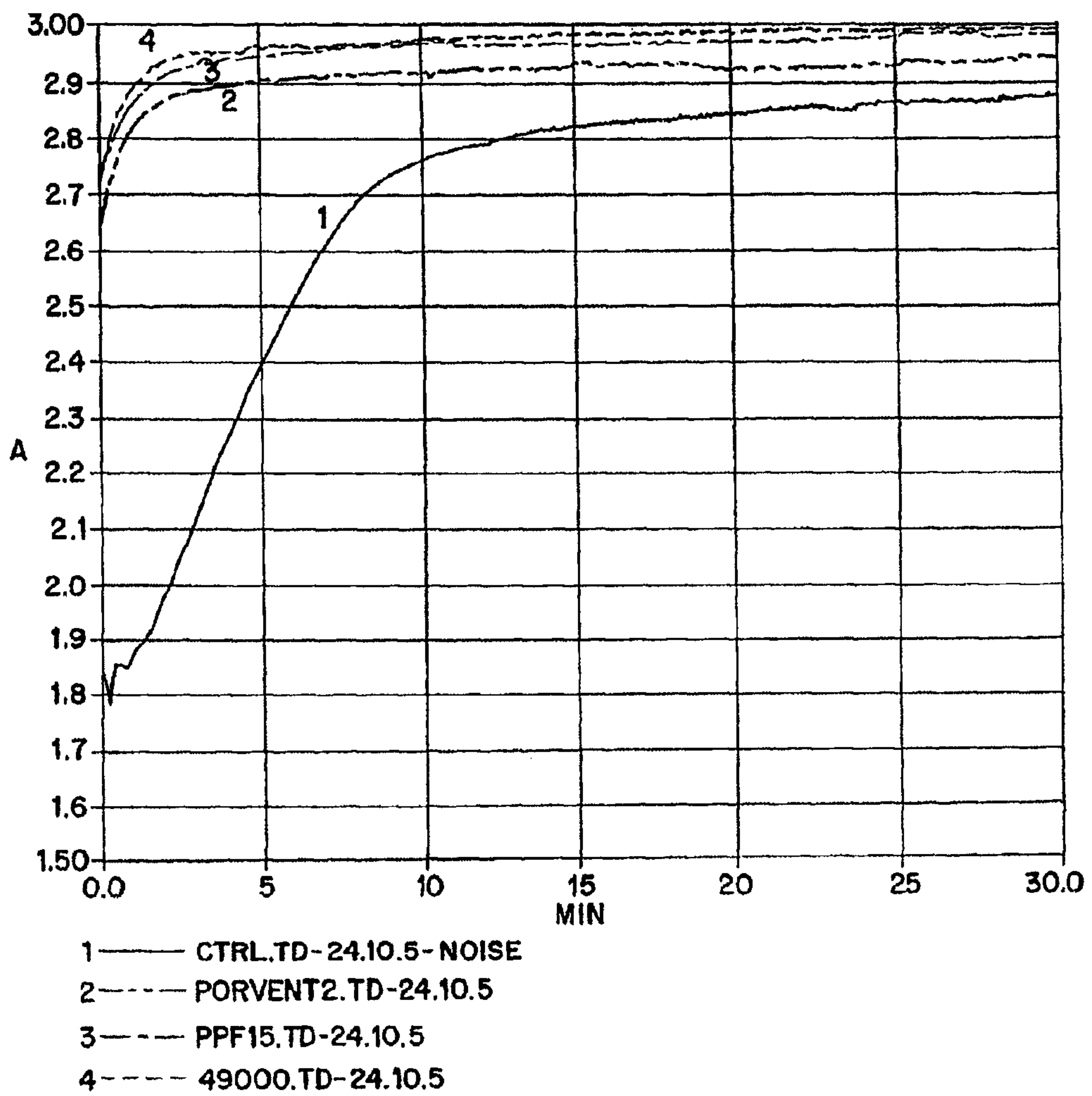


FIG.53



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FIG.54

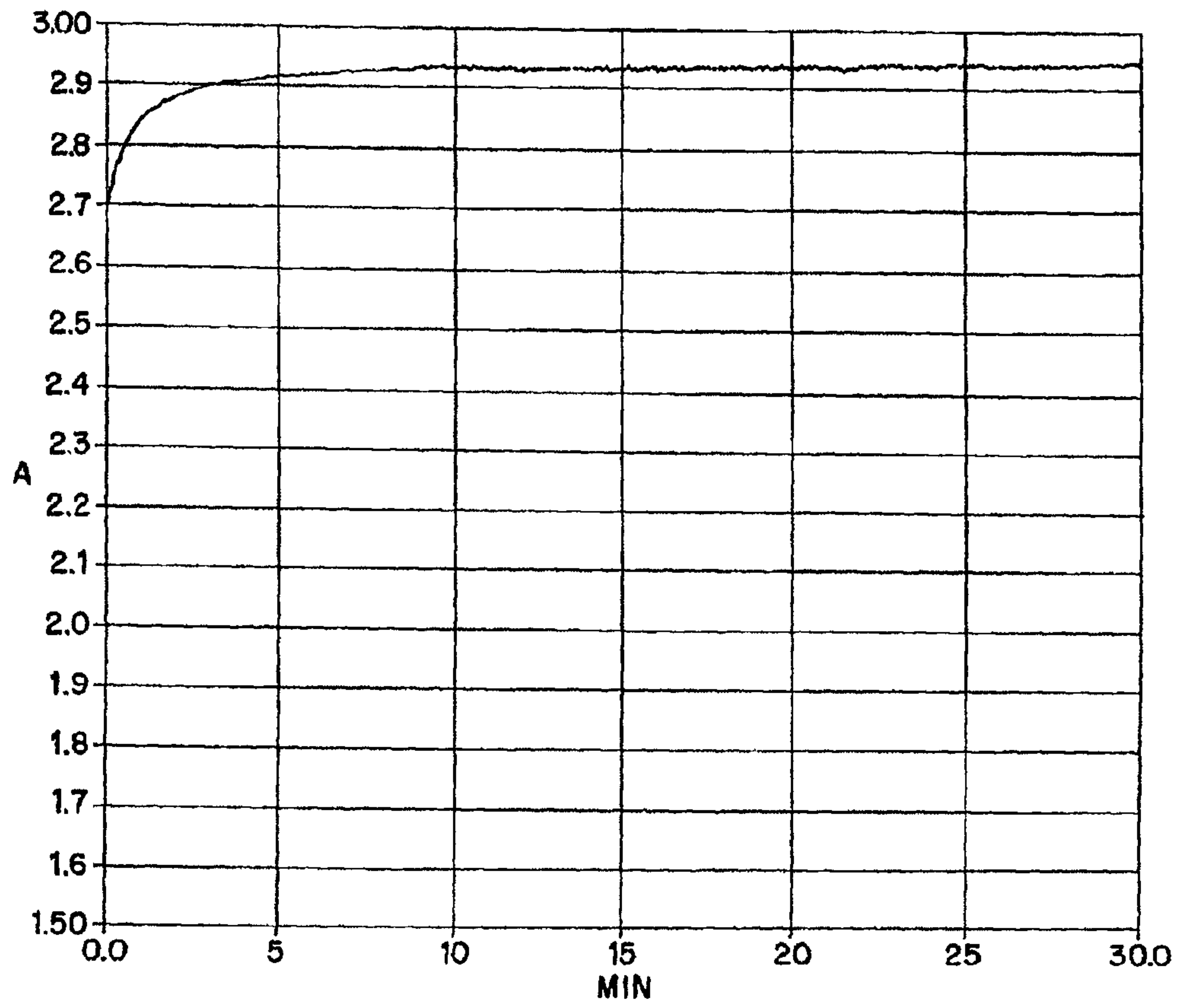
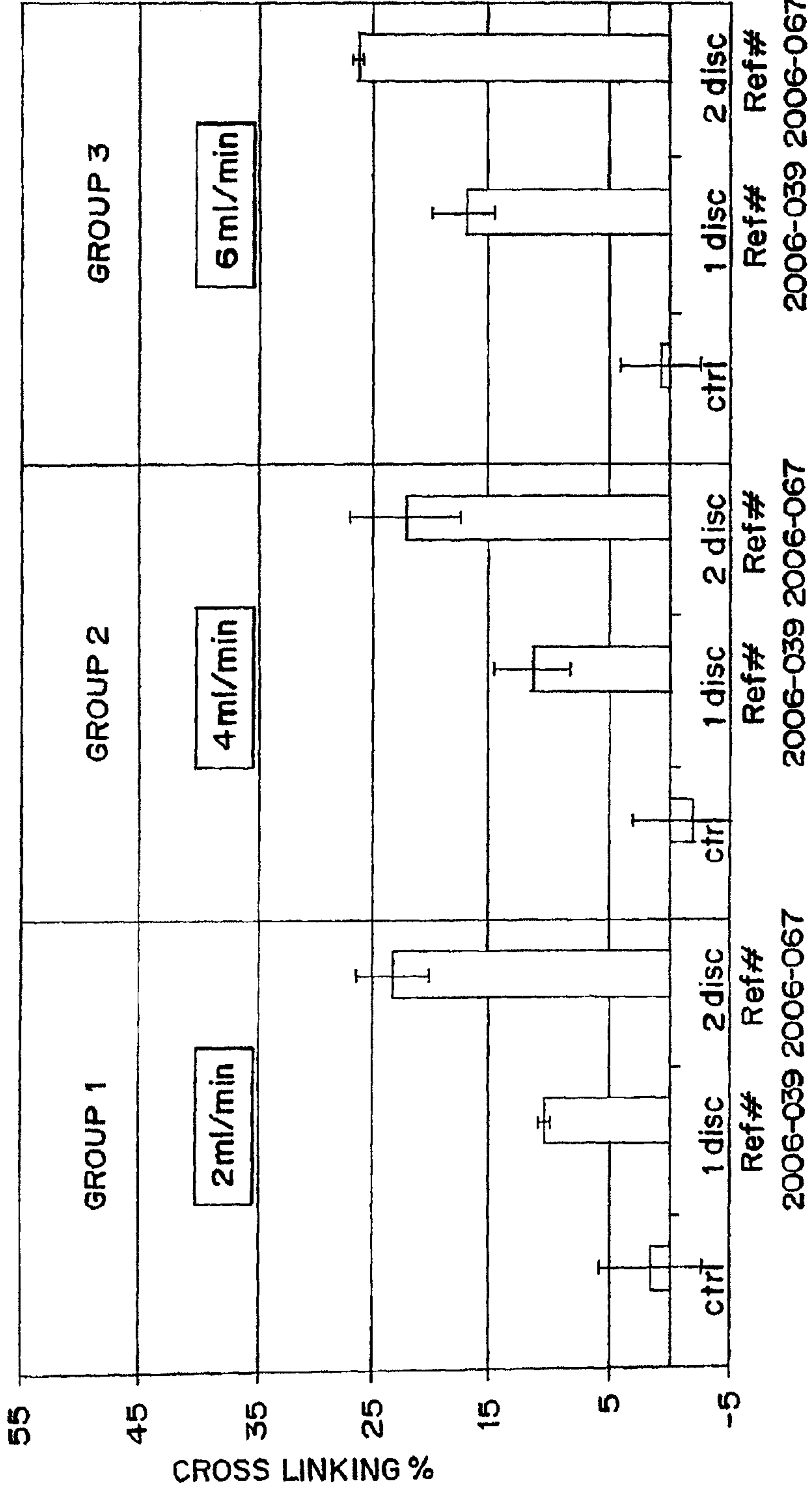


FIG.55

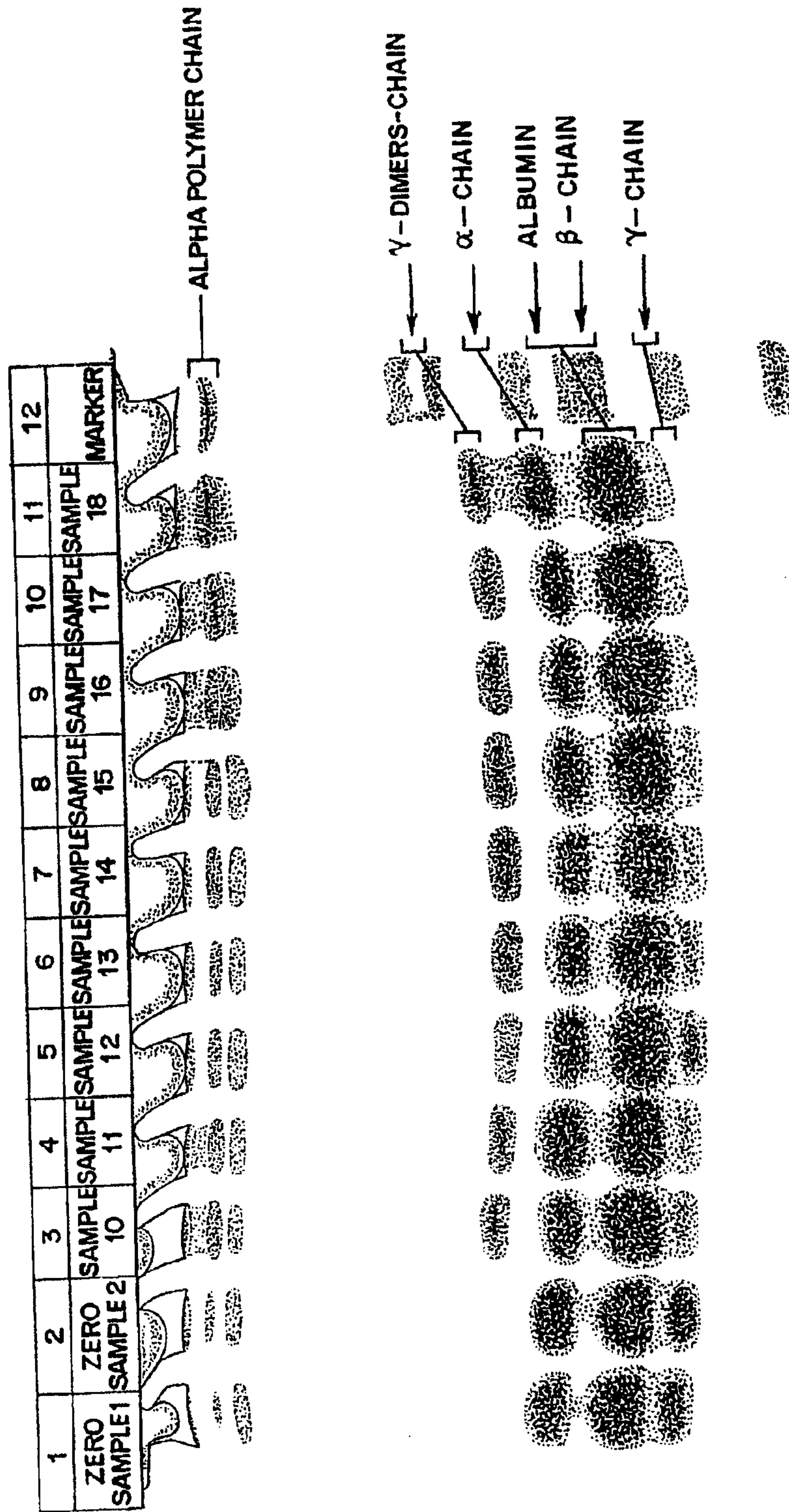
FLOWRATE INFLUENCE



Ref# 2006-039 2006-067 Ref# 2006-039 2006-067 Ref# 2006-039 2006-067

FIG. 56

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FIG.57

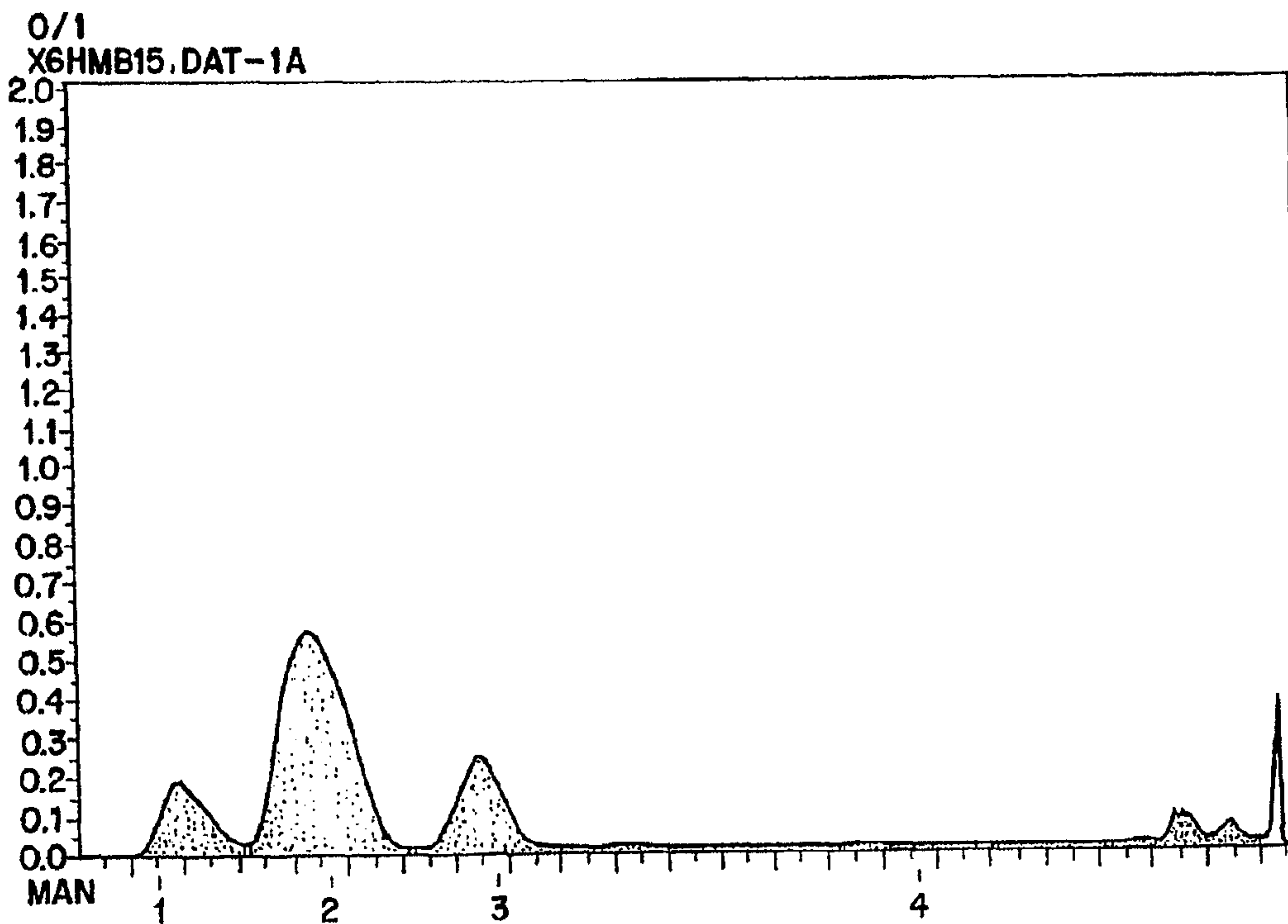
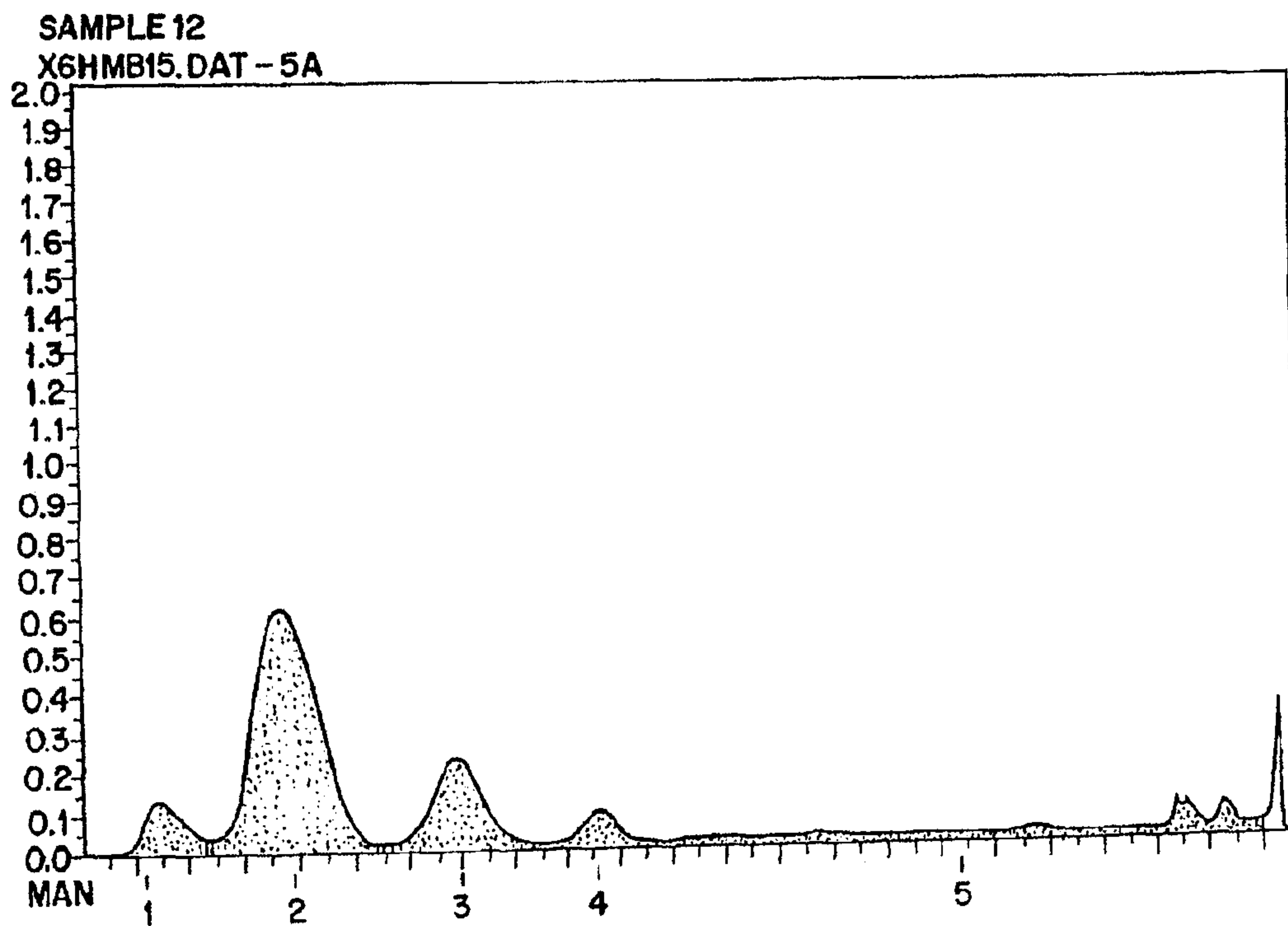


FIG.58



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FIG. 59

SAMPLE 13
X6HMB15.DAT-6A

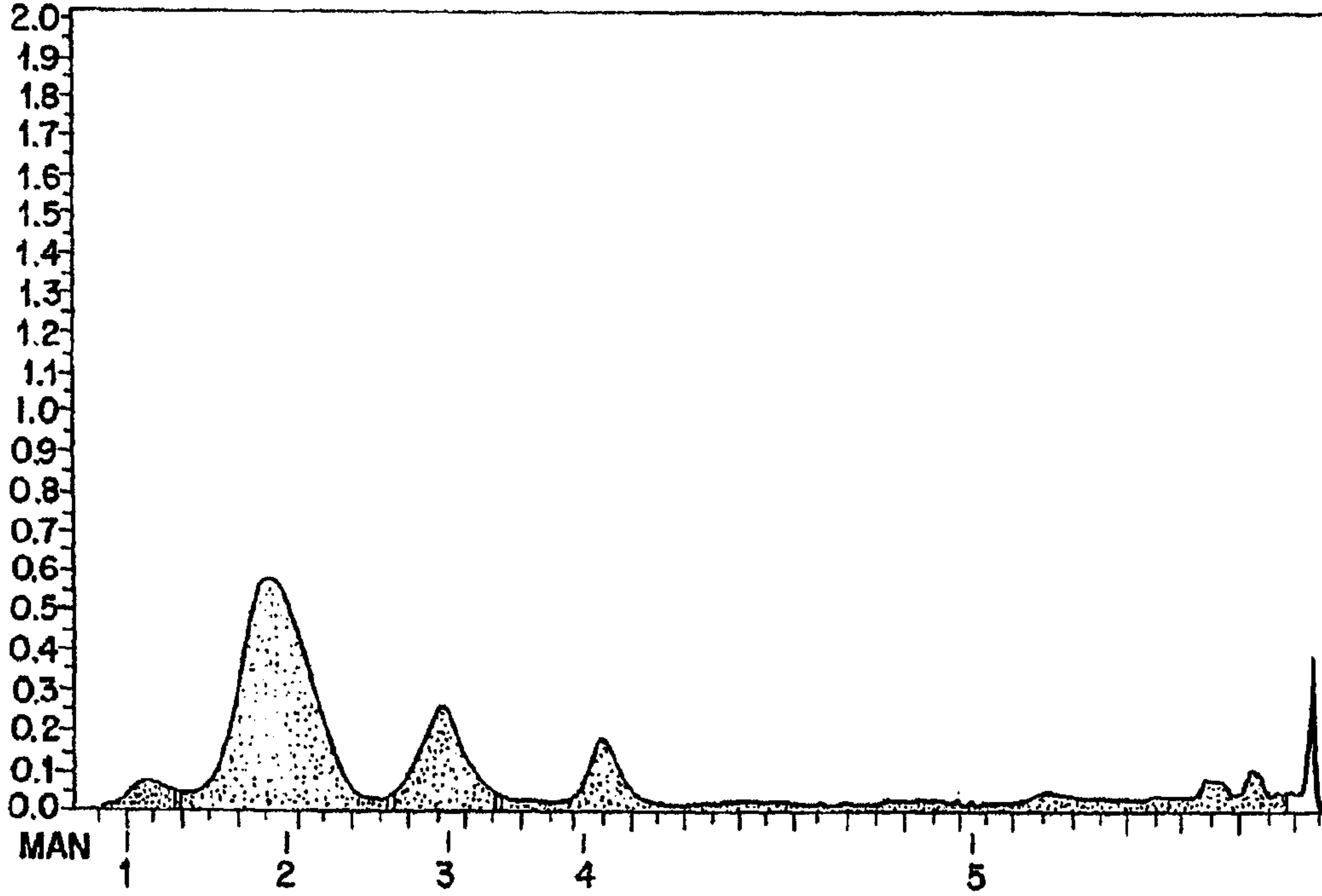


FIG. 60

SAMPLE 17
X6HMB15.DAT-10B

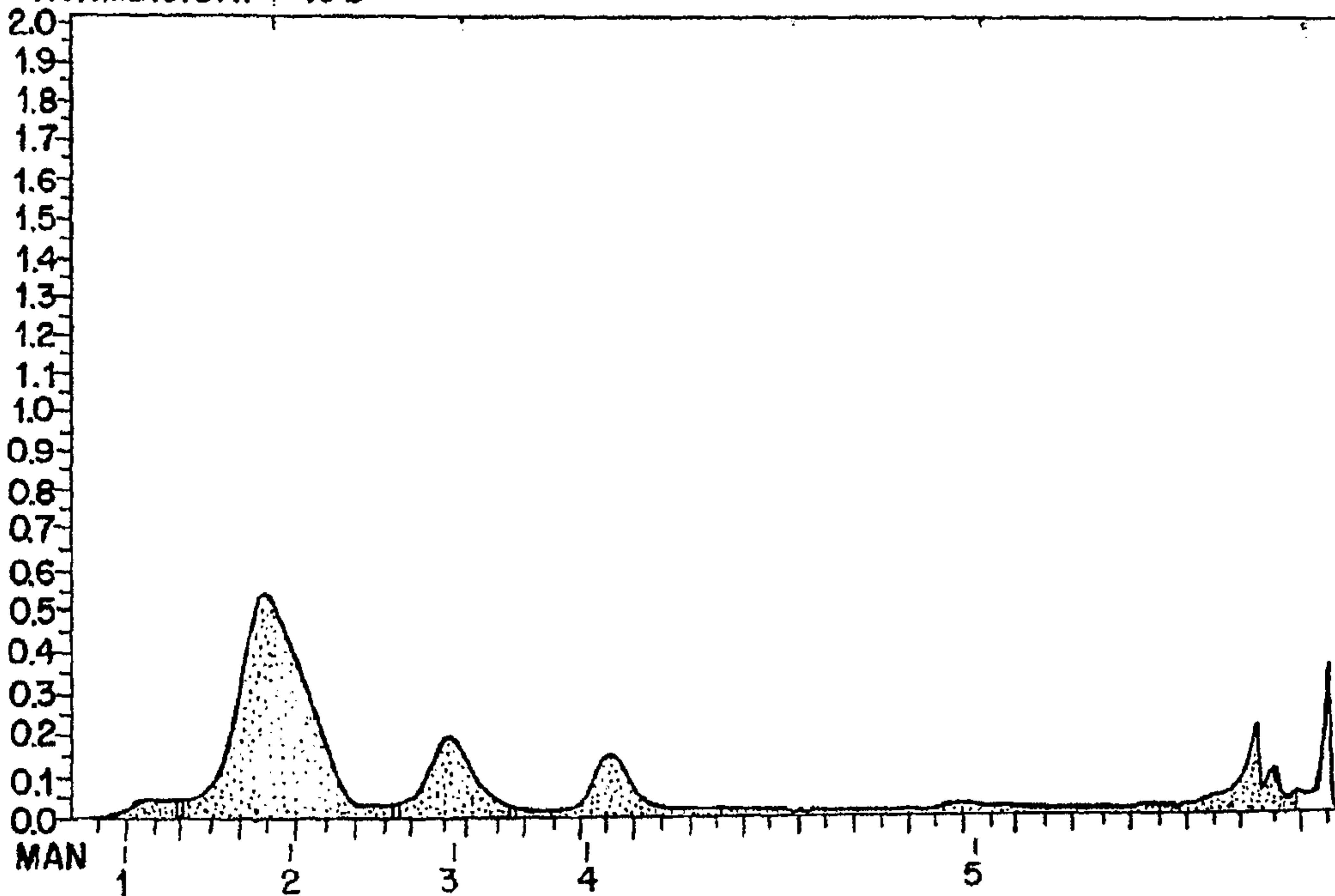
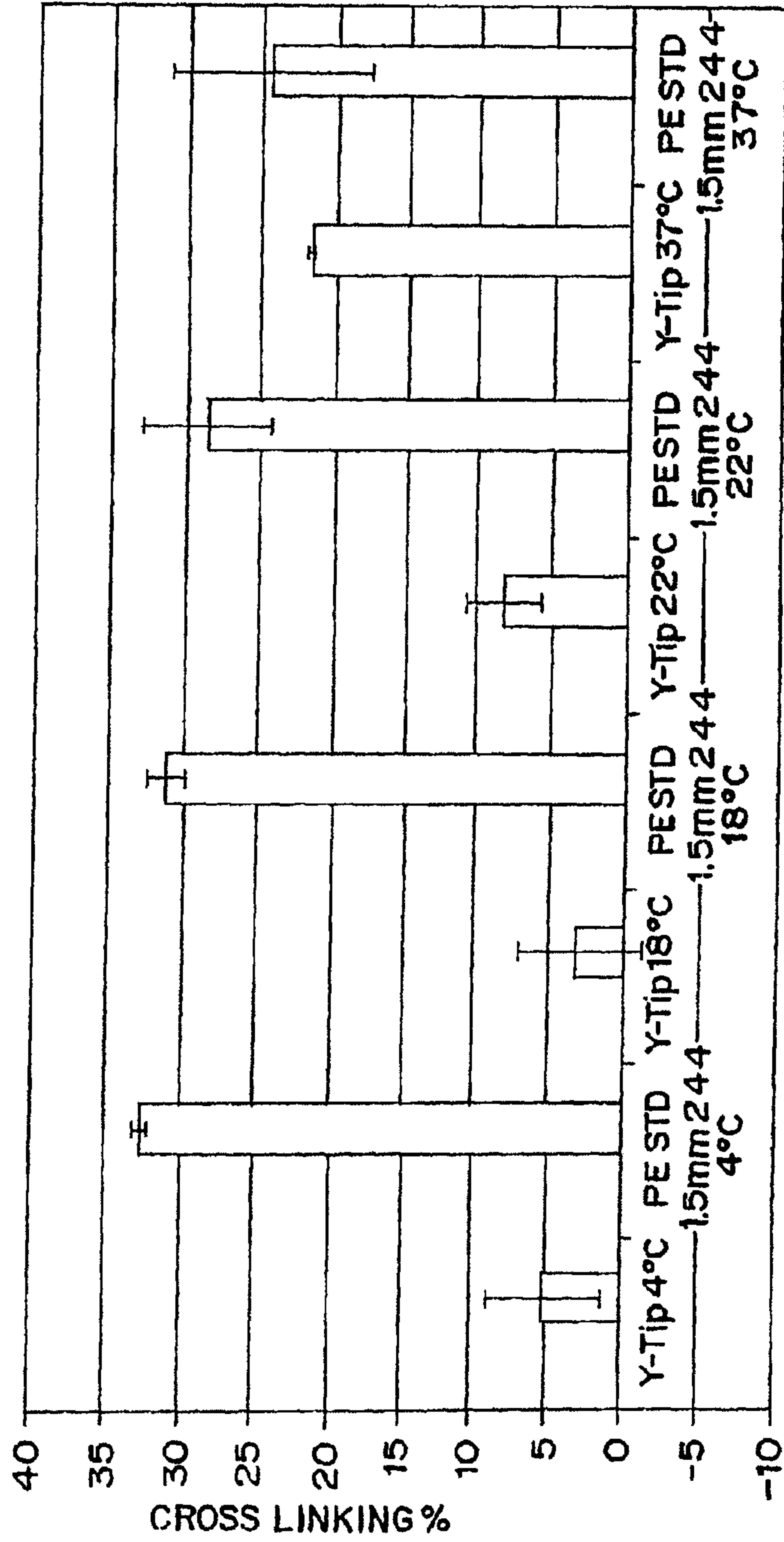


FIG.61

DEVICES SAMPLES 49-56 - INFLUENCE OF TEMPERATURE 09.08.2006



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FIG.62

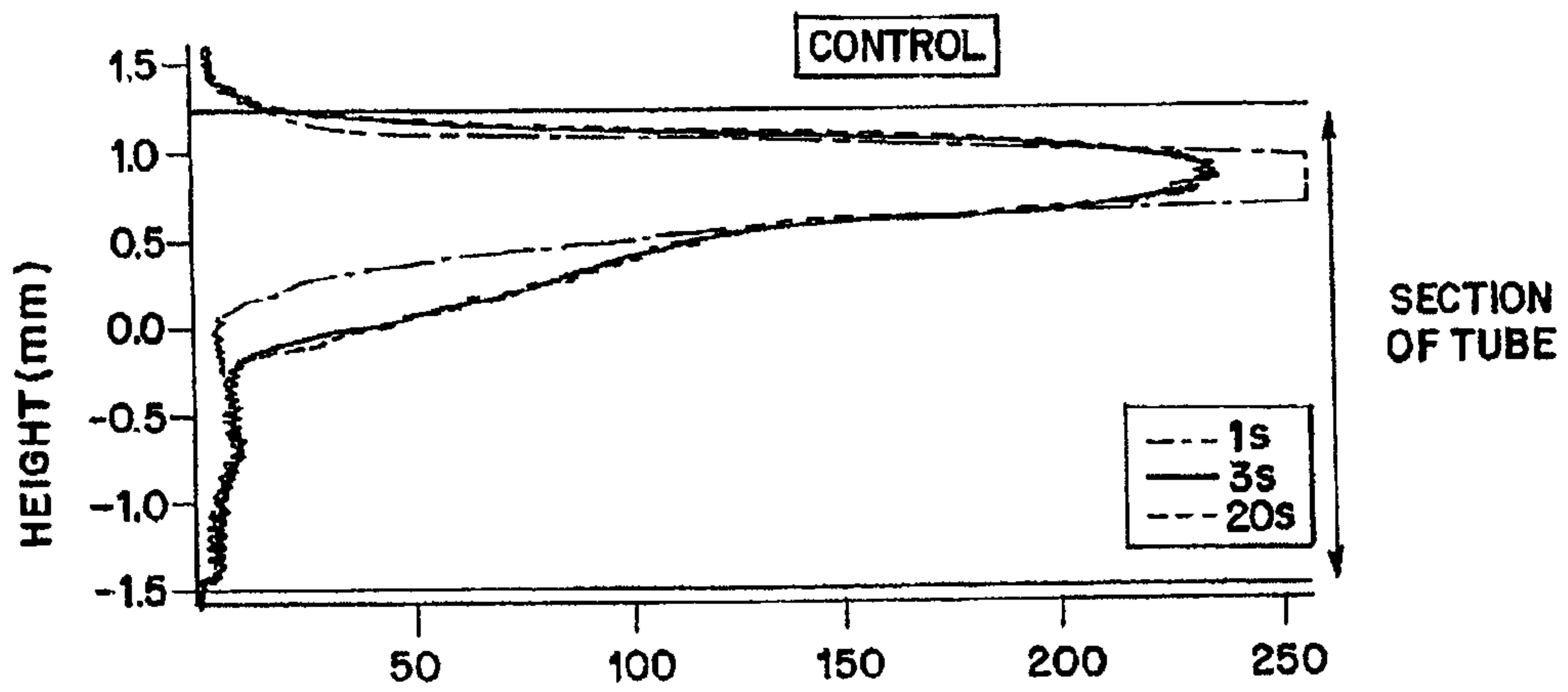
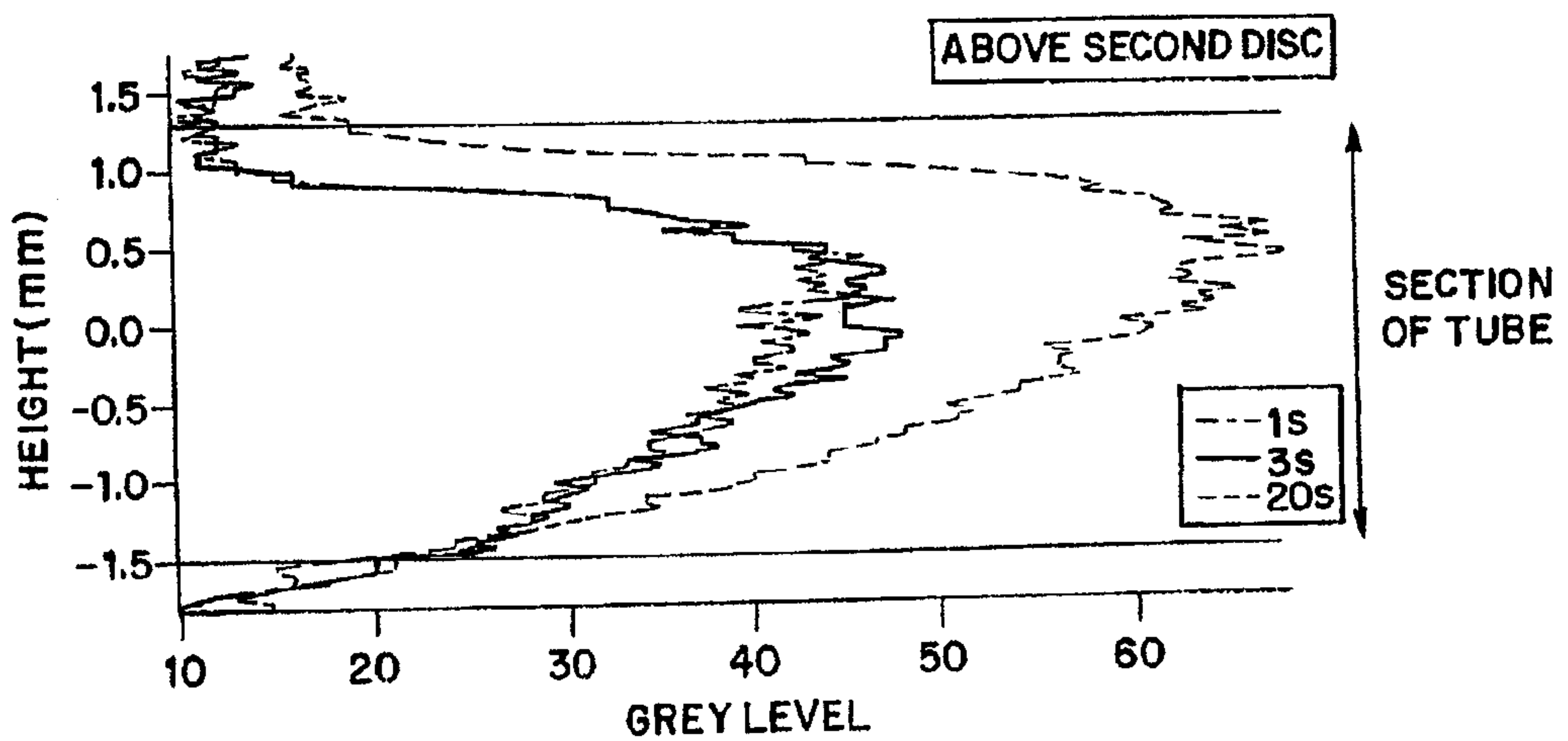


FIG.63



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FIG.64

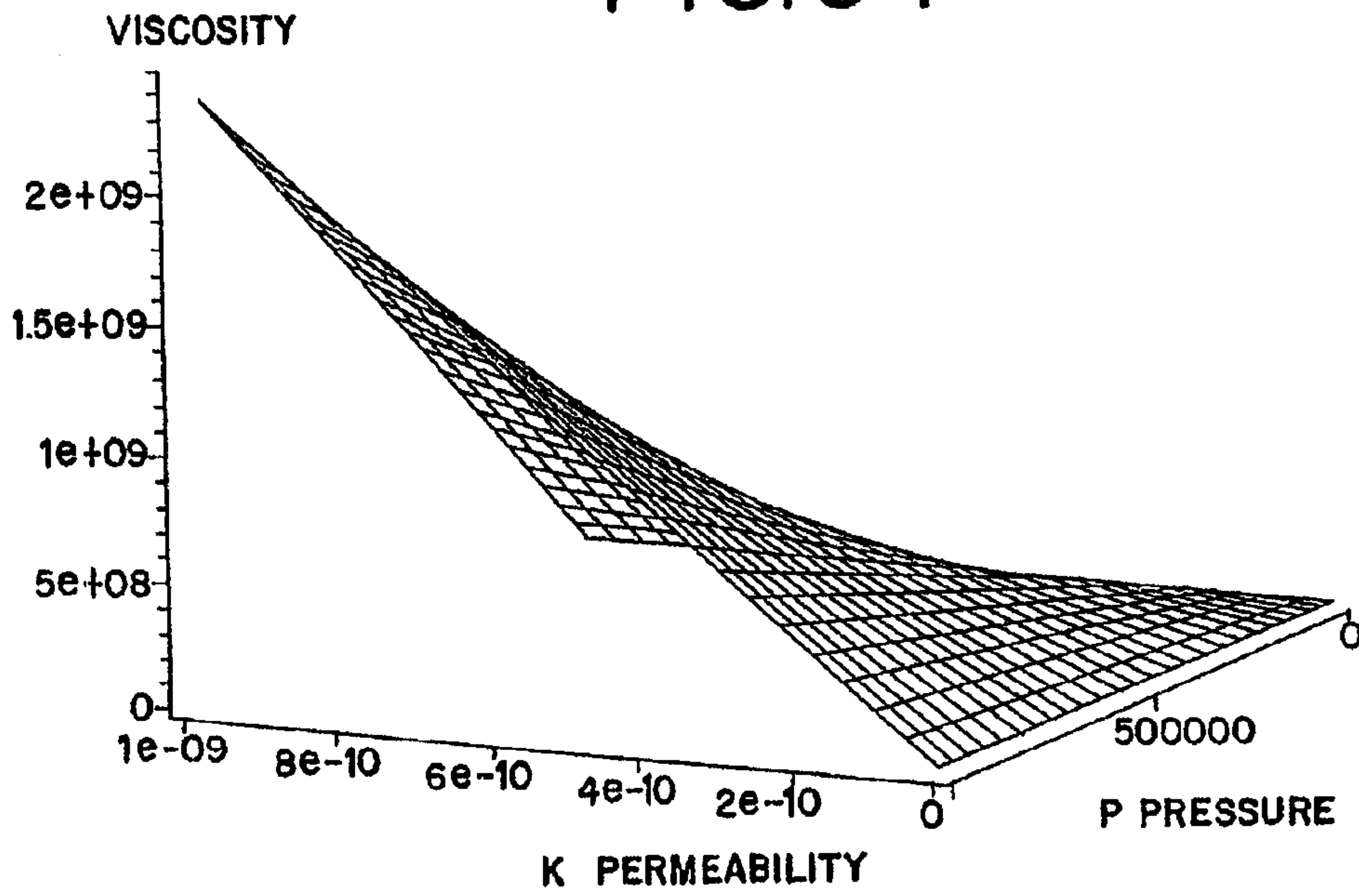


FIG.65

