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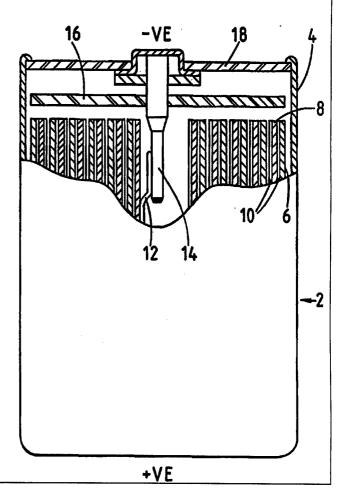
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(54) Title: A RECHARGEABLE ELECTROCHEMICAL CELL

(57) Abstract

A rechargeable electrochemical cell comprising a positive electrode, a negative electrode and an electrolyte, the positive electrode being such that it is a composition of an alkali or alkaline earth salt of a sulphur oxy-acid and a transition metal oxide, and the electrolyte being such that it is a non-aqueous electrolyte containing a soluble salt of the alkali or alkaline earth metal dissolved in the non-aqueous electrolyte.



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A RECHARGEABLE ELECTROCHEMICAL CELL

This invention relates to a rechargeable electrochemical cell. The rechargeable electrochemical cell may be used as a storage battery or as a capacitor.

Non-rechargeable lithium electrochemical cells are well known. In one application a two cell battery is used in the consumer field and it has a manganese dioxide positive electrode. In another application a battery used in the military field employs a lithium sulphur dioxide liquid electrolyte de-polarizer system. Both of these battery systems are renowned for their high energy densities of more than 300 Watt hours/Kg, high power densities and modest raw material costs. Attempts to recharge such primary cells have met with little or no success. In the case of the manganese dioxide cell, the product formed on electrochemical reduction with lithium at the positive electrode has a radically altered chemical structure the lithium intercalated on discharge and recoverable to a small extent only on current reversal. With the lithium sulphur dioxide liquid electrolyte/depolarizer system, the presence of sulphur dioxide in direct contact with lithium metal at the negative electrode gives an immediate reaction

product on the surface of the lithium metal. This makes the plating of bulk lithium metal, as required on recharge, grossly inefficient since the regenerated electrode is being consumed as it is formed. Cells containing the highly volatile sulphur dioxide as a major electrolyte constituent have the attendant disadvantages of requiring expensive reinforced cell containers and corrosion resistant hermetic seals to obviate the expulsion of noxious sulphur dioxide fumes into the atmosphere, such as would occur under abuse conditions.

It is an aim of the present invention to provide a rechargeable electrochemical cell which combines the flat voltage characteristic of a sulphur dioxide electrode on discharge, with an immobilizing host in the form of a transition metal oxide.

Accordingly, the present invention provides a rechargeable electrochemical cell comprising a positive electrode, a negative electrode and an electrolyte, the positive electrode being such that it is a composition of an alkali or alkaline earth salt of a sulphur oxy-acid and a transition metal oxide, and the electrolyte being such that it is a non-aqueous electrolyte containing a soluble salt of the alkali or alkaline earth metal dissolved the non-aqueous electrolyte.

Preferably, the salt of a sulphur oxy-acid is a lithium salt. The lithium salt is preferably lithium sulphite ($\text{Li}_2\text{S0}_3$), lithium dithionate ($\text{Li}_2\text{S}_2\text{O}_6$) or lithium dithionite ($\text{Li}_2\text{S}_2\text{O}_4$).

The transition metal is preferably one or more of ferrous oxide (FeO), titanium monoxide (TiO), manganous oxide (MnO), manganic oxide (Mn $_2$ O $_3$), vanadium trioxide (V $_2$ O $_3$), vanadium dioxide (VO $_2$), cuprous oxide (Cu $_2$ O) or nickelous oxide (NiO). Many other transition metal oxides may be used as will be familiar to those versed in this technology. The oxides may be used singly or in combination.

The alkali or alkaline salt in solution is preferably present in approximately 1 molar concentration. Other concentrations may however be employed with a preferred molar concentration range being 0.5 - 2 molar concentration.

The alkali or alkaline salt in solution in the electrolyte is preferably a lithium salt. Other alkali or alkaline earth salts may however be employed, with the corresponding sulphur oxy-acid salt in the cathode.

A soluble salt of the alkali or alkaline earth metal must always be present in the non-aqueous electrolyte solution. For lithium this can be lithium fluoroborate or lithium hexafluorophosphate or a

number of other complex lithium fluorides, for example, lithium trifluoromethane sulphonimide LiN(CF₃SO₂)₂. The said salt provides a source of alkali-metal ions or alkaline earth metal ions in solution for electroplating alkali metal or alkaline earth metal from the cathode compound or complex, for example lithium sulphite which is totally insoluble in the electrolyte. The alkali or alkaline earth metal in solution must be the same as the alkali or alkaline earth salt of the sulphur oxy-acid in the cathode. The process of operation of say the rechargeable lithium electrochemical cell may be thought of as a shuttle of lithium going from a lithium compound in the cathode to lithium metal at the anode following the charge process.

The cell may include a separator which is permeable to the lithium ions. The rechargeable electrochemical cell may then be one in which the lithium salt is lithium fluoroborate (LiBF $_4$) and/or lithium hexafluorophosphate LiPF $_6$ or LiN(CF $_3$ SO $_2$) $_2$. Suitable solvents are a mixture of a linear carbonate and a cyclic ester. The linear carbonate is preferably diethyl carbonate or dimethyl carbonate. The cyclic ester is preferably polypropylene carbonate or ethylene carbonate. The separator is preferably a microporous polypropylene. In the case of lithium

ions, the separator allows permeation of lithium ions but will not allow lithium metal plated at the anode to get in electrical contact with the cathode.

The negative electrode current collector is preferably copper. Nickel or other metals may also be employed.

The negative electrode current collector may alternatively be coated with a porous substrate into which deposited alkali or alkaline earth metal will intercalate. The porous substrate may be a porous substrate of conductive finely divided carbon.

Both electrodes may include a binding agent. The binding agent has two functions. It holds the constituents of the cathode together so that a thin layer or film can be applied to the substrate electrode collector. It also enables adhesion of this layer to be effective to the substrate. Many organic polymers are suitable, examples being polyvinylidene fluoride and ethylene propylene diene terpolymer.

The rechargeable electrochemical cell may be cylindrical in shape.

The cylindrical rechargeable electrochemical cell may be one in which the composition of the alkali or alkaline earth salt of the sulphur oxy-acid and the transition metal oxide is provided on a substrate which is wound in the form of a roll. The substrate

is preferably a foil substrate. A presently preferred foil substrate is an aluminium foil substrate.

The rechargeable electrochemical cell may be in the shape of a disc. The disc may be in the shape of a button or a coin.

The rechargeable electrochemical cell may be rectangular in shape and have multiple layers folded zig zag fashion.

The rechargeable electrochemical cell may be in the form of a battery or a super capacitor.

Preferably, the rechargeable electrochemical cell uses a lithium salt of a sulphur oxy-acid as the uncharged cathode. In order to ensure that the charged or active cathode material takes the form of an insoluble solid, the sulphur oxides formed by electrode decomposition of lithium oxy-acid salts must combine or complex with an appropriate substrate in order to preclude action with the lithium negative electrode. In the rechargeable electrochemical cell of the present invention, the transition metal oxides react with the sulphur oxides formed on charging the lithium sulphur oxy-acid composition, thereby acting in the role of a de-fluidizing agent.

If desired, in accordance with the present invention, the composition may also include one or more polymeric tertiary amines.

The electrolyte is non-aqueous because the presence of water at concentrations as low as 10 parts per million is detrimental since the water would react instantly with the alkali metal or alkaline earth metal formed in a finely divided state on charge. The non-aqueous electrolyte is preferably a non-aqueous organic solvent. It is essential that none of the constituents of the positive electrode composition in either the charged or the discharged state, are soluble in the electrolyte solution.

The electrochemical process taking place in the rechargeable electrochemical cell of the present invention may be represented as follows:

 Li_2SO_3 + x MO_y \longrightarrow 2 Li + $(\text{M}_x\text{SO}_{3+xy})$ complex in which M is the transition metal atom, and in which 1 \leq x \leq 4 and 0.5 \leq y \leq 2.5.

Lithium sulphite (Li_2SO_3) is an efficient source of lithium because it has two lithium atoms per sulphur atom present. The utilisation of lithium metal in the discharge process is thus up to twice that obtainable in competitive systems, especially those based on cobalt and manganese oxide.

In order that the invention is fully understood, reference will now be made to the following Examples.

EXAMPLE I

A mixture of lithium sulphite and vanadium dioxide in a 1:2 molar ratio was intimately ground together using a pestle and mortar. mixture was then heated for 3 hours at 200°C under vacuum in order to remove traces of water absorbed on standing. A 3% solution of polyvinylidene fluoride in N-methylpyrrolidone was prepared and to this was added carbon black which was obtained from MMM Sedema under the trade name Super S+. The carbon black was added in proportion to give 60% by weight carbon black and by weight polyvinylidene fluoride resulting dried powder. 20% by weight of the dried powder was added to the mixture of the lithium sulphite and the vanadium dioxide, the composite positive electrode thus containing 80% of the active After thorough mixing together of the composite, a 25mm diameter disc, approximately 1mm thick, was prepared by pressing with a load of 15 tonnes.

The disc was placed in a test cell in which a microporous polypropylene separator 25 microns thick was used, together with a copper disc as a target negative electrode. A 1 molar solution of lithium fluoborate in an anhydrous mixture of equal volumes of propylene carbonate and diethyl carbonate was used as an electrolyte to saturate the positive electrode and

the separator. The rechargeable electrochemical cell was charged at a current density of 0.8 ma/cm² for 6 hours, the applied voltage starting at 3.5 volts and rising to a maximum of 4.25 volts. On discharge at a current density of 1 ma/cm², the average voltage was 3.35 volts and all the energy removed was at around 2.7 volts, the discharge curve being remarkably flat. Repeated charge/discharge cycling resulted in a coulometric efficiency greater than 98% on successive cycles.

EXAMPLE II

A mixture of lithium sulphite and ferrous oxalate $(\text{FeC}_2\text{O}_4.2\text{H}_2\text{O}$ in a 1:2 molar ratio was intimately ground together using a pestle and mortar. mixture was then heated at 300°C for 2 hours under vacuum in order to convert the oxalate to oxide and to remove all the water present. After cooling, the product was mixed with carbon black and polyvinylidene fluoride as described in Example I, the active materials content again being 80% by weight. Α rechargeable electrochemical cell was prepared as described in Example I and the cell was placed on charge. The voltage range necessary to charge at 0.8 $\mathrm{ma/cm^2}$ started at 3.2 volts and rose to a maximum of 3.9 volts. On discharge at a current density of 1 $\mathrm{ma/cm^2}$ the average running voltage was just above 3

volts and the end point was selected at 2.4 volts. The discharge curve was not as flat as in Example I, the active material appearing to develop a higher internal resistance on cycling. A coulometric efficiency greater than 95% was realised.

EXAMPLE III

A mixture of lithium sulphite and nickelous oxide in a 1:2 molar ratio was intimately ground together using a pestle and mortar. The mixture was heated at 200°C for 2 hours under vacuum and then reground. The mixture was then prepared and formed into a rechargeable electrochemical cell as described in Example I. For a 0.8 ma/ca² charging current, the applied voltage ranged between 3.4 volts and 4.0 volts. On discharge at a current density of 1 ma/cm², and average voltage of 3.2 volts was observed with an end point of around 2.5 volts. The form of the discharge curve and the coulometric efficiency was similar to that observed in Example II.

EXAMPLE IV

A mixture of lithium sulphite and cuprous oxide in a 1:1 molar ratio was intimately ground together using a pestle and mortar. The mixture was heated at 200°C for 2 hours under vacuum and then reground. A rechargeable electrochemical cell was produced as described in Example I. For a 0.8 ma/cm² charging

current, the applied voltage required was between the limits of 3.2 volts and 3.9 volts. On discharge at a current density of 1 ma/cm², a two step discharge curve was observed with a joining plateau at around 2.85 volts. With this composition, the average discharge voltage was just below 3 volts but the cycling efficiency was greater than 95%.

From the above Examples, it is evident that the voltage characteristics of the composite ${\rm Li}_2{\rm SO}_3/{\rm xMO}_{\rm y}$ positive electrode on charging are at a higher level in every instance than the individual voltages of either the ${\rm MO}_{\rm y}$ material alone or ${\rm SO}_2$ which is the redox or valency state in ${\rm Li}_2{\rm SO}_3$. Assuming the initial product of the electrolytic decomposition of ${\rm Li}_2{\rm SO}_3$ which occurs on charging is ${\rm SO}_3$ (along with ${\rm Li}$ metal) the strong oxidising nature of ${\rm SO}_3$ will be targeted to attack the metal oxide ${\rm MO}_{\rm y}$. It is postulated that an equilibrium will be established, governed by the free energy factor and the complex shown in above equation may be more properly represented as:

$$M_x SO_{3+xy} \longrightarrow M_x O_{xy}.SO_3 \longleftrightarrow M_x O_{y+1}.SO_2$$

This infers that the valency state of sulphur in the charged complex is between 4 and 6. The higher voltage realised in the rechargeable electrochemical cells is believed to be due to the presence of a substantial proportion of sulphur oxide in the 6-valent state which is formed from Li_2SO_3 as the result of electrolytic decomposition taking place on charging.

Embodiments of the invention will now be described solely by way of example and with reference to the accompanying drawings in which:

Figure 1 shows a first rechargeable electrochemical cell, partially in section;

Figure 2 is a section through a second rechargeable electrochemical cell;

Figure 3 is a cross section through a third rechargeable electrochemical cell; and

Figure 4 is a top plan view of the rechargeable electrochemical cell shown in Figure 3.

Referring to Figure 1, there is shown rechargeable electrochemical cell 2. The cell 2 has a cylindrical outer body 4 which is preferably made of aluminium. The cell 2 has a composite positive electrode 6 formed of lithium sulphite on aluminium foil. The cell 2 further comprises copper foil 8 having a lithium negative electrode. A separator 10 is employed as shown and the composite positive electrode 6, the copper foil 8 and the separator 10 are wound to form a roll as shown. The roll then fits inside the body 4, also as shown.

A copper tab 12 extends from the copper foil 8 to a copper tube 14 which serves as feed through. The body 4 is closed by a polypropylene insulating disc 16 and a polypropylene insulating cap 18.

Preferably, the cell 2 is fabricated in the uncharged state. This is primarily for safety considerations since no lithium metal is then present and should the wound sub-assembly develop a short circuit prior to final assembly with electrolyte, there is no danger of heat generation and fire or explosion. The starting materials in the uncharged state are also much less costly than would be the case for the charged state.

Referring now to Figure 2, there is shown a rechargeable electrochemical cell 20 which is in the form of a disc. The cell 20 has a lithium negative electrode 22, and a lithium sulphite/transition metal oxide positive electrode 24. An anode current collector 26 forms a negative hole. A positive electrode current collector 28 made of aluminium is provided. The cell 20 also includes a separator 30 and a polypropylene plastics insulator/seal 32.

Referring now to Figures 3 and 4, there is shown a rechargeable electrochemical cell 34 in which similar parts as in Figure 2 have been given the same reference numerals. In Figures 3 and 4, it will be

seen that the cell 34 is produced in a flat rectangular shape. The cell 34 includes a plastics sheet 36 which is heat sealed on four sides.

When the rechargeable electrochemical cell of the present invention is in the form of a large rechargeable battery, then one or more such batteries may be used to power electric vehicles. Raw material cost are an important commercial consideration and an iron oxide used as the transition metal is especially appropriate in such applications. The environmental impact will be minimal since the iron and sulphur oxides are in a chemically bound state even when the battery is fully charged.

It is to be appreciated that the embodiments of the invention described above with reference to the accompanying drawings have been given by way of example only and that modifications may be effected.

CLAIMS

- 1. A rechargeable electrochemical cell comprising a positive electrode, a negative electrode and an electrolyte, the positive electrode being such that it is a composition of an alkali or alkaline earth salt of a sulphur oxy-acid and a transition metal oxide, and the electrolyte being such that it is a non-aqueous electrolyte containing a soluble salt of the alkali or alkaline earth metal dissolved in the non-aqueous electrolyte.
- 2. A rechargeable electrochemical cell according to claim 1 in which the salt of a sulphur oxy-acid is a lithium salt.
- 3. A rechargeable electrochemical cell according to claim 2 in which the lithium salt is lithium sulphite (Li_2SO_3) .
- 4. A rechargeable electrochemical cell according to claim 2 in which the lithium salt is lithium dithionate ($\text{Li}_2\text{S}_2\text{O}_6$).

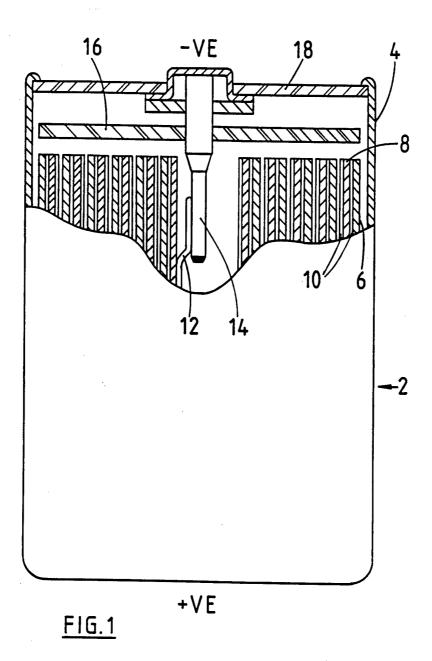
- 5. A rechargeable electrochemical cell according to claim 2 in which the lithium salt is lithium dithionite ($\text{Li}_2S_2O_4$).
- 6. A rechargeable electrochemical cell according to any one of the preceding claims in which the transition metal is one or more of ferrous oxide (FeO), titanium monoxide (TiO), manganous oxide (MnO), manganic oxide (Mn $_2$ O $_3$), vanadium trioxide (V $_2$ O $_3$), vanadium dioxide (VO $_2$), cuprous oxide (Cu $_2$ O) or nickelous oxide (NiO).
- 7. A rechargeable electrochemical cell according to any one of the preceding claims in which the alkali or alkaline earth salt in solution is present in approximately one molar concentration.
- 8. A rechargeable electrochemical cell according to any one of the preceding claims in which the alkali or alkaline earth salt in solution in the electrolyte is a lithium compound.
- 9. A rechargeable electrochemical cell according to claim 8 in which the electrolyte includes a separator which is permeable to lithium ions.

- 10. A rechargeable electrochemical cell according to claim 9 in which the lithium salt is lithium fluoroborate (LiBF $_4$), and/or lithium hexafluorophosphate (LiPF $_6$), and/or lithium trifluoromethane sulphonimide [LiN(CF $_3$ SO $_2$) $_2$] in which the solvents are a mixture of a linear carbonate and a cyclic ester.
- 11. A rechargeable electrochemical cell according to claim 10 in which the linear carbonate is diethyl carbonate or dimethyl carbonate, and in which the cyclic ester is polypropylene carbonate or ethylene carbonate.
- 12. A rechargeable electrochemical cell according to any one of the preceding claims in which the negative electrode current collector is a metal.
- 13. A rechargeable electrochemical cell according to claim 12 in which the metal is copper or nickel.
- 14. A rechargeable electrochemical cell according to any one of claims 1 11 in which the negative electrode current collector is coated with a porous substrate into which deposited alkali or alkaline earth metal will intercalate.

- 15. A rechargeable electrochemical cell according to claim 14 in which the porous substrate is a porous substrate of conductive finely divided carbon.
- 16. A rechargeable electrochemical cell according to any one of the preceding claims in which the rechargeable electrochemical cell is cylindrical in shape.
- 17. A rechargeable electrochemical cell according to claim 16 in which the composition of the alkali or alkaline earth sait of a sulphur oxy-acid and the transition metal oxide is provided on a substrate which is wound in the form of a roll.
- 18. A rechargeable electrochemical cell according to claim 17 in which the substrate is a foil substrate.
- 19. A rechargeable electrochemical cell according to claim 18 in which the foil substrate is an aluminium foil substrate.
- 20. A rechargeable electrochemical cell according to any one of claims 1 15 in which the rechargeable electrochemical cell is in the shape of a disc.

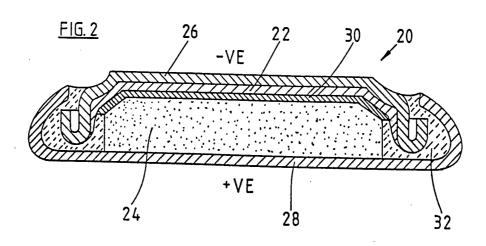
- 21. A rechargeable electrochemical cell according to any one of claims 1 15 in which the rechargeable electrochemical cell is rectangular in shape.
- 22. A rechargeable electrochemical cell according to any one of the preceding claims and including one or more polymeric tertiary amines.
- 23. A rechargeable electrochemical cell according to any one of the preceding claims and in the form of a battery.
- 24. A rechargeable electrochemical cell according to any one of claims 1 22 and in the form of a super capacitor.
- 25. A rechargeable electrochemical cell substantially as herein described with reference to the Examples.
- 26. A rechargeable electrochemical cell substantially as herein described with reference to the accompanying drawings.

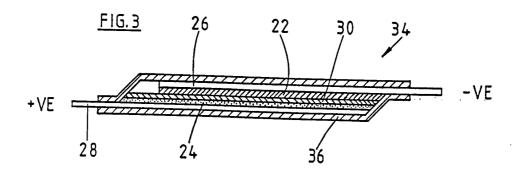
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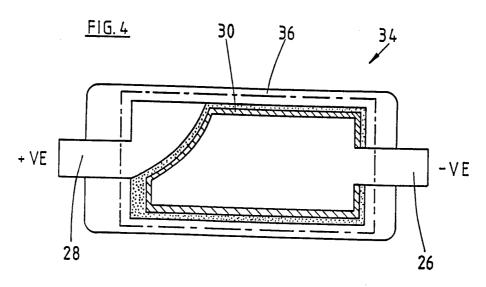


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INTERNATIONAL SEARCH REPORT

International Application No. PCT/GB 95/01337

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According to International Patent Classification (IPC) or to both national classification and IPC								
B. FIELDS SEARCHED								
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Documenta	tion searched other than minimum documentation to the extent th	at such documents are included in the fields	rearched					
Electronic o	data base consulted during the international search (name of data l	base and, where practical, search terms used)						
C. DOCUA	MENTS CONSIDERED TO BE RELEVANT							
Category *	Citation of document, with indication, where appropriate, of the	e relevant passages	Relevant to claim No.					
A	EP, A, 0 571 858 (MITSUBISHI CABLE) 01 December 1993 (01 * Abstract *	1.12.93),	1					
P	PATENT ABSTRACTS OF JAPAN, unexamined applications, E field, vol. 18, no. 493, issued 1994, September 14, THE PATENT OFFICE JAPANESE GOVERNMENT, page 140 E 1606; & JP-A-06 168 724 (JAPAN STORAGE BATTERY)		1					
P	CHEMICAL ABSTRACTS, vol. no. 26, issued 1995, (Columbus, Ohio, USA KAWAI, TERUMI et al.	, June 26, A),	1					
χ Fur	ther documents are listed in the continuation of box C.	Patent family members are listed	in annex.					
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Name and	mailing address of the ISA European Patent Office, P.B. 5818 Patentiaan 2 NL - 2280 HV Rijswijk Tel. (+31-70) 340-2040, Tx. 31 651 epo nl, Fax: (+31-70) 340-3016	Authorized officer LUX e.h.						

INTERNATIONAL SEARCH REPORT

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C.(Continuation) DOCUMENTS CONSIDERED TO BE RELEVANT Citation of document, with indication, where appropriate, of the relevant passages Relevant to claim No. "Secondary lithium batteries using improved cathodes", page 272, no. 318 747b; & JP,A,07 085 890 (FUJI ELECTROCHEMICAL CO.LTD.)

ANHANG

ANNEX

ANNEXE

zum internationalen Recherchenbericht über die internationale Patentanmeldung Nr. to the International Search Report to the International Patent Application No. au rapport de recherche international relatif à la demande de brevet international n°

PCT/GB 95/01337 SAE 111495

In diesem Anhang sind die Mitglieder der Patentfamilien der im obengenannten internationalen Recherchenbericht angeführten Patentdokumente angegeben. Diese Angaben dienen nur zur Unterrichtung und erfolgen ohne Gewähr.

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EP A1 571858	01-12-93	GA AA 2096386 JP A2 6275277	19-11-93 30-09-94	