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**PROCESS FOR PREPARING A FLEXIBLE POLYURETHANE FOAM**
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- (57) Claim

1. A process for preparing a flexible polyurethane foam by reacting
  - 1) an organic polyisocyanate with
  - 2) a polyol having an average nominal hydroxyl functionality of 2-3 and a number average molecular weight of 1000 to 12000; and with
  - 3) an isocyanate-reactive compound containing at least two isocyanate-reactive hydrogen atoms and having a number average molecular weight of 60 to 999; using
  - 4) a blowing agent; and
  - 5) a catalyst; characterised in that
    - a) the polyisocyanate is a polyisocyanate composition having an NCO value of 11-22% by weight which is a blend of
      - a1. 75-95 parts by weight of an isocyanate-terminated semi-prepolymer having an NCO value of 9-20% by weight, prepared by reacting an excessive amount of a polyisocyanate composition, consisting of 35-75% by weight of diphenylmethane

diisocyanate and 25-65% by weight of polymethylene polyphenylene polyisocyanate containing 30-65% by weight of diphenylmethane diisocyanate, with a polyol having an average nominal hydroxyl functionality of 2-3 and a number average molecular weight of 1000 to 12000; and

a2. 5-25 parts by weight of a polymethylene polyphenylene polyisocyanate containing 30-65% by weight of diphenylmethane diisocyanate;

b) 25-120 parts by weight of polyol 2) is used per 100 parts by weight of organic polyisocyanate;

c) water is used as the blowing agent in an amount of 3-15 parts by weight per 100 parts by weight of polyol 2); and

d) the reaction is conducted at an NCO-index of 40-130.

**4. Reaction system comprising**

- 1) an organic polyisocyanate;
- 2) a polyol having an average nominal hydroxyl functionality of 2-3 and a number average molecular weight of 1000 to 12000; and
- 3) an isocyanate-reactive compound containing at least two isocyanate-reactive hydrogen atoms and having a number average molecular weight of 60 to 999;
- 4) a blowing agent; and
- 5) a catalyst; characterised in that

a) the polyisocyanate is a polyisocyanate composition having an NCO value of 11-22% by weight which is a blend of

- a1. 75-95 parts by weight of an isocyanate-terminated semi-prepolymer having an NCO value of 9-20% by weight, prepared by reacting an excessive amount of a polyisocyanate composition, consisting of 35-75% by weight of diphenylmethane diisocyanate and 25-65% by weight of polymethylene polyphenylene polyisocyanate containing 30-65% by weight of diphenylmethane

diisocyanate, with a polyol having an average nominal hydroxyl functionality of 2-3 and a number average molecular weight of 1000 to 12000; and

- a2. 5-25 parts by weight of a polymethylene polyphenylene polyisocyanate containing 30-65% by weight of diphenylmethane diisocyanate;
- b) 25-120 parts by weight of polyol 2) is used per 100 parts by weight of organic polyisocyanate;
- c) water is used as the blowing agent in an amount of 3-15 parts by weight per 100 parts by weight of polyol 2); and
- d) the relative amount of polyisocyanate 1) with respect to the other ingredients is such that when combined the NCO index is 40-130; with the proviso that the polyisocyanate is kept in a container separate from the isocyanate-reactive compounds.

7. Organic polyisocyanate composition, characterised in that the composition has an NCO value of 11-22% by weight and is a blend of

- a1. 75-95 parts by weight of an isocyanate-terminated semi-prepolymer having an NCO value of 9-20% by weight, prepared by reacting an excessive amount of a polyisocyanate composition, consisting of 35-75% by weight of diphenylmethane diisocyanate and 25-65% by weight of polymethylene polyphenylene polyisocyanate containing 30-65% by weight of diphenylmethane diisocyanate, with a polyol having an average nominal hydroxyl functionality of 2-3 and a number average molecular weight of 1000 to 12000; and
- a2. 5-25 parts by weight of a polymethylene polyphenylene polyisocyanate containing 30-65% by weight of diphenylmethane diisocyanate.



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**(54) Title:** PROCESS FOR PREPARING A FLEXIBLE POLYURETHANE FOAM

**(57) Abstract**

Process for preparing a flexible foam by reacting a polyisocyanate composition having an NCO value of 11-22 % by weight with an isocyanate-reactive compound having a number average molecular weight of 1000-12000 using water as blowing agent.

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Title : Process for preparing a flexible polyurethane foam.

The present invention is concerned with a process for preparing flexible polyurethane foams and with a polyisocyanate composition 5 for preparing such flexible foams.

It is widely known to prepare flexible polyurethane foams by reacting an organic polyisocyanate and a high molecular weight isocyanate-reactive compound in the presence of a blowing agent. 10 More in particular it has been disclosed in EP-111121 to prepare flexible polyurethane foams from a polyisocyanate composition comprising a semi-prepolymer. The polyisocyanate composition is prepared by reacting a diphenylmethane diisocyanate and a polyol; a polymethylene polyphenylene polyisocyanate (polymeric MDI) is used 15 as well. This polyisocyanate is either completely used in the preparation of the semi-prepolymer or added after the semi-prepolymer has been made. We have found that the use of polymeric MDI as proposed in EP-111121 does not provide satisfactory stability combined with low viscosity in particular for those polyisocyanate 20 compositions having a relatively low NCO value, e.g. 11-22% by weight.

In EP-392788 flexible foams are prepared by reacting semi-prepolymers or prepolymers with an isocyanate-reactive composition containing a high amount of water.

25 In EP-296449 flexible foams are prepared by reacting polyisocyanates, polyols and water at a relatively low NCO-index.

Surprisingly it was found that when part of the polymethylene polyphenylene polyisocyanate (polymeric MDI) is used to prepare a 30 semi-prepolymer and the other part of the polymeric MDI is added to the semi-prepolymer so formed the polyisocyanate compositions according to the present invention are stable, clear liquids having a low viscosity; consequently their processing in preparing the foams is improved as well. When the polymeric MDI is either 35 completely used in the preparation of the semi-prepolymer or



completely added after the semi-prepolymer has been made the stability and/or viscosity are adversely effected.

Further it was found that the polyisocyanate compositions may contain higher amounts of polymeric MDI while remaining stable and therefore flexible foams having a lower density can be prepared; the lower density does not significantly effect the other physical properties of the foam in a negative way.

Accordingly the present invention is concerned with a process for preparing a flexible polyurethane foam by reacting

- 1) an organic polyisocyanate with
- 2) a polyol having an average nominal hydroxyl functionality of 2-3 and a number average molecular weight of 1000 to 12000; and optionally with
- 3) an isocyanate-reactive compound containing at least two isocyanate-reactive hydrogen atoms and having a number average molecular weight of 60 to 999; using
- 4) a blowing agent; and optionally
- 5) a catalyst; characterised in that
  - a) the polyisocyanate is a polyisocyanate composition having an NCO value of 11-22% by weight, preferably of 13-20% by weight and most preferably of more than 15 to 20% by weight which is a blend of
    - a1. 75-95 parts by weight of an isocyanate-terminated semi-prepolymer having an NCO value of 9-20, preferably 11-18% by weight and most preferably 13-18% by weight, prepared by reacting an excessive amount of a polyisocyanate composition, consisting of 35-75% by weight of diphenylmethane diisocyanate and 25-65% by weight of polymethylene polyphenylene polyisocyanate containing 30-65% by weight of diphenylmethane diisocyanate, with a polyol having an average nominal hydroxyl functionality of 2-3 and a number average molecular weight of 1000 to 12000; and
    - a2. 5-25 parts by weight of a polymethylene polyphenylene polyisocyanate containing 30-65% by weight of



diphenylmethane diisocyanate;

- 5
- b) 25-120 parts by weight and preferably 35-100 parts by weight of polyol 2) is used per 100 parts by weight of organic polyisocyanate;
  - c) water is used as blowing agent in an amount of 3-15 parts by weight, preferably 5-12 parts by weight and most preferably more than 8 to 12 parts by weight per 100 parts by weight of polyol 2); and
  - d) the reaction is conducted at an NCO-index of 40-130 and preferably above 70 to 100.

10 Other known auxiliaries and additives may also be used in the process.

Further the present invention is concerned with a reaction system comprising the above mentioned ingredients with the proviso that the polyisocyanate is kept in a container separate from the isocyanate-reactive compounds.

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Still further the present invention is concerned with the aforementioned polyisocyanate. Specifically the invention provides organic polyisocyanate composition, characterised in that the composition has an NCO value of 11-22% by weight and is a blend of

- a1. 75-95 parts by weight of an isocyanate-terminated semi-prepolymer having an NCO value of 9-20% by weight, prepared by reacting an excessive amount of a polyisocyanate composition, consisting of 35-75% by weight of diphenylmethane diisocyanate and 25-65% by weight of polymethylene polyphenylene polyisocyanate containing 30-65% by weight of diphenylmethane diisocyanate, with a polyol having an average nominal hydroxyl functionality of 2-3 and a number average molecular weight of 1000 to 12000; and
- a2. 5-25 parts by weight of a polymethylene polyphenylene polyisocyanate containing 30-65% by weight of diphenylmethane diisocyanate.

30 In the context of the present invention the following terms have the following meaning:



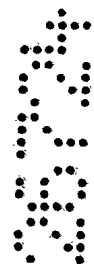
- 1) **isocyanate index or NCO index or index:**  
the ratio of NCO-groups over isocyanate-reactive hydrogen atoms present in a formulation, given as a percentage:

$$\frac{[\text{NCO}] \times 100}{[\text{active hydrogen}]} \quad \%$$

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In other words the NCO-index expresses the percentage of isocyanate actually used in a formulation with respect to the amount of isocyanate theoretically required for reacting with the amount of isocyanate-reactive hydrogen used in a formulation.

- 10 It should be observed that the isocyanate index as used herein is considered from the point of view of the actual foaming process involving the isocyanate ingredient and the isocyanate-reactive





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ingredients. Any isocyanate groups consumed in a preliminary step to produce the semi-prepolymer or other modified polyisocyanates or any active hydrogens reacted with isocyanate to produce modified polyols or polyamines, are not taken into account in the calculation  
5 of the isocyanate index. Only the free isocyanate groups and the free isocyanate-reactive hydrogens (including those of the water) present at the actual foaming stage are taken into account.

2) The expression "isocyanate-reactive hydrogen atoms" as used  
10 herein for the purpose of calculating the isocyanate index refers to the total of hydroxyl and amine hydrogen atoms present in the reactive compositions in the form of polyols, polyamines and/or water; this means that for the purpose of calculating the isocyanate index at the actual foaming process one hydroxyl group is  
15 considered to comprise one reactive hydrogen and one water molecule is considered to comprise two active hydrogens.

3) Reaction system : a combination of components wherein the polyisocyanate component is kept in a container separate from the  
20 isocyanate-reactive components.

4) The expression "polyurethane foam" as used herein generally refers to cellular products as obtained by reacting polyisocyanates with isocyanate-reactive hydrogen containing compounds, using  
25 foaming agents, and in particular includes cellular products obtained with water as reactive foaming agent (involving a reaction of water with isocyanate groups yielding urea linkages and carbon dioxide and producing polyurea-urethane foams).

30 5) The term "average nominal hydroxyl functionality" is used herein to indicate the number average functionality (number of hydroxyl groups per molecule) of the polyol composition on the assumption that this is the number average functionality (number of active hydrogen atoms per molecule) of the initiator(s) used in their  
35 preparation although in practice it will often be somewhat less because of some terminal unsaturation.

6) "MDI functionality" is the number average isocyanate functionality of all diphenylmethane diisocyanate and all polymethylene polyphenylene polyisocyanate used in preparing the polyisocyanate composition according to the present invention with the proviso that the NCO groups used in the preparation of the semi-prepolymer are also taken into account in determining this functionality.

The diphenylmethane diisocyanate (MDI) used may be selected from pure 4,4'-MDI and isomeric mixtures of 4,4'-MDI and 2,4'-MDI and less than 10% by weight of 2,2'-MDI and modified variants thereof containing carbodiimide, uretonimine, isocyanurate, urethane, allophanate, urea or biuret groups. Most preferred are pure 4,4'-MDI, isomeric mixtures with 2,4'-MDI, and uretonimine and/or carbodiimide modified MDI having an NCO content of at least 25% by weight and urethane modified MDI obtained by reacting excess MDI and polyol (preferably having a molecular weight of at most 999) and having an NCO content of at least 25% by weight.

The polymethylene polyphenylene polyisocyanates used in the preparation of semi-prepolymer a1) and used as polyisocyanate a2) are known as such and are polyisocyanates comprising MDI and MDI homologues having isocyanate functionalities of 3 or more. These polyisocyanates are often referred to as "crude MDI" or "polymeric MDI" and are made by the phosgenation of a mixture of polyamines obtained by the acid condensation of aniline and formaldehyde. The manufacture of both the polyamine mixtures and the polyisocyanate mixtures is well known. The condensation of aniline with formaldehyde in the presence of strong acids such as hydrochloric acid gives a reaction product containing diaminodiphenylmethane together with polymethylene polyphenylene polyamines of higher functionality, the precise composition depending in known manner on the aniline/formaldehyde ratio. The polyisocyanates are made by phosgenation of the polyamine mixtures and the various proportions of diamines, triamines and higher polyamines give rise to related proportions of diisocyanates,



triisocyanates and higher polyisocyanates.

The relative proportions of diisocyanate, triisocyanate and higher polyisocyanates in the crude diphenylmethane diisocyanate  
5 compositions determine the average functionality of the compositions, that is the average number of isocyanate groups per molecule. By varying the proportions of starting materials, the average functionality of the polyisocyanate compositions can be varied from little more than 2 to 3 or even higher. In practice,  
10 however, the number average isocyanate functionality preferably ranges from 2.35-2.9. The NCO value of these polymeric MDIs is at least 30% by weight.

Such compositions contain from 30 to 65% by weight of diphenylmethane diisocyanate, the remainder being polymethylene  
15 polyphenylene polyisocyanates of functionality greater than two together with by-products formed in the manufacture of such polyisocyanates by phosgenation. These products, being liquids, are convenient to use according to the present invention.

20 The polyols having an average nominal hydroxyl functionality of 2-3 and a number average molecular weight of 1000 to 12000 (polyol 2) and the polyol used in preparing semi-prepolymer a1) may be selected from polyester polyols, polyesteramide polyols, polythioether polyols, polycarbonate polyols, polyacetal polyols, polyolefin  
25 polyols, polysiloxane polyols and especially polyether polyols.

Polyether polyols which may be used include products obtained by the polymerisation of a cyclic oxide, for example ethylene oxide, propylene oxide, butylene oxide or tetrahydrofuran in the presence,  
30 where necessary, of polyfunctional initiators. Suitable initiator compounds contain a plurality of active hydrogen atoms and include water, butanediol, ethylene glycol, propylene glycol, diethylene glycol, triethylene glycol, dipropylene glycol, ethanolamine, diethanolamine, triethanolamine, toluene diamine, diethyl toluene  
35 diamine, cyclohexane diamine, cyclohexane dimethanol, glycerol, trimethylolpropane and 1,2,6-hexanetriol. Mixtures of initiators

and/or cyclic oxides may be used.

Especially useful polyether polyols include polyoxypropylene diols and triols and polyoxyethylene-polyoxypropylene diols and triols  
5 obtained by the simultaneous or sequential addition of ethylene and propylene oxides to di- or trifunctional initiators as fully described in the prior art. Random copolymers having oxyethylene contents of 10-80%, block copolymers having oxyethylene contents of up to 50%, based on the total weight of oxyalkylene units may be  
10 mentioned, in particular those having at least part of the oxyethylene groups at the end of the polymer chain. Mixtures of the said diols and triols can be particularly useful. Small amounts of polyoxyethylene diols and triols may be used as well; the amount in general is less than 20% by weight on the amount of polyol 2) used.

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Polyester polyols which may be used include hydroxyl-terminated reaction products of polyhydric alcohols such as ethylene glycol, propylene glycol, diethylene glycol, 1,4-butanediol, neopentyl glycol, 1,6-hexanediol, cyclohexane dimethanol, glycerol,  
20 trimethylolpropane or polyether polyols or mixtures of such polyhydric alcohols, and polycarboxylic acids, especially dicarboxylic acids or their ester-forming derivatives, for example succinic, glutaric and adipic acids or their dimethyl esters, sebacic acid, phthalic anhydride, tetrachlorophthalic anhydride or  
25 dimethyl terephthalate or mixtures thereof. Polyesters obtained by the polymerisation of lactones, for example caprolactone, in conjunction with a polyol, or of hydroxy carboxylic acids such as hydroxy caproic acid, may also be used.

30 Polyesteramides may be obtained by the inclusion of aminoalcohols such as ethanolamine in polyesterification mixtures.

Polythioether polyols which may be used include products obtained by condensing thiodiglycol either alone or with other glycols,  
35 alkylene oxides, dicarboxylic acids, formaldehyde, amino-alcohols or aminocarboxylic acids.

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Polycarbonate polyols which may be used include products obtained by reacting diols such as 1,3-propanediol, 1,4-butanediol, 1,6-hexanediol, diethylene glycol or tetraethylene glycol with diaryl carbonates, for example diphenyl carbonate, or with phosgene.

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Polyacetal polyols which may be used include those prepared by reacting glycols such as diethylene glycol, triethylene glycol or hexanediol with formaldehyde. Suitable polyacetals may also be prepared by polymerising cyclic acetals.

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Suitable polyolefin polyols include hydroxy-terminated butadiene homo- and copolymers and suitable polysiloxane polyols include polydimethylsiloxane diols and triols.

15 Other polyols which may be used as polyol 2) and/or in preparing semi-prepolymer a1) comprise dispersions or solutions of addition or condensation polymers in polyols of the types described above. Such modified polyols, often referred to as "polymer polyols" have been fully described in the prior art and include products obtained  
20 by the in situ polymerisation of one or more vinyl monomers, for example styrene and/or acrylonitrile, in polymeric polyols, for example polyether polyols, or by the in situ reaction between a polyisocyanate and an amino- and/or hydroxy-functional compound, such as triethanolamine, in a polymeric polyol. Polyoxyalkylene  
25 polyols containing from 5 to 50% by weight of dispersed polymer are particularly useful. Particle sizes of the dispersed polymers of less than 50 microns are preferred.

The number average molecular weight of polyols 2) and the polyols  
30 used in preparing semi-prepolymer a1) preferably is 1000-8000 and most preferably 1500-7000; the hydroxyl value preferably ranges from 15-200 and most preferably from 20-100.

Most preferred are polyoxyethylene polyoxypropylene polyols having  
35 a number average molecular weight of 2000-7000, an average nominal functionality of 2-3 and an oxyethylene content of 10-25% by weight,

preferably having the oxyethylene groups at the end of the polymer chain.

During the last years several methods have been described to prepare  
5 polyether polyols having a low level of unsaturation. These  
developments have made it possible to use polyether polyols at the  
higher end of the molecular weight range since much polyols can now  
be prepared with an acceptably low level of unsaturation. According  
to the present invention polyols having a low level of unsaturation  
10 may be used as well. In particular such high molecular weight  
polyols having a low level of unsaturation may be used for preparing  
flexible foams having a high ball rebound.

The isocyanate-terminated semi-prepolymer a1. is prepared by first  
15 mixing the diphenylmethane diisocyanate and the polymethylene  
polyphenylene polyisocyanate. Subsequently the polyol is added and  
the mixture is allowed to react. Such reaction is allowed to take  
place at 60-100°C and in general the use of catalyst is not  
necessary. The relative amount of polyisocyanate and polyol depends  
20 on the desired NCO-value of the semi-prepolymer, the NCO-value of  
the polyisocyanate used and the OH value of the polyol and can be  
easily calculated by those skilled in the art. After completion  
of the above reaction the polymethylene polyphenylene polyisocyanate  
a2. is added and mixed. The "MDI-functionality" of the  
25 polyisocyanate composition according to the present invention is  
2.15-2.35 and preferably 2.20-2.30.

The chain-extending and cross-linking agents which optionally may  
be used (isocyanate-reactive compound 3)) may be selected from  
30 amines and polyols containing 2-8 and preferably 2-4 amine and/or  
hydroxy groups like ethanolamine, diethanolamine, triethanolamine,  
ethylene glycol, diethylene glycol, triethylene glycol, propylene  
glycol, dipropylene glycol, butanediol, glycerol,  
trimethylolpropane, pentaerithritol, sorbitol, sucrose, polyethylene  
35 glycol having a molecular weight of at most 999, toluene diamine,  
diethyl toluene diamine, cyclohexane diamine, phenyl diamine,

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diphenylmethane diamine, alkylated diphenylmethane diamine and ethylene diamine.

The amount of chain-extending and cross-linking agents is, if applied, up to 25 and preferably up to 10 parts by weight per 100 parts by weight of polyol 2).

The auxiliaries and additives which amongst others may be used are formation of urea and urethane enhancing catalysts like tertiary amines and tin compounds, surfactants, stabilisers, flame retardants, fillers and anti-oxidants.

The flexible polyurethane foams are prepared by combining and mixing ingredients 1)-6) and allowing the mixture to foam. Preferably ingredients 2)-6) are premixed and subsequently combined with the polyisocyanate. The relative amounts of polyisocyanate on the one hand and ingredients 2)-6) on the other hand depend on the desired index and can be calculated easily by those skilled in the art.

The process may be used to make slab-stock or moulded flexible foams. The foams in general have a density of 15-80 kg/m<sup>3</sup> and may be used as cushioning material in furniture, car seats and mattresses.

The present invention is illustrated by the following Example.

#### Example

A semi-prepolymer was prepared by 1) mixing 29.6 parts by weight of a diphenylmethane diisocyanate containing 85% by weight of 4,4'-diphenylmethane diisocyanate and 15% by weight of 2,4'-diphenylmethane diisocyanate and 15 parts by weight of a polymethylene polyphenylene polyisocyanate having an NCO value of 30.7% by weight and a number average isocyanate functionality of 2.7, 2) adding to this mixture 45.4 parts by weight of a polyoxyethylene polyoxypropylene polyol having a nominal functionality of 3, a number average molecular weight of 6000 and

an oxyethylene content of 15% by weight (all tip) followed by mixing, and 3) allowing this mixture to react at 85°C for 4 hours. To the semi-prepolymer so obtained which had an NCO value of 15.1% by weight was added 10 parts by weight of the above polyisocyanate. 5 The composition obtained was an isocyanate composition according to the present invention; had an NCO value of 16.7% by weight and a viscosity of 1095 mPa.s at 25°C; the composition was clear and stable for more than 2 weeks at 0°C and room temperature (stability was determined visually; when solids and turbidity were visually 10 absent the composition was regarded as stable) and had an "MDI-functionality" of 2.25.

A flexible foam was prepared by mixing in a cup 100 parts of the above isocyanate composition according to the invention and an 15 isocyanate-reactive composition (index 77) comprising 50 parts by weight (pbw) of the above polyol, 4.3 pbw of water, 4.3 pbw of a polyoxyethylene polyol having a nominal functionality of 3 and a number average molecular weight of 1200, 1.45 pbw of SH210 surfactant, 0.85 pbw of 1,2-dimethyl imidazole as catalyst and 0.03 20 pbw of Niax A1 as catalyst. The mixture was allowed to react and to foam under free rise conditions. The foam obtained was a flexible foam having a free rise density of 32 kg/m<sup>3</sup>.

Where the terms "comprise", "comprises", "comprised" or "comprising" are used in this specification, they are to be interpreted as specifying the presence of the stated features, integers, steps or components referred to, but not to preclude the presence or addition of one or more other feature, integer, step, component or group thereof.





The claims defining the invention are as follows:

1. A process for preparing a flexible polyurethane foam by reacting
  - 1) an organic polyisocyanate with
  - 2) a polyol having an average nominal hydroxyl functionality of 2-3  
and a number average molecular weight of 1000 to 12000; and  
with
  - 3) an isocyanate-reactive compound containing at least two  
isocyanate-reactive hydrogen atoms and having a number average  
molecular weight of 60 to 999; using
  - 4) a blowing agent; and
  - 5) a catalyst; characterised in that
    - a) the polyisocyanate is a polyisocyanate composition having an  
NCO value of 11-22% by weight which is a blend of
      - a1. 75-95 parts by weight of an isocyanate-terminated  
semi-prepolymer having an NCO value of 9-20% by weight,  
prepared by reacting an excessive amount of a polyisocyanate  
composition, consisting of 35-75% by weight of diphenylmethane  
diisocyanate and 25-65% by weight of polymethylene  
polyphenylene polyisocyanate containing 30-65% by weight of  
diphenylmethane diisocyanate, with a polyol having an average  
nominal hydroxyl functionality of 2-3 and a number average  
molecular weight of 1000 to 12000; and
      - a2. 5-25 parts by weight of a polymethylene polyphenylene  
polyisocyanate containing 30-65% by weight of diphenylmethane  
diisocyanate;
    - b) 25-120 parts by weight of polyol 2) is used per 100 parts by  
weight of organic polyisocyanate;



c) water is used as the blowing agent in an amount of 3-15 parts by weight per 100 parts by weight of polyol 2); and

d) the reaction is conducted at an NCO-index of 40-130.

2. Process according to claim 1, wherein the organic polyisocyanate has an MDI functionality of 2.15-2.35.

3. Process according to claims 1-2, wherein the organic polyisocyanate has an NCO value of 13-20% by weight, the semi-prepolymer has an NCO value of 11-18% by weight, the amount of polyol 2) is 35-100 parts by weight per 100 parts by weight of organic polyisocyanate, the amount of water is 5-12 parts by weight per 100 parts by weight of polyol 2) and the NCO index is above 70 to 100.

4. Reaction system comprising

- 1) an organic polyisocyanate;
- 2) a polyol having an average nominal hydroxyl functionality of 2-3 and a number average molecular weight of 1000 to 12000; and
- 3) an isocyanate-reactive compound containing at least two isocyanate-reactive hydrogen atoms and having a number average molecular weight of 60 to 999;
- 4) a blowing agent; and
- 5) a catalyst; characterised in that
  - a) the polyisocyanate is a polyisocyanate composition having an NCO value of 11-22% by weight which is a blend of
    - a1. 75-95 parts by weight of an isocyanate-terminated semi-prepolymer having an NCO value of 9-20% by weight, prepared by reacting an excessive amount of a polyisocyanate composition, consisting of 35-75% by



weight of diphenylmethane diisocyanate and 25-65% by weight of polymethylene polyphenylene polyisocyanate containing 30-65% by weight of diphenylmethane diisocyanate, with a polyol having an average nominal hydroxyl functionality of 2-3 and a number average molecular weight of 1000 to 12000; and

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a2. 5-25 parts by weight of a polymethylene polyphenylene polyisocyanate containing 30-65% by weight of diphenylmethane diisocyanate;

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b) 25-120 parts by weight of polyol 2) is used per 100 parts by weight of organic polyisocyanate;

c) water is used as the blowing agent in an amount of 3-15 parts by weight per 100 parts by weight of polyol 2); and

d) the relative amount of polyisocyanate 1) with respect to the other ingredients is such that when combined the NCO index is 40-130; with the proviso that the polyisocyanate is kept in a container separate from the isocyanate-reactive compounds.

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5. Reaction system according to claim 4 wherein the organic polyisocyanate has an MDI functionality of 2.15-2.35.

20 6. Reaction system according to claims 4-5 wherein the organic polyisocyanate has an NCO value of 13-20% by weight, the semi-prepolymer has an NCO value of 11-18% by weight, the amount of polyol 2) is 35-100 parts by weight per 100 parts by weight of organic polyisocyanate, the amount of water is 5-12 parts by weight per 100 parts  
25 by weight of polyol 2) and the NCO index is above 70 to 100.



7. Organic polyisocyanate composition, characterised in that the composition has an NCO value of 11-22% by weight and is a blend of
- a1. 75-95 parts by weight of an isocyanate-terminated semi-prepolymer having an NCO value of 9-20% by weight, prepared by reacting an excessive amount of a polyisocyanate composition, consisting of 35-75% by weight of diphenylmethane diisocyanate and 25-65% by weight of polymethylene polyphenylene polyisocyanate containing 30-65% by weight of diphenylmethane diisocyanate, with a polyol having an average nominal hydroxyl functionality of 2-3 and a number average molecular weight of 1000 to 12000; and
- a2. 5-25 parts by weight of a polymethylene polyphenylene polyisocyanate containing 30-65% by weight of diphenylmethane diisocyanate.
8. Composition according to claim 7 wherein the MDI functionality of the composition is 2.15-2.35.
9. Composition according to claims 7-8 wherein the composition has an NCO value of 13-20% by weight and the semi-prepolymer has an NCO value of 11-18% by weight.
10. Composition according to claims 7-9 wherein the composition has an NCO value of more than 15 to 20% by weight and the semi-prepolymer has an NCO value of 13 to 18% by weight .



11. The process according to claim 1, the reaction system according to claim 4 or the composite according to claim 7 substantially as hereinbefore described according to the Example.

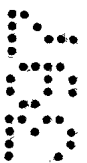
DATED this 18th day of March, 1998.

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IMPERIAL CHEMICAL INDUSTRIES PLC

By their Patent Attorneys:

CALLINAN LAWRIE



# INTERNATIONAL SEARCH REPORT

Intern. Application No  
**PCT/EP 95/02068**

**A. CLASSIFICATION OF SUBJECT MATTER**  
**IPC 6 C08G18/10 C08G18/76 C08G18/40 C08G18/65 //(C08G18/10, 101:00)**

According to International Patent Classification (IPC) or to both national classification and IPC

**B. FIELDS SEARCHED**

Minimum documentation searched (classification system followed by classification symbols)  
**IPC 6 C08G**

Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched

Electronic data base consulted during the international search (name of data base and, where practical, search terms used)

**C. DOCUMENTS CONSIDERED TO BE RELEVANT**

Category*	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
X	EP,A,0 344 551 (BAYER) 6 December 1989 see claims 1,5,9 see page 2, line 21 - line 37 see page 3, line 37 - line 57 see page 4, line 38 - page 5, line 11	1,7
X	WO,A,93 08224 (DOW) 29 April 1993 see claims 1-3 see page 4, line 18 - line 26 see page 5, line 20 - line 27 see page 6, line 16 - line 27	7
A	EP,A,0 010 850 (I.C.I.) 14 May 1980 see claims 1-3 see page 6, line 24 - page 7, line 15	1
	-/--	

Further documents are listed in the continuation of box C.       Patent family members are listed in annex.

\* Special categories of cited documents:

<p>"A" document defining the general state of the art which is not considered to be of particular relevance</p> <p>"B" earlier document but published on or after the international filing date</p> <p>"L" document which may throw doubt on priority claim(s) or which is cited to establish the publication date of another citation or other special reason (as specified)</p> <p>"O" document referring to an oral disclosure, use, exhibition or other means</p> <p>"P" document published prior to the international filing date but later than the priority date claimed</p>	<p>"T" later document published after the international filing date or priority date and not in conflict with the application but cited to understand the principle or theory underlying the invention</p> <p>"X" document of particular relevance; the claimed invention cannot be considered novel or cannot be considered to involve an inventive step when the document is taken alone</p> <p>"Y" document of particular relevance; the claimed invention cannot be considered to involve an inventive step when the document is combined with one or more other such documents, such combination being obvious to a person skilled in the art.</p> <p>"A" document member of the same patent family</p>
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Date of the actual completion of the international search	Date of making of the international search report
<b>24 August 1995</b>	<b>08.09.95</b>

Name and mailing address of the ISA European Patent Office, P.B. 5818 Patentlaan 2 NL - 2280 HV Rijswijk Tel. (+ 31-70) 340-2040, TX 31 651 epo nl, Fax (+ 31-70) 340-3016	Authorized officer  <p style="text-align: center;"><b>Van Puymbroeck, M</b></p>
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# INTERNATIONAL SEARCH REPORT

Internat. Application No  
PCT/EP 95/02068

C.(Continuation) DOCUMENTS CONSIDERED TO BE RELEVANT		
Category *	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
A	EP,A,0 111 121 (BASF) 20 June 1984 cited in the application see claims 1,2,6,7,10 see page 6, line 1 - line 13 see page 8, line 4 - line 33 see page 10, line 23 - line 24 see page 11, line 9 - line 12 -----	1

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**INTERNATIONAL SEARCH REPORT**

Information on patent family members

International Application No

**PCT/EP 95/02068**

Patent document cited in search report	Publication date	Patent family member(s)	Publication date
<b>EP-A-0344551</b>	<b>06-12-89</b>	<b>DE-A- 3818769</b>	<b>07-12-89</b>
		<b>AU-B- 612255</b>	<b>04-07-91</b>
		<b>AU-A- 3383489</b>	<b>07-12-89</b>
		<b>ES-T- 2043945</b>	<b>01-01-94</b>
		<b>JP-A- 2029417</b>	<b>31-01-90</b>
		<b>NO-C- 173418</b>	<b>15-12-93</b>
		<b>US-A- 4945117</b>	<b>31-07-90</b>
<b>WO-A-9308224</b>	<b>29-04-93</b>	<b>EP-A- 0609320</b>	<b>10-08-94</b>
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<b>EP-A-0111121</b>	<b>20-06-84</b>	<b>DE-A- 3241450</b>	<b>10-05-84</b>
		<b>CA-A- 1204121</b>	<b>06-05-86</b>
		<b>US-A- 4478960</b>	<b>23-10-84</b>